

Model Studies of Outfall Systems for Desalination Plants (Part II—Estuary Models)

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**United States Department of the Interior • Rogers C. B. Morton, Secretary
James R. Smith, Assistant Secretary for Water and Power Resources**

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The Department works to assure the wisest choice in managing all our resources so each will make its full contribution to a better United States—now and in the future.

FOREWORD

This is one of a continuing series of reports designed to present accounts of progress in saline water conversion and the economics of its application. Such data are expected to contribute to the long-range development of economical processes applicable to low-cost demineralization of sea and other saline water.

Except for minor editing, the data herein are as contained in a report submitted by the contractor. The data and conclusions given in the report are essentially those of the contractor and are not necessarily endorsed by the Department of the Interior.

PREFACE

The tests reported herein were conducted under Contract 14-30-2656 between the U. S. Department of the Interior and the U. S. Army Corps of Engineers. The study was performed in the Hydraulics Division of the U. S. Army Engineer Waterways Experiment Station during the period November 1970 to July 1971 under the direction of Messrs. E. P. Fortson, Jr., Chief of the Hydraulics Division; H. B. Simmons, Acting Chief of the Hydraulics Division; and F. A. Herrmann, Jr., Acting Chief of the Estuaries Branch. The tests were conducted by Mr. R. A. Boland, Jr., Project Engineer, and technicians of the Interior Channel Section, under the supervision of Mr. W. H. Bobb, Chief of the Interior Channel Section. This report was prepared by Messrs. Bobb and Boland with the assistance of Mr. Herrmann.

Messrs. Walter Rinne and C. L. Gransee of the Office of Saline Water, Professor R. O. Reid of Texas A&M University, and Dr. M. A. Zeitoun and Mr. W. F. McIlhenny of Dow Chemical Company visited the Waterways Experiment Station during the investigation phase of the study to observe and discuss test results.

COL Ernest D. Peixotto, CE, was Director of the Waterways Experiment Station during the conduct of the investigation and the preparation and publication of this report. Mr. F. R. Brown was Technical Director.

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CONVERSION FACTORS, BRITISH TO METRIC UNITS OF MEASUREMENT

British units of measurement used in this report can be converted to metric units as follows:

<u>Multiply</u>	<u>By</u>	<u>To Obtain</u>
inches	2.54	centimeters
feet	0.3048	meters
miles (U. S. statute)	1.609344	kilometers
feet per second	0.3048	meters per second
cubic feet per second	0.02831685	cubic meters per second
Fahrenheit degrees	5/9	Celsius or Kelvin degrees*
gallons (U. S.)	3.785412	cubic decimeters

* To obtain Celsius (C) temperature readings from Fahrenheit (F) readings, use the following formula: $C = (5/9)(F - 32)$. To obtain Kelvin (K) readings, use: $K = (5/9)(F - 32) + 273.15$.

SUMMARY

The existing comprehensive fixed-bed models of San Diego Bay, Galveston Bay, and Delaware River located at the Waterways Experiment Station were chosen to study the dispersion of heated waste brine from desalination plant outfalls. These three models were considered to be typical of estuaries on which saltwater conversion facilities are likely to be located, and it was intended that information obtained from tests in these models be readily applied to other similar estuaries. The objectives of the tests were to determine dispersion rates of the brine waste, to define the dynamic equilibrium distribution of the waste after the plant being simulated has been in operation for some time, and in the case of tests in the Delaware River model, to determine the effects of freshwater inflow on dispersion rates and equilibrium values.

Significant results of tests in the various models involving introduction of the heated effluent from a 10-mgd plant for considerable periods of time include: (a) in estuaries such as San Diego Bay, where minimal tidal current velocities exist and very little fresh water discharges into the system, the dispersion and flushing rates will be extremely slow, and the time required to reach dynamic equilibrium will be comparatively long; (b) in large, shallow estuaries such as Galveston Bay extreme care should be taken in selecting an outfall site since flow conditions in the immediate vicinity of the diffuser are highly significant in overall dispersion rates and may tend to trap the plant effluent; (c) in estuaries similar to the Delaware River, having appreciable freshwater discharge and tidal currents and a reasonably regular shape, sufficient mixing and dispersion of the effluent will probably occur after the energy of the jet leaving the diffuser is expended; and (d) the mixing and dispersion rates in estuaries similar to the Delaware River vary directly with total freshwater flow into the estuary, while the time to reach dynamic equilibrium varies inversely with total freshwater flow.

SECTION I: INTRODUCTION

Today, perhaps more so than at any time in the past, there is a growing concern with the preservation of tidal waters. Increasing industrial, municipal, and agricultural demands for available fresh water coupled with the often poor quality of return flows and heavy pollutional loadings pose serious problems to management of estuarine environments. Unrestricted waste and thermal loadings can disturb the ecological balances in tidal waters and destroy natural habitat for marine life.

Most of the major tidal water bodies along the coasts of the United States serve a multitude of uses that include recreation, sport and commercial fishing, navigation, the provision of spawning and nursery areas, and natural habitat for marine life. In many cases, these same waters also serve as the receiving water for industrial and municipal waste and for the heated water discharged from fossil- and nuclear-fueled power plants, desalination works, and other processes. The discussion that follows concerns the effluent from desalination works.

Large desalination plants to be built in the near future will employ either a variation of the multiple-effect, falling-film or multiple-stage, flash distillation processes in combination with the production of power. Such plants are most likely to be located on the shores of our oceans and estuaries where sea water would be used as the feed, and the effluents would be discharged into the marine environment.

The design of an intake-outfall system to handle the large quantity of saline water required for the operation of a dual-purpose plant involves many disciplines such as oceanography, geology, and biology as well as hydraulic and structural engineering. The problem is essentially a fluid mechanics problem involving the physical characteristics of the effluent and the receiving water. The behavior of the effluents injected into the marine environment must be studied to allow prediction of the maximum physical and chemical changes to be expected in the receiving water in the vicinity of the outfall and to develop guides for the design of an optimum outfall with respect to predetermined water-quality criteria.

At coastal locations, an obvious means of disposal of desalination plant effluents is through a properly designed outfall located offshore. When a dense effluent is discharged from one or many ports of a diffuser, it is immediately subjected to a negative buoyancy force proportional to the difference in density between the effluent and the lighter receiving water. The kinetic energy resulting from the velocity through the port is dissipated in the turbulent mixing produced by the jet, while the negative buoyancy force drives the effluent toward the sea bottom. This initial jet mixing causes a field of diluted effluent to be formed near the bottom of the receiving water, and the diluted effluent then moves with the tidal currents to be dispersed throughout the bay or estuary.

Dow Chemical Company, under contract with the Office of Saline Water,

Department of the Interior, developed conceptual designs for outfall diffusers for disposal of brine and other wastes produced by desalination plants, of various types and sizes, to be located on the banks of estuaries or on the shores of the oceans. In addition to literature and other studies to determine the effects of these wastes on environmental factors, Dow Chemical Company conducted a series of laboratory experiments and formulated mathematical models to define the characteristics of an emerging jet of greater density than the receiving water. Both Dow Chemical Company and the Office of Saline Water believed that the conceptual designs developed under the contract should be subjected to hydraulic model testing before being recommended for field installation.

The hydraulic model study reported herein involved modeling the entire diffuser system and testing it under conditions that would be encountered at various probable plant locations. The variables to be investigated included depth and slope of the receiving water bottom, presence of thermal and/or salinity stratification in the receiving water, alongshore or tidal currents that would increase dispersion of the wastes, freshwater inflow into the estuary, and other factors. In connection with this study hydraulic models were useful in two principal areas. The first was concerned with the design of diffusers to ensure optimum initial mixing of the waste with the receiving water in the near field. The second was concerned with the effects of the waste on environmental factors (dispersion, flushing, and salinity concentrations) in the far field in coastal waters or estuaries and will be referred to as the estuary model dispersion studies. Only the dispersion studies in estuary models will be discussed in the remainder of this report. The diffuser design studies are discussed in Part I of this report under separate cover.

Of the several comprehensive models at the U. S. Army Engineer Waterways Experiment Station, it was decided that the dispersion studies should be made in the San Diego Bay, Galveston Bay, and Delaware River models. These three models were typical of the estuaries on which salt-water conversion facilities are likely to be located; and it was believed that information obtained from tests in these models could be readily applied to other estuaries. The objectives of the tests were to determine dispersion rates of the brine waste and to define the dynamic equilibrium distribution of the waste after the plant being simulated had been in operation for some time.

SECTION II: SAN DIEGO BAY MODEL

A. Description

The first dispersion study was conducted in the existing comprehensive model of San Diego Bay, the limits of which are shown in plate 1. The model was constructed of concrete to linear scale ratios, model to prototype, of 1:500 horizontally and 1:100 vertically. Other scale ratios, computed from the linear scales, were: velocity 1:10, time 1:50, discharge 1:500,000, and volume 1:25,000,000. Both the temperature and salinity scale ratios were 1:1. However, since the waters within the bay and adjacent ocean areas are essentially homogeneous, it was not necessary to use salt water in the model to reproduce prototype conditions of tides, currents, flow patterns, and dispersion characteristics; therefore, fresh water was used for the ocean supply. One prototype diurnal tidal cycle of 24 hr and 50 min was reproduced in the model in 29 min and 48.5 sec.

B. Test Procedure

The dispersion test involved simulation of an average size plant designed to produce 10 million gallons* per day (mgd) of fresh water. A typical profile of the outfall line and diffuser for a coastal rather than estuarine installation is shown in fig. 1, and the specifications of the 10-mgd plant are given below along with the model equivalents:

	<u>Prototype</u>	<u>Model</u>
Mixed effluent flow rate	21.23 mgd	42.46 gpd
Δt of effluent, $^{\circ}\text{F}$	20	20
Difference between effluent and receiving water salinities, ppt	11.4	11.4
Diffuser length, ft	195	0.39
Diffuser diameter, in.	30	0.30
Diffuser ports:		
Number	16	16
Spacing, ft	13	0.026
Diameter, in.	6	3/64

The diffuser was located approximately 4000 ft offshore from the San Diego Power Plant as shown in plate 1. The depth of water at the diffuser site was about 11 ft referred to mean sea level (msl). In the model, the diffuser port size was adjusted to obtain a plume height and shape approximating the height and shape of the plume observed in the flume tests.

* A table of factors for converting British units of measurement to metric units is presented on page v.

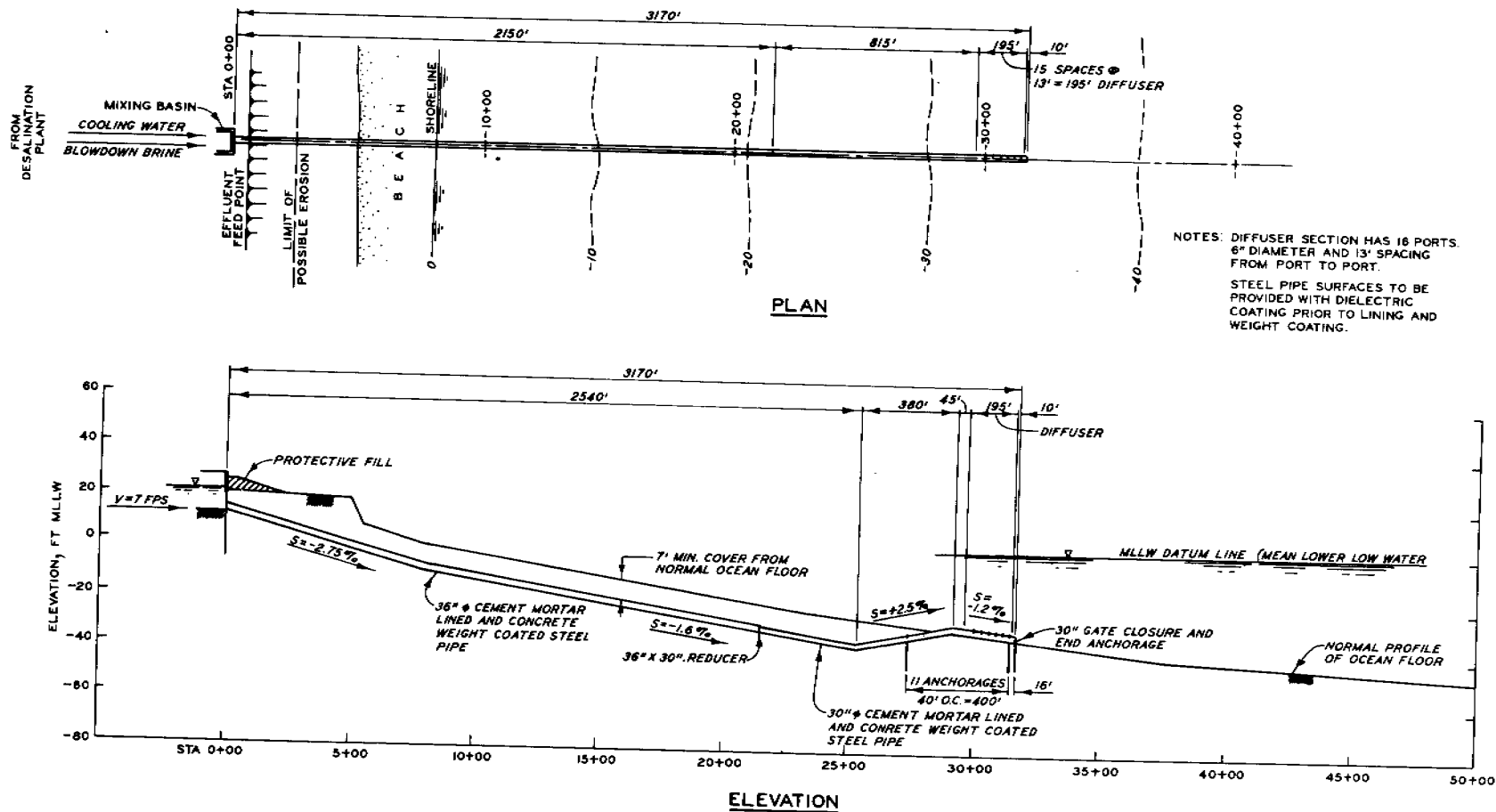


Fig. 1. Plan and profile of typical outfall-diffuser, 10-mgd plant

Because there are no significant salinity gradients in San Diego Bay, it was unnecessary to reproduce the ocean and bay salinity in the model. Thus, the salinity of the brine effluent in the model was adjusted to the difference in concentration between the prototype effluent and the receiving water. The brine concentration in the model was 11.4 parts per thousand (ppt) (45.4 ppt effluent salinity minus 34.0 ppt bay salinity), instead of 45.4 ppt as would be the case in the prototype. Use of the lower model brine salinity was possible because the difference in density between the brine and the receiving water, rather than their absolute densities, was the pertinent parameter in the dispersion process. A fluorescent dye was added to the model brine to observe dispersion of the brine during the test. The concentrations of both salt and dye in all water samples were measured to determine if the dye and salinity dispersion could be correlated to facilitate analysis of samples obtained in later tests in other models where salt water was used for the ocean supply.

After establishing conditions of dynamic hydraulic stability in the model, the dyed brine was heated to a temperature 20°F above that of the receiving water to reproduce the temperature-induced density difference in addition to the salinity-induced density difference. The heated brine was then discharged into the model at a uniform rate through the diffuser for 60 tidal cycles, or for about 30 hours actual time. About 53 gal of brine solution was introduced into the model during the test.

Salinity and dye concentration measurements were made of water samples obtained from surface and bottom depths every other tidal cycle at the times of local high- and low-water slack of the tidal current at all stations shown in plate 1. The purpose of these observations was to determine the dispersion rates of the brine waste throughout the bay and to define when the dynamic equilibrium distribution of the waste was established after the plant being simulated had been in continuous operation for some time. Water samples were withdrawn from the model manually with 10-cc pipettes and transferred to 5-cc vials that were immediately closed with rubber stoppers. Dye concentrations were subsequently determined by use of fluorometers, and salinities were then determined by conductivity cells specially built and calibrated for this purpose. The dye concentration data were compared with corresponding salinity measurements to check the correlation between the dispersion characteristics of the fluorescent dye and those of the saline effluent, since it is intended to use dye to determine dispersion patterns of the brine solution in future studies in the two other estuary models. It was concluded that within the range of salinity changes anticipated in the other studies resulting from the addition of the plant effluent to the saline receiving water the dye movement would accurately indicate the dispersion characteristics of the effluent.

During this test, a mean tide having a diurnal range (higher-high water to lower-low water) of 6.2 ft at the Ballast Point gage in the bay entrance was reproduced in the model. Plates 2 and 3 show tidal data taken during the test, while plates 4-7 show current velocities at a number of stations in the bay. There was no freshwater inflow to the bay.

C. Test Results

The salinity concentration of each sample was determined in parts per thousand, total salt, and subsequently converted to a percentage of the initial difference between the effluent and receiving water salinities (11.4 ppt). Plots of these percentages, with respect to time in tidal cycles after the effluent injection was started, were prepared for each observation station by plotting the values on semilog paper and drawing a smooth, best-fit curve (plates 8-37). The curves show the arrival time and dispersion rate of the brine waste, define the dynamic equilibrium value of the waste, and show when equilibrium was obtained at both surface and bottom depths. Tabulations of the model data used to construct these plots are presented in Appendix A to this report under separate cover. Plates 38-41 are contour maps showing lines of equal percentages of initial salinity concentration at the surface and bottom at the times of local high- and low-water slack after reaching the dynamic equilibrium distribution of the effluent throughout the bay.

D. Discussion of Results

The maximum salinity increase detected at the bottom was about 8 percent of the initial salinity difference at the diffuser; and this value extended downstream from the diffuser for about 6000 ft at low-water slack and about 4000 ft at high-water slack as shown in plates 41 and 39, respectively. The maximum salinity increase detected at the surface was about 3 percent within an area about 800 ft long downstream from the diffuser at low-water slack, and about 3000 ft long at high-water slack. Apparently the dynamic equilibrium distribution of the effluent was achieved about 30 to 50 cycles after injection of the effluent was initiated, depending on the distance from the diffuser. The grouping of the contours around the diffuser in both plates 39 and 41 indicates that although the salinities were not greatly increased (8 percent of 11.4 ppt is only 0.9 ppt) by the addition of the brine effluent to the system the flushing rate in this type of estuary is extremely slow. This characteristic would be a significant factor in evaluating this site for the location of a desalination plant outfall.

SECTION III: GALVESTON BAY MODEL

A. Description

The second dispersion study was conducted in the existing comprehensive model of the Galveston Bay complex, the limits of which are shown in plate 42. The model was constructed of concrete to linear scale ratios, model to prototype, of 1:600 horizontally and 1:60 vertically.. Other scale ratios, computed from the linear scales, were: velocity 1:7.75, time 1:77.46, discharge 1:278,855, and volume 1:21,600,000. One prototype diurnal tidal cycle of 24 hr and 50 min was reproduced in the model in 19 min and 14.4 sec. Both the temperature and salinity scale ratios were 1:1.

B. Test Procedure

The dispersion test involved simulation of the same prototype 10-mgd plant simulated in the San Diego Bay model, and the specifications are repeated below along with the model equivalents determined by the scales of the Galveston Bay model.

	<u>Prototype</u>	<u>Model</u>
Mixed effluent flow rate	21.23 mgd	76.13 gpd
Δt of effluent, °F	20	20
Difference between effluent and receiving water salinities, ppt	11.4	11.4
Diffuser length, ft	195	0.33
Diffuser diameter, in.	30	0.50
Diffuser ports:		
Number	16	16
Spacing, ft	13	0.0217
Diameter, in.	6	3/32

The diffuser was located approximately 5000 ft offshore from the P. H. Robinson Power Plant discharge structure as shown in plate 42. The depth of water at the diffuser was about 12 ft msl. The diffuser port size was adjusted to obtain a plume height and shape approximating the height and shape obtained in the flume tests. Because of the necessity to introduce salt water in the model to properly reproduce prototype conditions of tides, currents, flow patterns, and dispersion characteristics, the concentration of the brine effluent was treated differently than in the preceding model test. The average salinity over a tidal cycle at the diffuser site was found to be 19.6 ppt in the model. The required effluent concentration was 11.4 ppt greater than the average salinity of the receiving water and was thus adjusted to 31.0 ppt. A fluorescent dye was added to the effluent to indirectly determine dispersion of the brine during the test. This method was used rather than direct observation of salinity

because it is difficult to accurately measure small salinity differentials at high absolute salinities. Since the San Diego Bay test indicated that a direct correlation exists between dye and salinity dispersion, only the dye concentrations of the water samples were measured for the Galveston Bay model test. The dye concentrations were converted to a percentage of the initial salinity difference between the effluent salinity and the average receiving water salinity rather than to a percentage of the absolute salinity concentration, because the salinity (or density) difference is the pertinent parameter in the dispersion process.

After establishing conditions of dynamic hydraulic and salinity stability in the model, the brine was heated to a temperature 20°F above that of the receiving water to reproduce the temperature-induced density difference. The heated brine was then discharged into the model through the diffuser, which was embedded in the concrete model bottom, for 78 tidal cycles or for about 26 hours actual time. About 88 gal of brine solution was introduced into the model during the course of the test.

Dye concentration measurements were made of water samples obtained from surface and bottom depths every other tidal cycle at the times of local high- and low-water slack of the tidal current at all stations shown in plate 42. The purpose of the observations, as in the preceding test, was to determine the dispersion rates of the brine waste and define when equilibrium distribution of the waste was obtained with the plant being simulated in continuous operation. Samples were withdrawn from the model manually with 10-cc pipettes and transferred to 5-cc vials. Dye concentrations were determined by use of fluorometers.

During this test, a mean tide with a range of 2.1 ft at the Pleasure Pier gage (Galveston) was reproduced in the model. Plate 43 shows tidal data taken during the test at three bay stations and at Pleasure Pier, the tide control station for the Gulf. Total freshwater inflow to the bay from the various inflow points shown in plate 42 was 11,929 cfs and represented a mean discharge. Gulf salinity was 32.5 ppt.

C. Test Results

The dye concentration of each sample was determined in parts per billion (ppb), and subsequently converted to a percentage of the initial difference between the effluent and receiving water salinities (11.4 ppt). Plots of these percentages, as a function of time in tidal cycles after the effluent injection started, were prepared for each observation station by plotting the values on semilog paper and drawing smooth, best-fit curves (plates 44-87). Tabulations of the model data used to construct these plots are presented in Appendix A to this report under separate cover. Plates 88 and 89 are contour maps showing lines of equal percent of initial salinity difference (11.4 ppt) at the surface and bottom at the times of local high- and low-water slack and define the approximate dynamic equilibrium distribution of the effluent throughout the bay.

D. Discussion of Results

The maximum salinity increase detected at the bottom was about 13 percent of the initial salinity difference at the diffuser for a distance of about 2000 ft downstream from the diffuser at the times of both high- and low-water slack. A salinity increase of about 10 percent of the initial salinity difference was detected at the bottom 9000 ft downstream of the diffuser at the time of low-water slack, and this distance was reduced to 6000 ft by the time of high-water slack. The maximum increase detected at the surface was about 1 percent for a distance of about 5000 ft downstream from the diffuser at low-water slack and about 2 percent for a distance of about 4000 ft at high-water slack. Apparently the dynamic equilibrium distribution of the effluent was achieved in about 20 to 50 cycles after injection of the effluent was initiated, depending on the distance from the diffuser. Maximum current velocities in the vicinity of the diffuser are about 0.5 fps; consequently, little mixing or dispersion occurs after the energy of the jet leaving the diffuser is expended. The effluent rises from 5 to 7 ft above the bottom immediately upon leaving the diffuser, settles back to the bottom in a thin layer as a result of the density gradient, and subsequently slowly spreads over the model bottom as a result of the tidal action. Although tide and salinity conditions at this site are considerably different from those at the site investigated in the San Diego Bay model, flushing characteristics in these two areas are similar. Bays of this type are not considered to be good locations for releasing wastes from desalination plants.

SECTION IV: DELAWARE RIVER MODEL

A. Description

Three additional dispersion studies were conducted in the existing comprehensive model of the Delaware River estuary, the limits of which are shown in plate 90. The model was constructed of concrete to linear scale ratios, model to prototype, of 1:1000 horizontally and 1:100 vertically. Other scale ratios, computed from the linear scales, were: velocity 1:10, time 1:100, discharge 1:1,000,000, and volume 1:100,000,000. One prototype tidal cycle of 12 hr and 25 min was reproduced in the model in 7 min and 27 sec. Both the temperature and salinity scale ratios were 1:1.

B. Test Procedure

Since the freshwater inflow to the Delaware estuary varies over much wider limits than that for the other two estuaries studied in this investigation, it was decided that tests in this model should be made for conditions of low, mean, and high freshwater inflows to determine inflow effects on dispersion patterns and rates. The dispersion tests involved simulation of the same prototype 10-mgd plant simulated in the other two models, and the specifications are repeated below along with the model equivalents determined by the scales of the Delaware River model.

	<u>Prototype</u>	<u>Model</u>
Mixed effluent flow rate	21.23 mgd	21.23 gpd
Δt of effluent, $^{\circ}F$	20	20
Difference between effluent and receiving water salinities, ppt	11.4	11.4
Diffuser diameter, in.	30	0.30
Diffuser ports:		
Number	16	16
Spacing, ft	13	0.013
Diameter, in.	6	3/64

The diffuser was located in a depth of about 18 ft referred to local mean low water, approximately 5000 ft offshore, and approximately perpendicular to channel station 365 (see plate 90). Because of the necessity to introduce salt water in the Delaware River model to properly reproduce prototype conditions of tides, currents, flow patterns, and dispersion characteristics (as in the Galveston Bay model test), the brine effluent concentration in the model was the same as it would be in nature. The average salinities over a tidal cycle at the diffuser site for low, mean, and high freshwater inflow conditions were found to be 21.0, 17.6, and 11.0 ppt, respectively. The required effluent concentration was again 11.4 ppt greater than that of the receiving water; therefore, the effluent concentrations for the three inflow conditions were adjusted to 32.4, 29.0, and

22.4 ppt for the low, mean, and high inflow tests, respectively. A fluorescent dye was added to the effluent to indirectly observe dispersion of the brine as in the Galveston Bay test. Since the San Diego Bay test indicated that a direct correlation exists between dye and salinity dispersion, only dye concentrations were measured for each sample taken during the Delaware River model tests. The dye concentrations were converted to a percentage of the initial difference between the effluent salinity and the average receiving water salinity rather than a percentage of absolute salinity concentration, because the salinity (or density) difference is the pertinent parameter in the dispersion process.

After establishing conditions of dynamic hydraulic and salinity stability in the model for each of the three river flows, the brine was heated to a temperature 20°F above that of the receiving water to reproduce the temperature-induced density difference. The heated brine was then discharged into the model through the diffuser for 60 tidal cycles, or for about 8 hours actual time. About 7 gal of the brine solution was introduced into the model during the course of each test.

Dye concentration measurements were made of water samples obtained from surface and bottom depths every other tidal cycle at times of local high- and low-water slack of the tidal current at all stations shown in plate 91. The purpose of the observations, as in the preceding tests, was to determine dispersion rates of the brine waste and define when equilibrium distribution of the waste was obtained with the plant being simulated in continuous operation. Samples were withdrawn from the model manually with 10-cc pipettes and transferred to 5-cc vials. Dye concentrations were determined by use of fluorometers.

During these tests, a mean tide with a range of 5.5 ft at the Miah Maull gage in Delaware Bay was reproduced in the model. Total freshwater inflows to the estuary from the various freshwater inflow points shown in plate 89 were 6542, 20,200 and 60,600 cfs for the low, mean, and high freshwater flow tests, respectively. Source salinity at the Capes was 31.0 ppt.

Tidal measurements made throughout the model for mean conditions of tide and freshwater inflow are shown in plate 92. The range of tide is shown in the top plot, mean tide level is shown in the middle plot, and high- and low-water slack times are shown in the bottom plot. These phenomena were not changed significantly in the vicinity of the diffuser for low- and high-flow conditions.

C. Low-Flow Test Results

The dye concentration of each sample was determined in parts per billion, and subsequently converted to a percentage of the initial difference between the effluent and the average receiving water salinities (11.4 ppt). Plots of these percentages, as a function of time in tidal cycles after effluent injection started, were prepared for each observation station by

plotting the values on semilog paper and drawing a smooth, best-fit curve (see plates 93-124). Tabulations of the model data used to construct these plots are presented in Appendix A to this report under separate cover. Plates 125-128 are contour maps showing lines of equal percent of initial salinity difference (11.4 ppt) at the surface and bottom at the times of local high- and low-water slack of the tidal current and define the dynamic equilibrium distribution of the effluent throughout the estuary.

D. Discussion of Low-Flow Test Results

After 60 tidal cycles of simulation of continuous plant operation, the plant effluent had spread throughout a major portion of Delaware Bay. The effluent had been carried upstream to beyond Artificial Island and downstream to within 5 miles of the Capes. The dispersion was excellent, and salinity increases are considered minimal. The maximum salinity increase detected at the bottom during the low-flow test was about 0.30 percent of initial salinity difference at the diffuser, and this value was found in an area about 500 ft wide and 25,000 ft long in a downstream direction from the diffuser at the time of low-water slack as shown in plate 128. This represents a maximum increase in salinity concentration in that area of only 0.03 ppt ($11.4 \text{ ppt} \times 0.30 \text{ percent}$). Maximum current velocities in the vicinity of the diffuser are about 2.2 fps, and the flow is quite turbulent; consequently, a considerable amount of mixing or diffusion occurs after the energy of the jet leaving the diffuser is expended. Maximum salinity increases at surface and bottom at high-water slack and at the surface at low-water slack were about 0.02 ppt and were confined to generally small areas in the immediate vicinity of the diffuser. Apparently the dynamic equilibrium distribution of the effluent was achieved in about 30-50 cycles after injection of the effluent was initiated, depending on the distance from the diffuser.

E. Mean-Flow Test Results

As in the preceding test, the dye concentration of each sample was determined in parts per billion and subsequently converted to a percentage of the initial difference between the effluent and receiving water salinities (11.4 ppt). Plots of these percentages, as a function of time in tidal cycles after effluent injection started, were prepared for each observation station by plotting the values on semilog paper and drawing a smooth, best-fit curve (see plates 129-156). Tabulations of the model data used to construct the above plots are presented in Appendix A to this report under separate cover. Plates 157-160 are contour maps showing lines of equal percent of initial salinity difference (11.4 ppt) at the surface and bottom at the times of local high- and low-water slack of the tidal current and define the dynamic equilibrium distribution of the effluent throughout the estuary.

F. Discussion of Mean-Flow Test Results

The maximum salinity increase detected during the mean-flow test was about 0.30 percent of the initial salinity difference (11.4 ppt), and this

value was found in an area at the bottom about 15,000 ft long and 500 ft wide extending in a downstream direction from the diffuser at the time of low-water slack. This represents a maximum increase in salinity concentration in that area of about 0.03 ppt ($11.4 \text{ ppt} \times 0.30 \text{ percent}$). Comparison of the contours of salinity increase presented in plates 160 and 128 indicates a definite correlation between river discharge and dispersion of the effluent. As the river discharge increases, the mixing or dispersion rate increases. Thus, the area within each corresponding contour line is less for mean flow than for low flow. Apparently the dynamic equilibrium distribution of the effluent was achieved in about 20-40 cycles after injection of the effluent was initiated, depending on the distance from the diffuser.

G. High-Flow Test Results

As in the preceding tests, the dye concentration of each sample was determined in parts per billion, and subsequently converted to a percentage of the initial difference between the effluent and the receiving water salinities (11.4 ppt). Plots of these percentages, as a function of time in tidal cycles after effluent injection started, were prepared for each observation station where dye was detected by plotting the values on semilog paper and drawing a smooth, best-fit curve (see plates 161-167). The model data used to construct the above plots are tabulated in Appendix A to this report under separate cover.

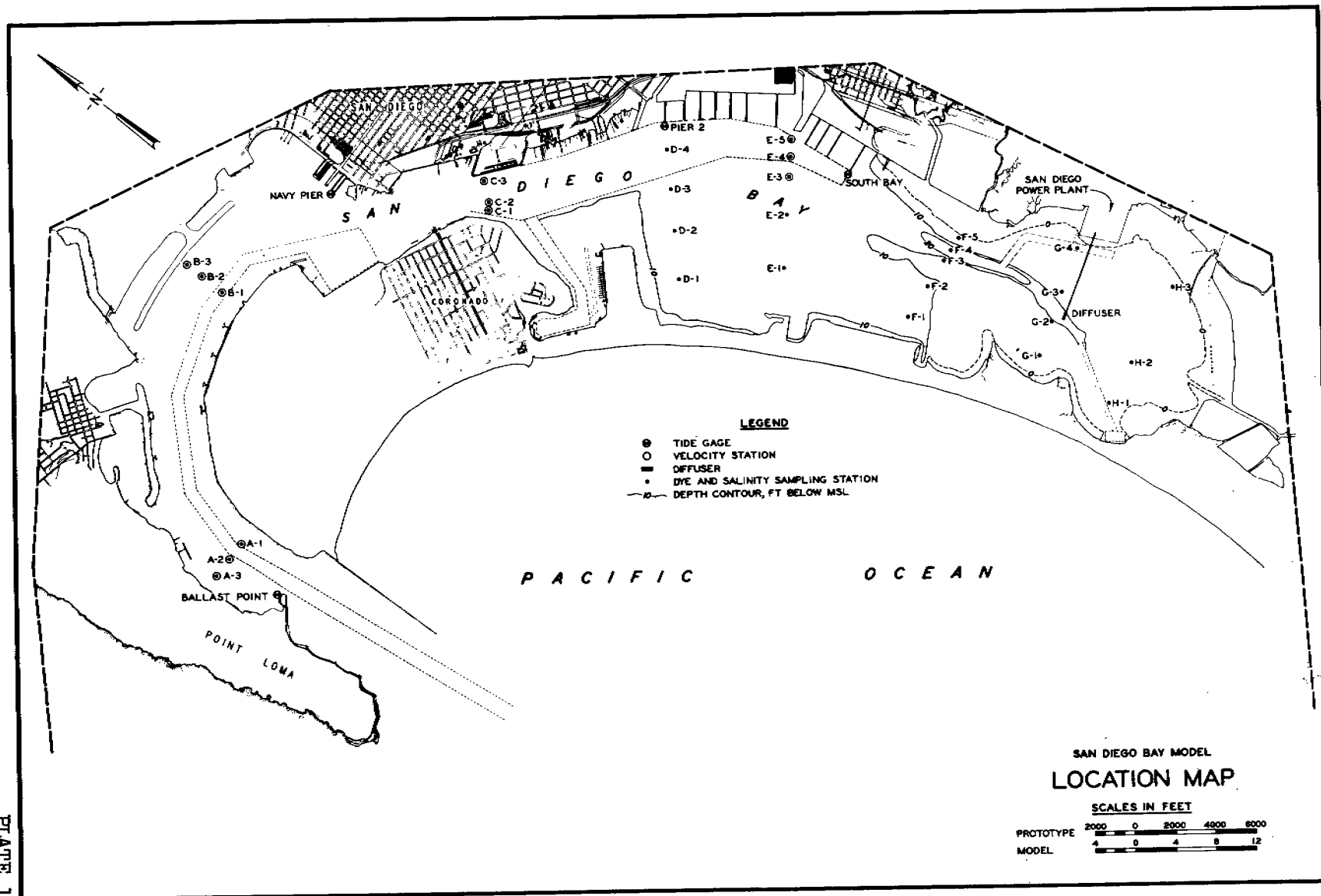
H. Discussion of High-Flow Test Results

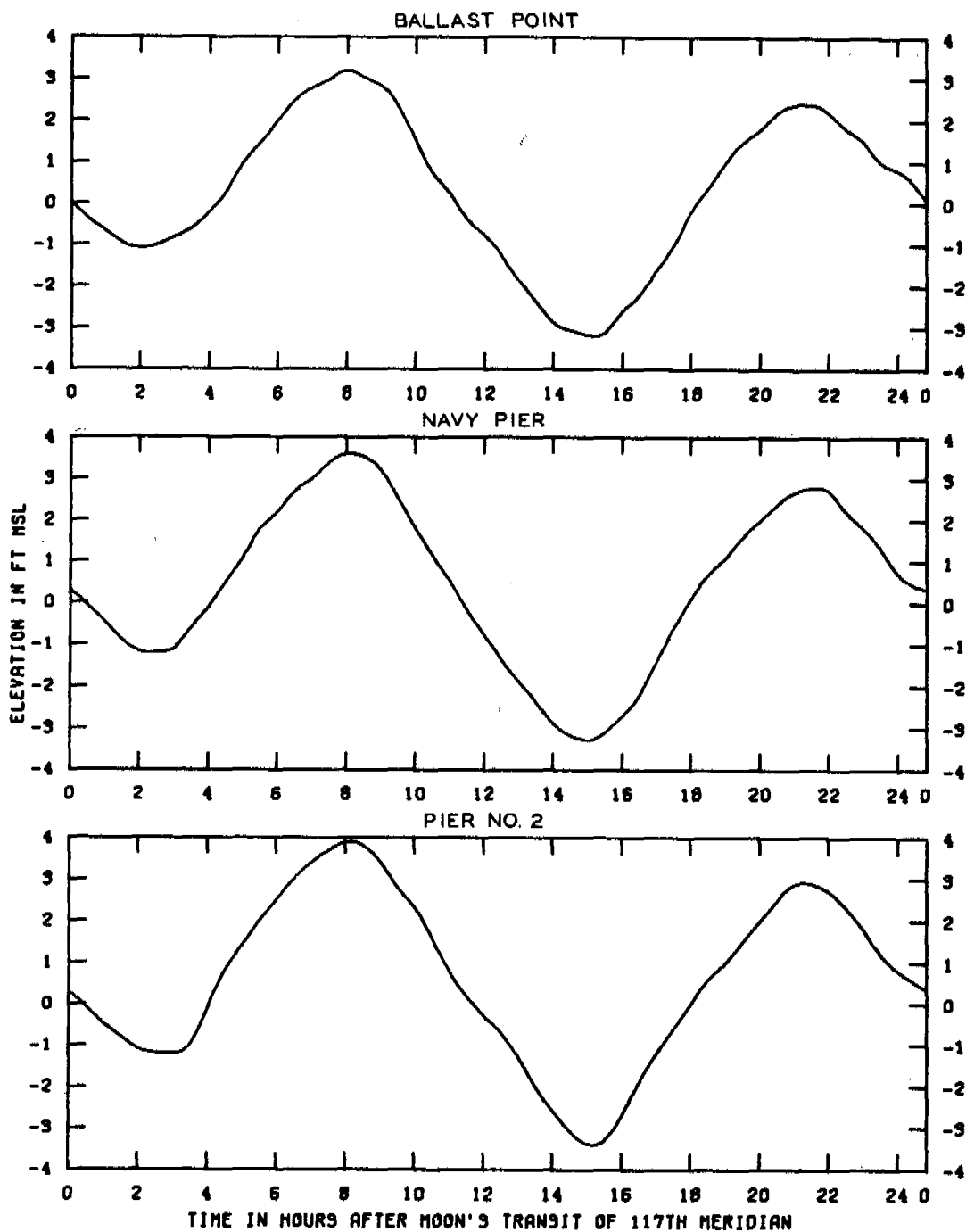
The maximum salinity increase detected during the high-flow test was about 0.16 percent of the initial salinity difference (11.4 ppt) and was found in a comparatively small area on the bottom about 3000 ft long in a downstream direction from the diffuser (station D2) at the time of low-water slack, as shown in plate 168. This represents a maximum increase in salinity concentration in that area of about 0.02 ppt ($11.4 \text{ ppt} \times 0.16 \text{ percent}$). At bottom depth at high-water slack, significant concentrations of dye extended only 6000 ft upstream (sta U2) and 10,000 ft downstream (sta D3) from the diffuser, as shown in plate 169. Maximum observations were only about 0.09 percent of the initial salinity difference (11.4 ppt). As in the case of the mean-flow test, dispersion of the effluent was increased with increasing freshwater inflow. Apparently the dynamic equilibrium distribution of the effluent was achieved in about 10-30 cycles after effluent injection was initiated, depending on the distance from the diffuser.

SECTION V: CONCLUSIONS

Based on the results of model tests of a 10-mgd desalination plant reported herein, the following conclusions have been reached:

1. Test results for the plant outfall located in the San Diego Bay model indicated that for an estuary similar to San Diego Bay where minimal tidal current velocities exist and very little fresh water discharges into the system the dispersion and flushing rates will be extremely slow. Even though the dispersion rate in such a system will be quite slow, the maximum salinity increase to be expected will probably be about 1 to 2 ppt close to the outfall. These characteristics would be significant factors in evaluating the potential effects of desalination plants located on estuaries of this type.
2. The results of the tests in the Galveston Bay model indicated that care should be taken in selecting an outfall site. Velocities in the vicinity of the proposed site should be great enough to generate sufficient mixing or dispersion after the energy of the jet leaving the diffuser is expended. The site investigated in the Galveston Bay model is not considered to be a good location for releasing the waste from a desalination plant because of the low velocities at the diffuser location, even though there is a significant freshwater inflow to the bay. Wind-induced mass circulation phenomena can be significant in a broad, shallow bay (like Galveston Bay) subject to appreciable and essentially constant winds. This factor was not included in the model investigation but should be considered in any proposed site investigation.
3. The results of tests in the Delaware River model indicated that in an estuary of this type (having appreciable freshwater discharge, relatively strong tidal current velocities, and a reasonably regular shape) sufficient mixing and dispersion of the effluent will probably occur after the energy of the jet leaving the diffuser is expended. The freshwater discharge and tidal currents generate high turbulence (thus mixing) throughout the system, and the regular shape reduces the possibility of "dead water" which can develop in side embayments, etc.
4. The results of tests in the Delaware River model also showed, as would be expected, that the mixing or dispersion rate in this type of system is directly related to the river discharge. As the river discharge increases, the mixing or dispersion rate also increases.





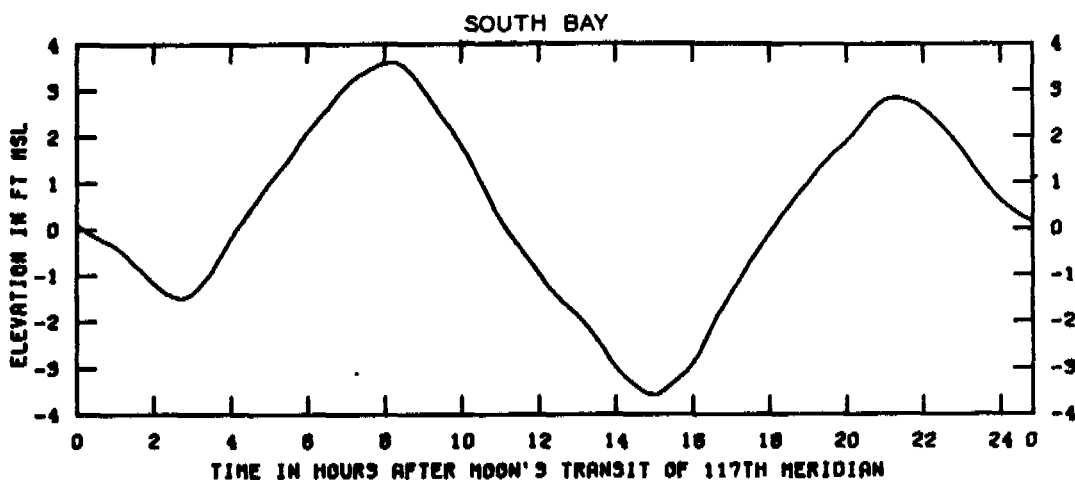
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

6.2 FT
0.0 PPT

SAN DIEGO MODEL

TIDAL OBSERVATIONS

STATIONS: BALLAST POINT,
NAVY PIER, AND PIER NO. 2



TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

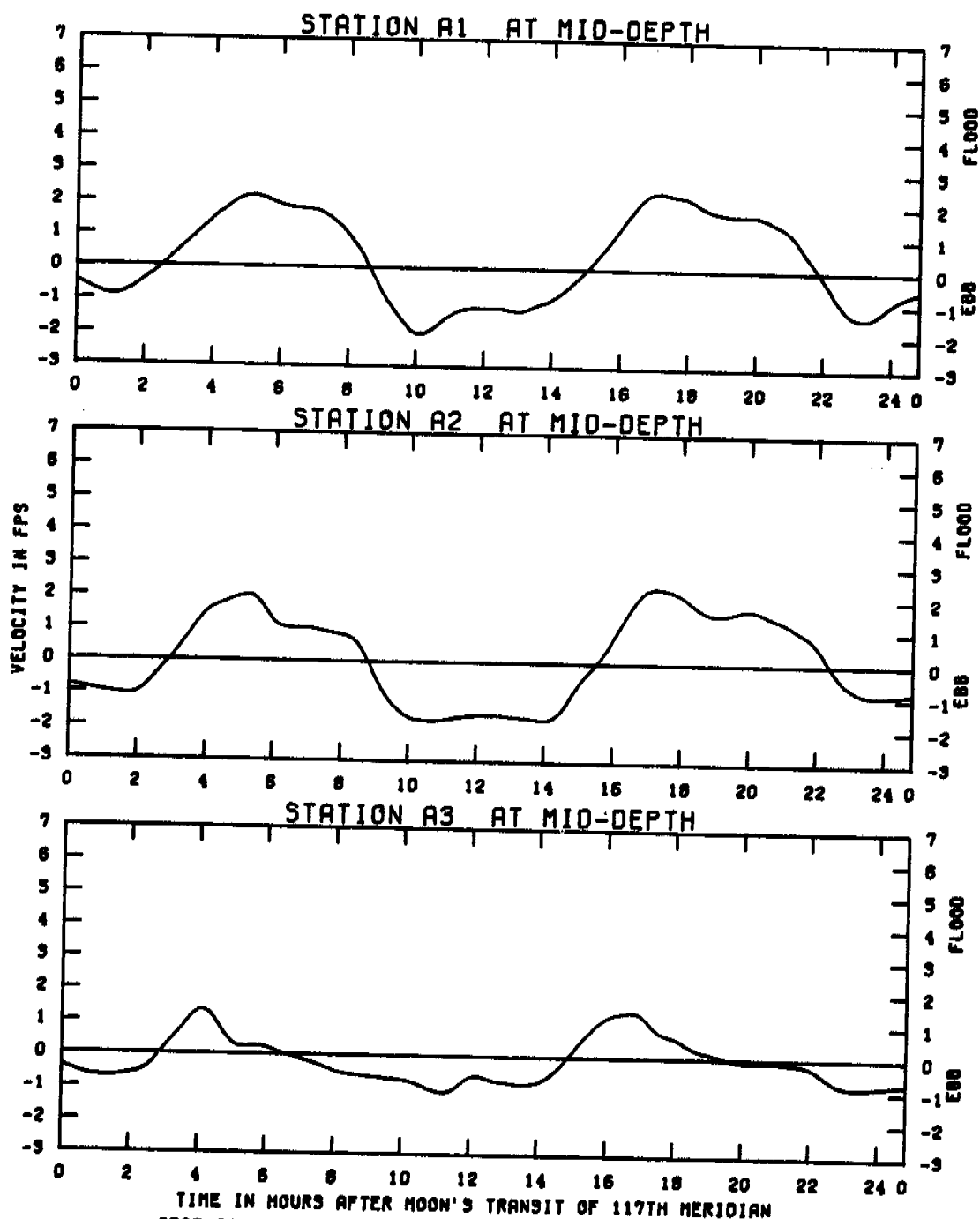
6.2 FT
0.0 PPT

SAN DIEGO MODEL

TIDAL
OBSERVATIONS

STATION: SOUTH BAY

PLATE 3



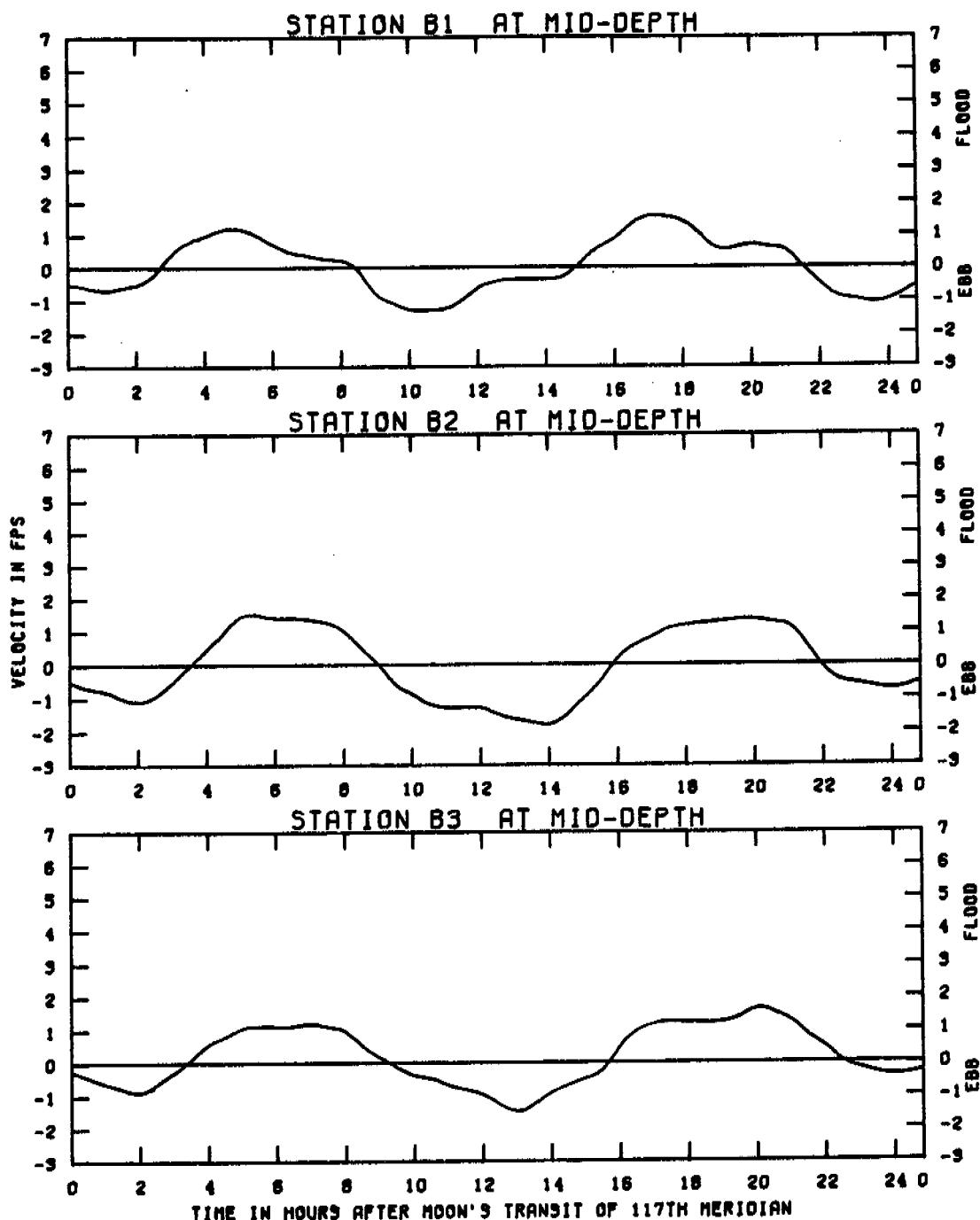
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

8.2 FT
0.0 PPT

SAN DIEGO MODEL

VELOCITY
OBSERVATIONS

STATIONS
A1 . A2 . AND A3



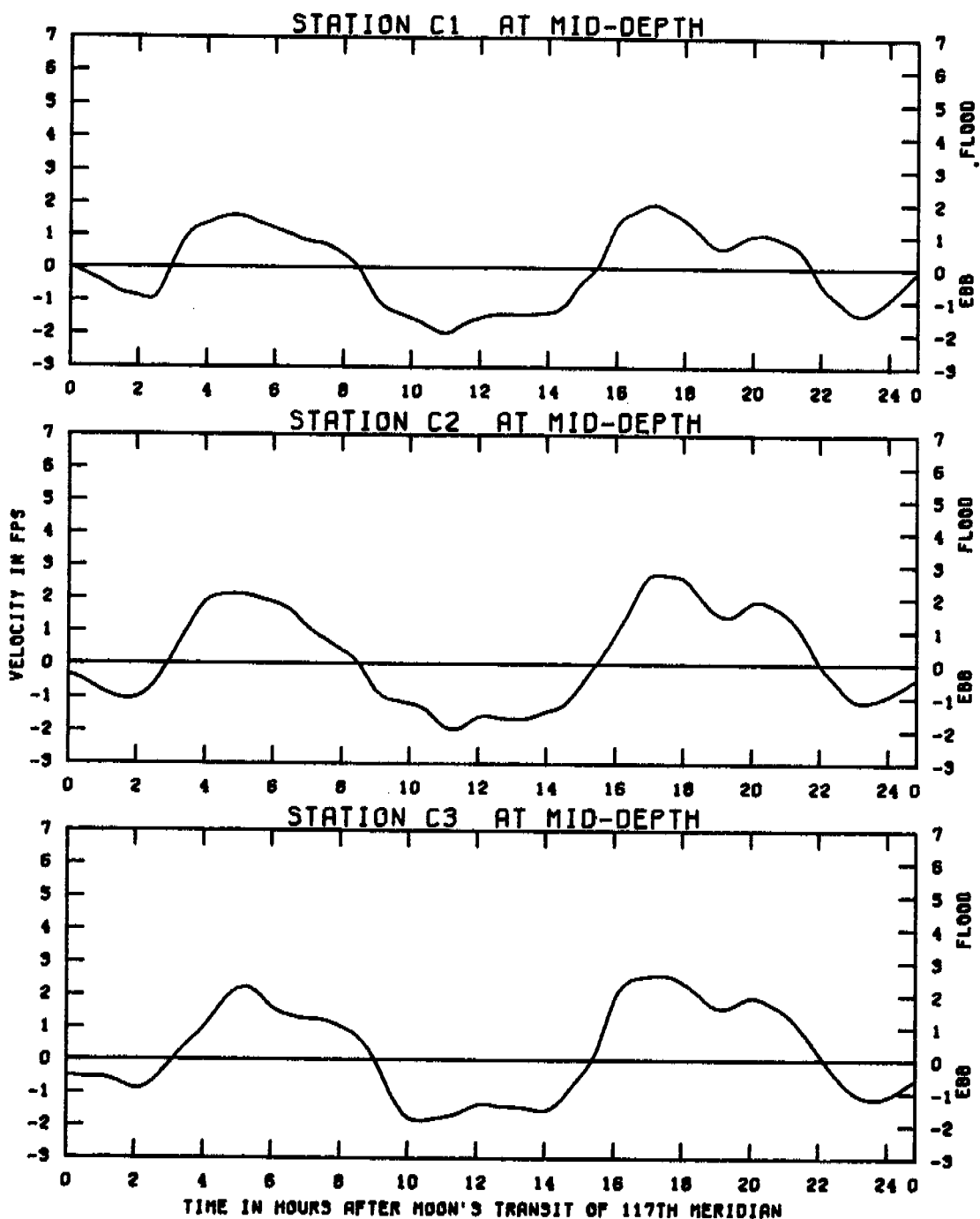
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

6.2 FT
0.0 PPT

SAN DIEGO MODEL

VELOCITY
OBSERVATIONS

STATIONS
B1 . B2 . AND B3



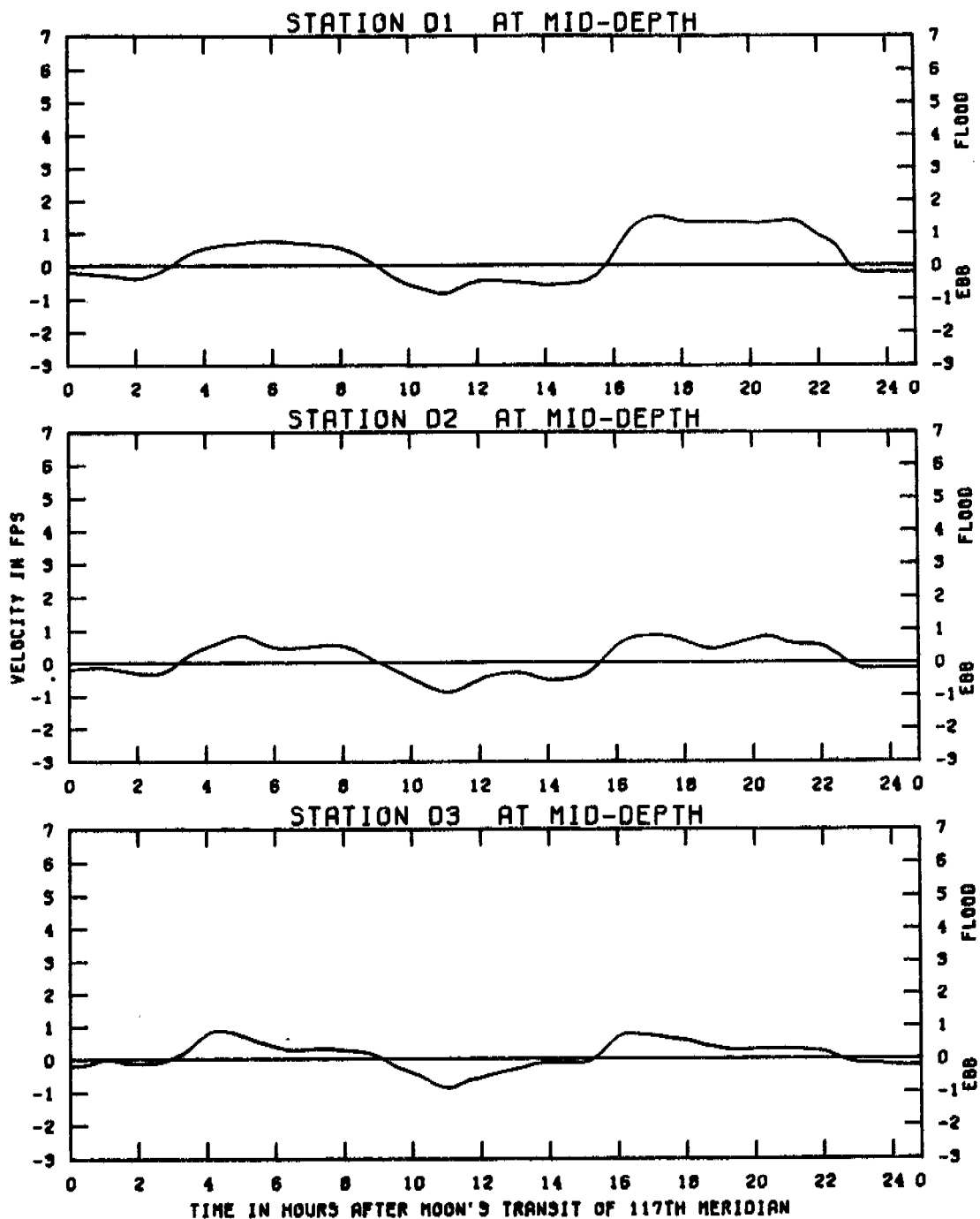
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

6.2 FT
0.0 PPT

SAN DIEGO MODEL

VELOCITY
OBSERVATIONS

STATIONS
C1 . C2 . AND C3



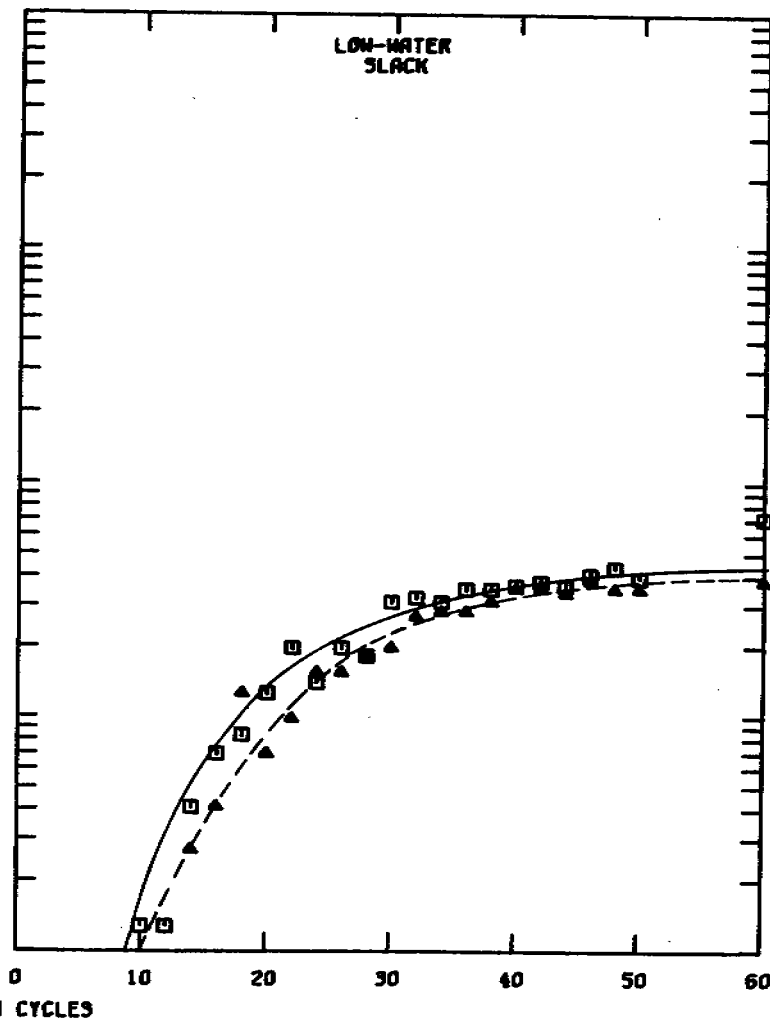
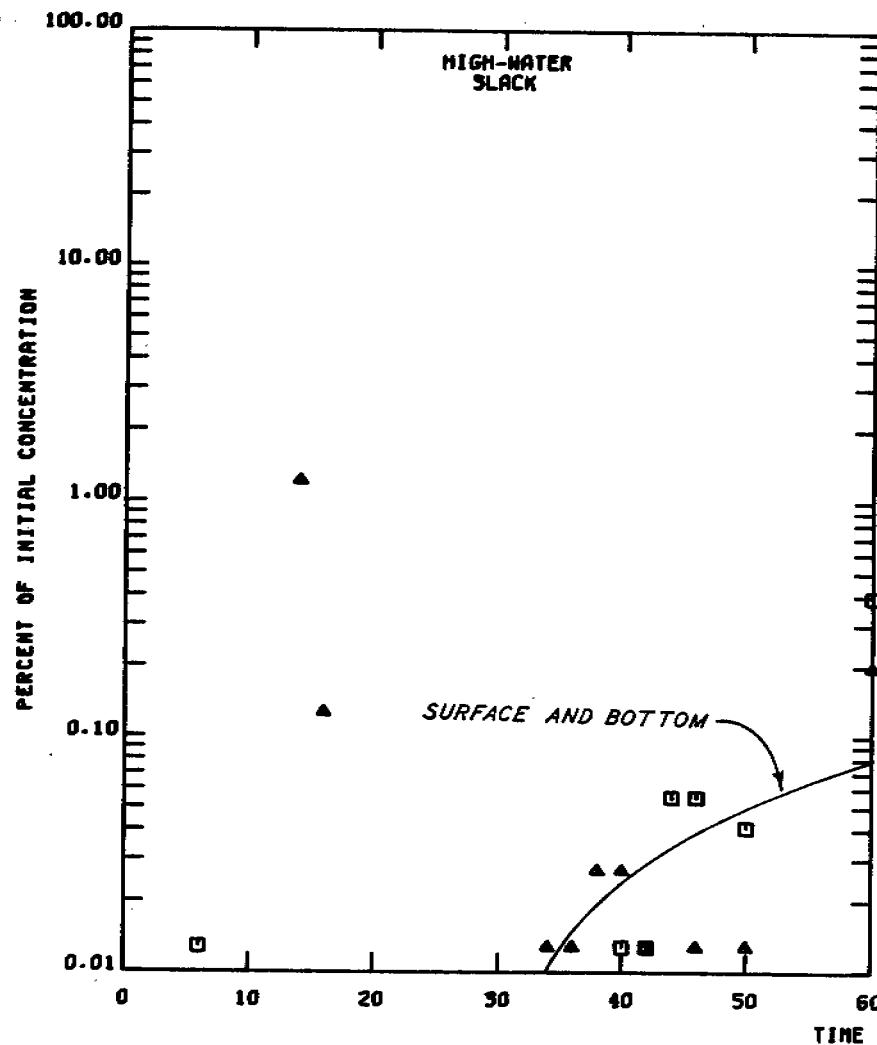
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)

6.2 FT
0.0 PPT

SAN DIEGO MODEL

VELOCITY
OBSERVATIONS

STATIONS
01 . 02 . AND 03

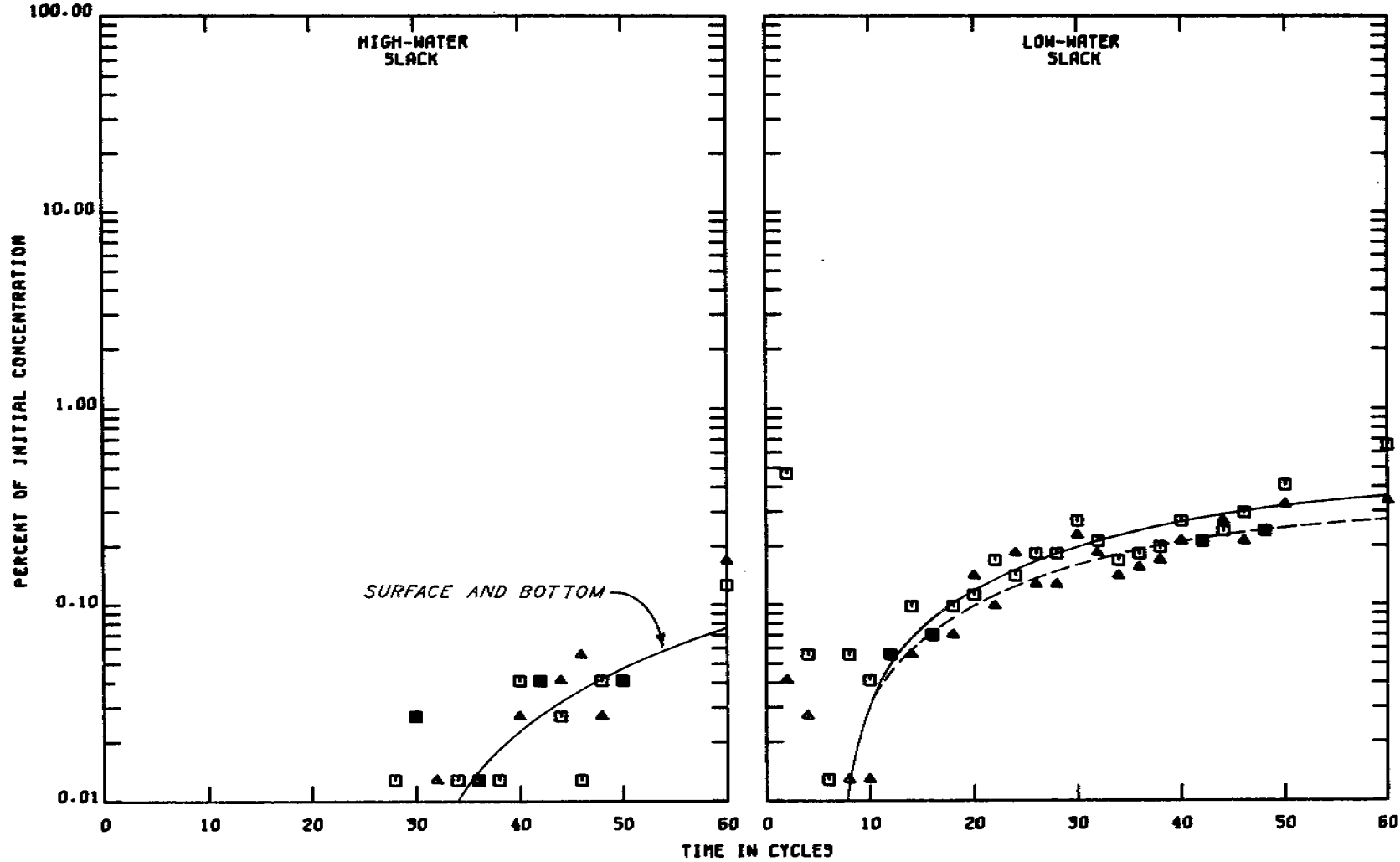


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 8.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

8.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION A1

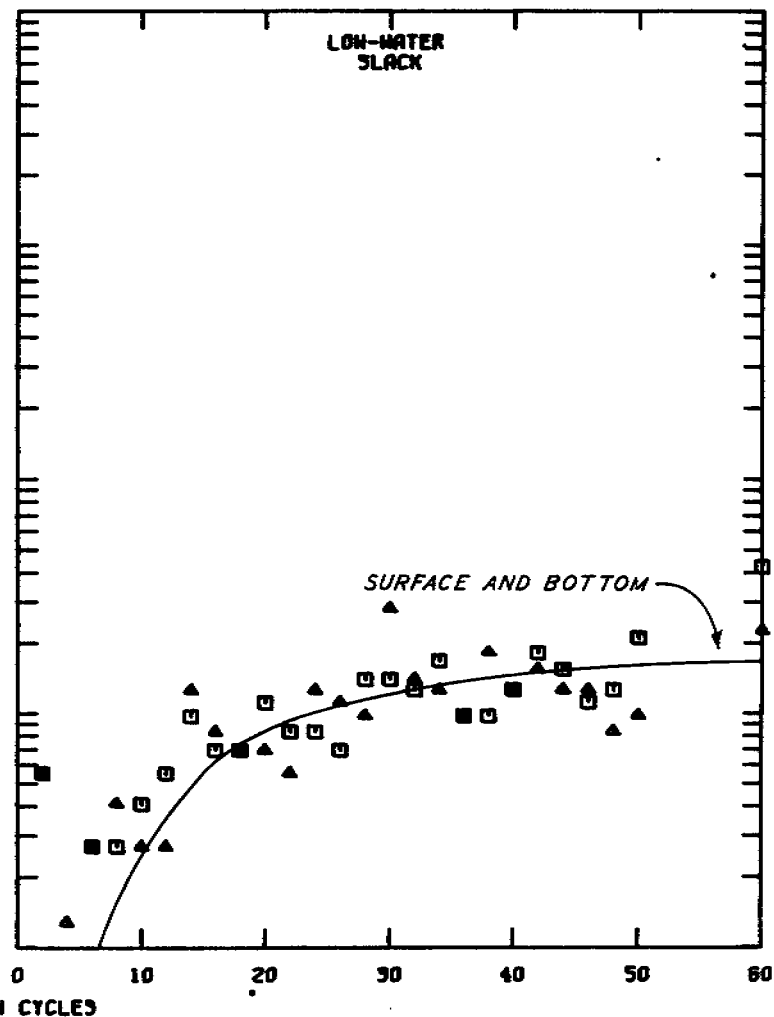
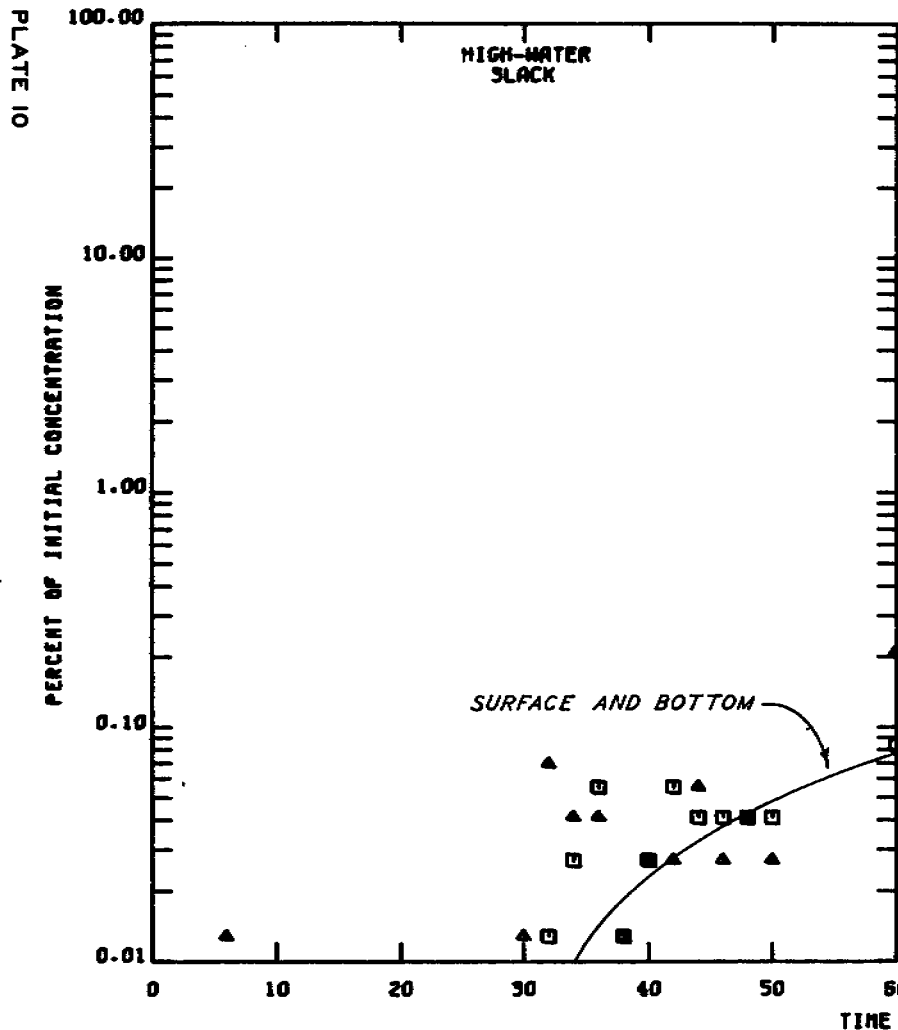


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION A2

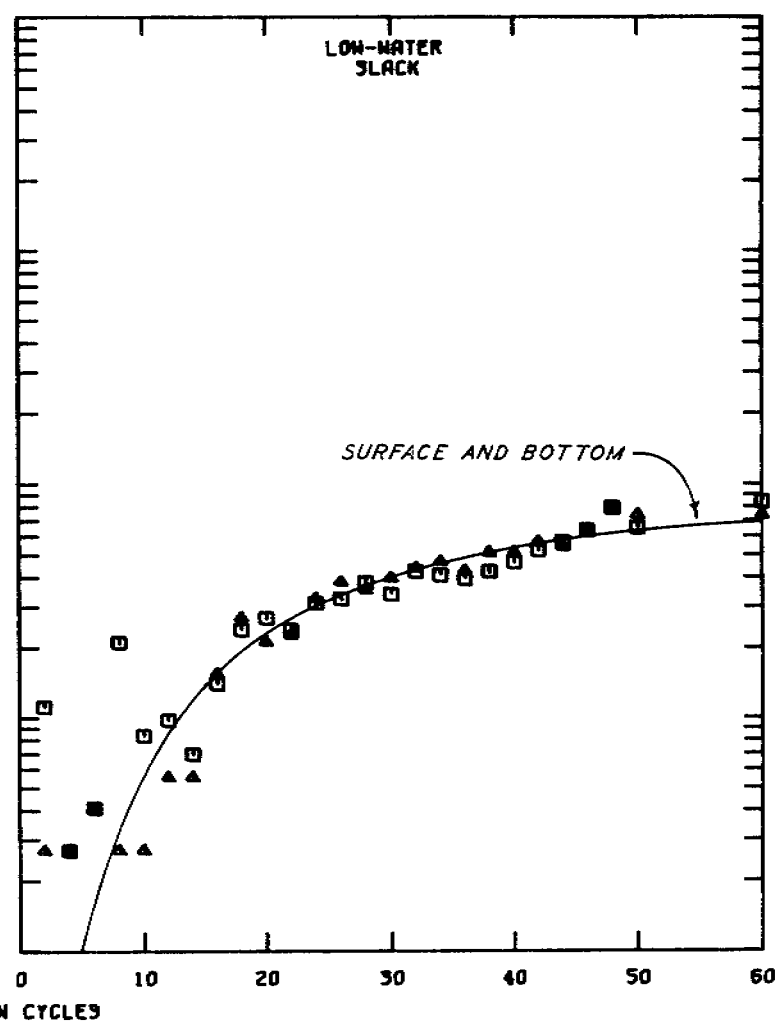
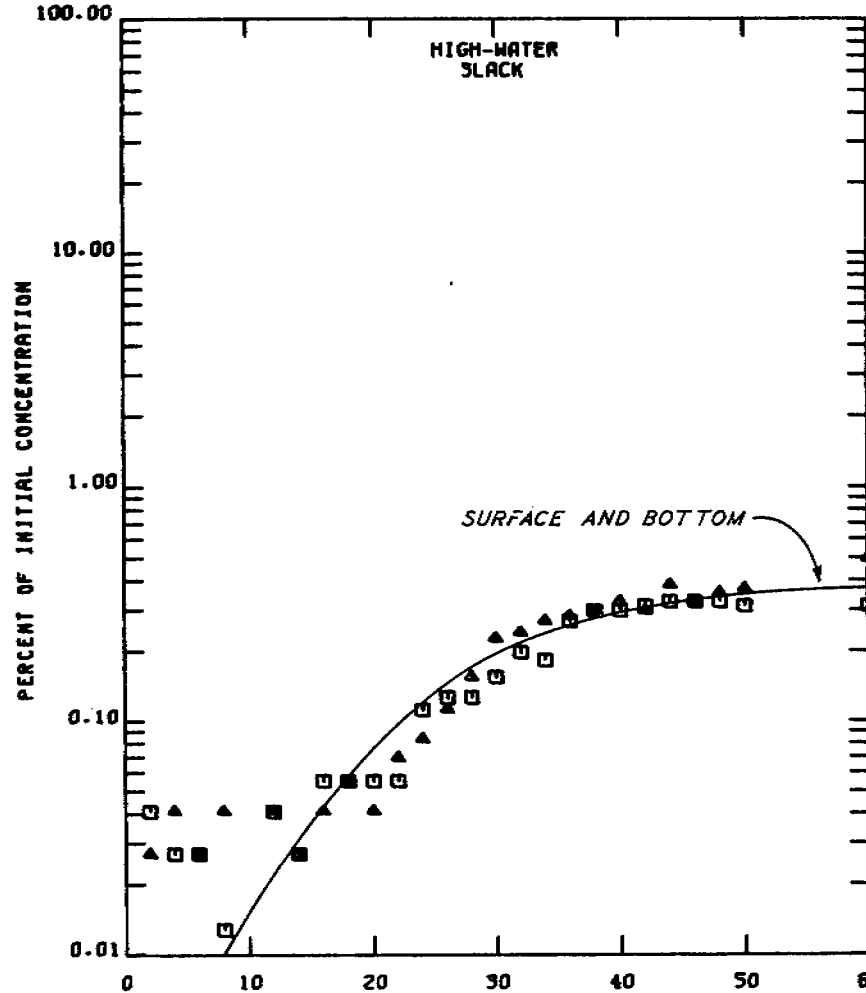


TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ — SURFACE
△ — — — BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION A3

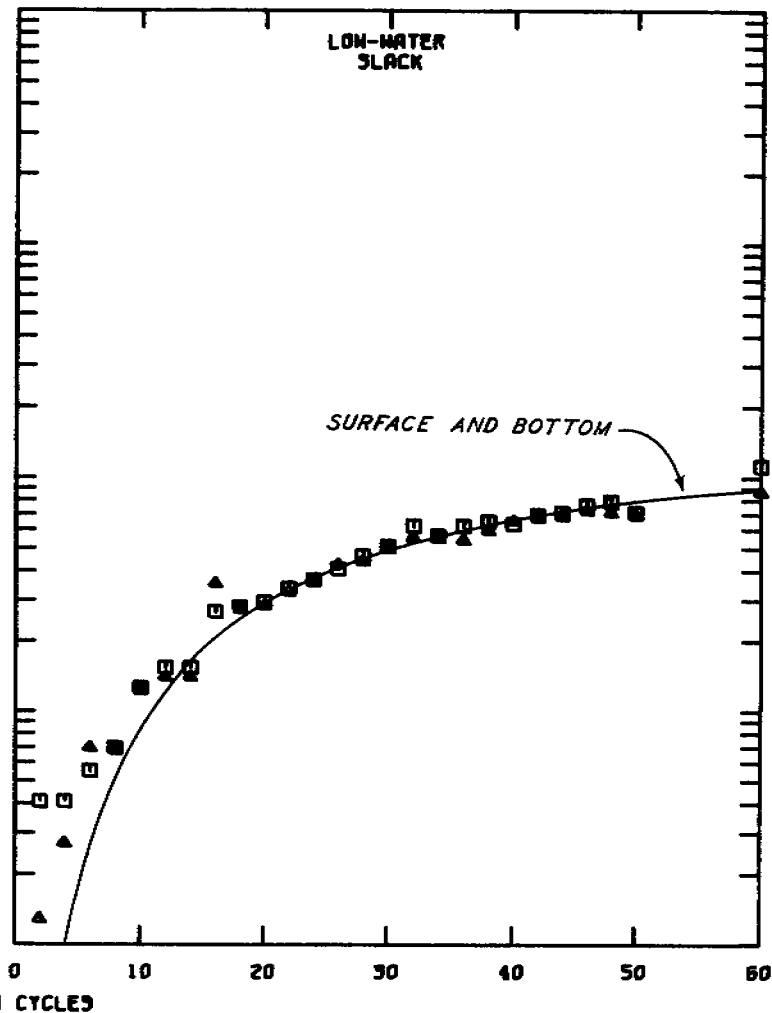
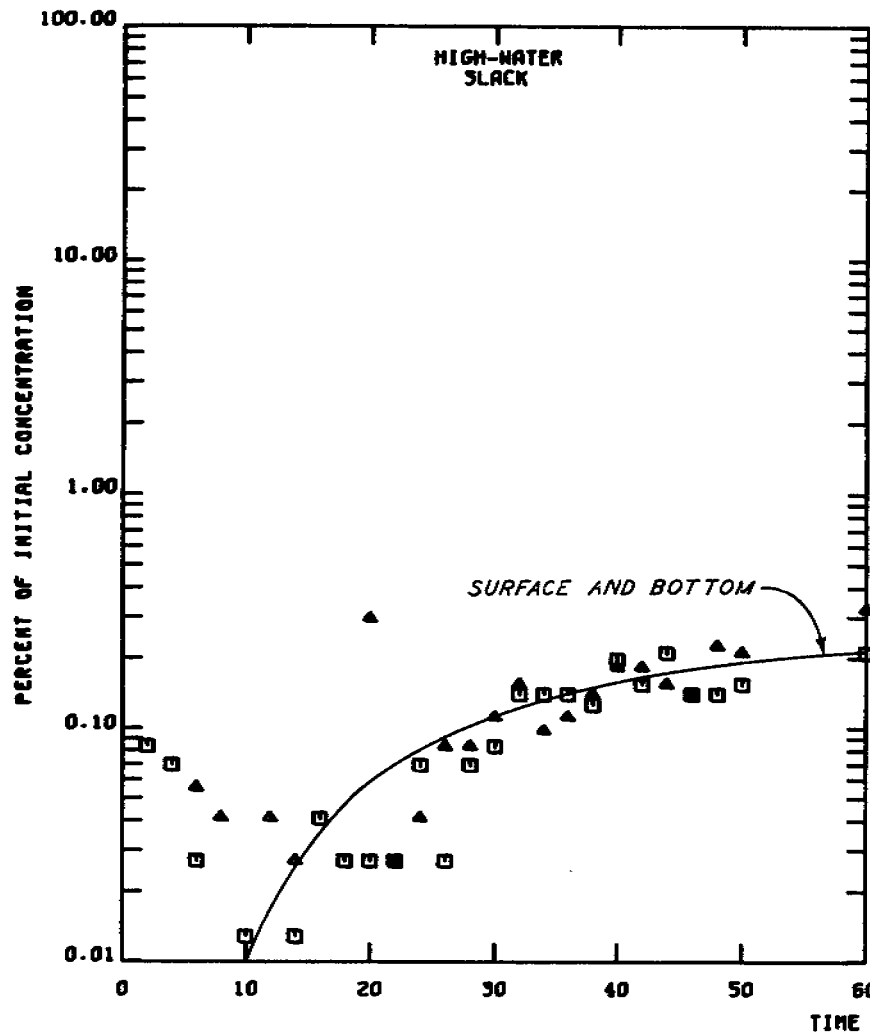


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION 81**

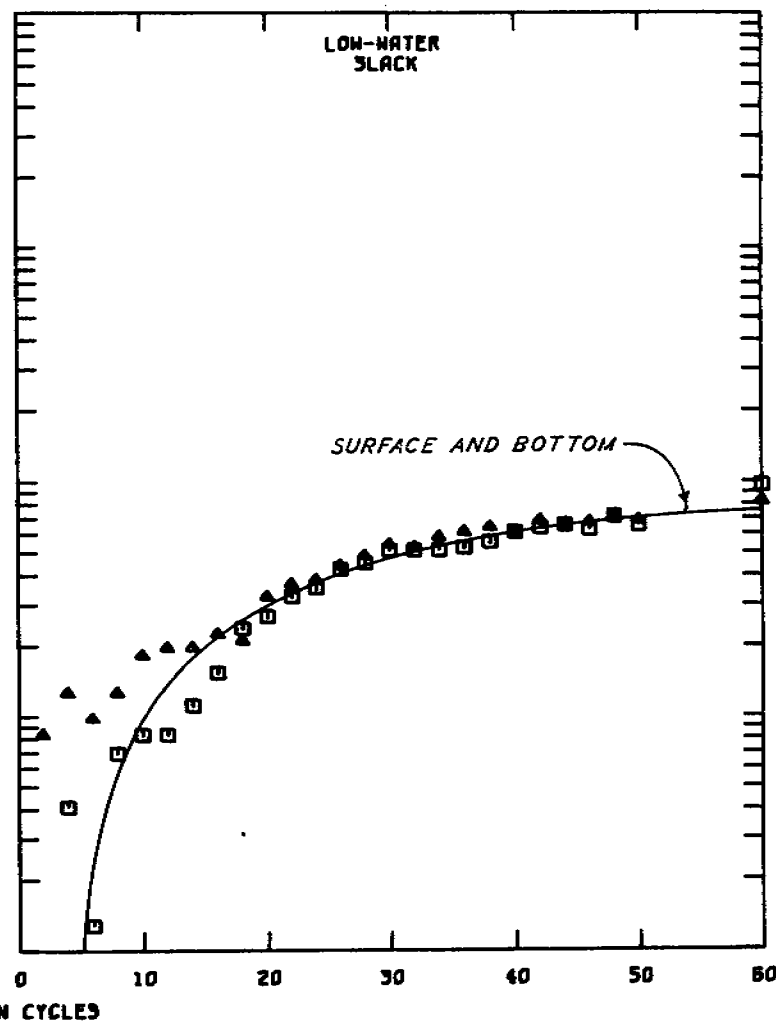
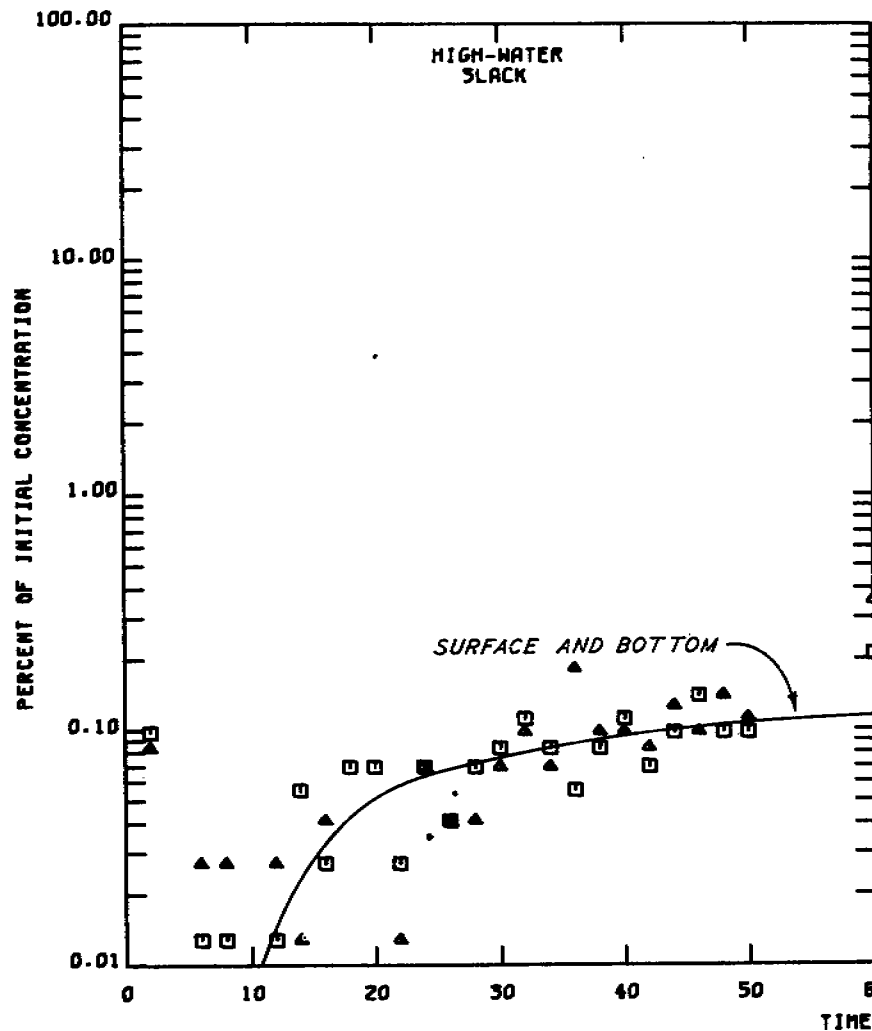


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION 82



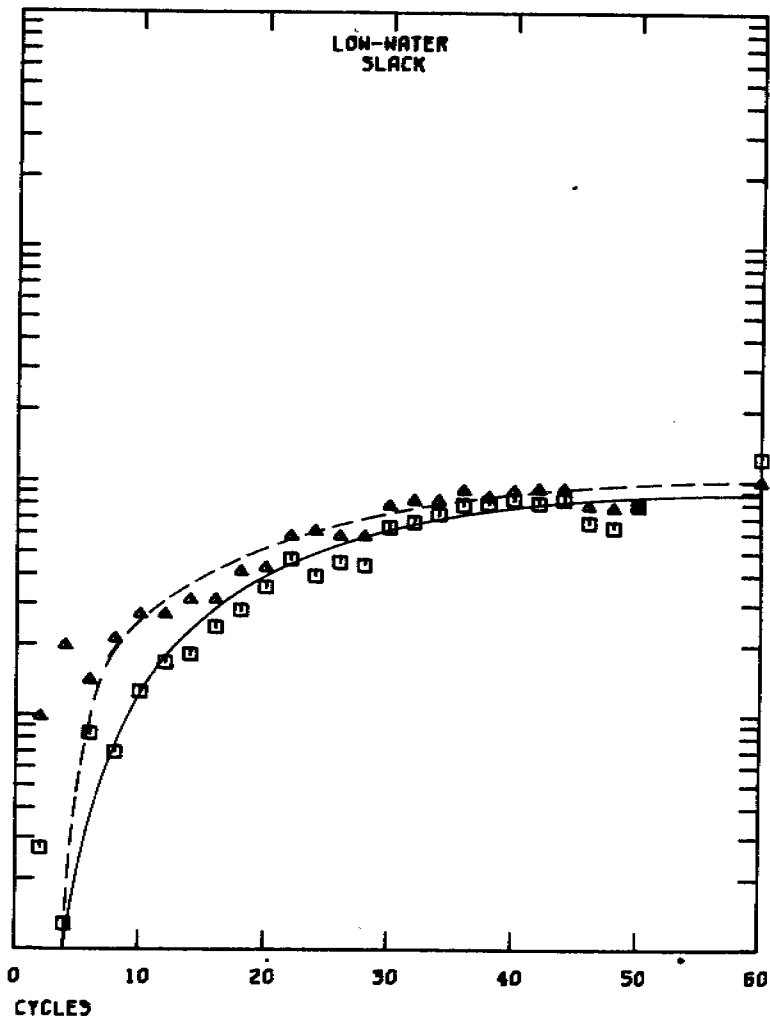
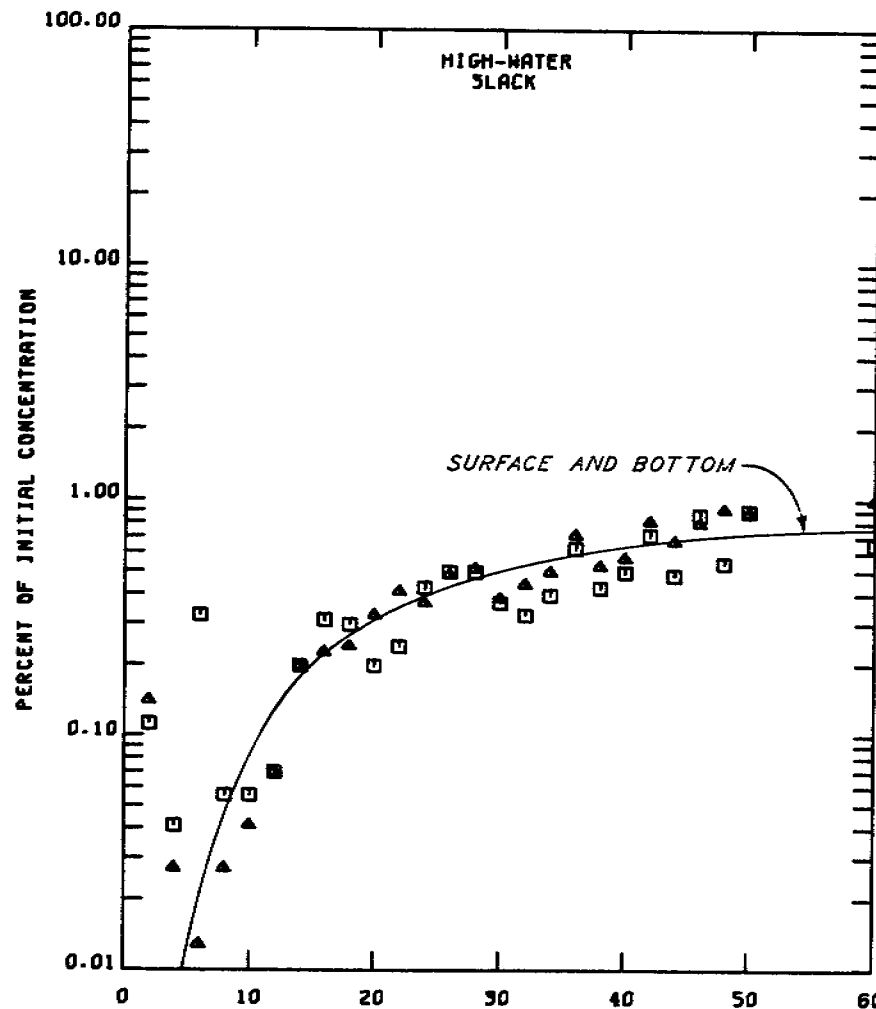
TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND

□ — SURFACE
▲ - - - BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION 83

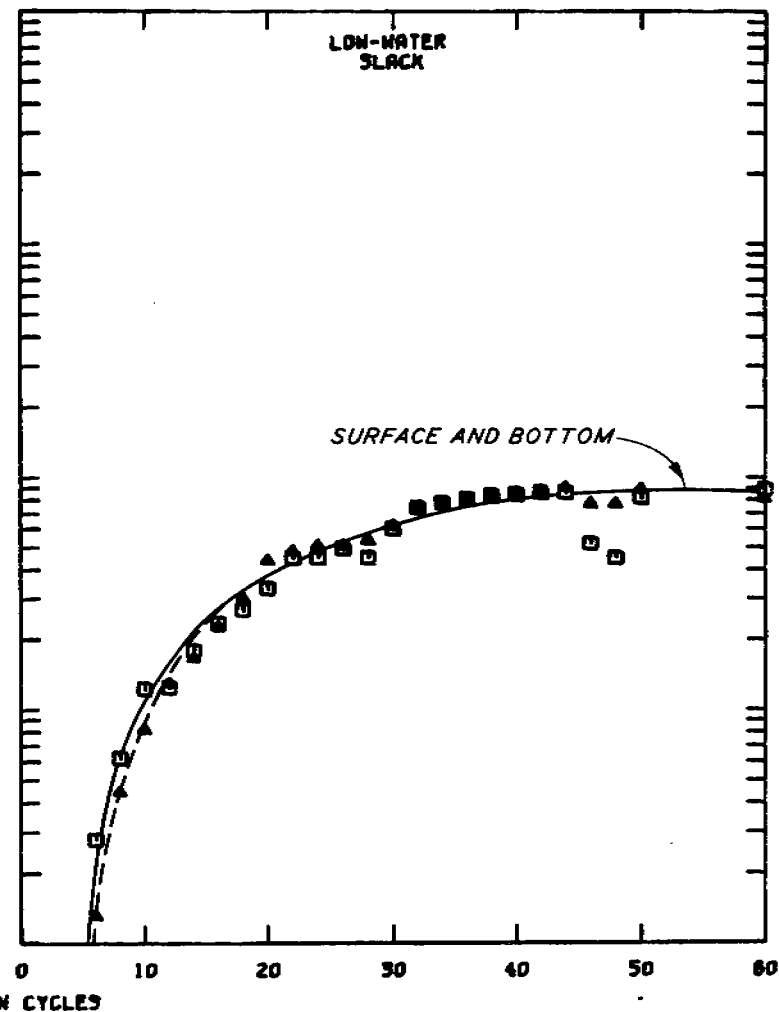
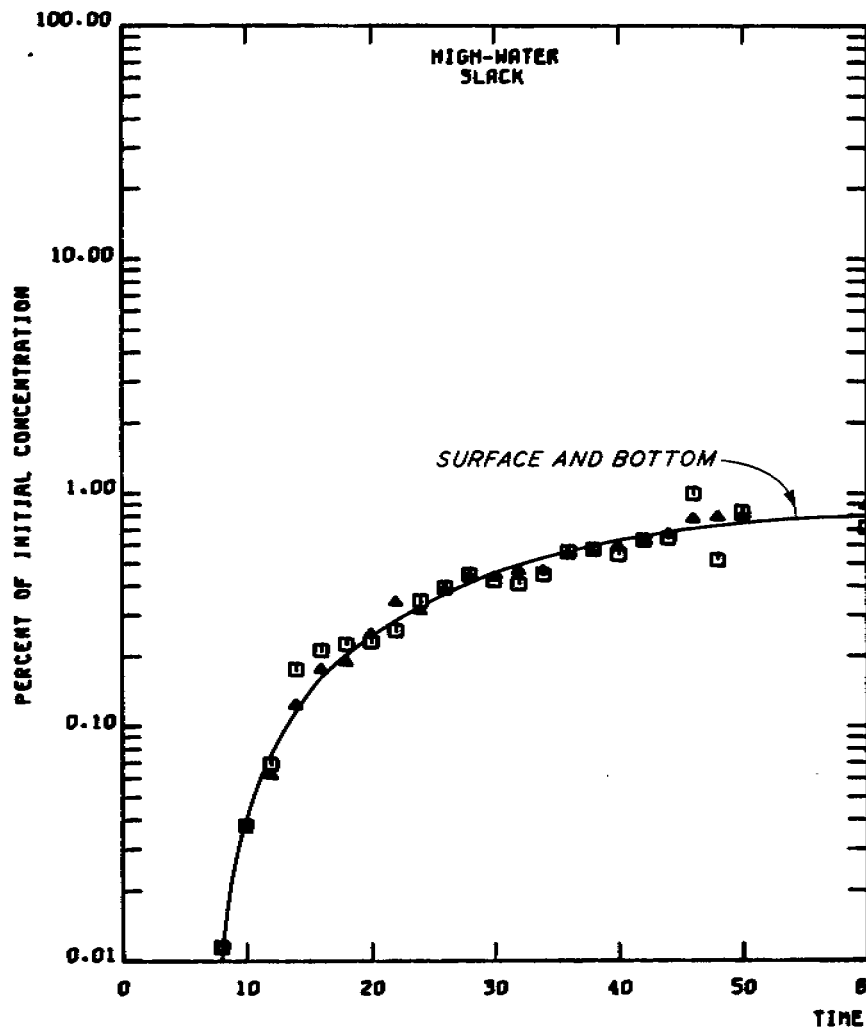


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C1



TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

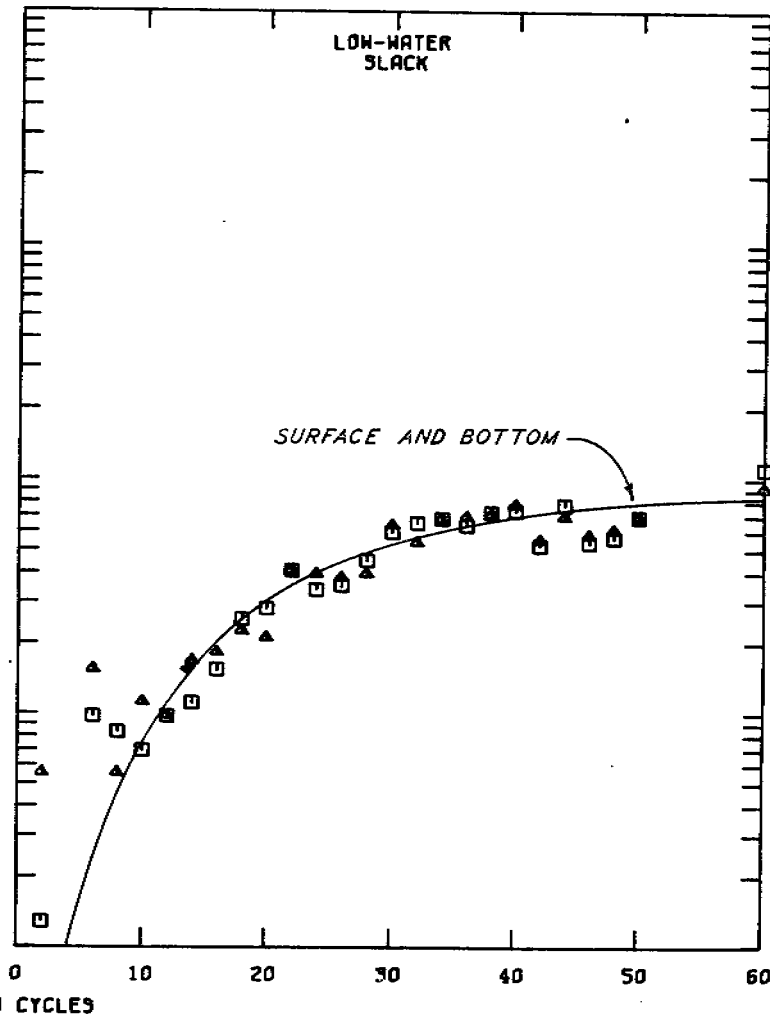
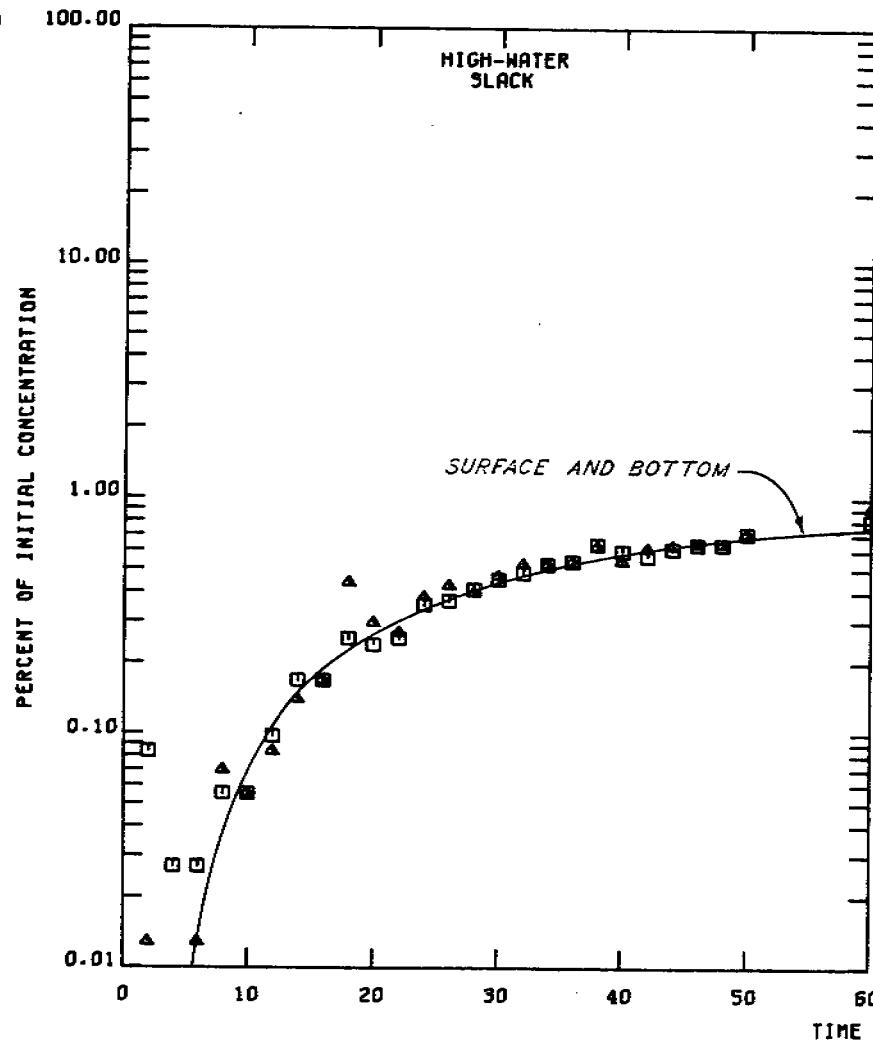
6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND

□ ——— SURFACE
△ ——— BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT

STATION C2



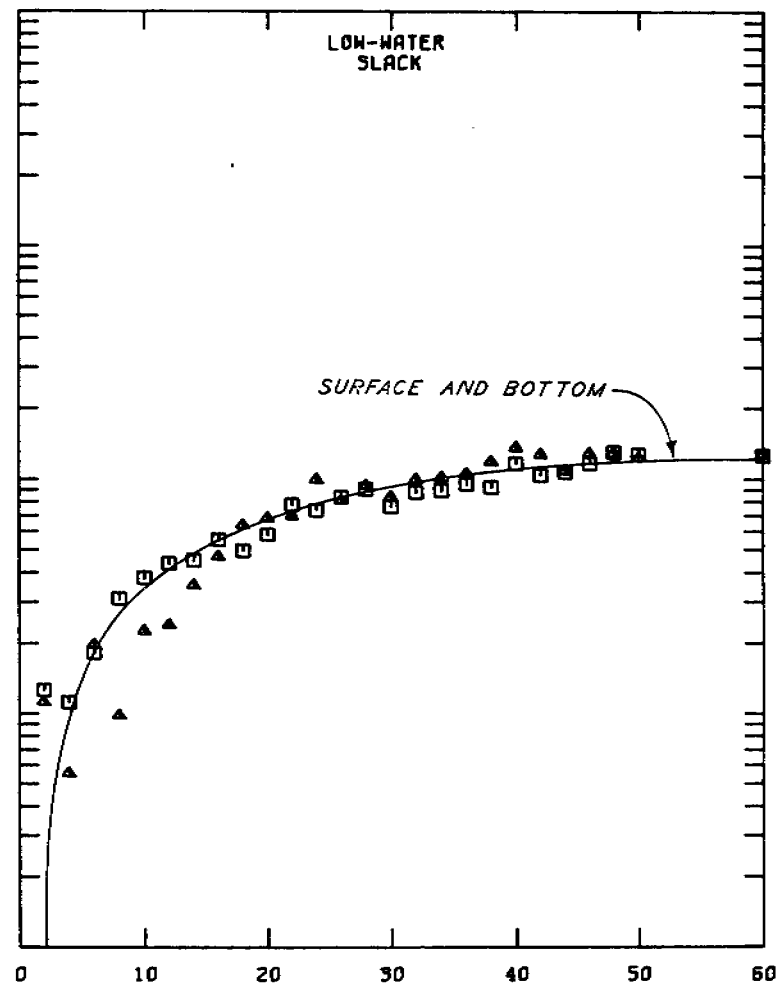
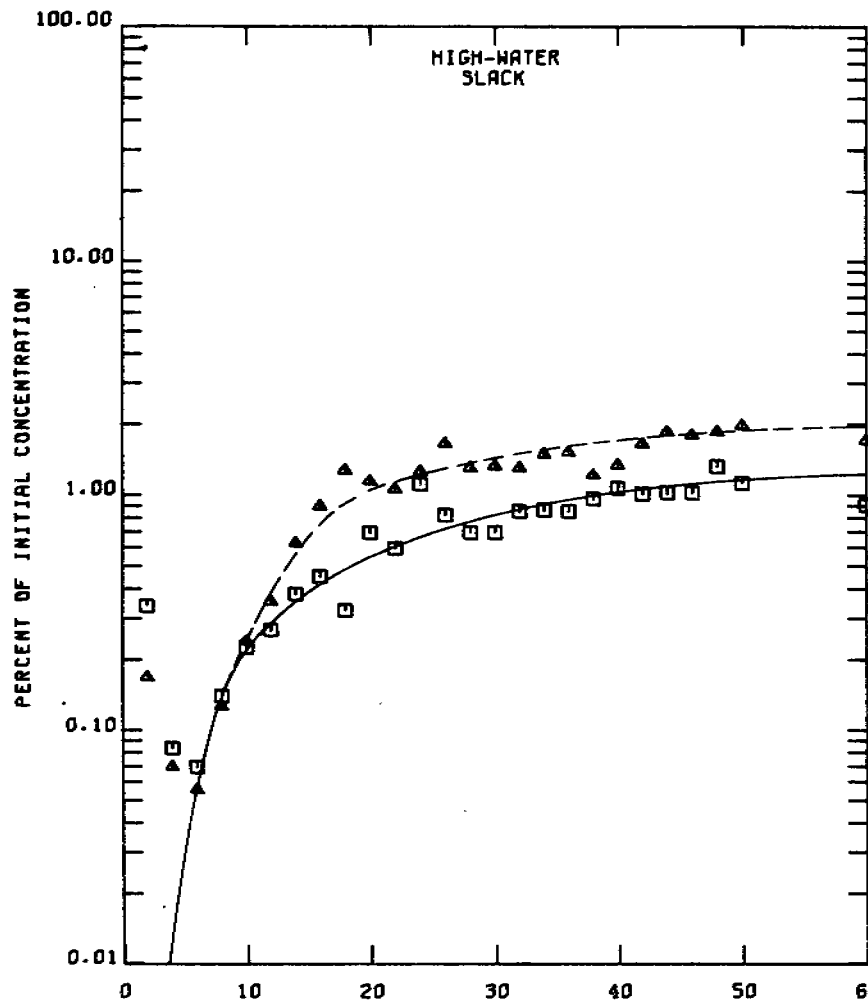
TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ — — — BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C3

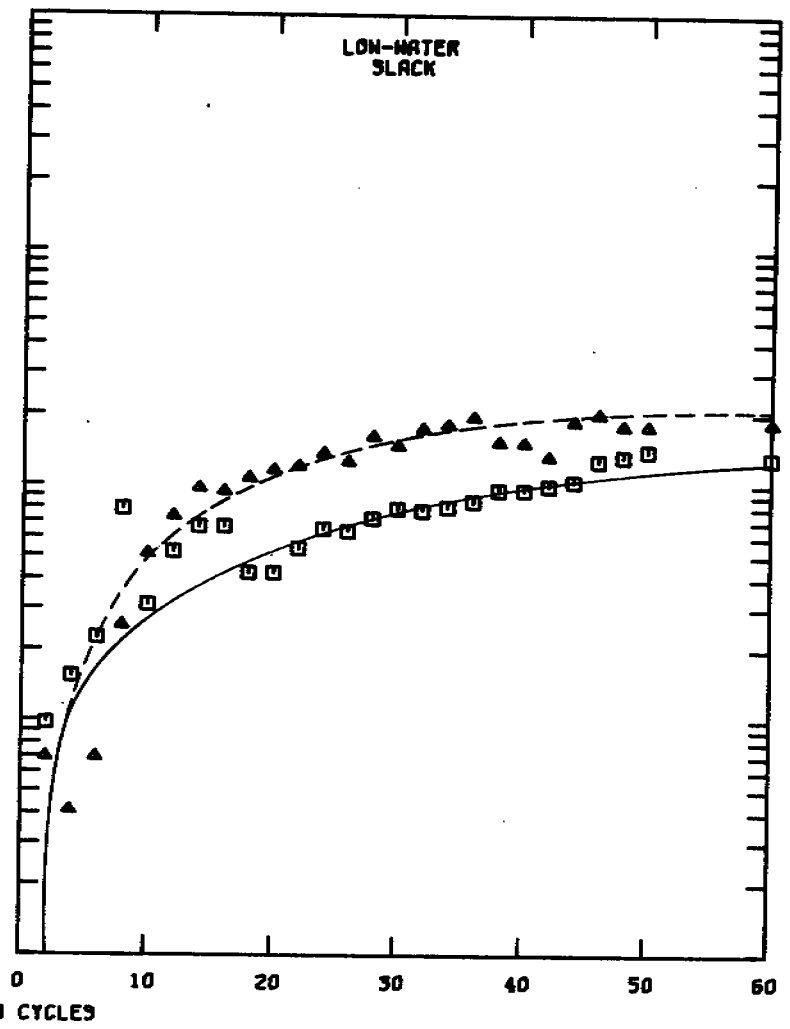
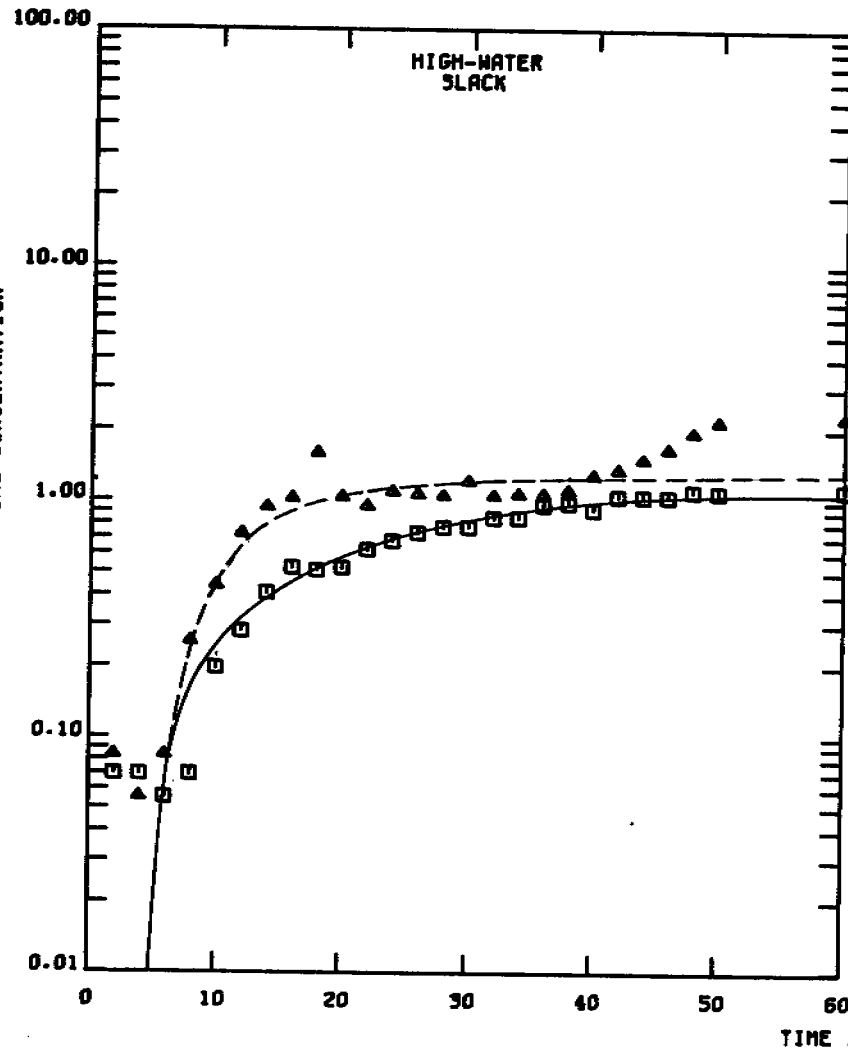


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

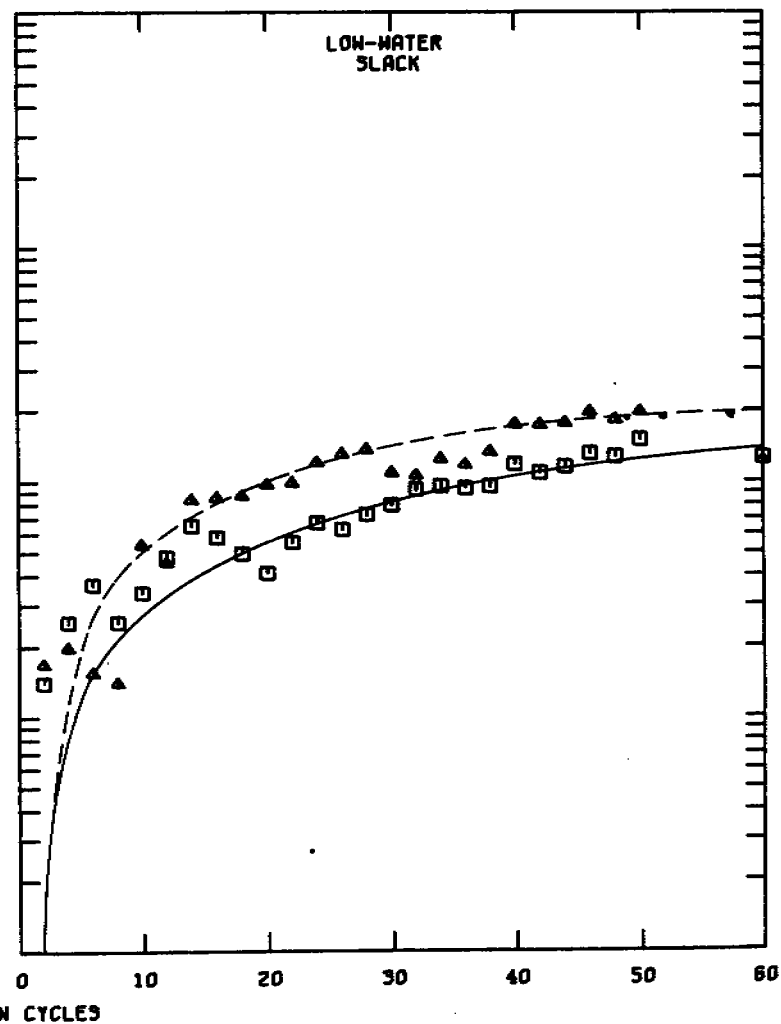
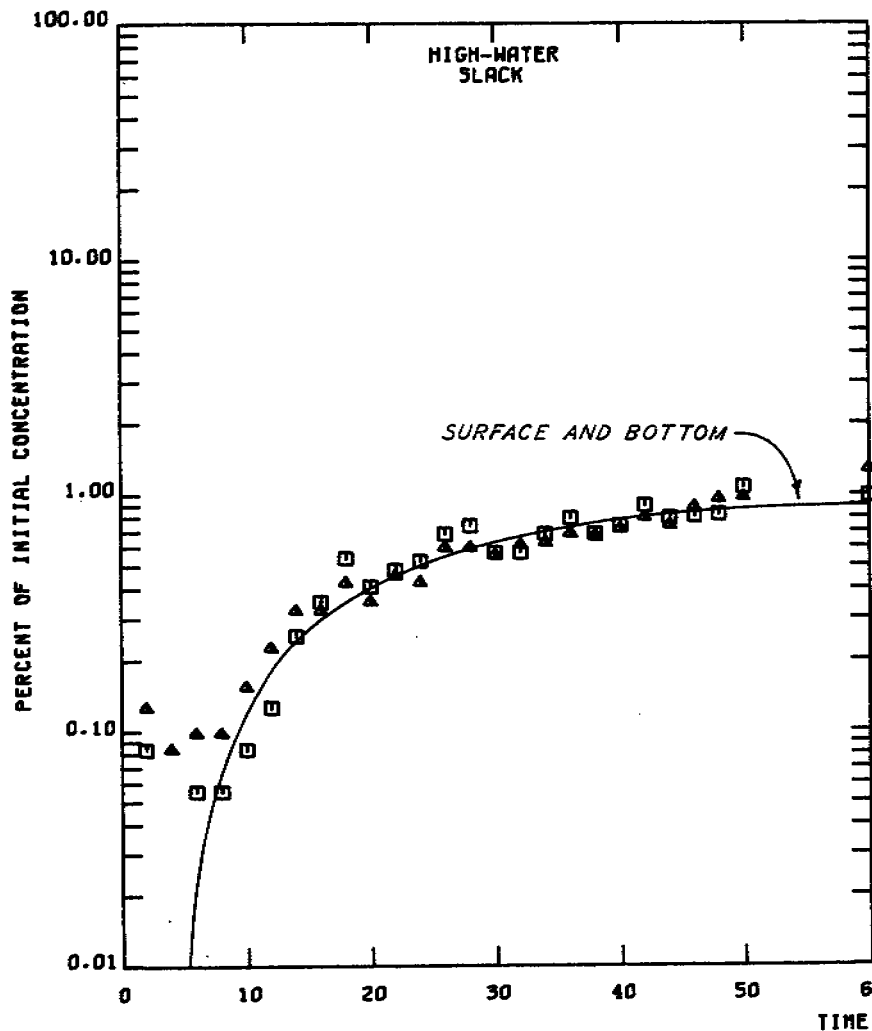
LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD. PLANT
 STATION D1



TEST CONDITIONS		LEGEND	
TIDAL RANGE AT BALLAST POINT	6.2 FT	□ ———	SURFACE
OCEAN SALINITY (TOTAL SALT)	0.0 PPT	▲ - - -	BOTTOM
EFFLUENT CONCENTRATION	11.4 PPT		
EFFLUENT INJECTION RATE	21.2 MGD		

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION 02



TEST CONDITIONS

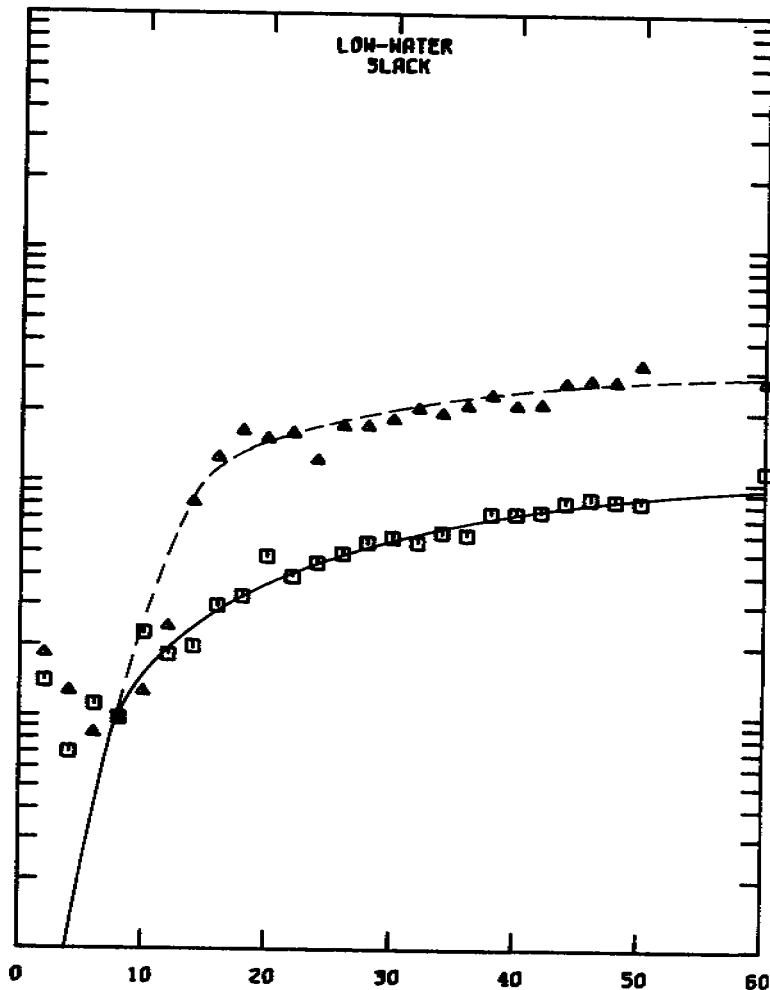
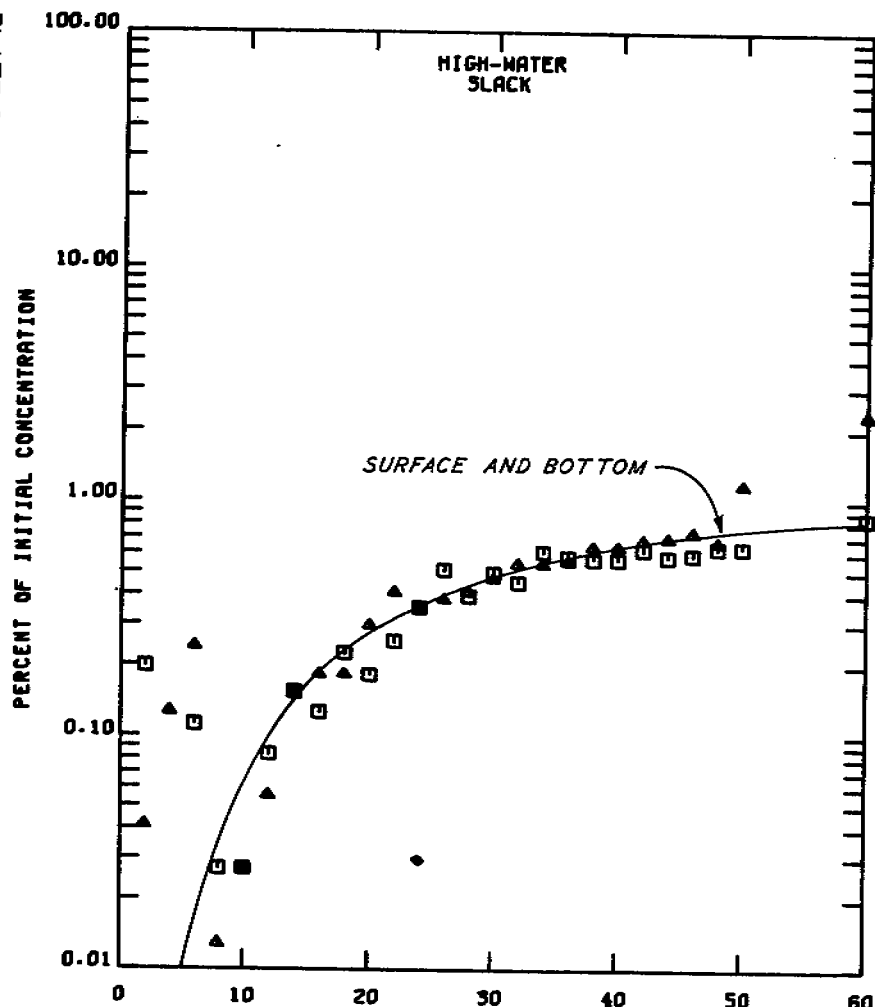
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND

□ ——— SURFACE
△ - - - - BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION 03

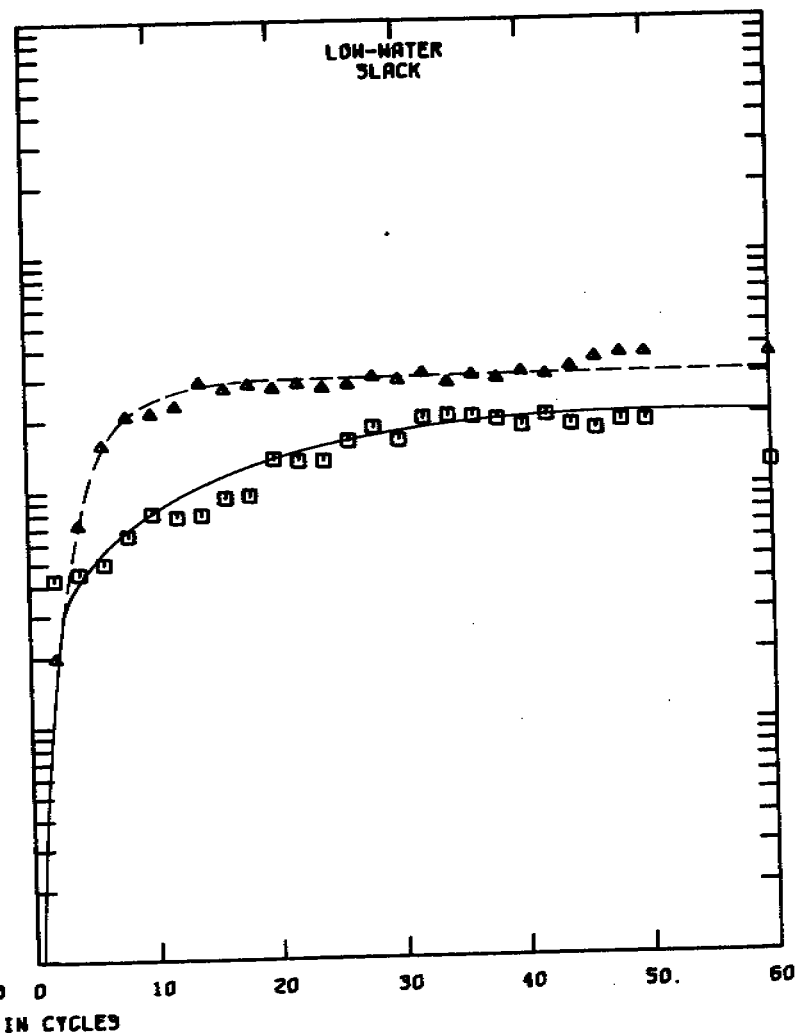
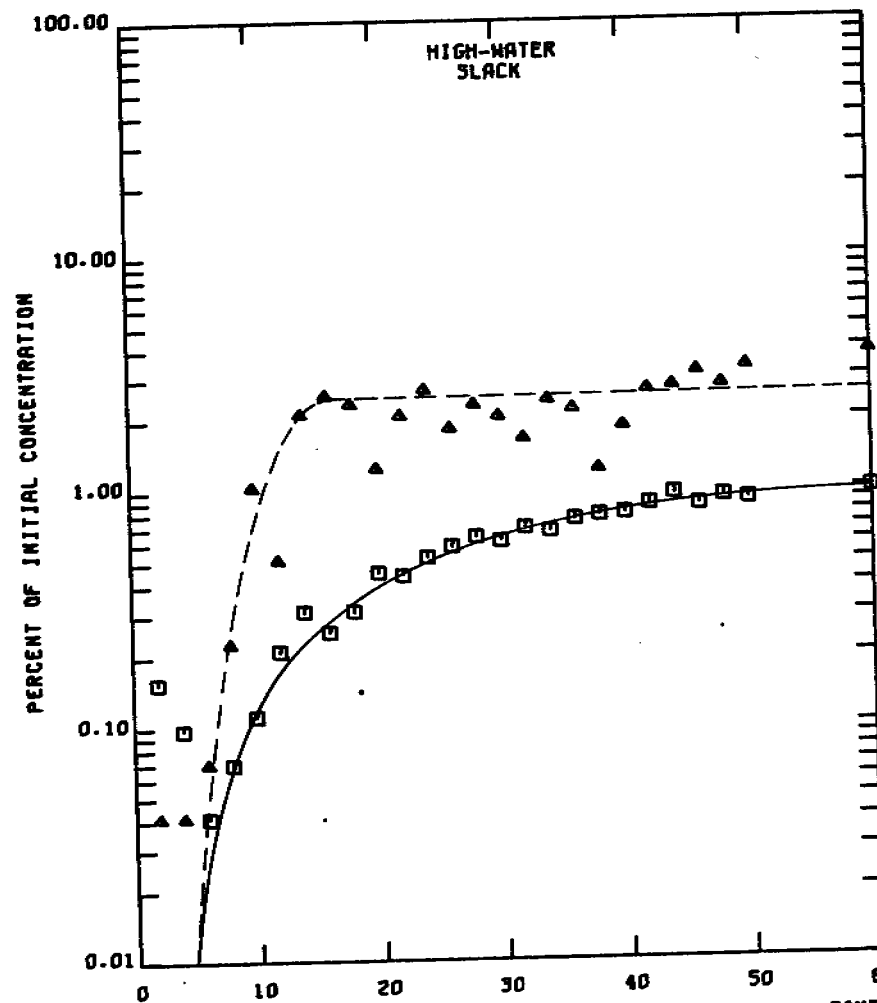


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION D4

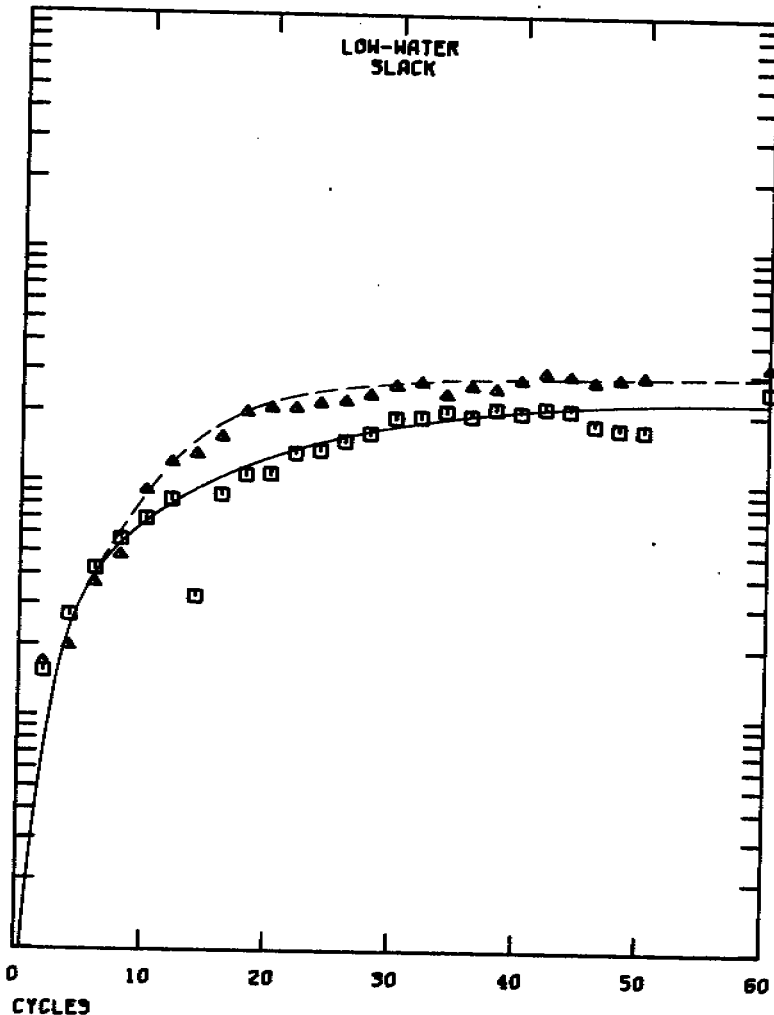
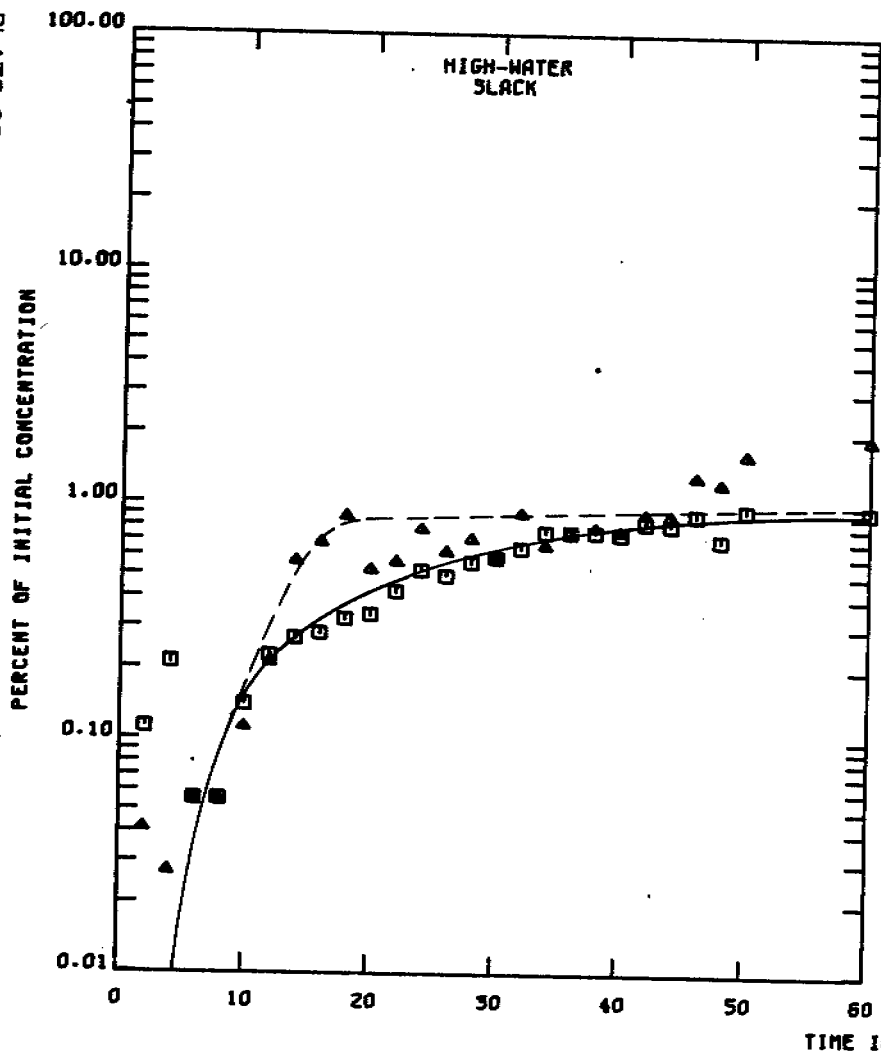


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 △ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION E1



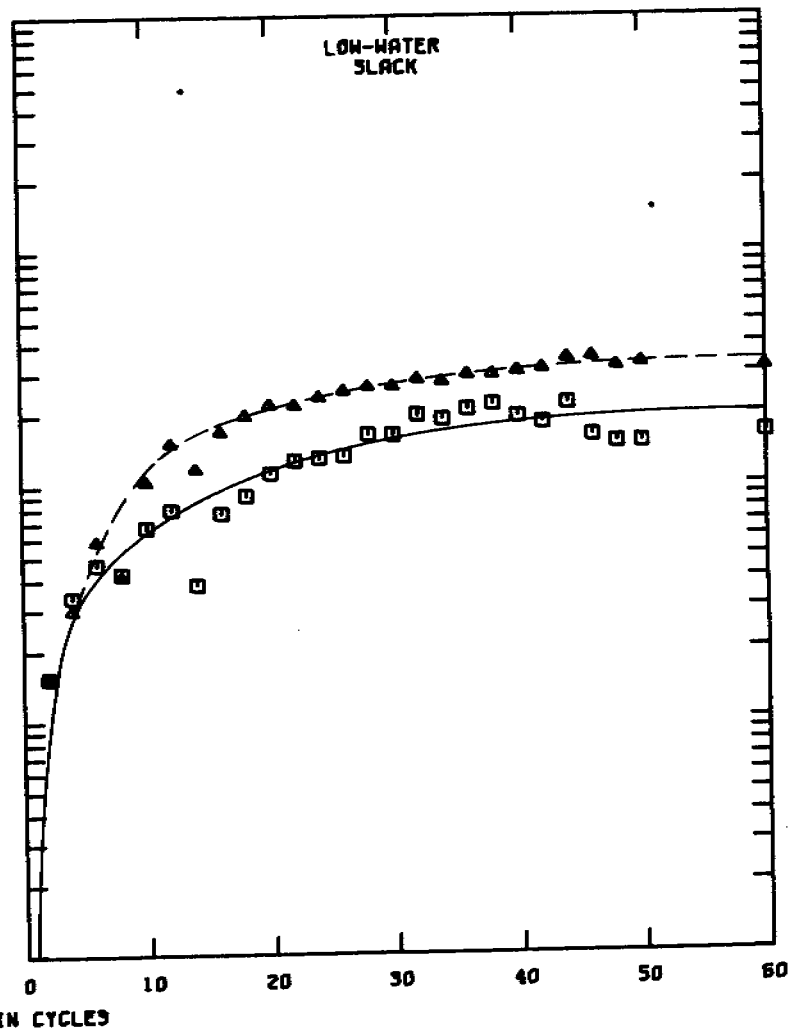
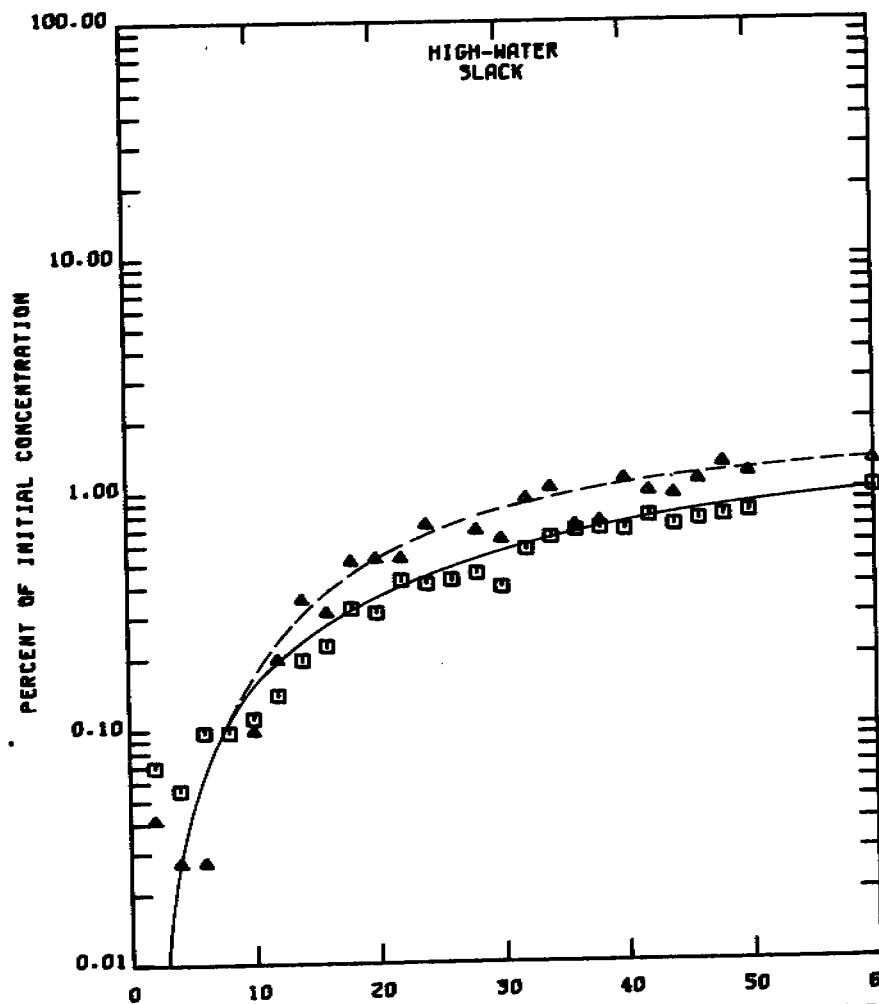
TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION E2

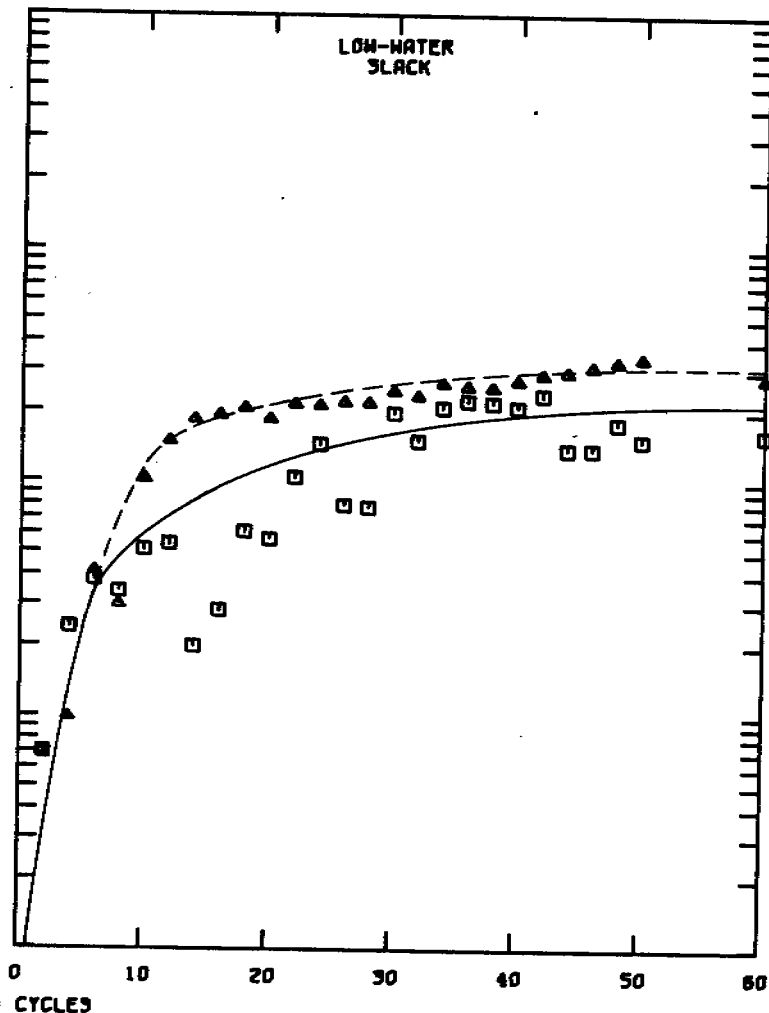
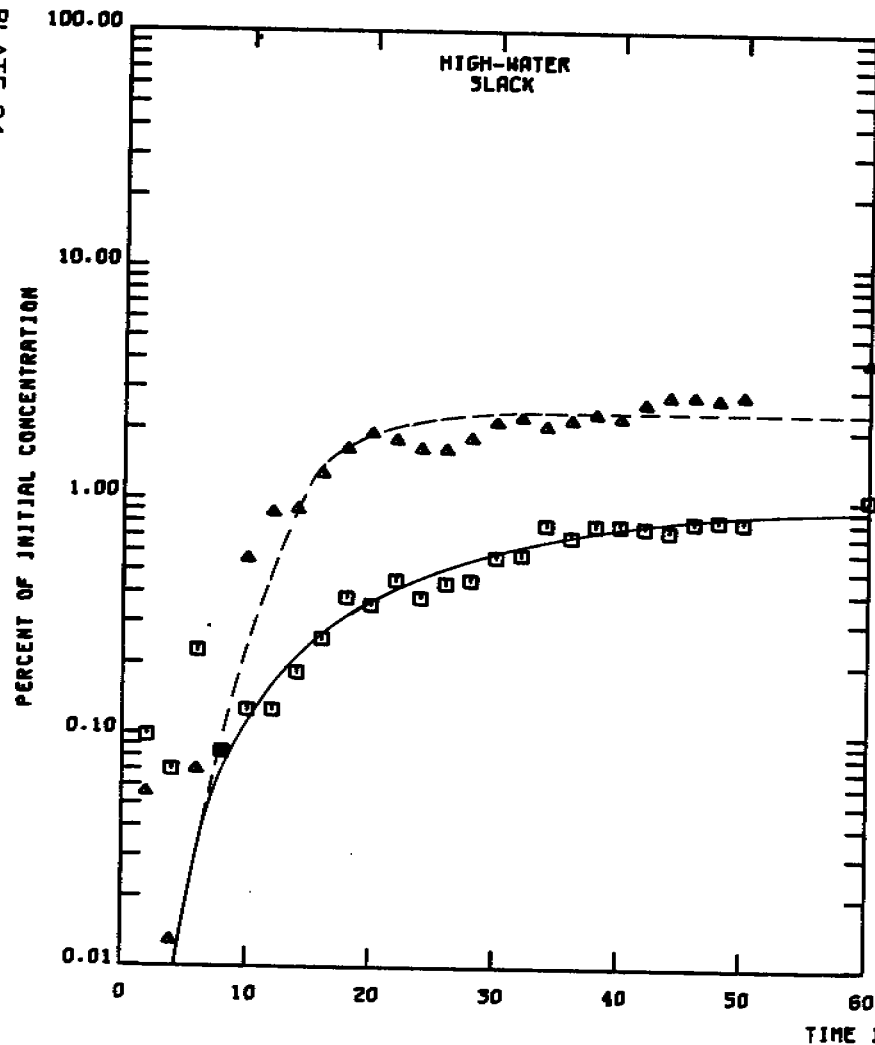


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 △ — — — BOTTOM

**SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION E3**



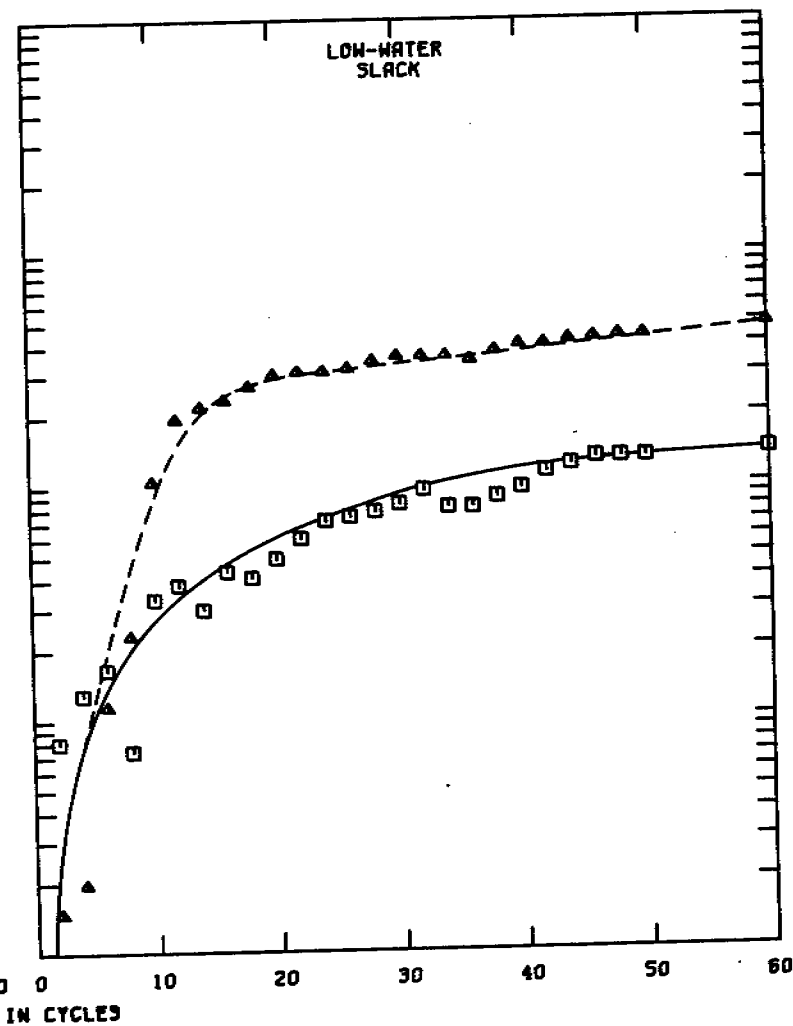
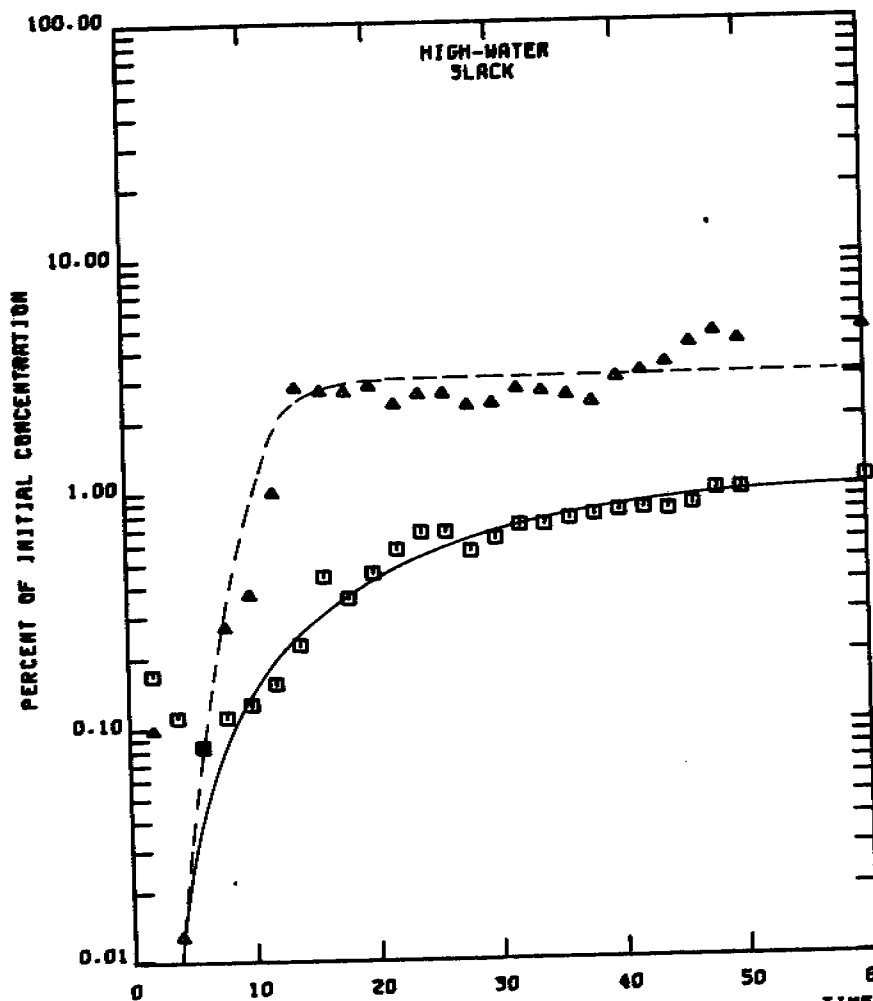
TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

8.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION FA

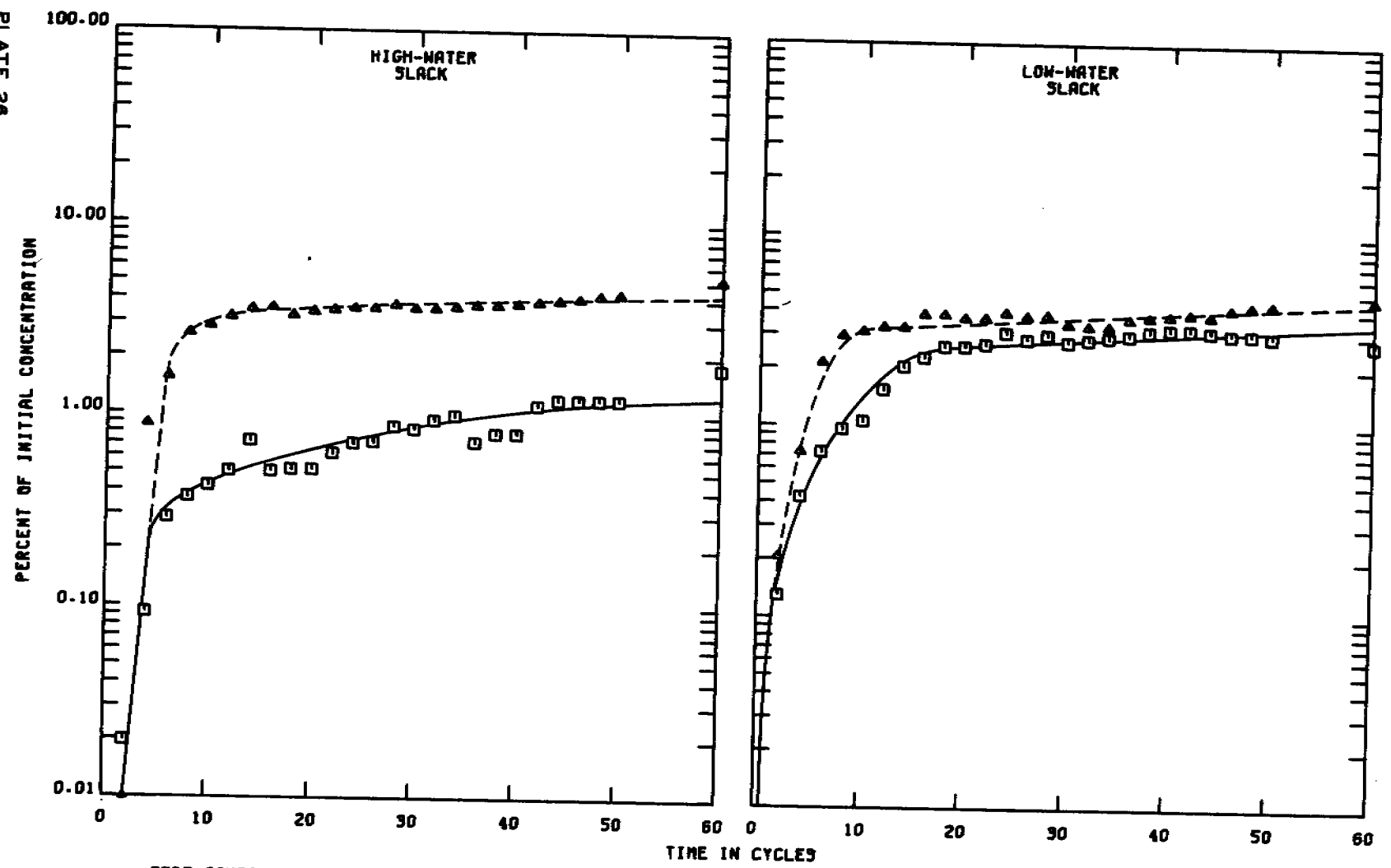


TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ — SURFACE
△ - - - BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION E5



TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION F1

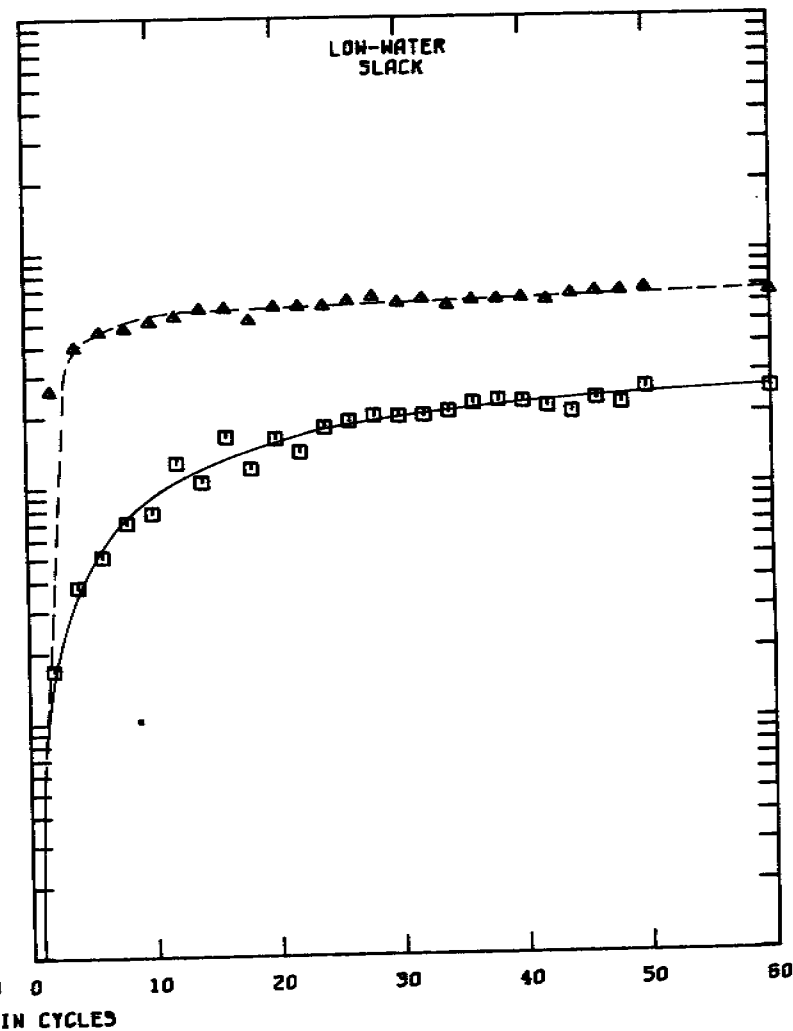
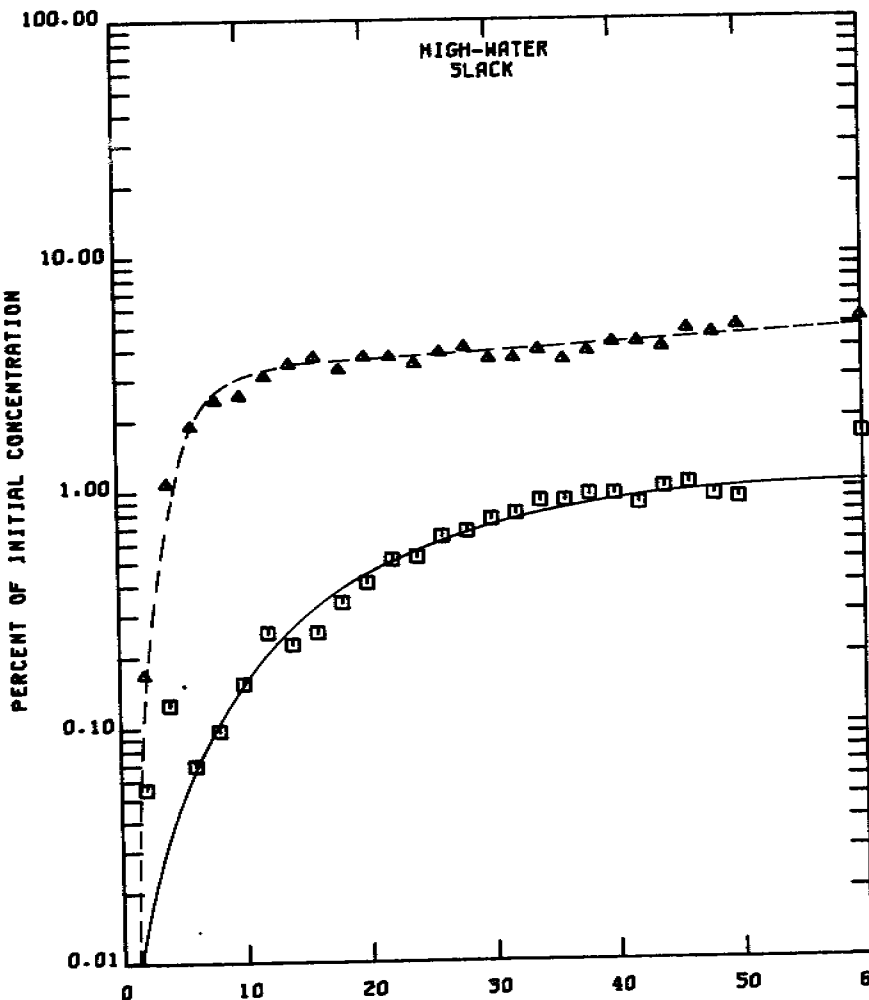


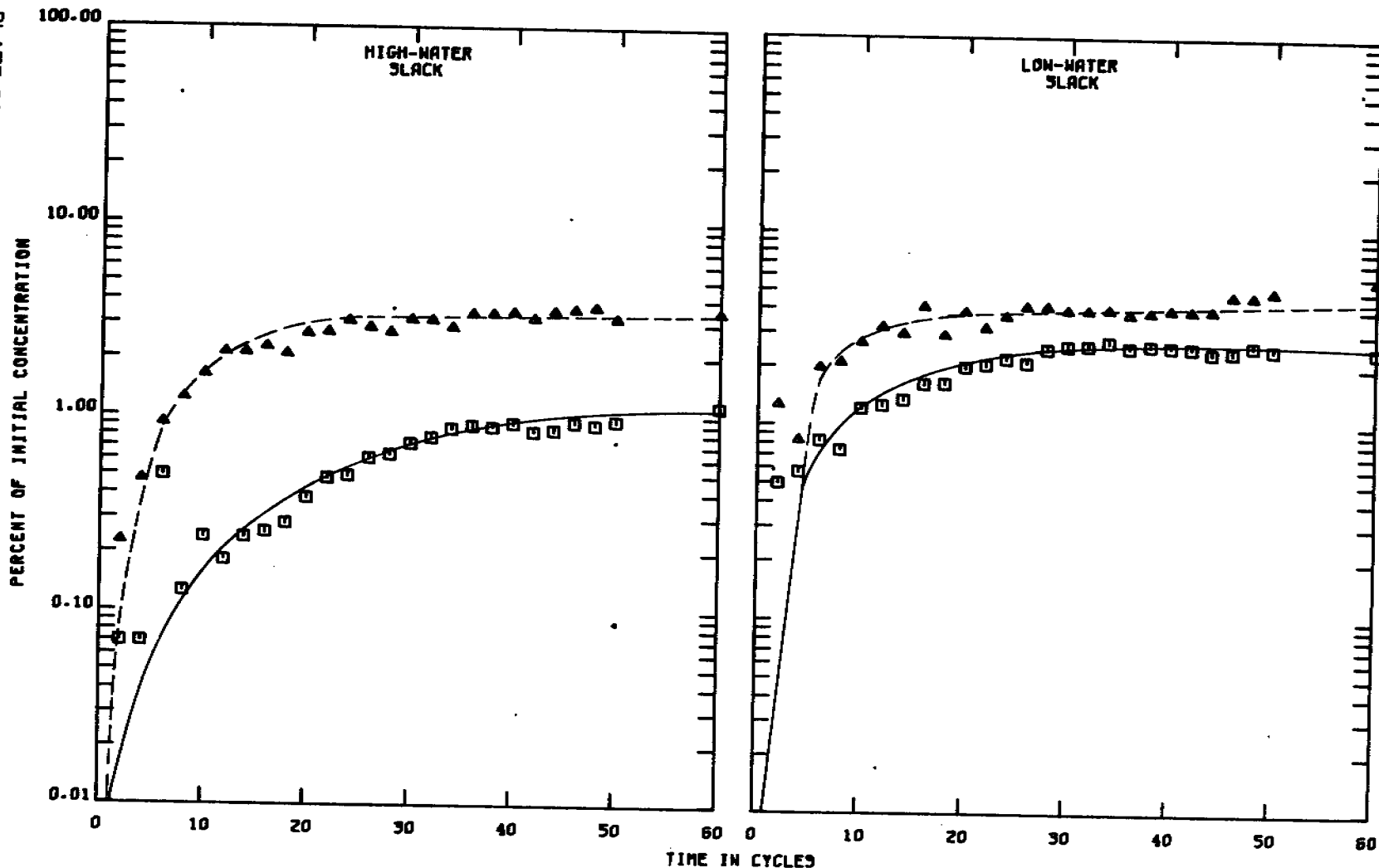
PLATE 27

TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

8.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ — SURFACE
▲ - - - BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION F2

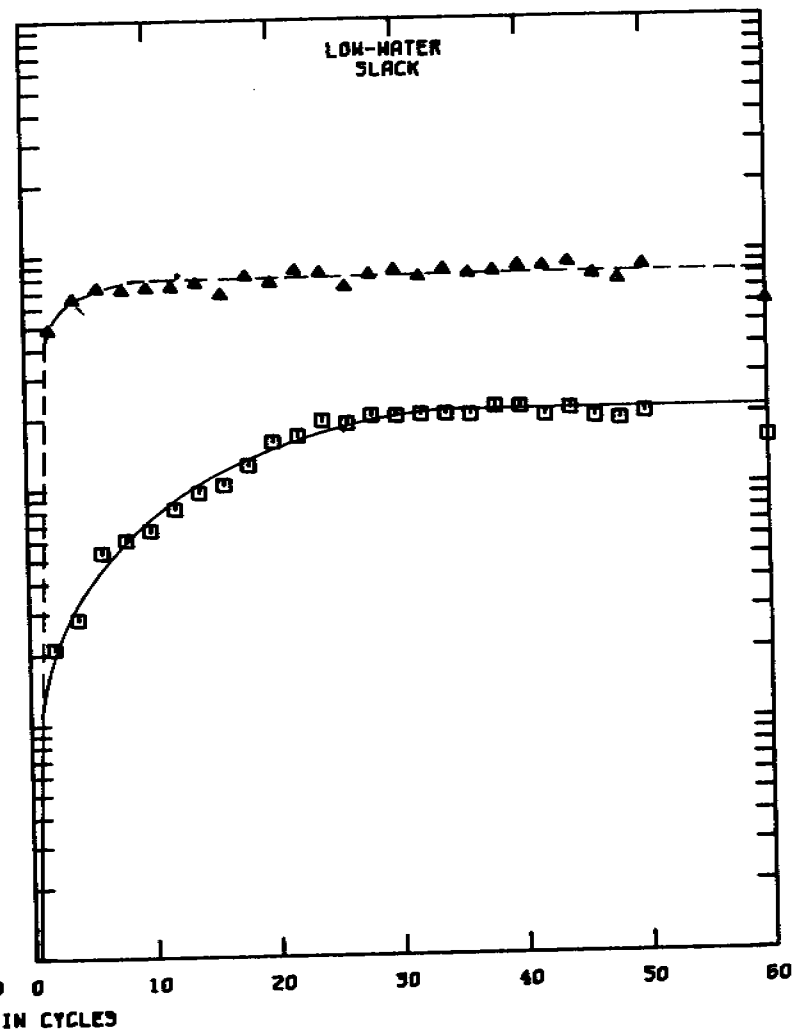
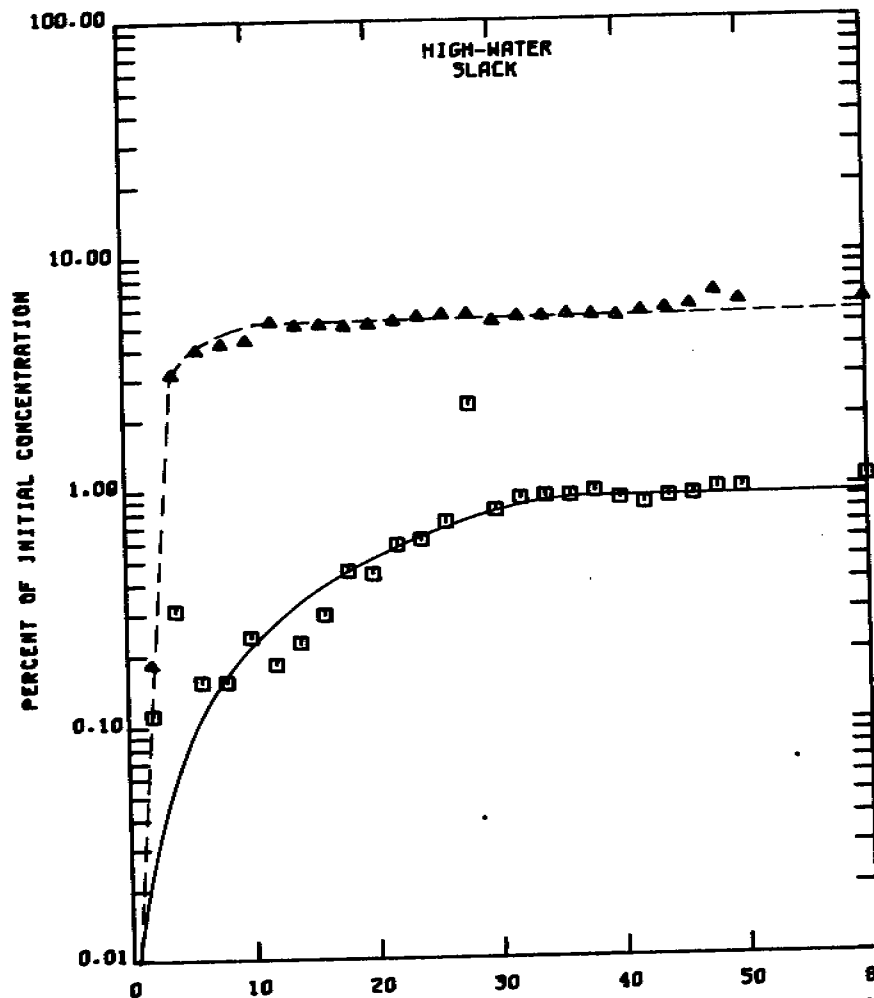


TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ ——— SURFACE
△ — — — BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION F3

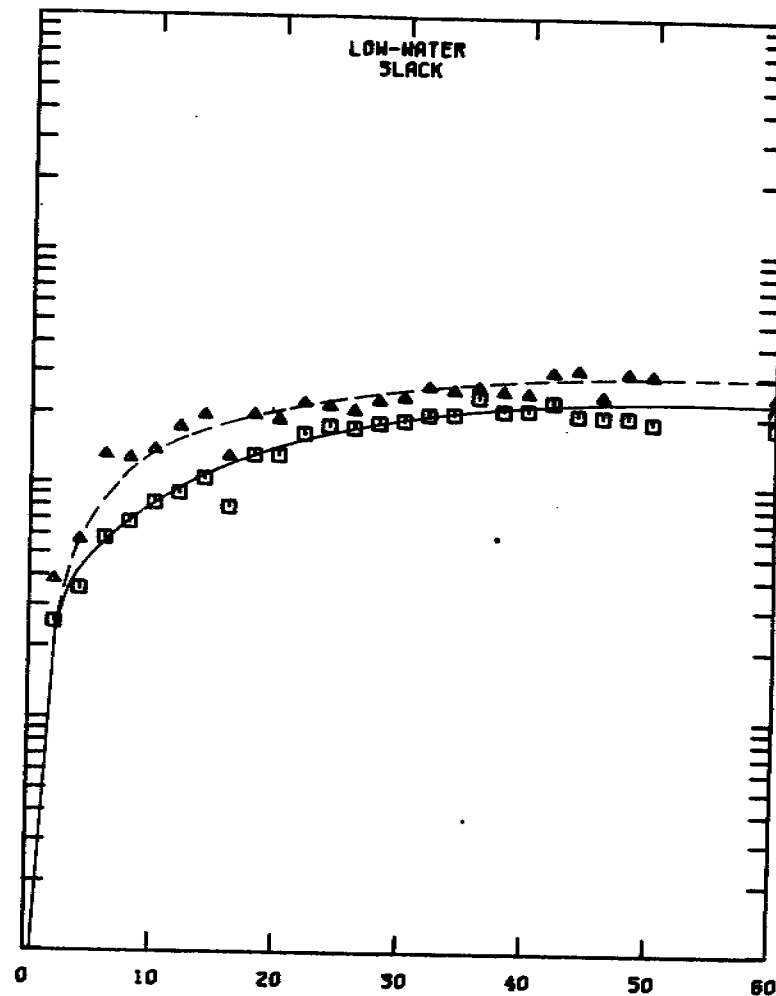
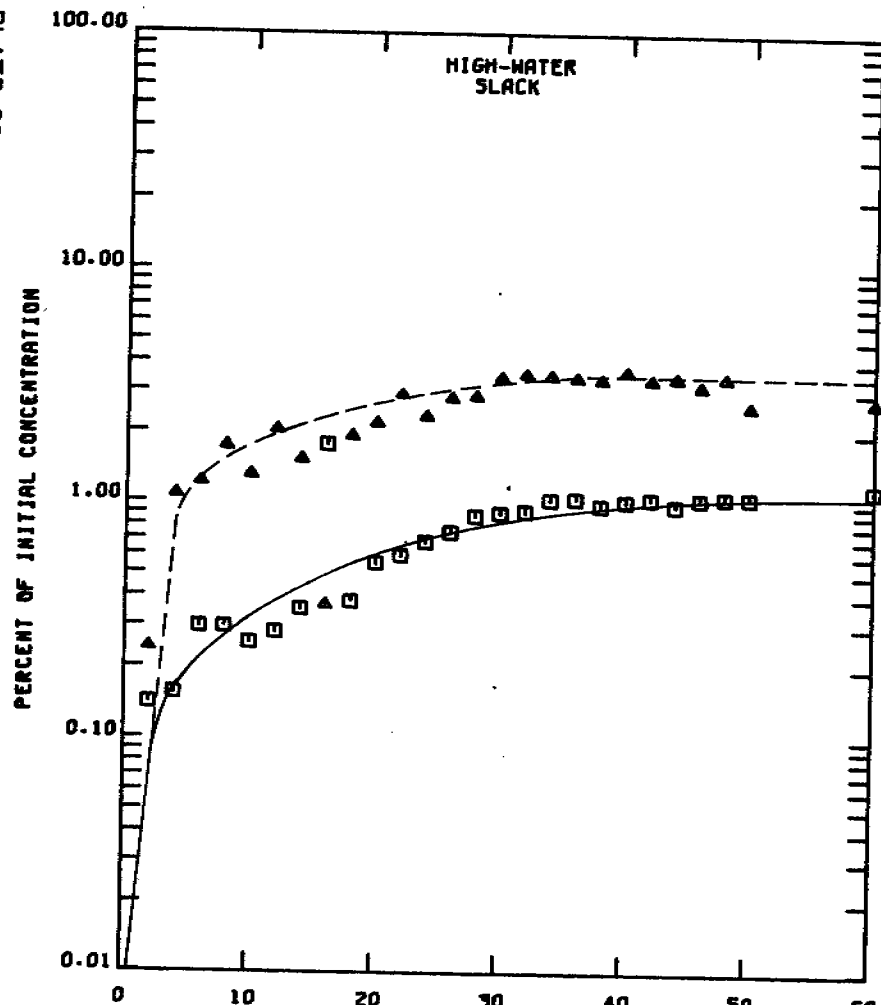


TEST CONDITIONS
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

8.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ — SURFACE
▲ — — — BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION F4

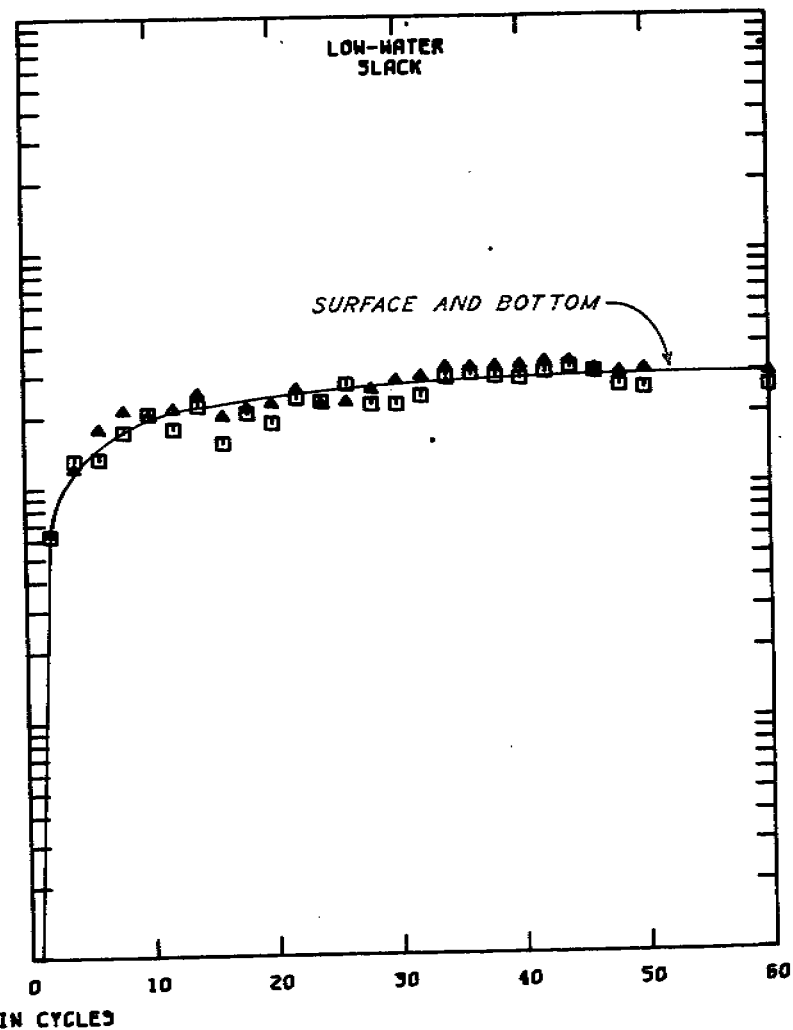
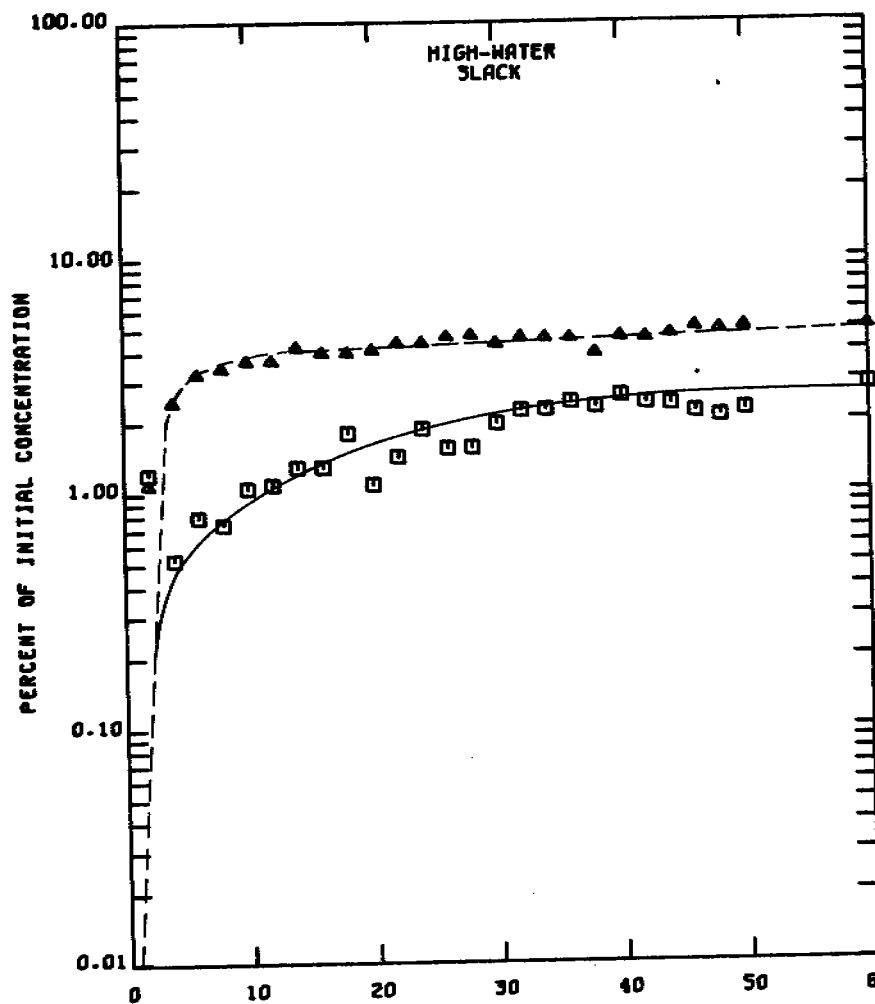


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION F5



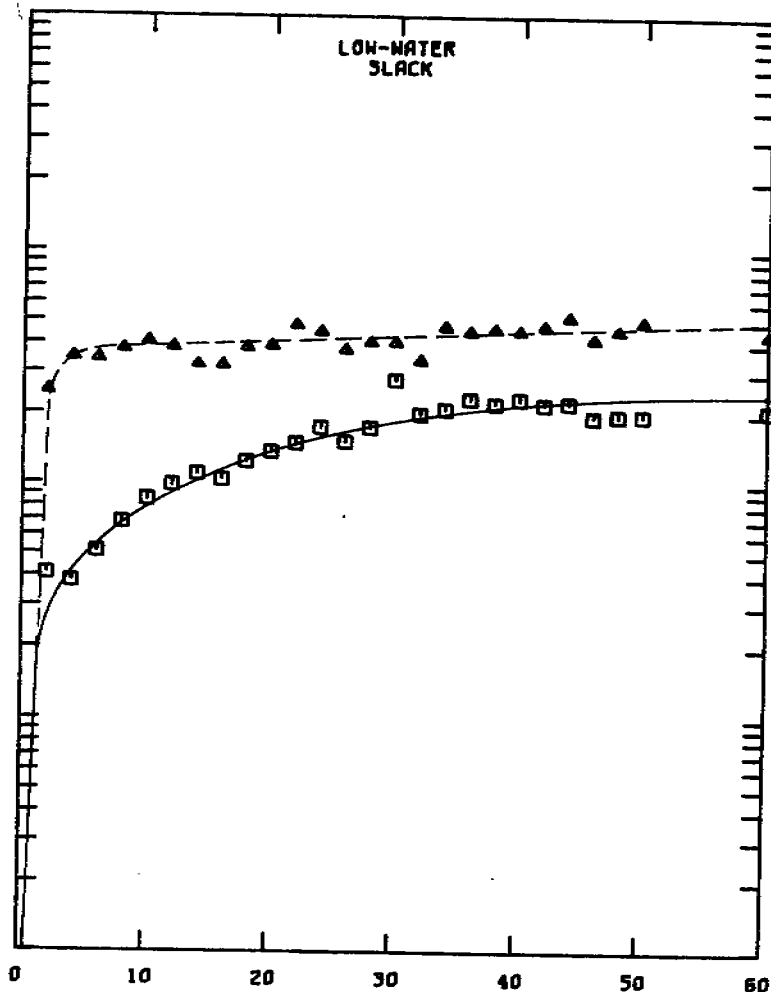
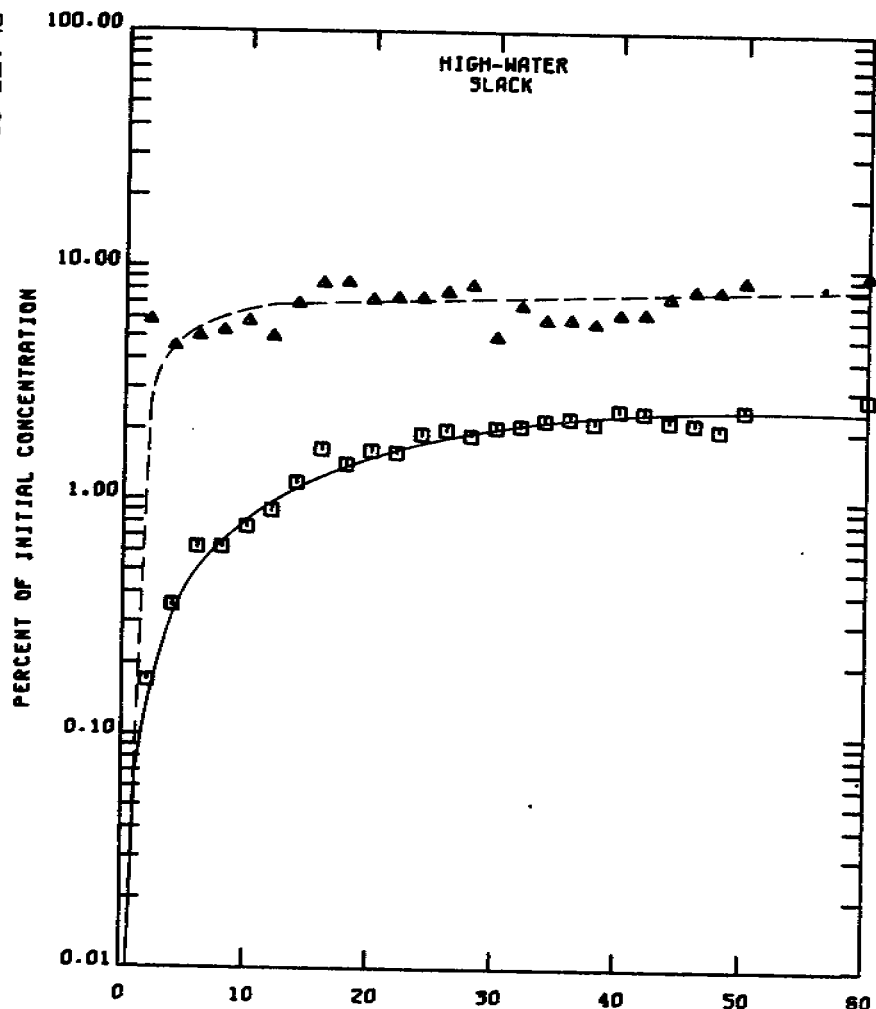
TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

8.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION G1

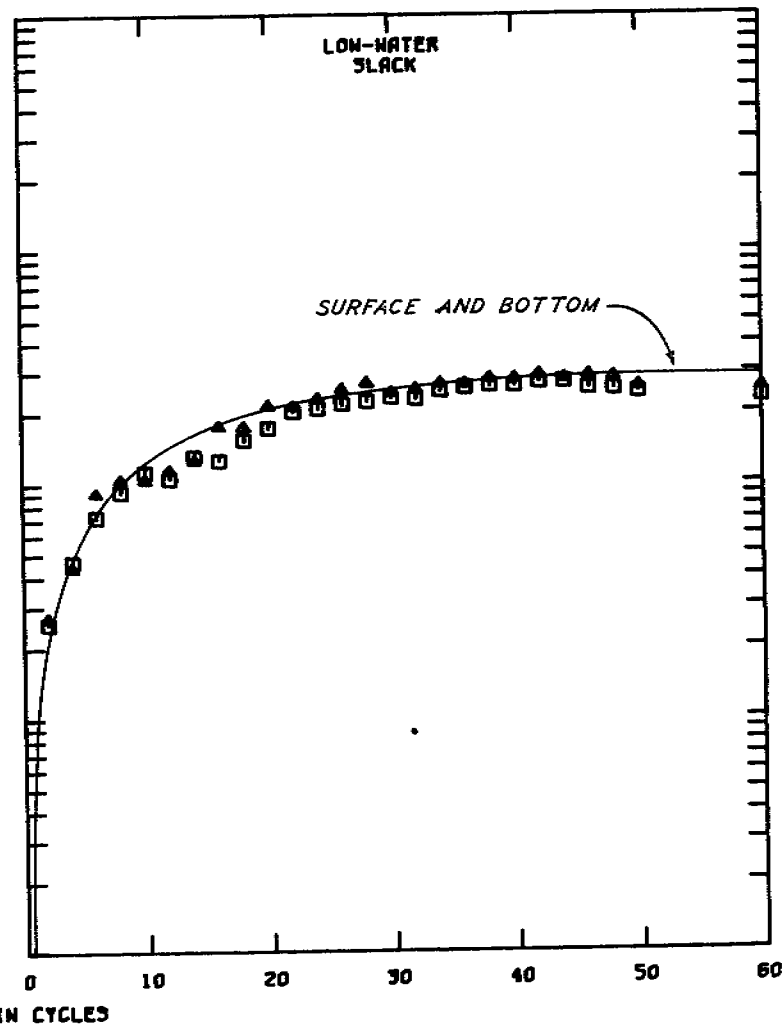
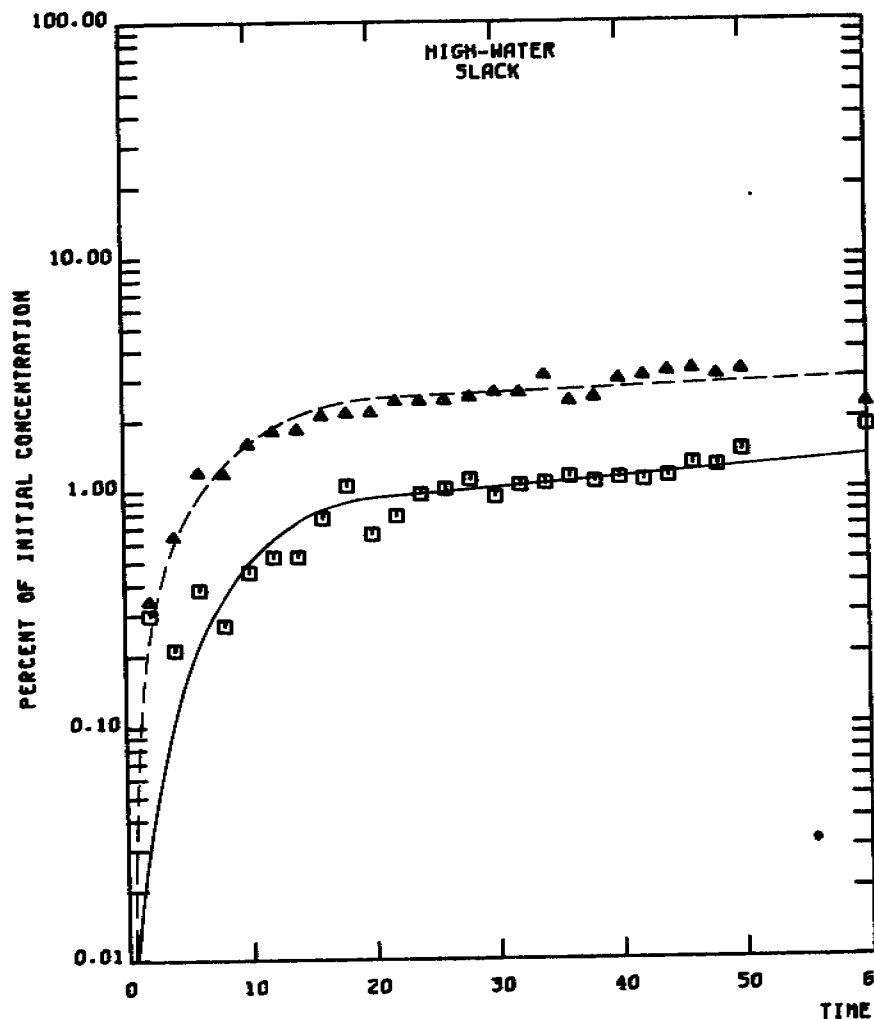


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION G2

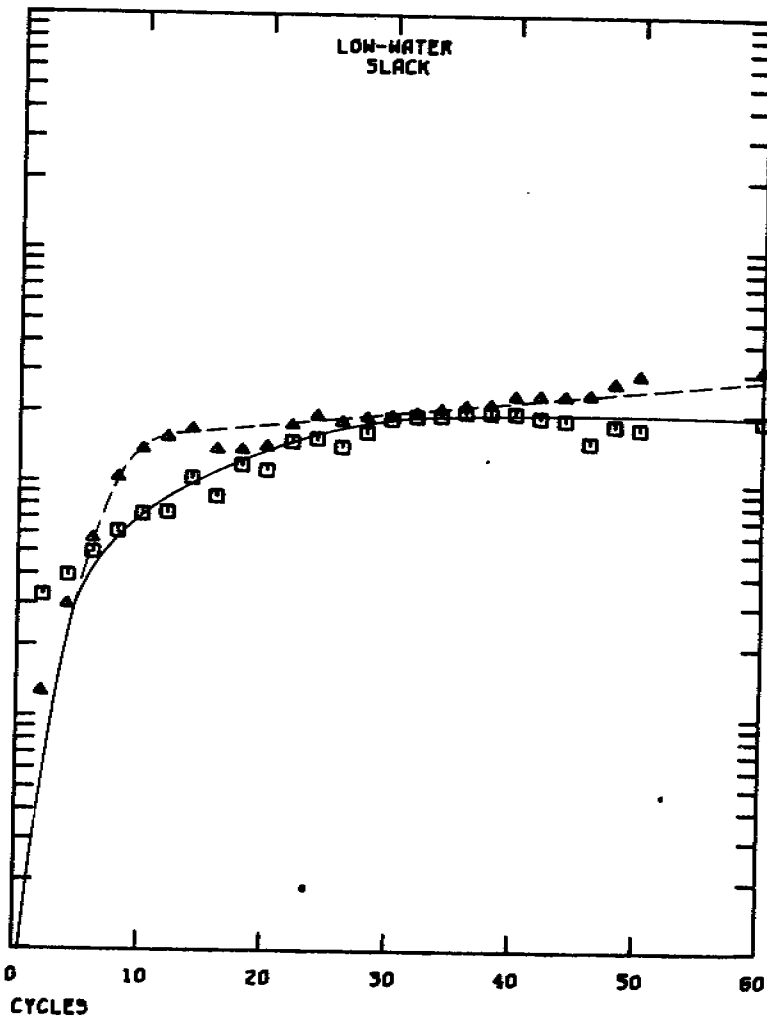
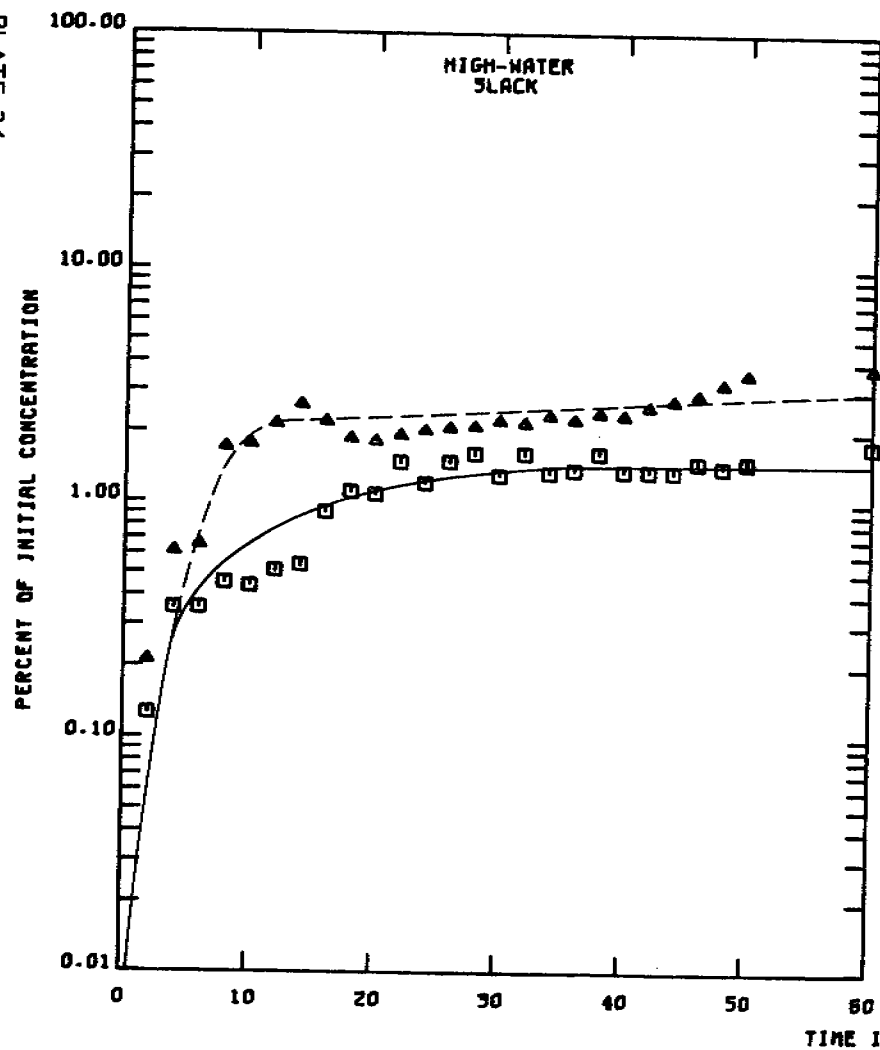


TEST CONDITIONS.
TIDAL RANGE AT BALLAST POINT
OCEAN SALINITY (TOTAL SALT)
EFFLUENT CONCENTRATION
EFFLUENT INJECTION RATE

6.2 FT
0.0 PPT
11.4 PPT
21.2 MGD

LEGEND
□ ——— SURFACE
△ ——— BOTTOM

SAN DIEGO MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION G3

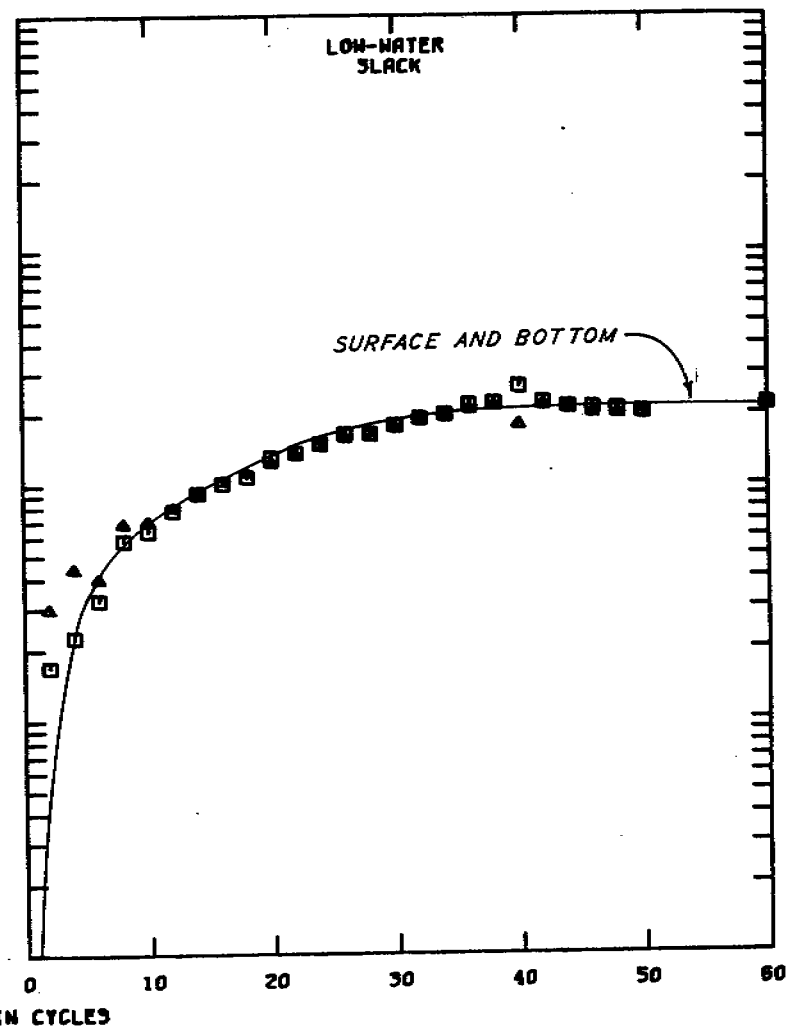
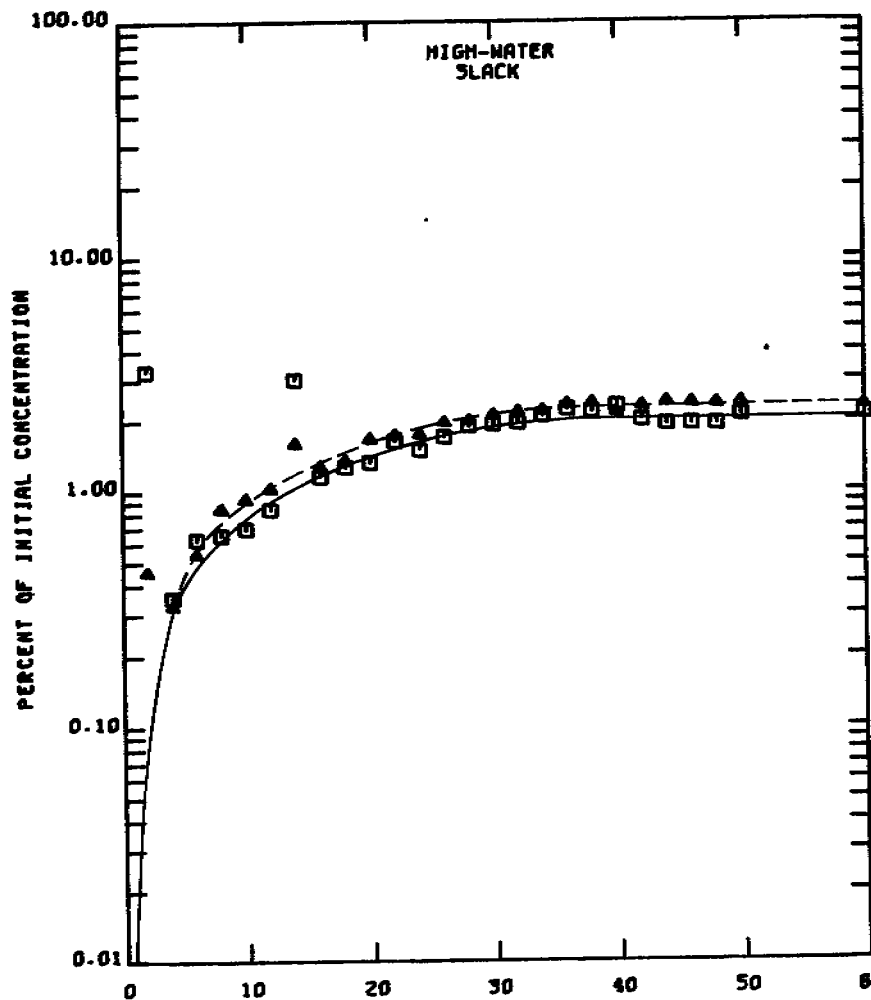


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ — — — BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION 64

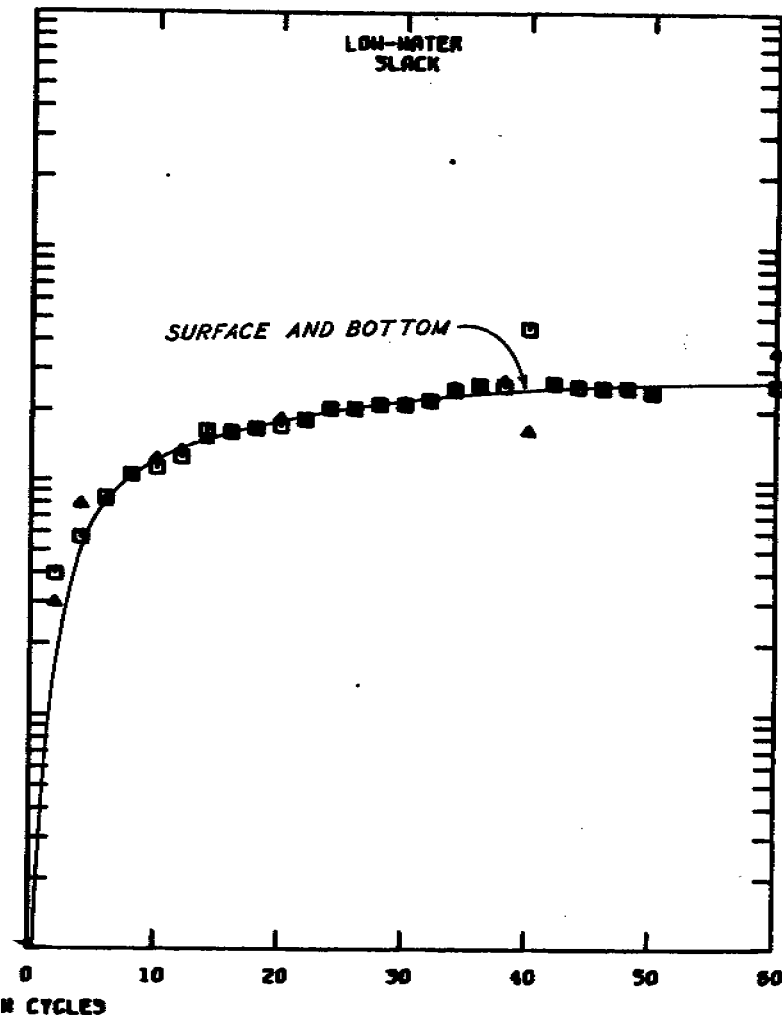
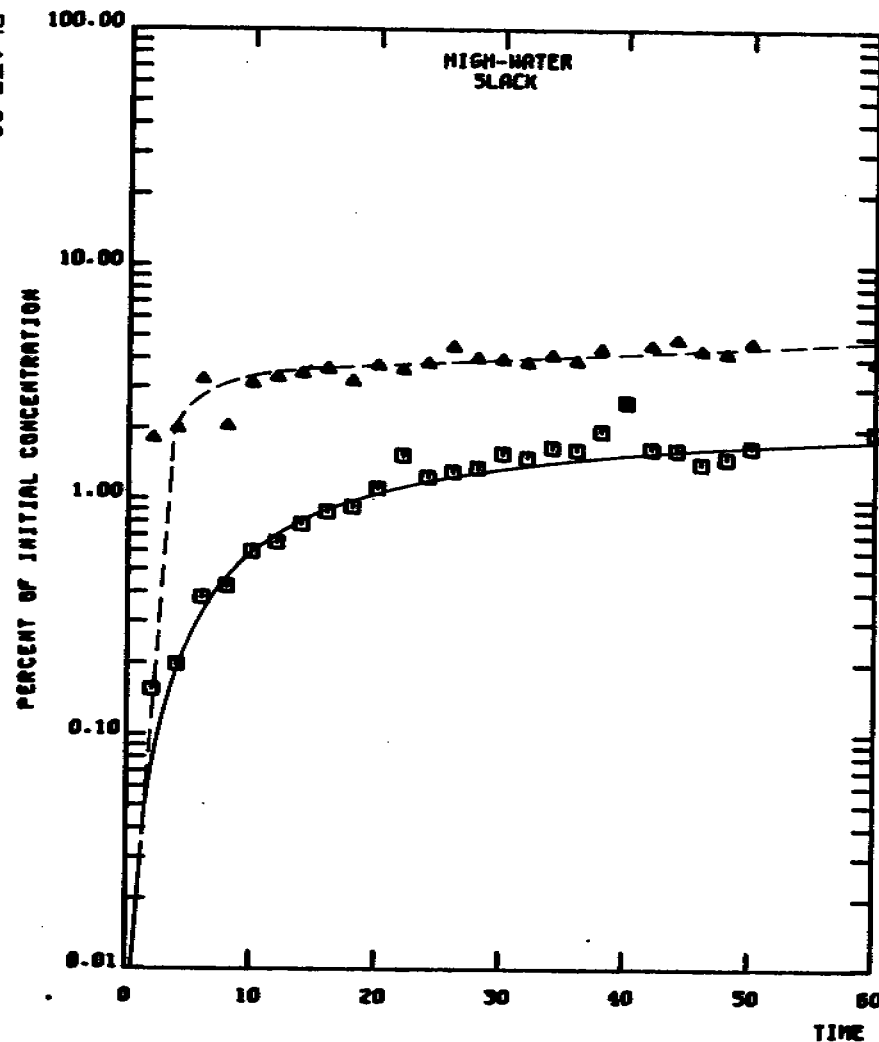


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION H1

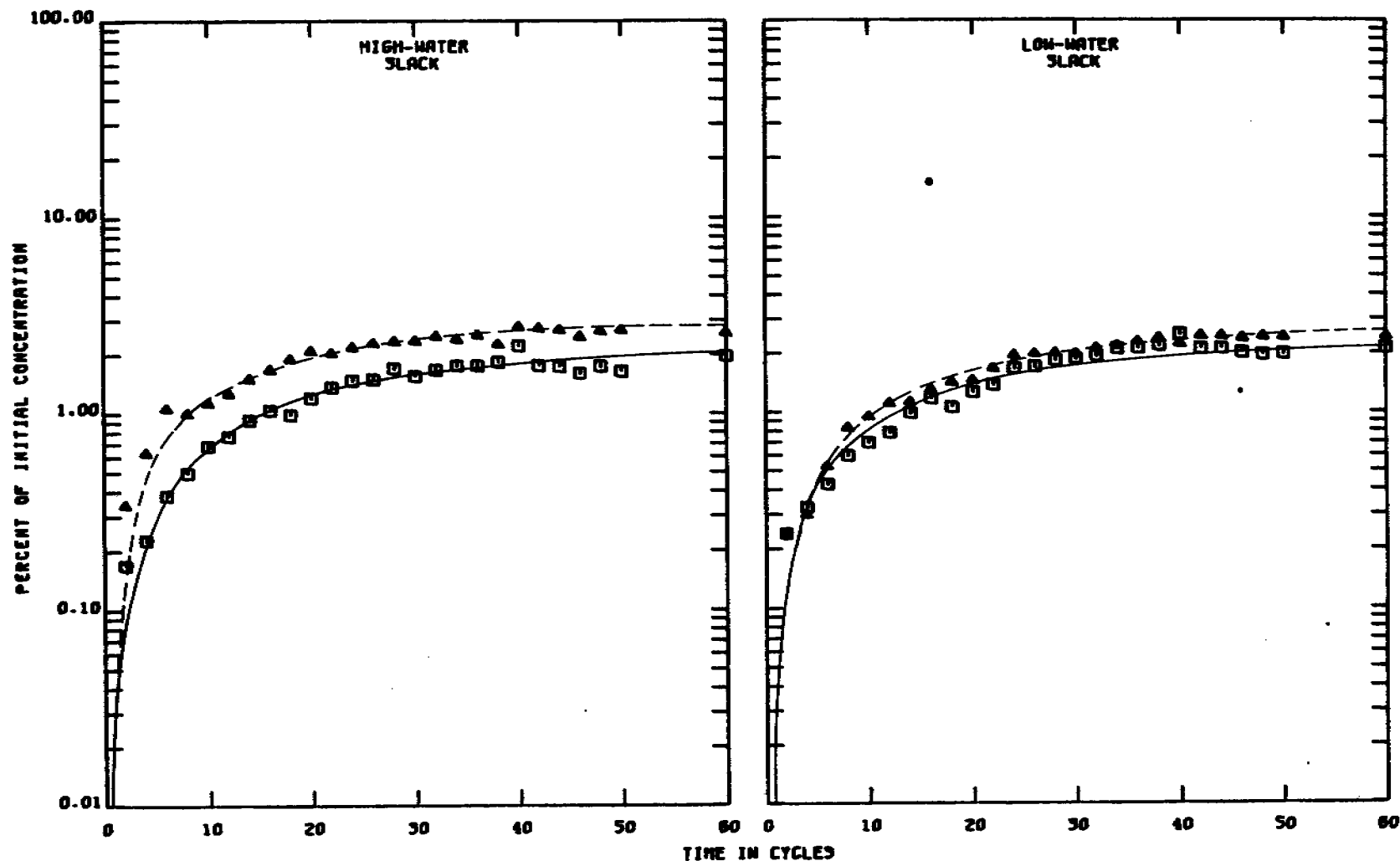


TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT 6.2 FT
 OCEAN SALINITY (TOTAL SALT) 0.0 PPT
 EFFLUENT CONCENTRATION 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

6.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ — — — BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION N2



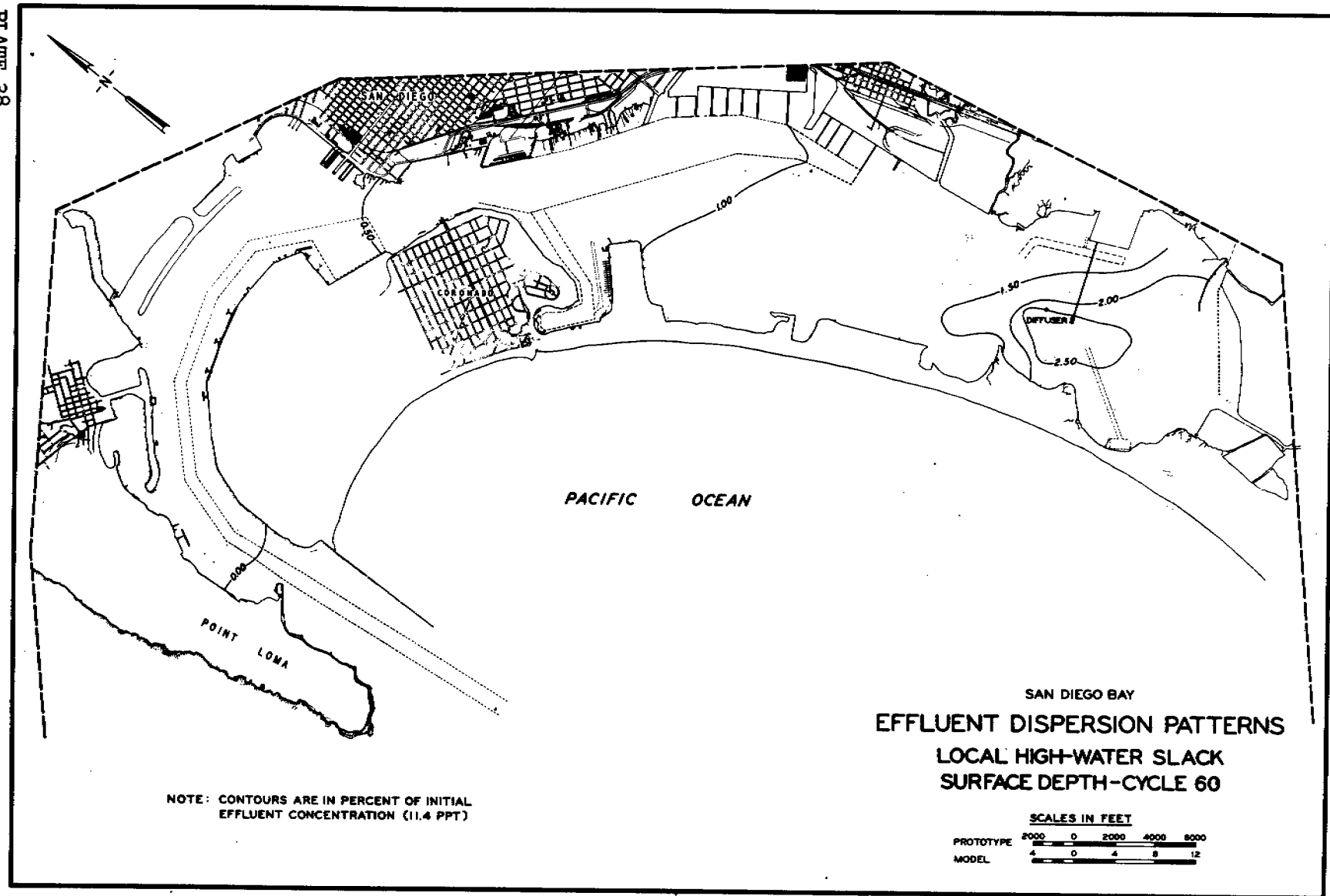
TEST CONDITIONS
 TIDAL RANGE AT BALLAST POINT
 OCEAN SALINITY (TOTAL SALT)
 EFFLUENT CONCENTRATION
 EFFLUENT INJECTION RATE

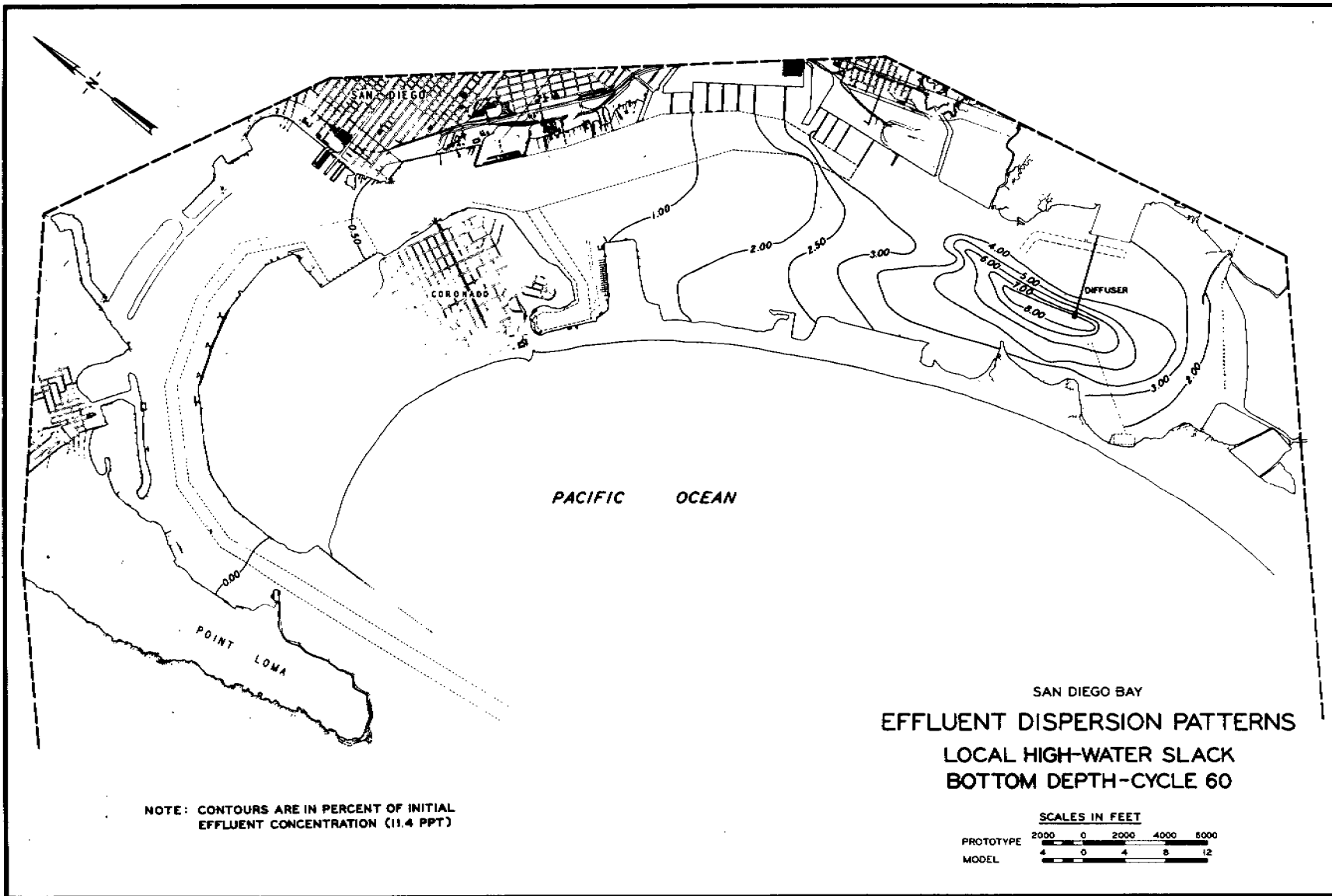
8.2 FT
 0.0 PPT
 11.4 PPT
 21.2 MGD

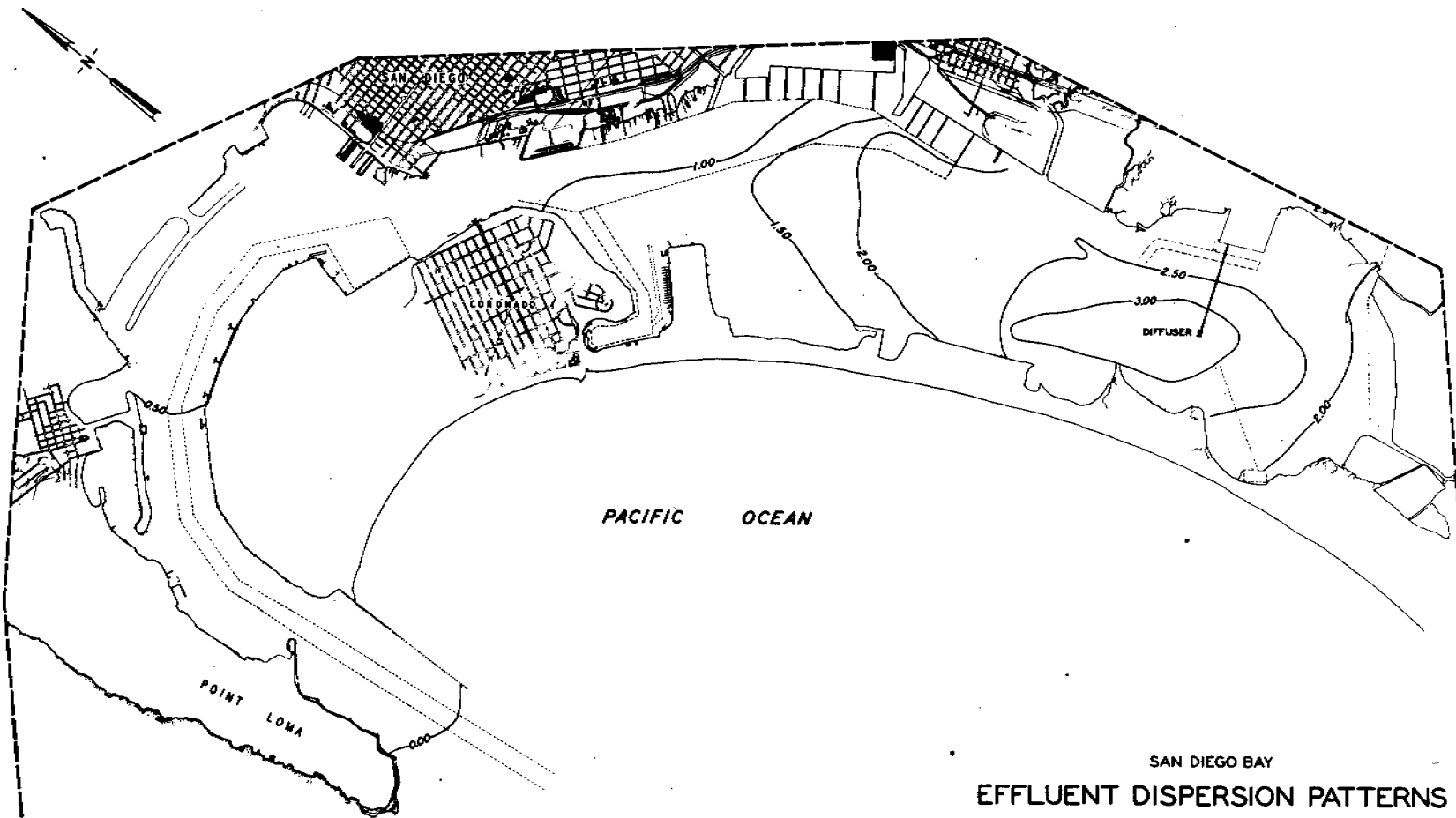
LEGEND

□ — SURFACE
 ▲ — — — BOTTOM

SAN DIEGO MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION M3

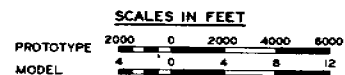


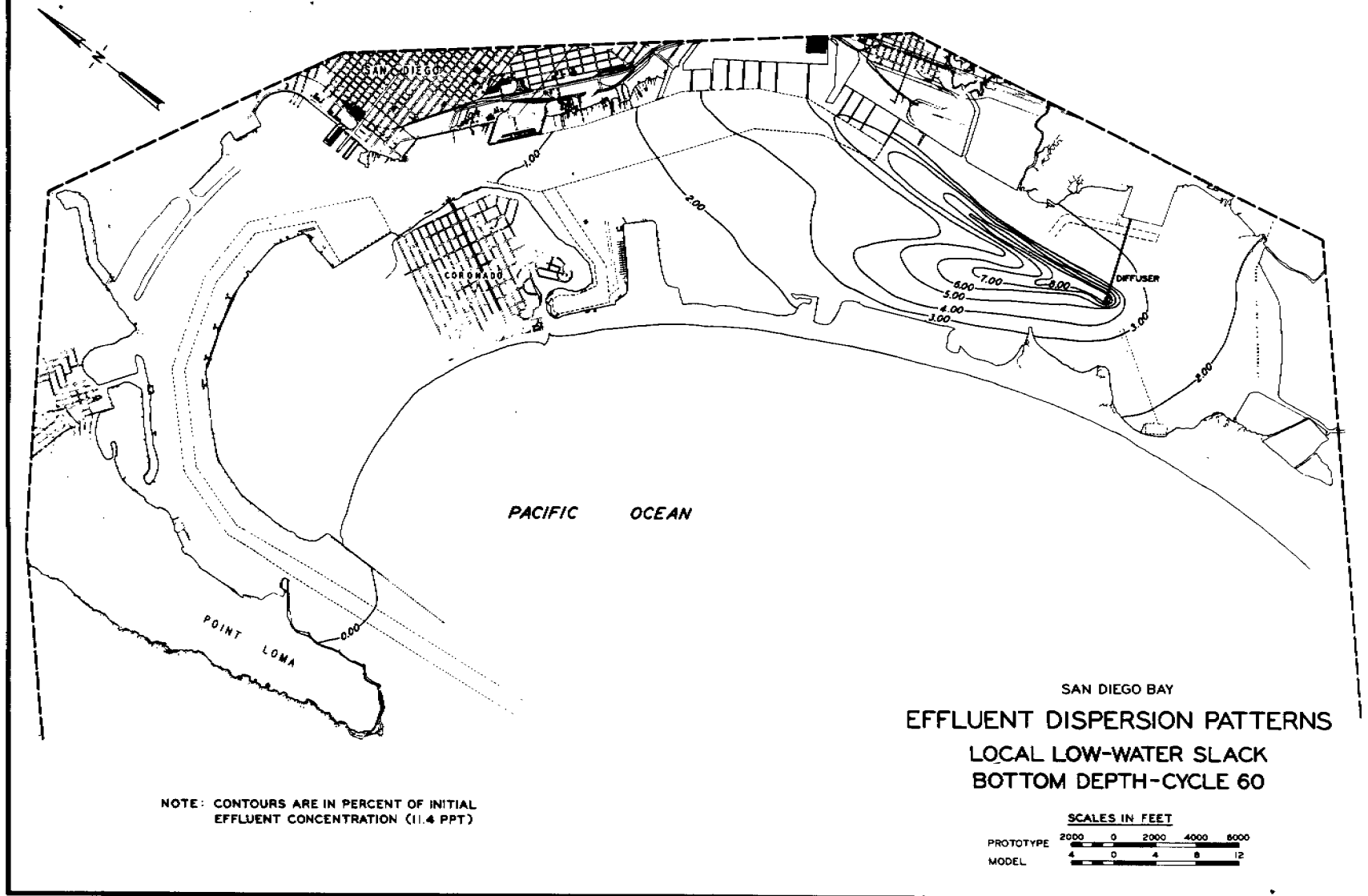


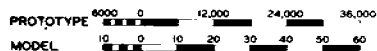


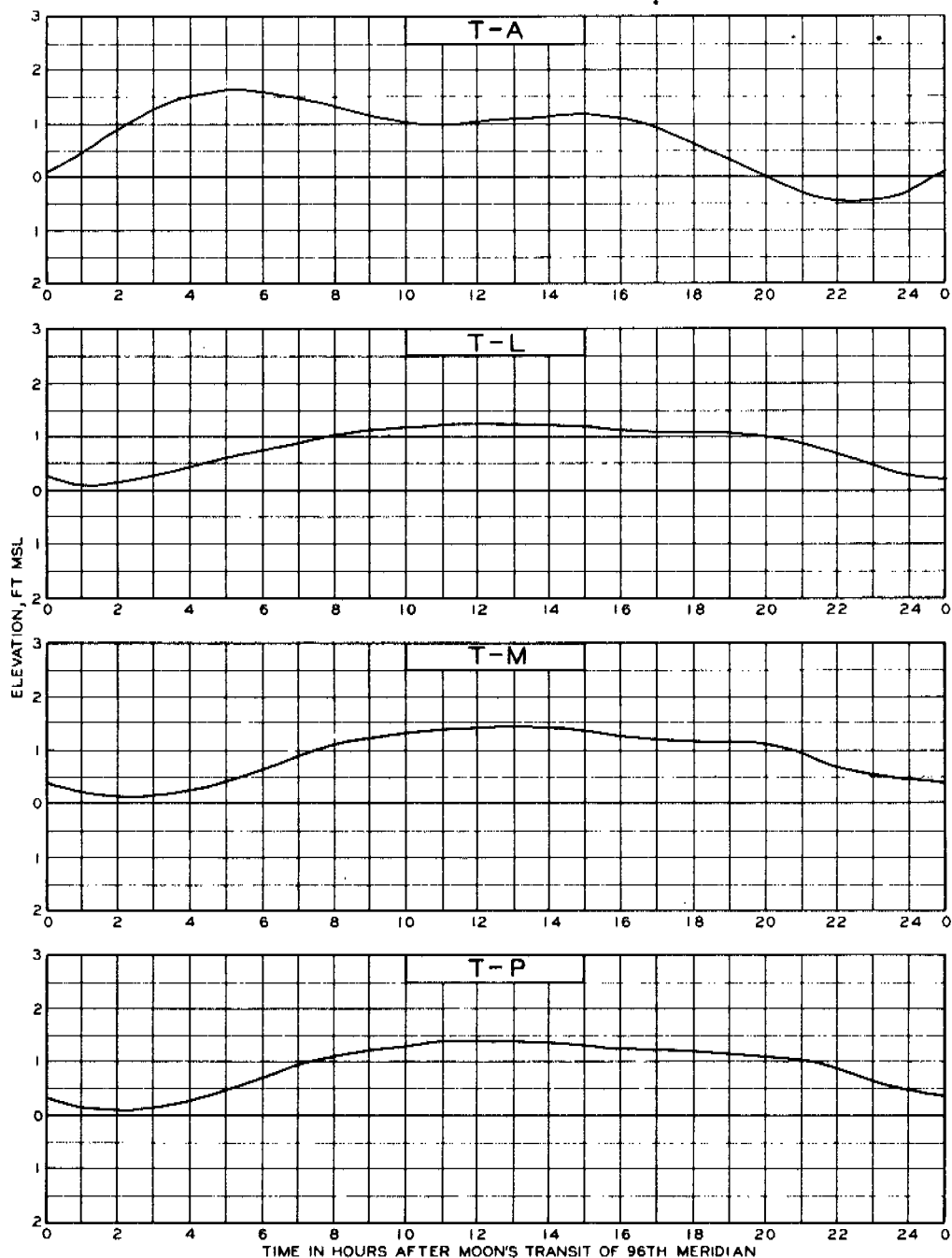
NOTE: CONTOURS ARE IN PERCENT OF INITIAL
EFFLUENT CONCENTRATION (11.4 PPT)

SAN DIEGO BAY
EFFLUENT DISPERSION PATTERNS
LOCAL LOW-WATER SLACK
SURFACE DEPTH-CYCLE 60





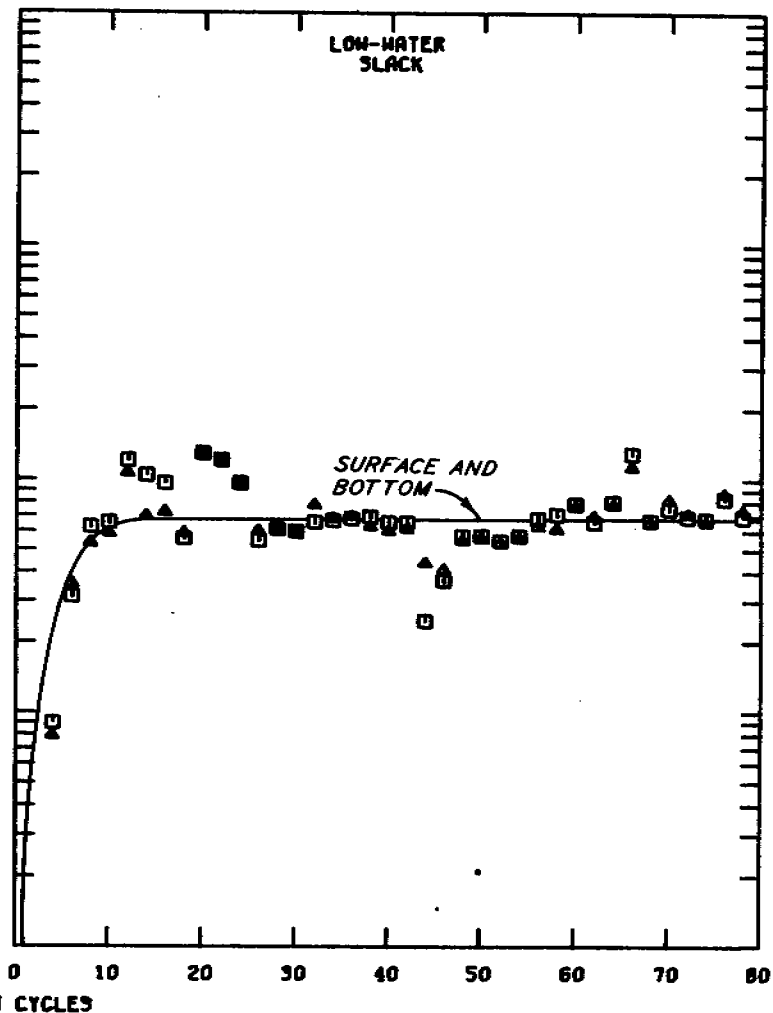
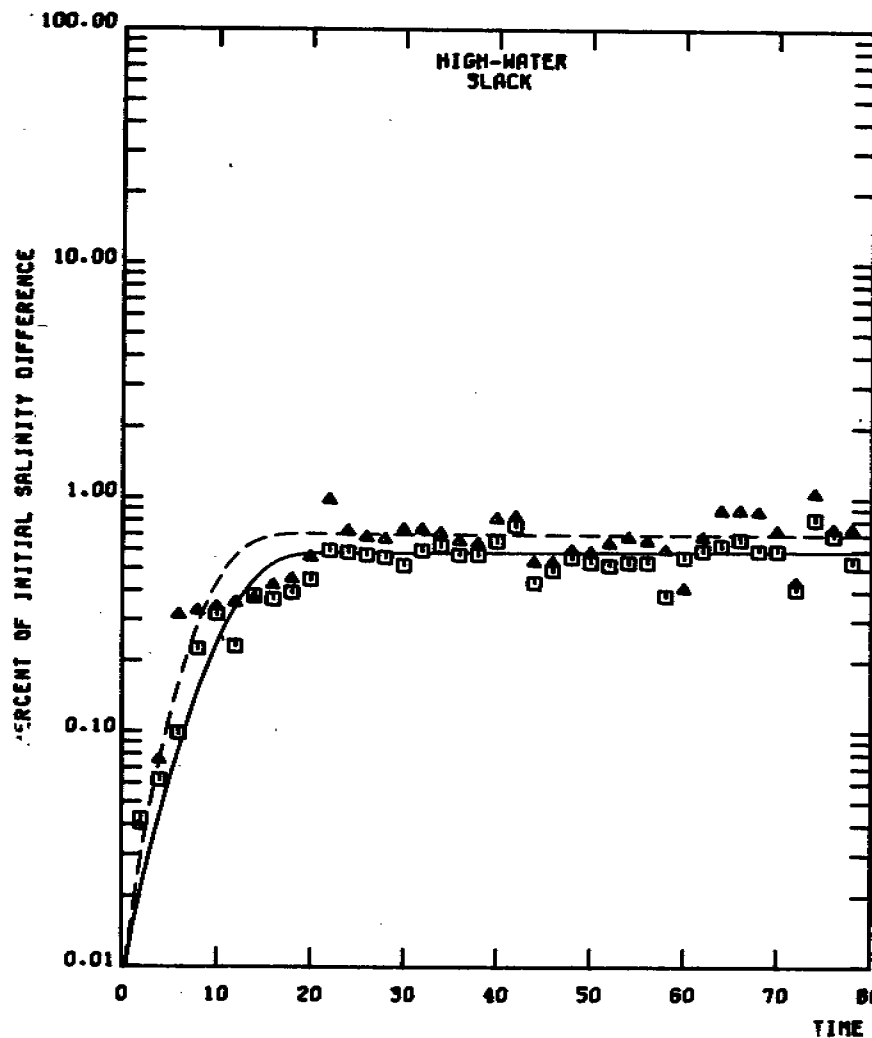




MODEL TEST DATA

TIDE..... MEAN
 FRESH-WATER DISCHARGE 11,323 CFS
 SOURCE SALINITY..... 32.5 PPT

**GALVESTON BAY MODEL
 TIDAL OBSERVATIONS
 STATIONS T-A, T-L,
 T-M, AND T-P**



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U1**

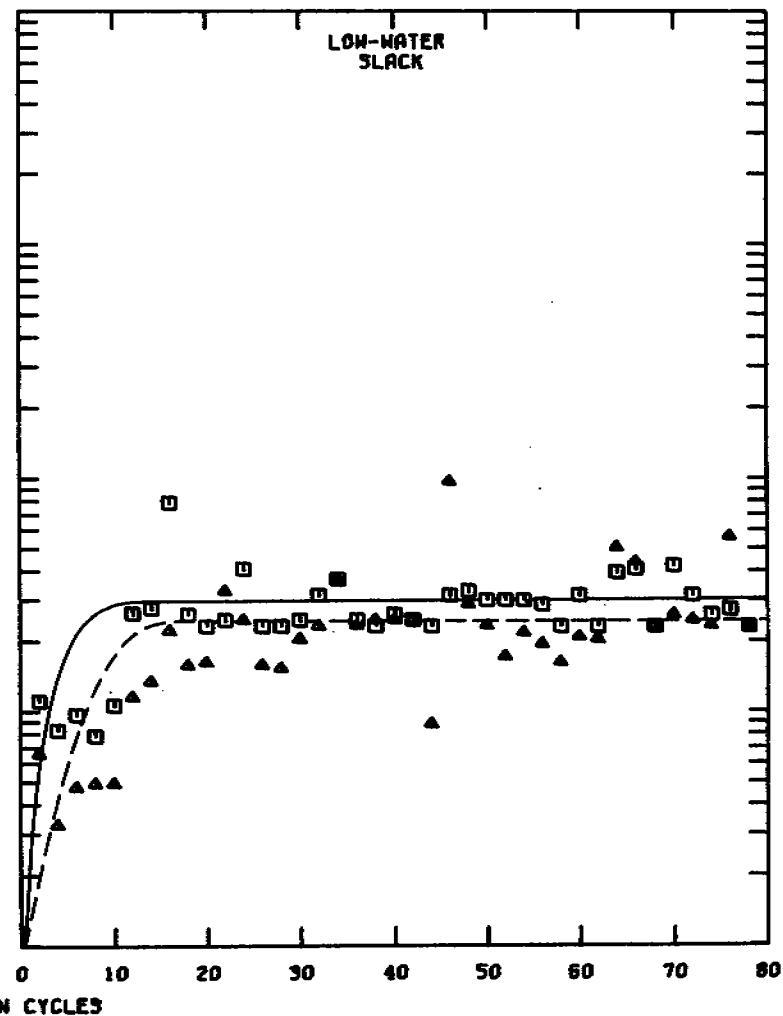
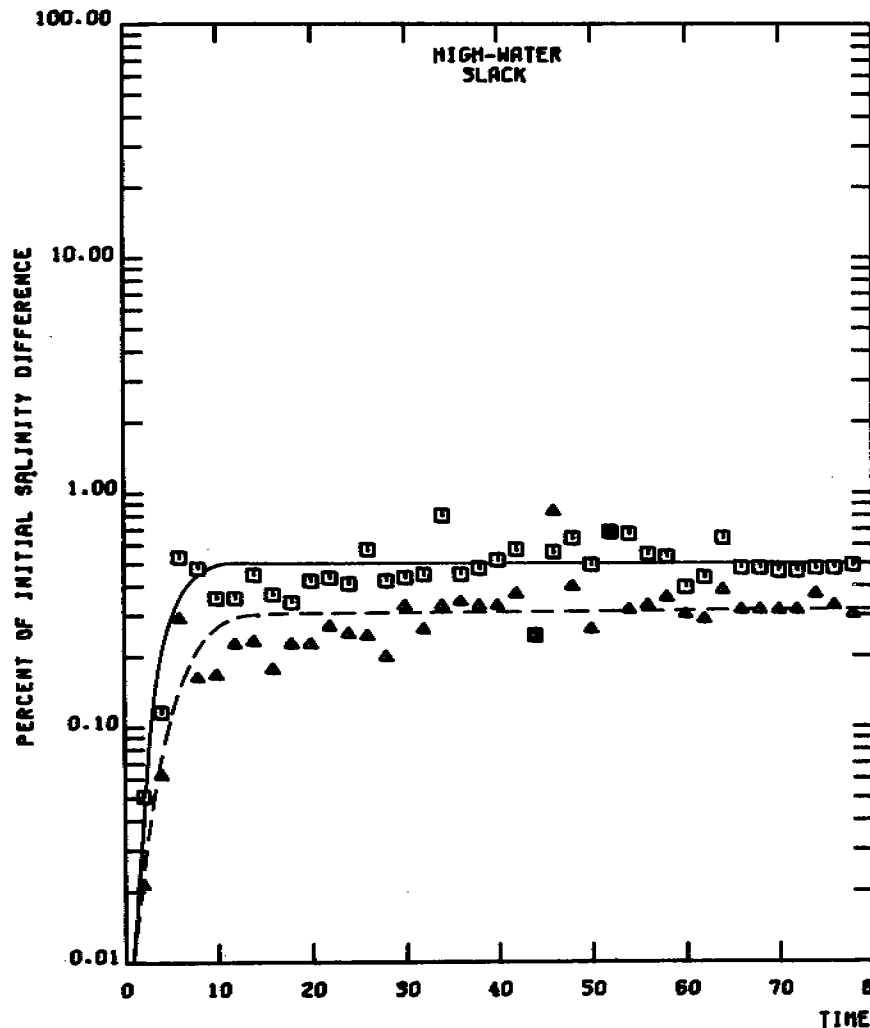


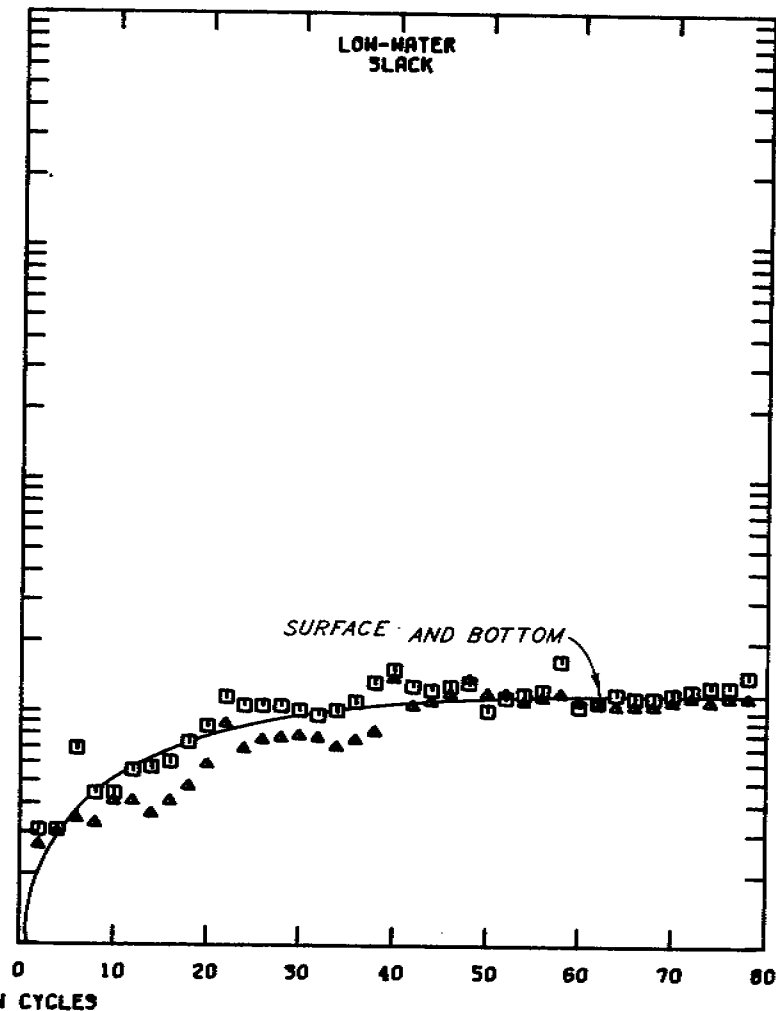
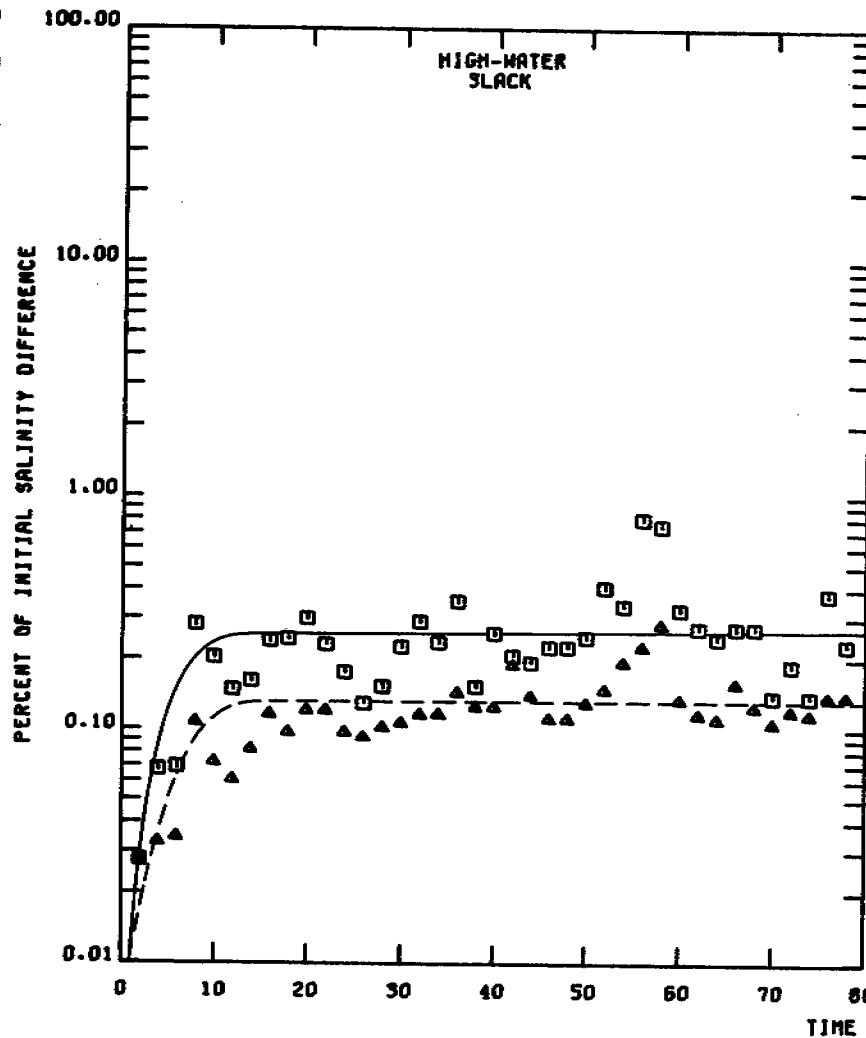
PLATE 45

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U2**



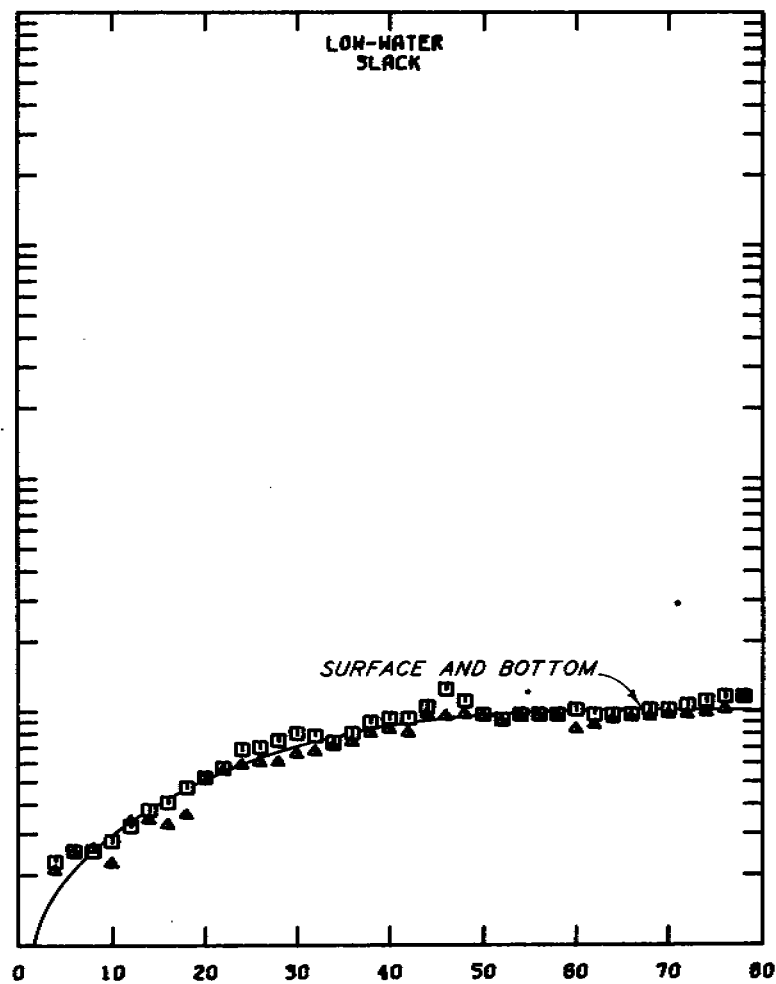
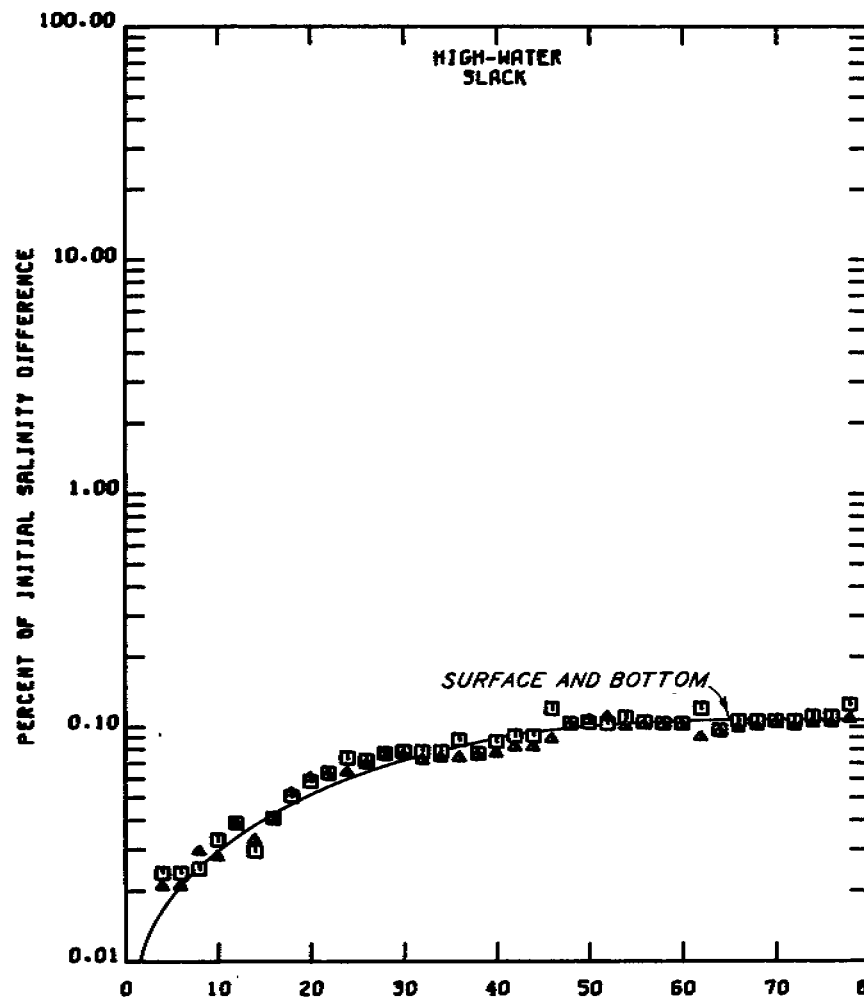
TEST CONDITIONS

FRESH-WATER DISCHARGE	11523 CF3
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
▲ - - -	BOTTOM

**GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION 05**



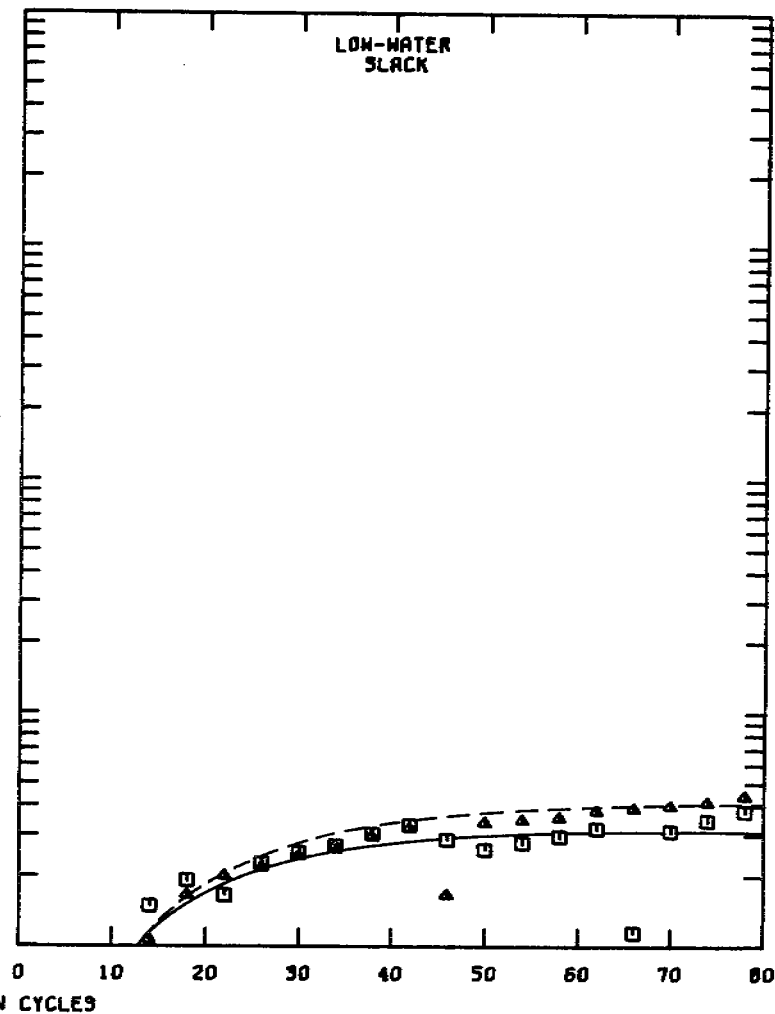
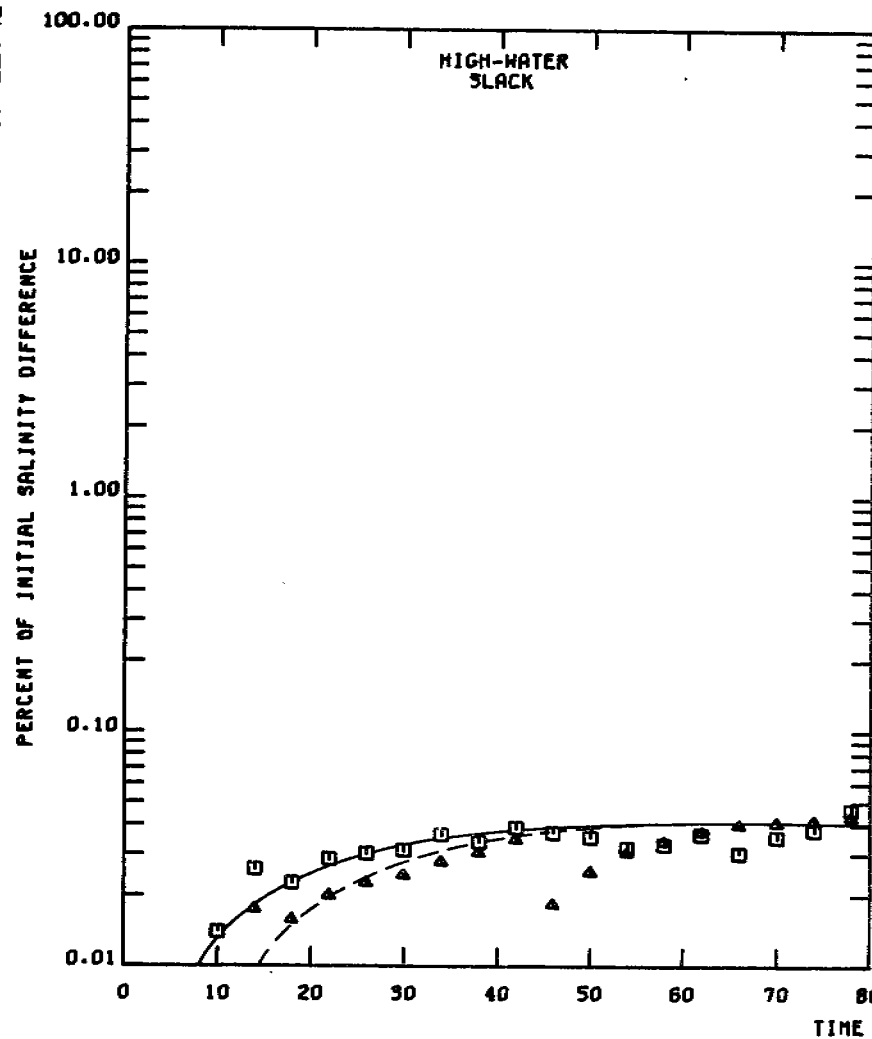
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ - - - BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U4**



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ — — — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION US

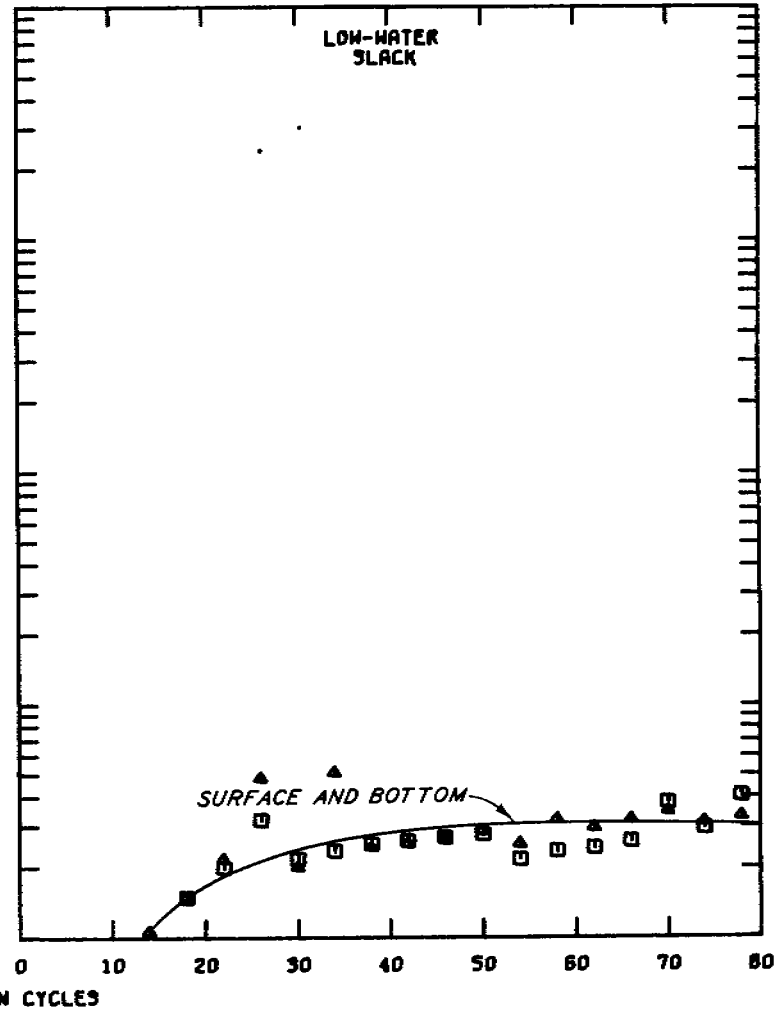
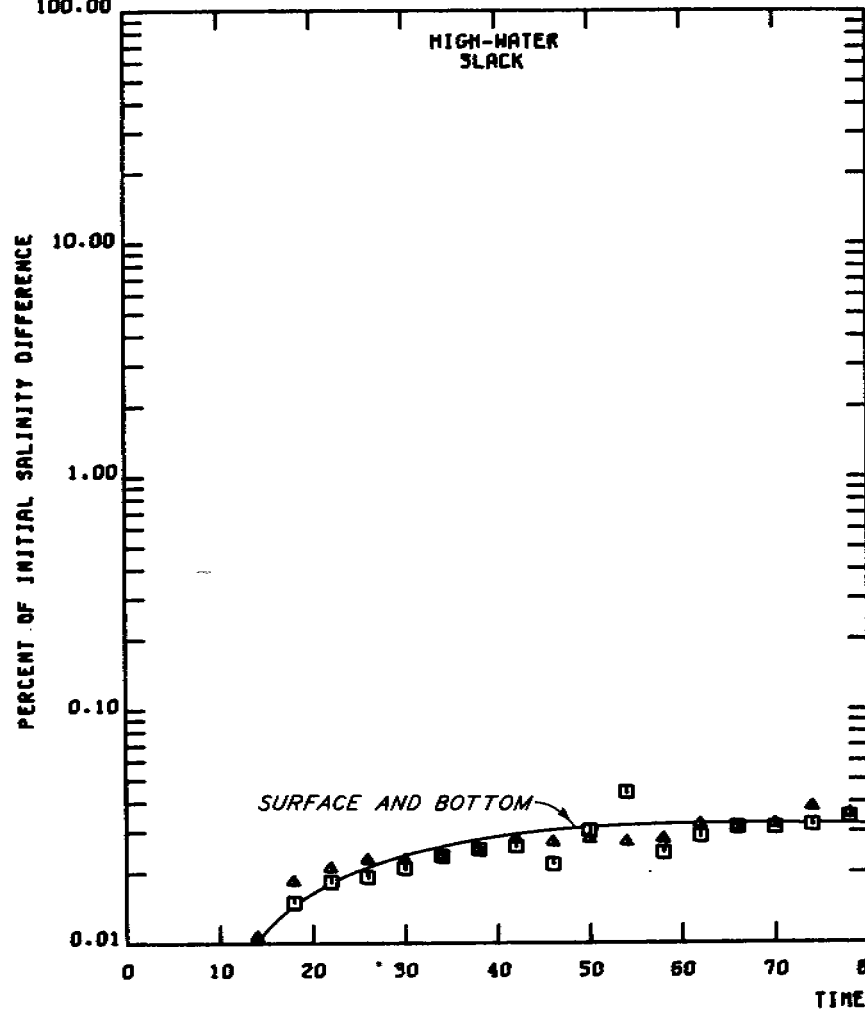


PLATE 49

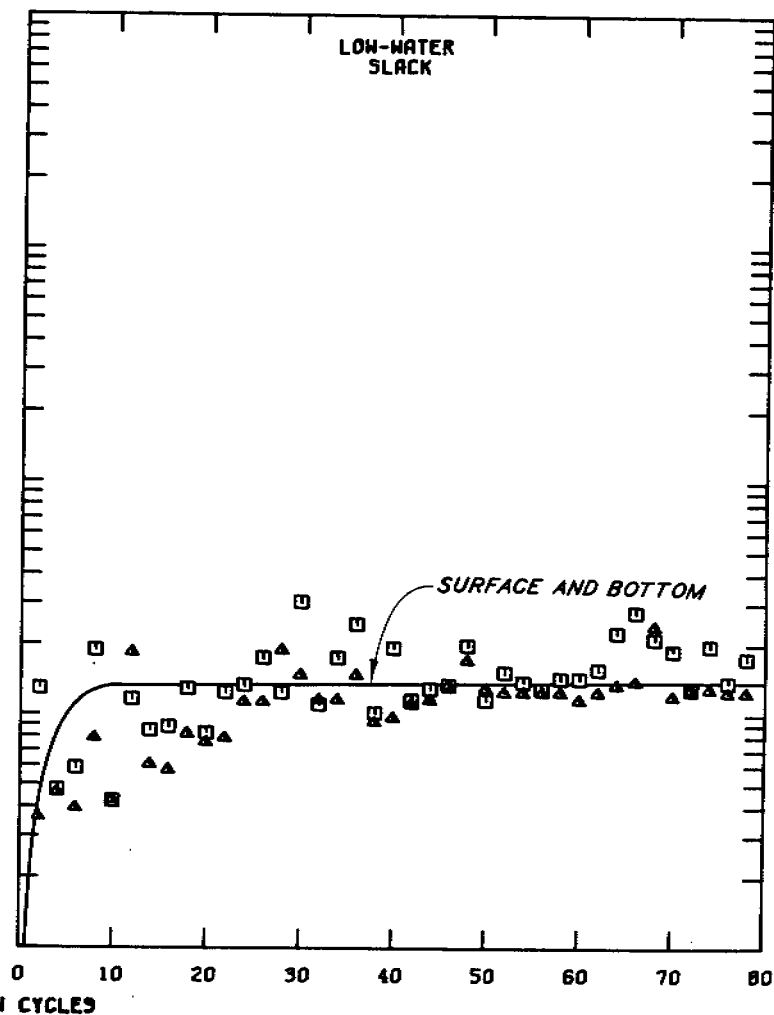
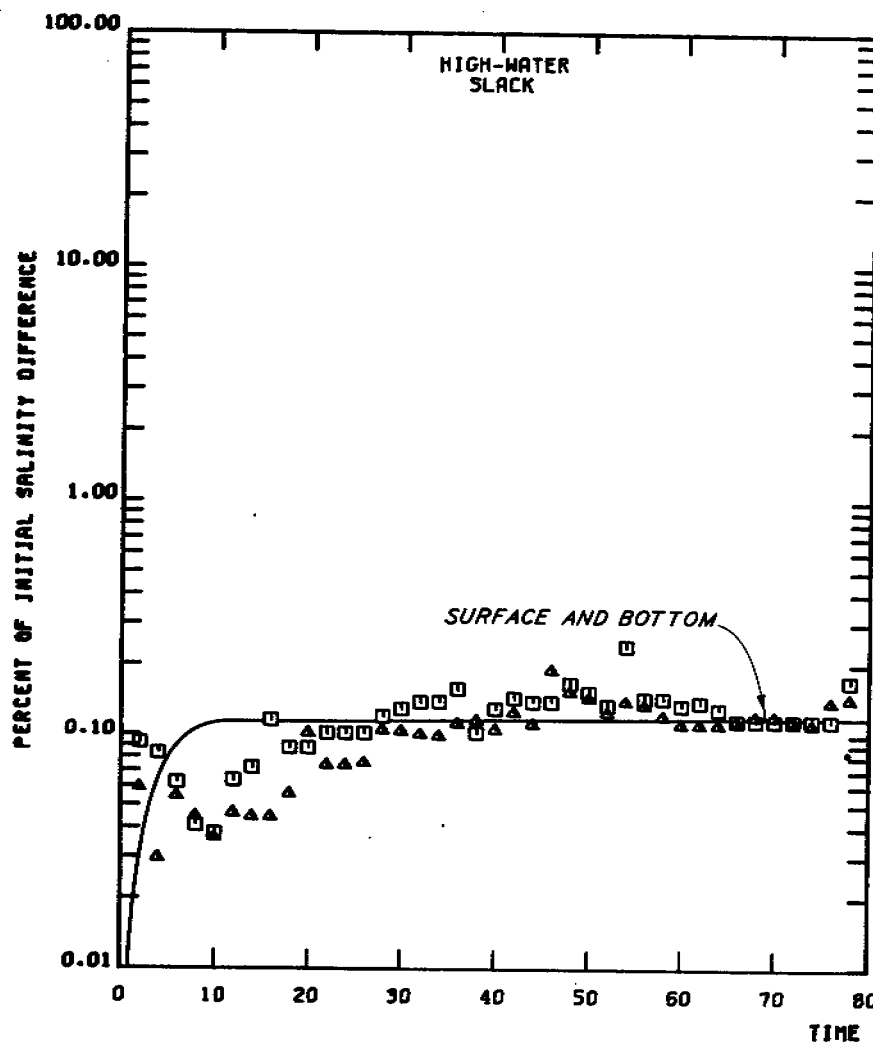
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ - - - BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U6**



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

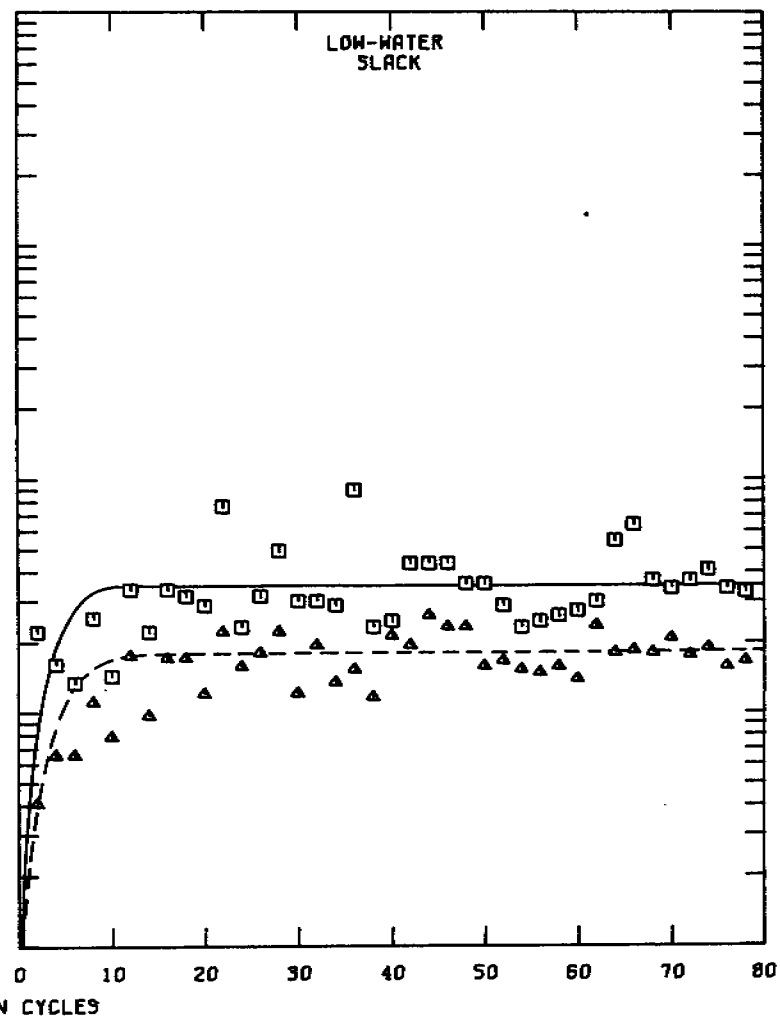
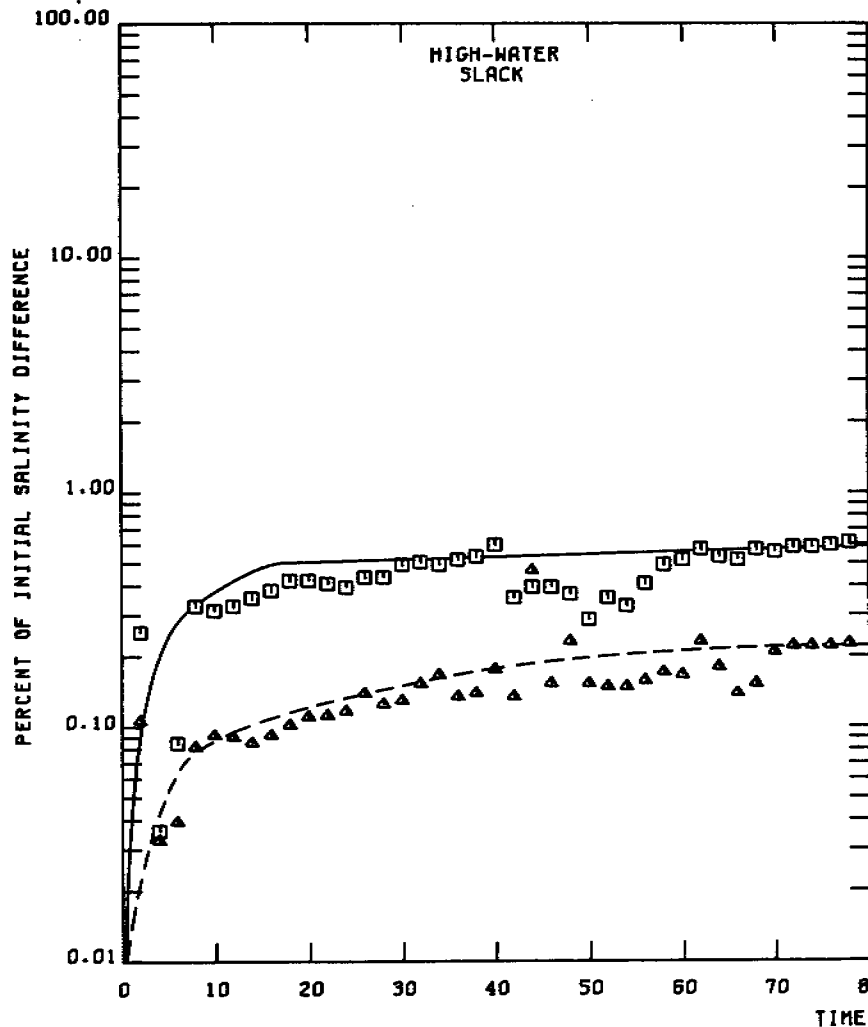
11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ - - - BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT**

STATION 112



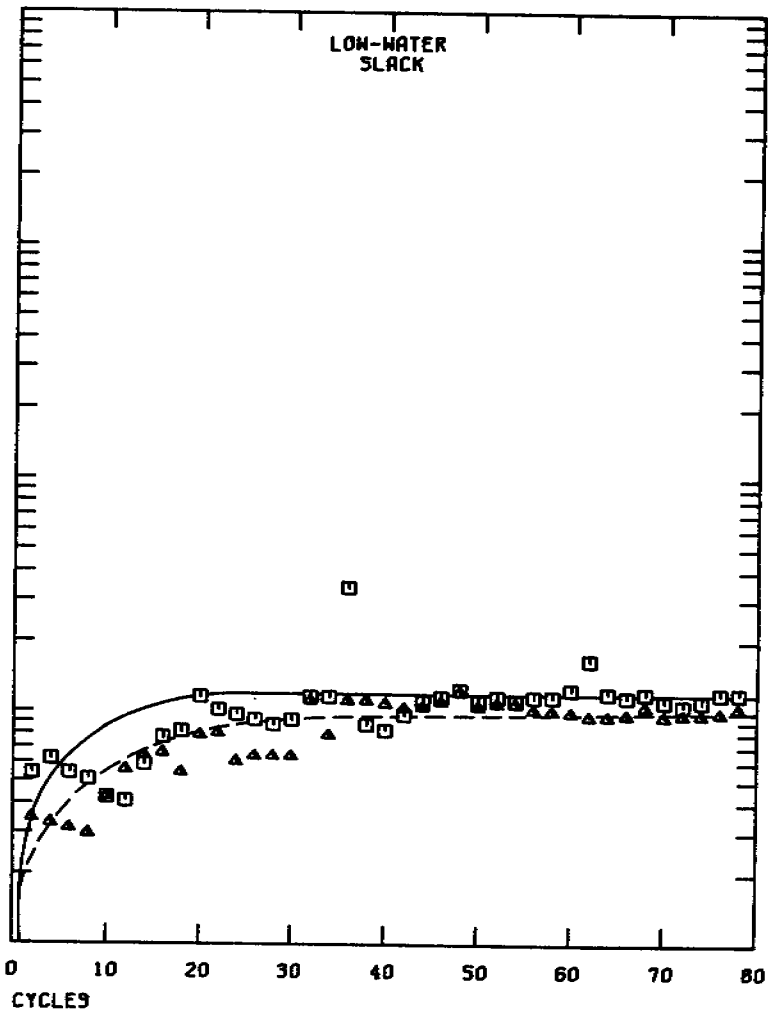
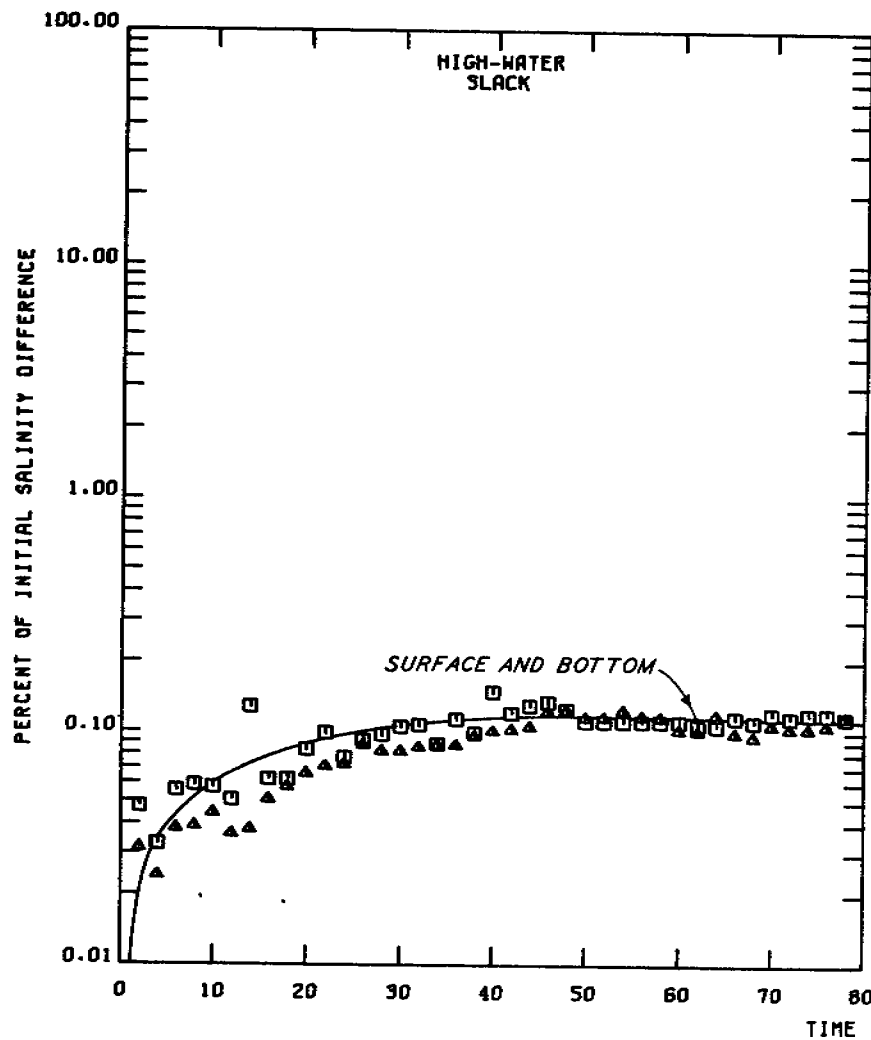
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION U8



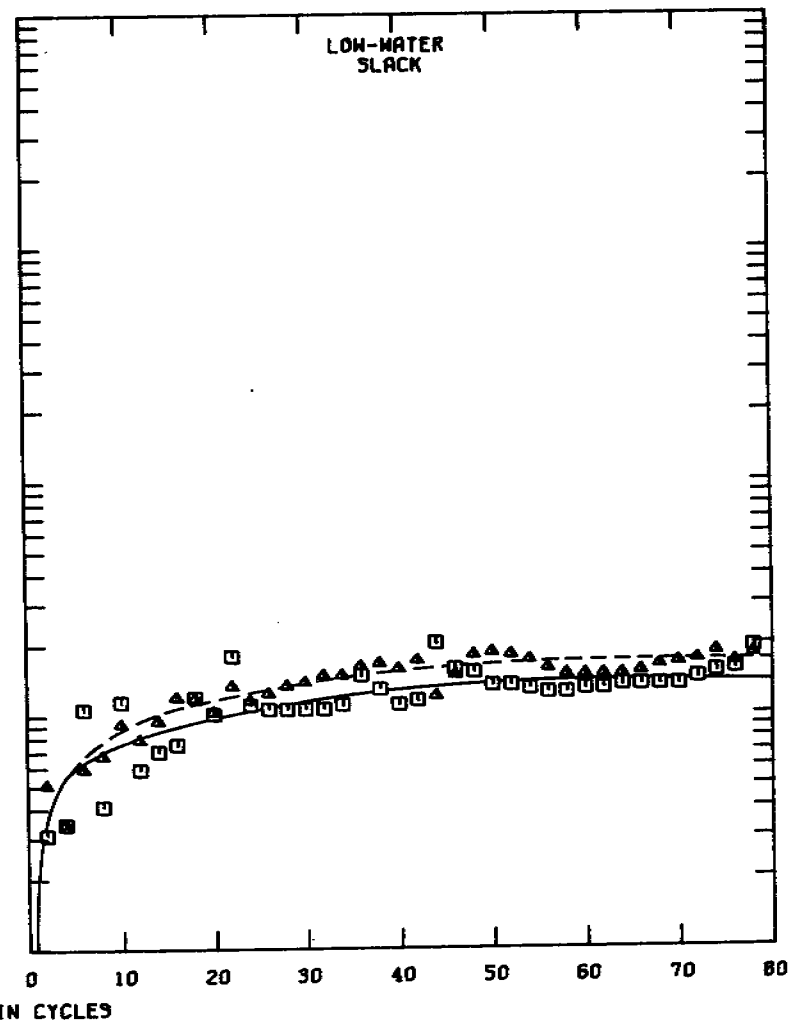
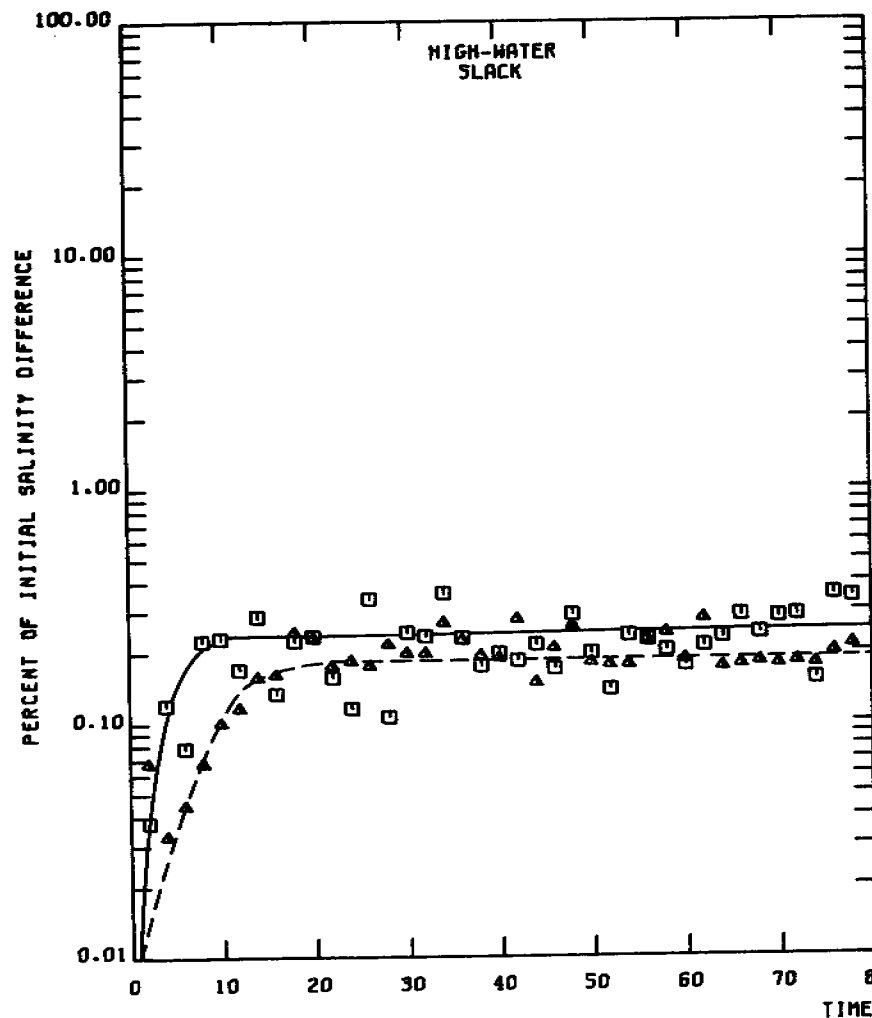
TEST CONDITIONS

FRESH-WATER DISCHARGE	11329 CFS
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ - - -	BOTTOM

GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION U9



TIME IN CYCLES

LEGEND

□ ——— SURFACE
△ ——— BOTTOM

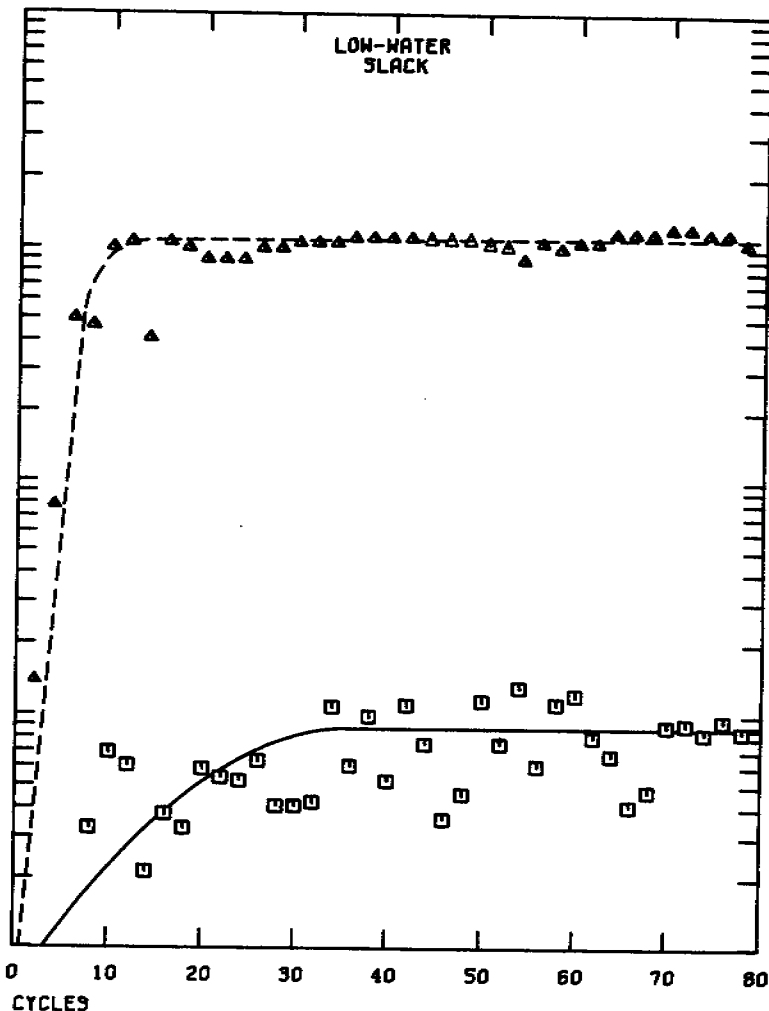
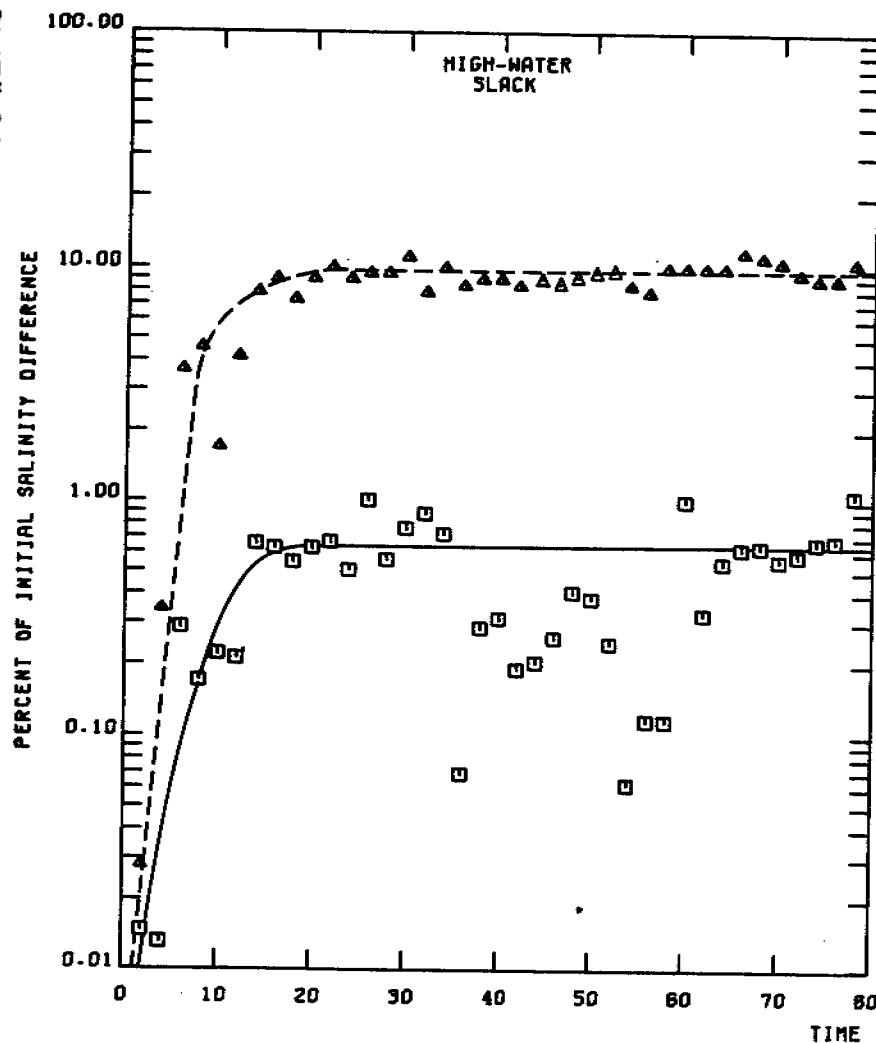
TEST CONDITIONS

FRESH-WATER DISCHARGE
BASE SALINITY AT DIFFUSER
EFFLUENT SALINITY
INITIAL SALINITY DIFFERENCE
EFFLUENT INJECTION RATE

11329 CF3
19.6 PPT
31.0 PPT
11.4 PPT
21.2 MGD

GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT

STATION U10

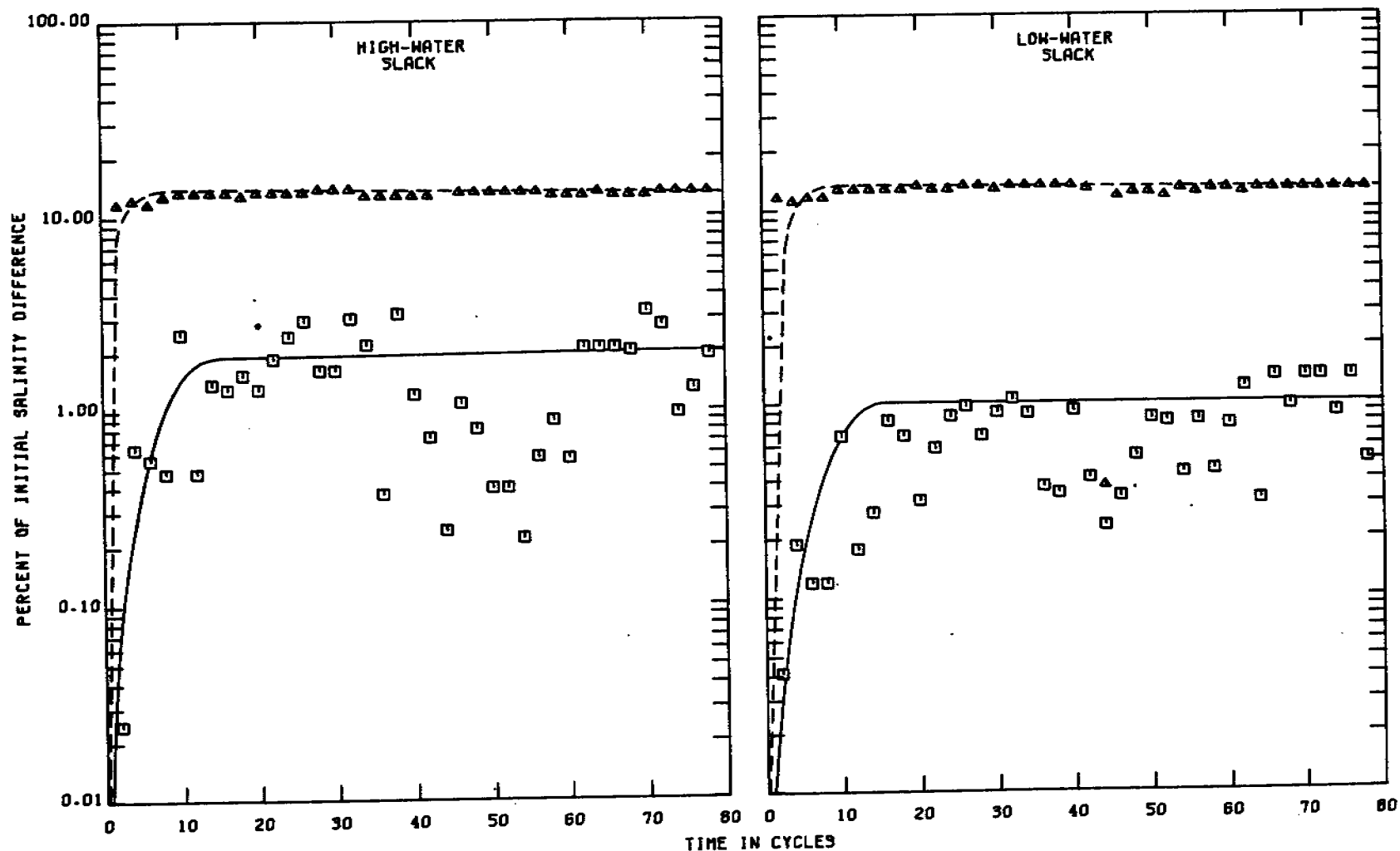


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ - - - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U11

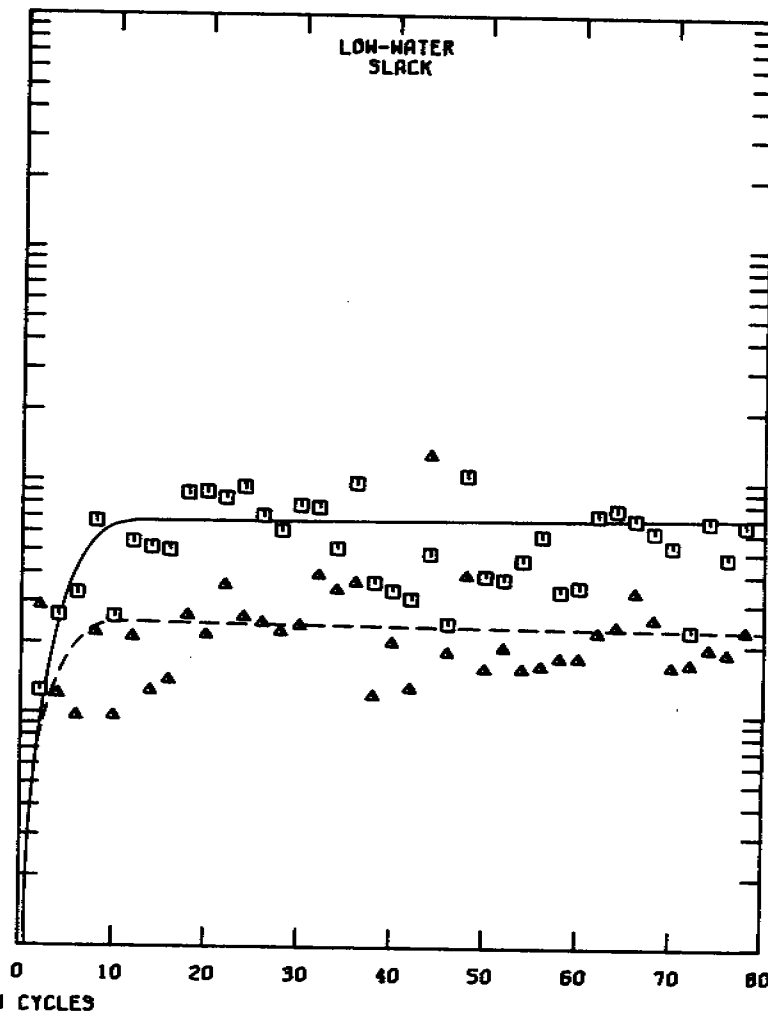
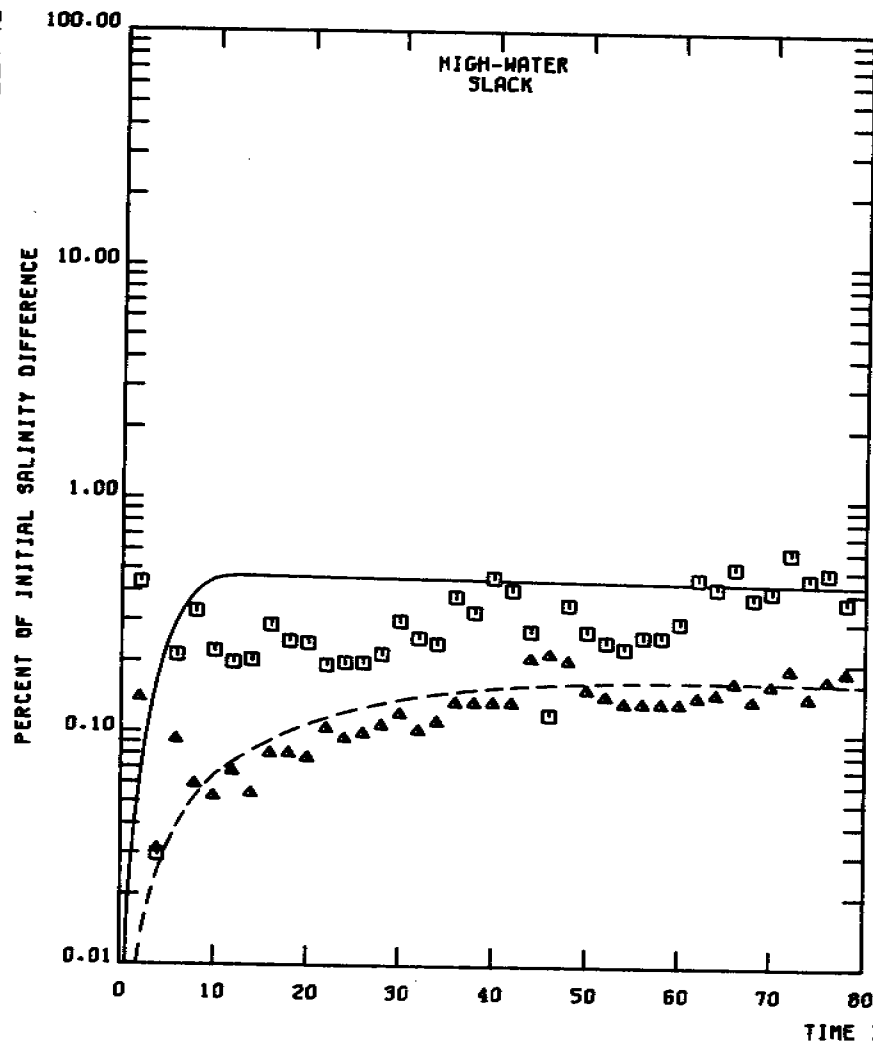


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CFS
 19.6 PPT
 91.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U12



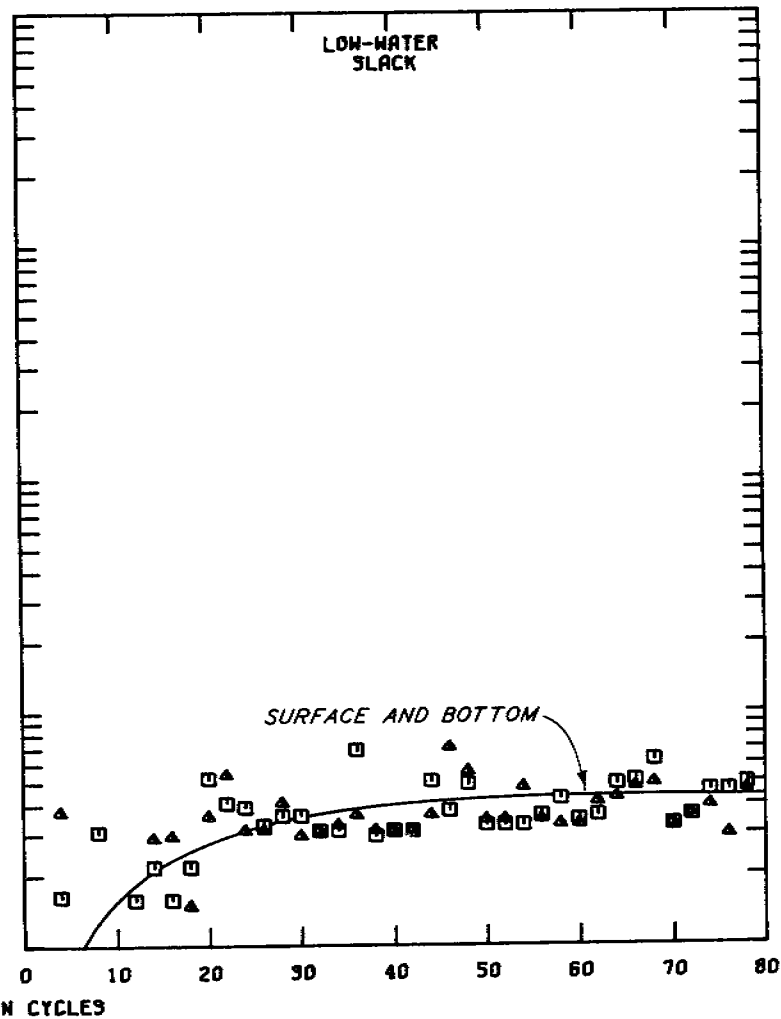
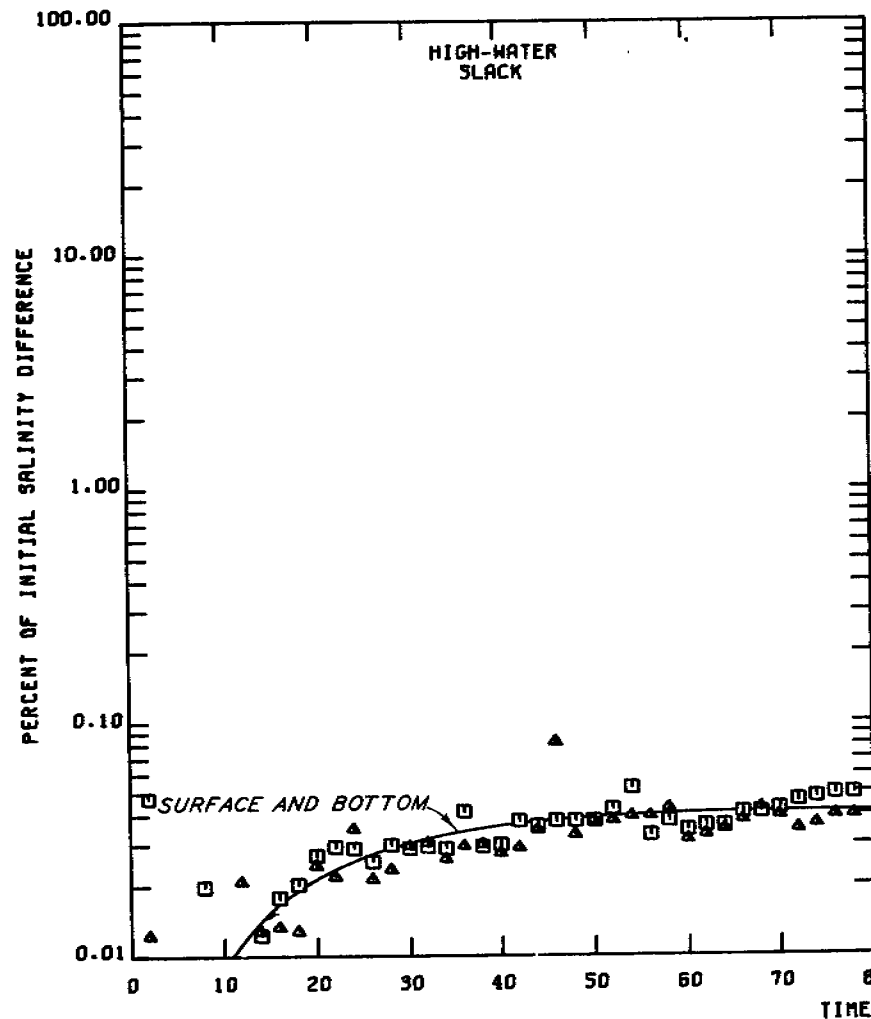
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CF9
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION 411

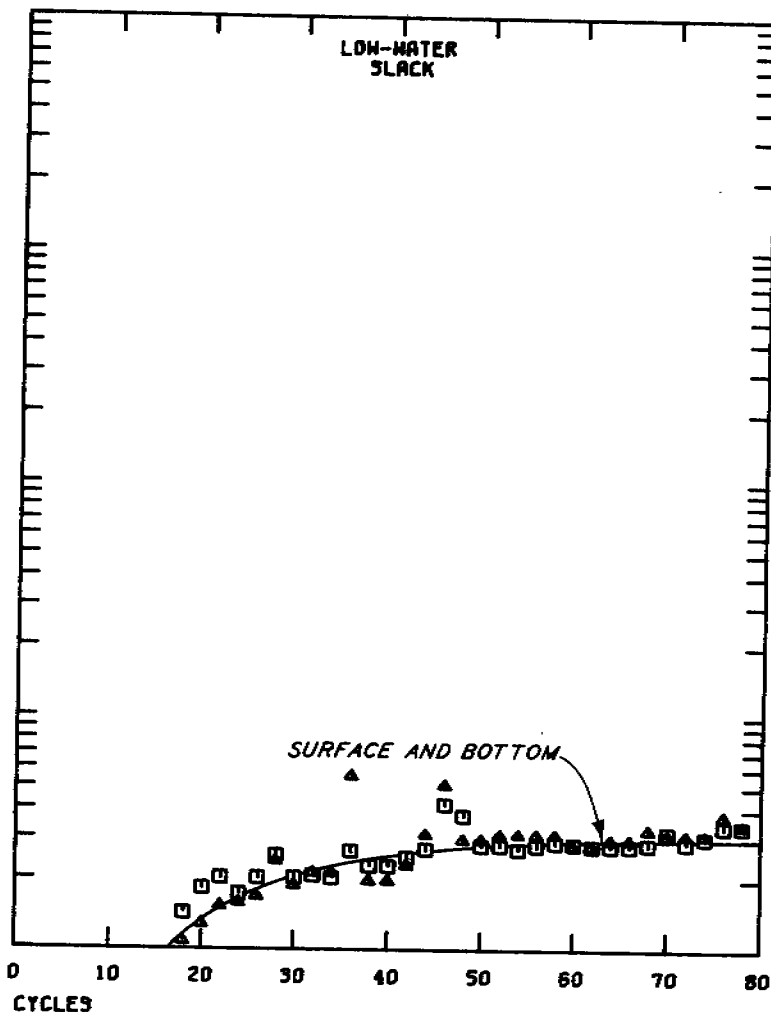
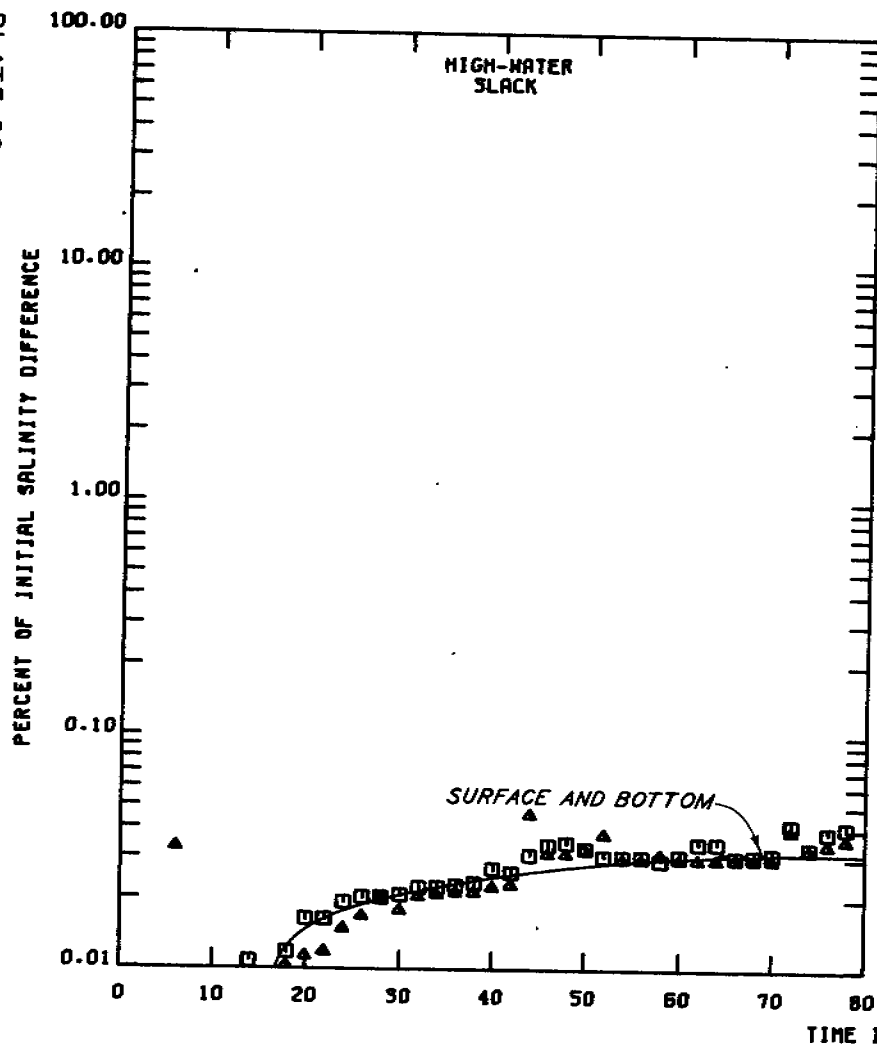


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ — — — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U14



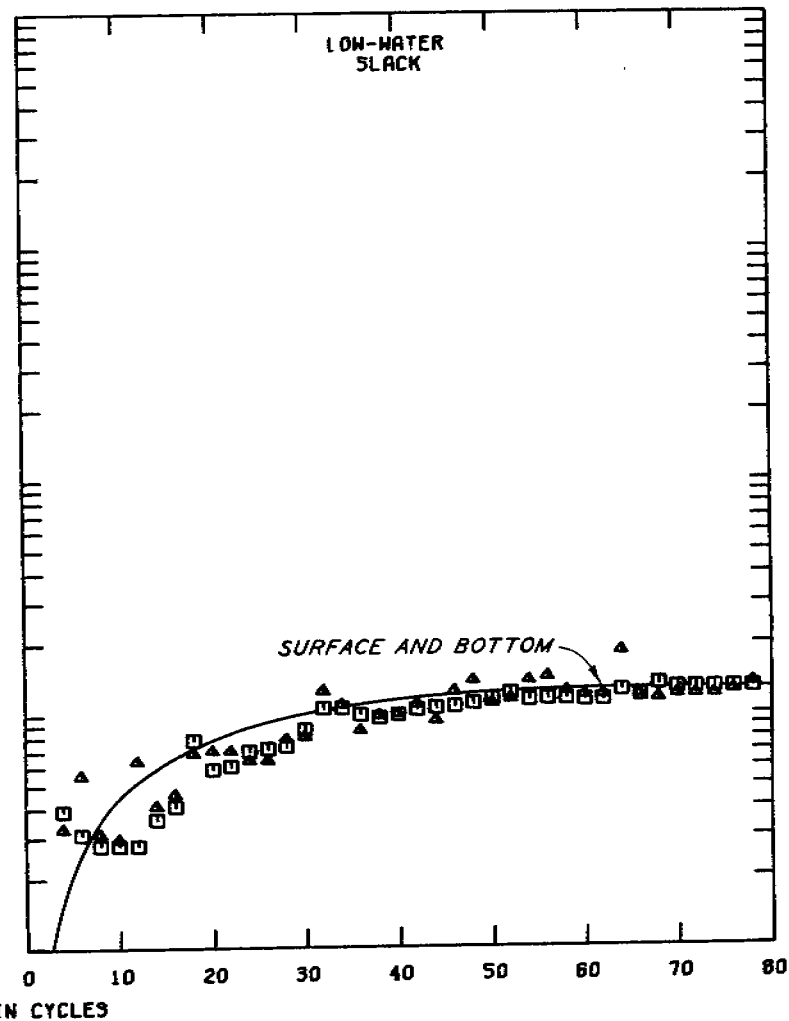
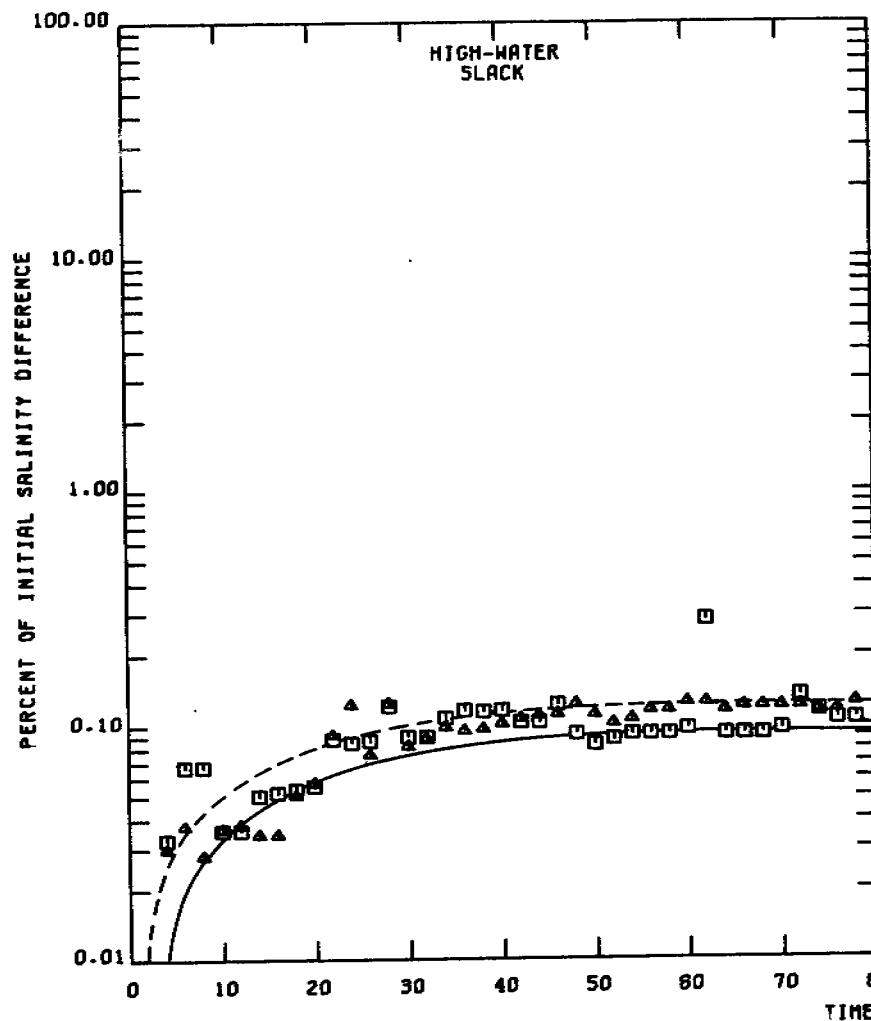
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION U15

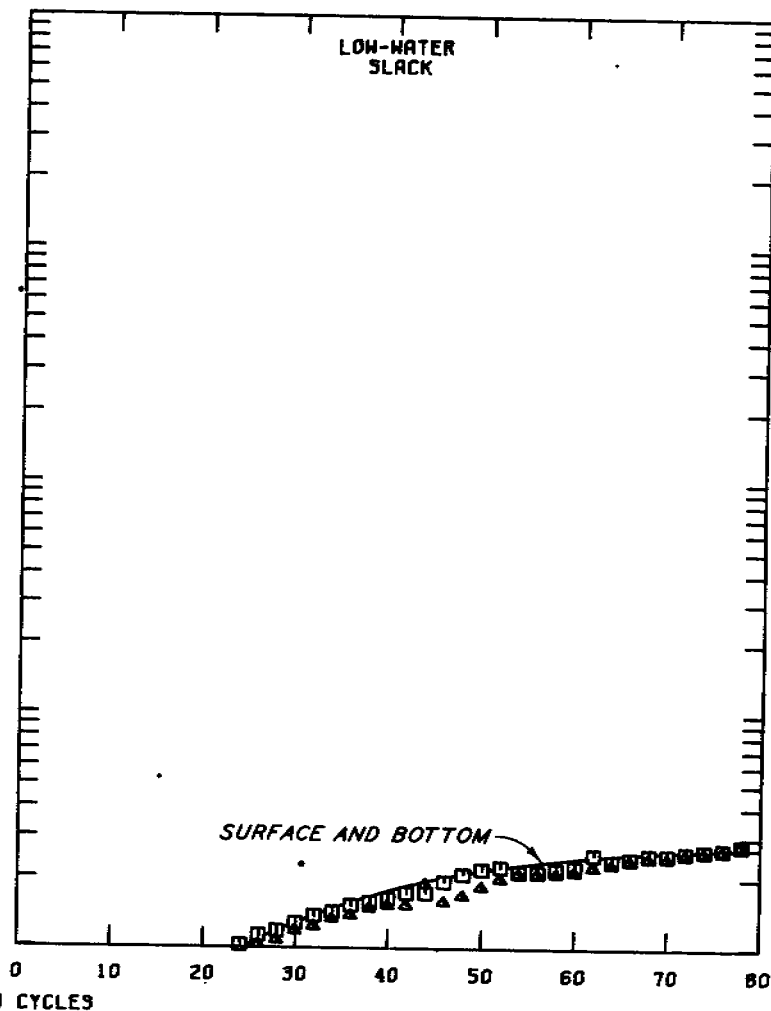
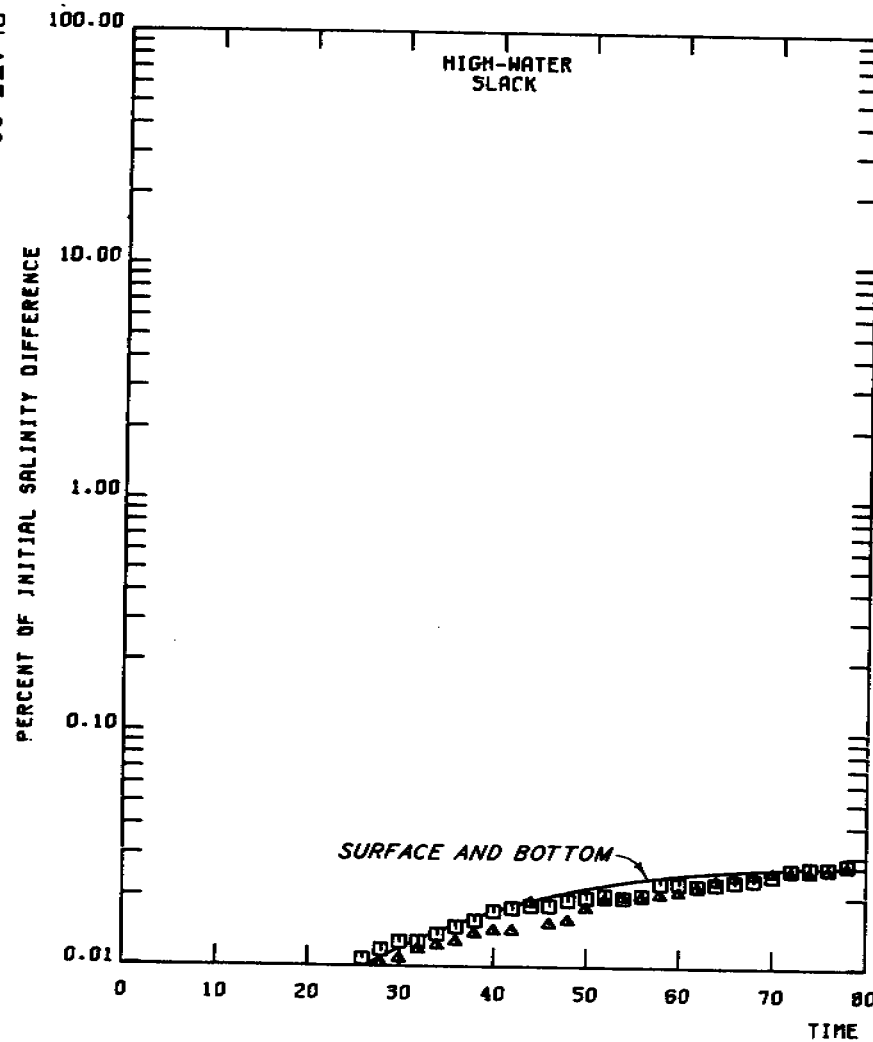


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11329 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION CL



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION M92

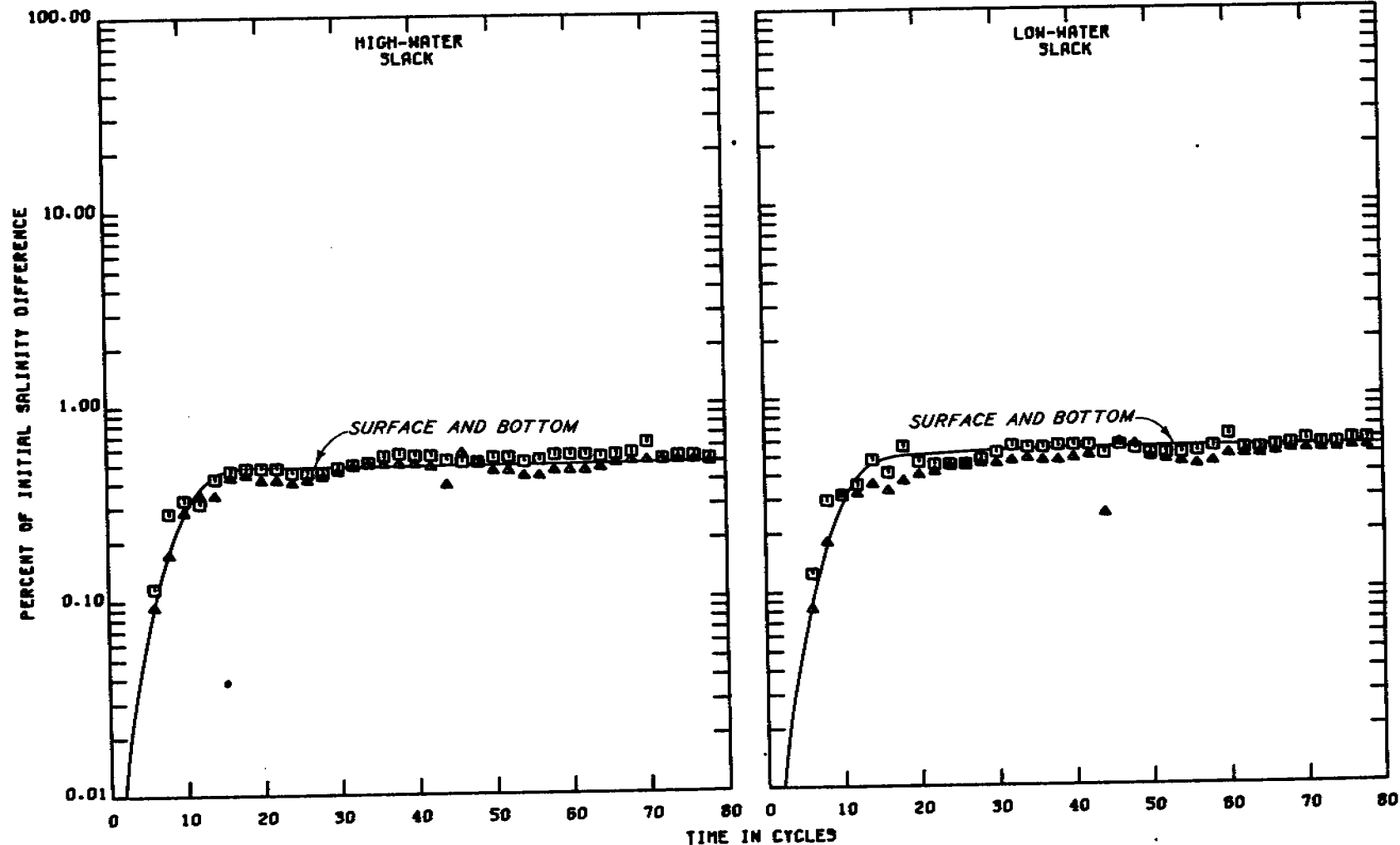


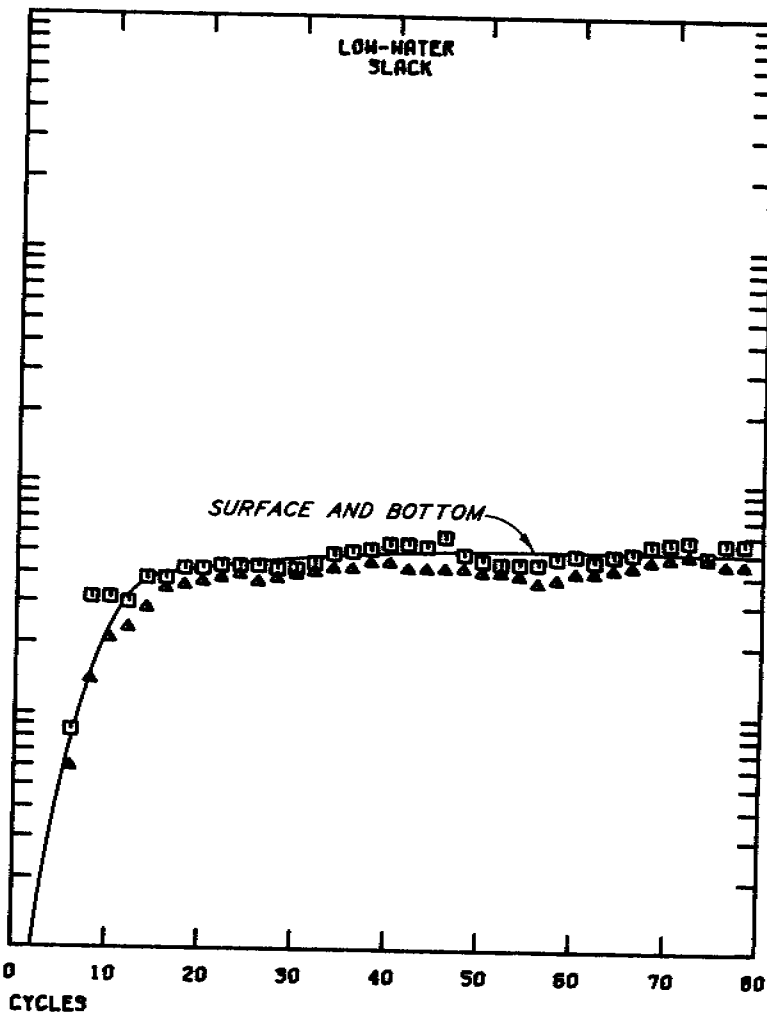
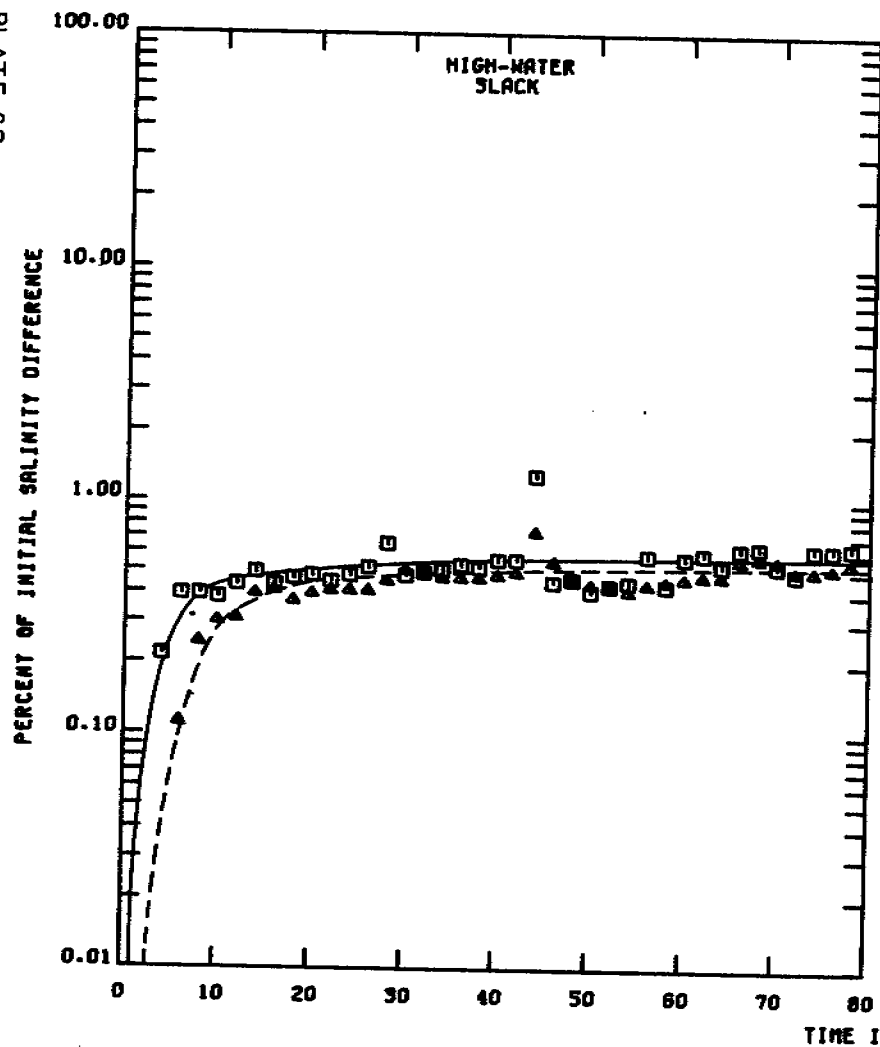
PLATE 61

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION LG1**

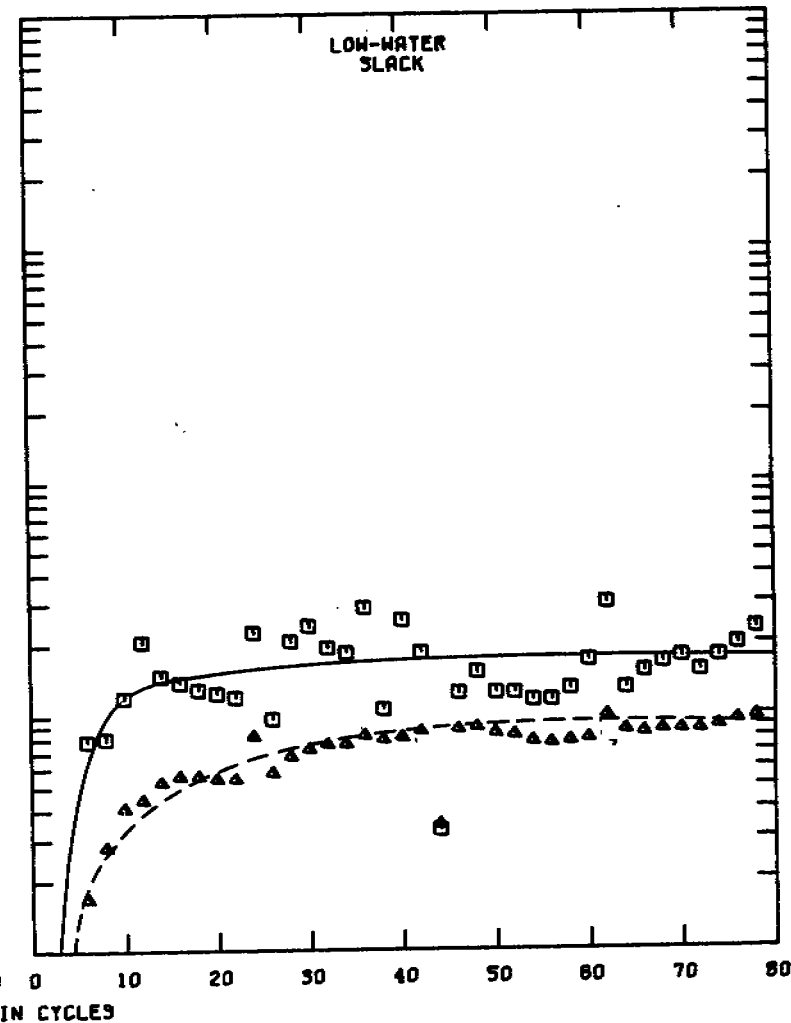
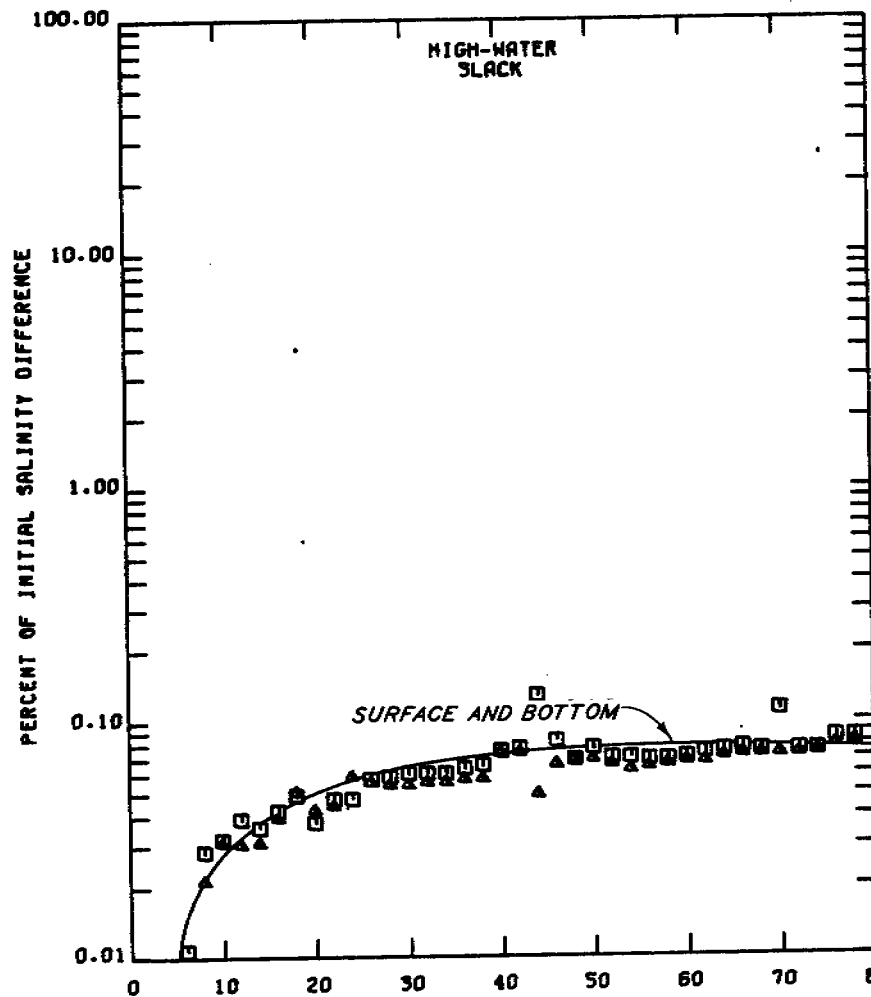


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION LG2

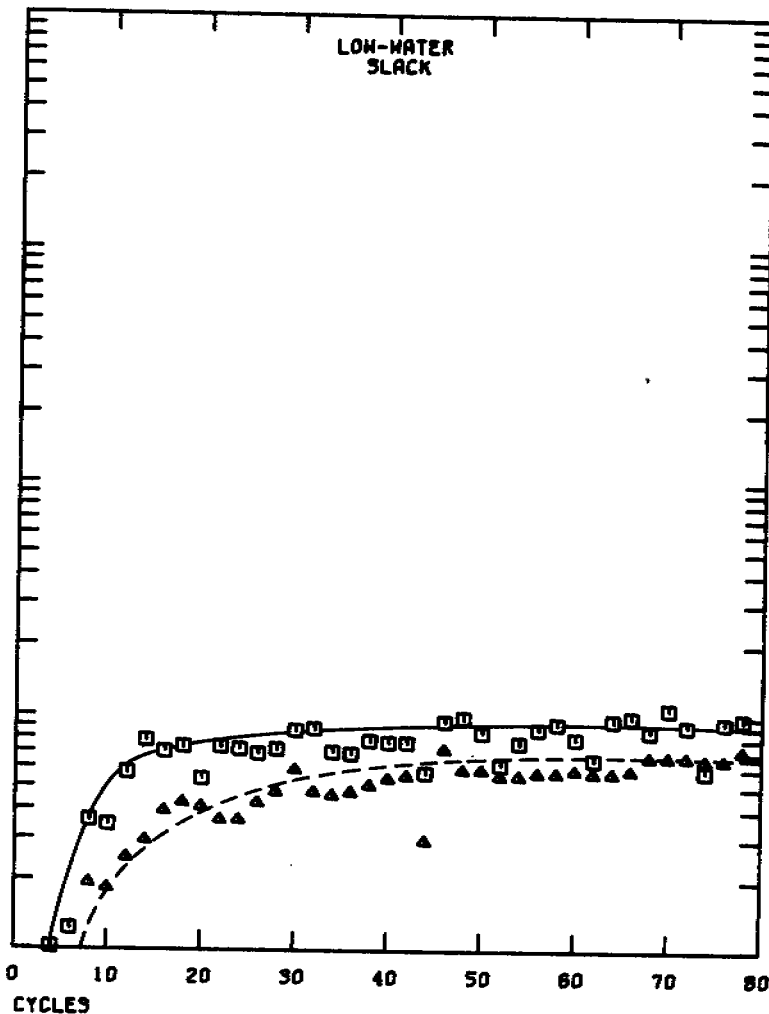
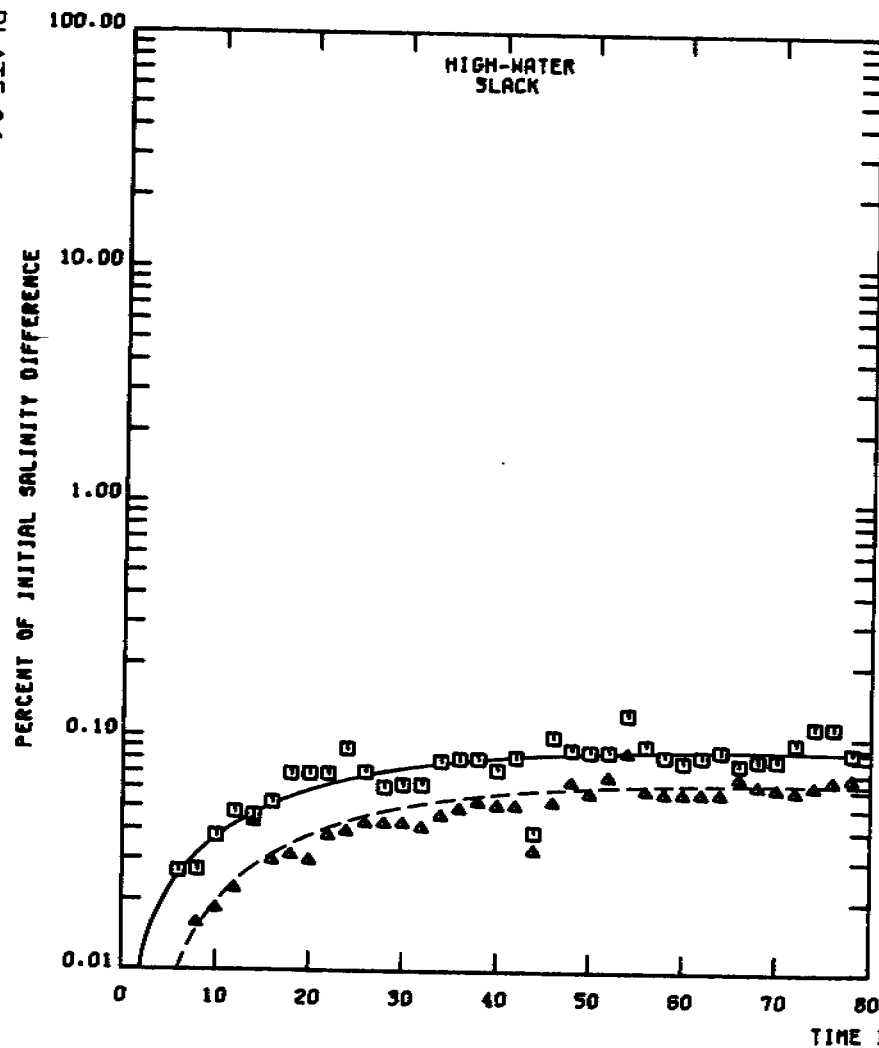


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11329 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION LG3



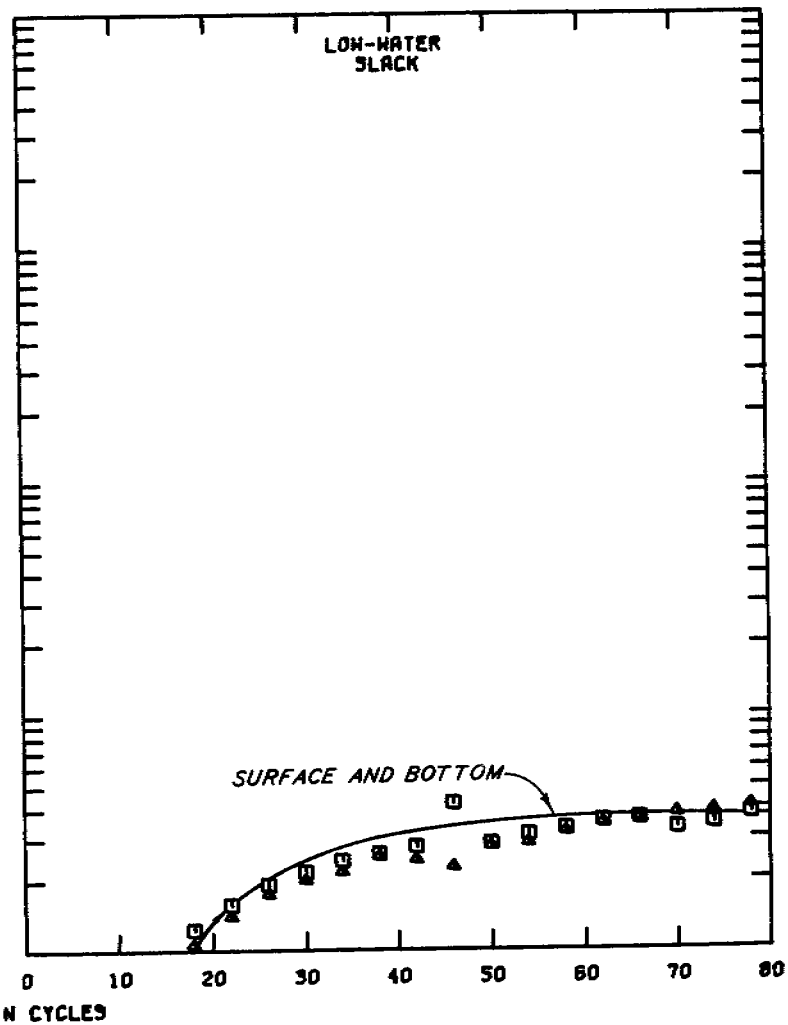
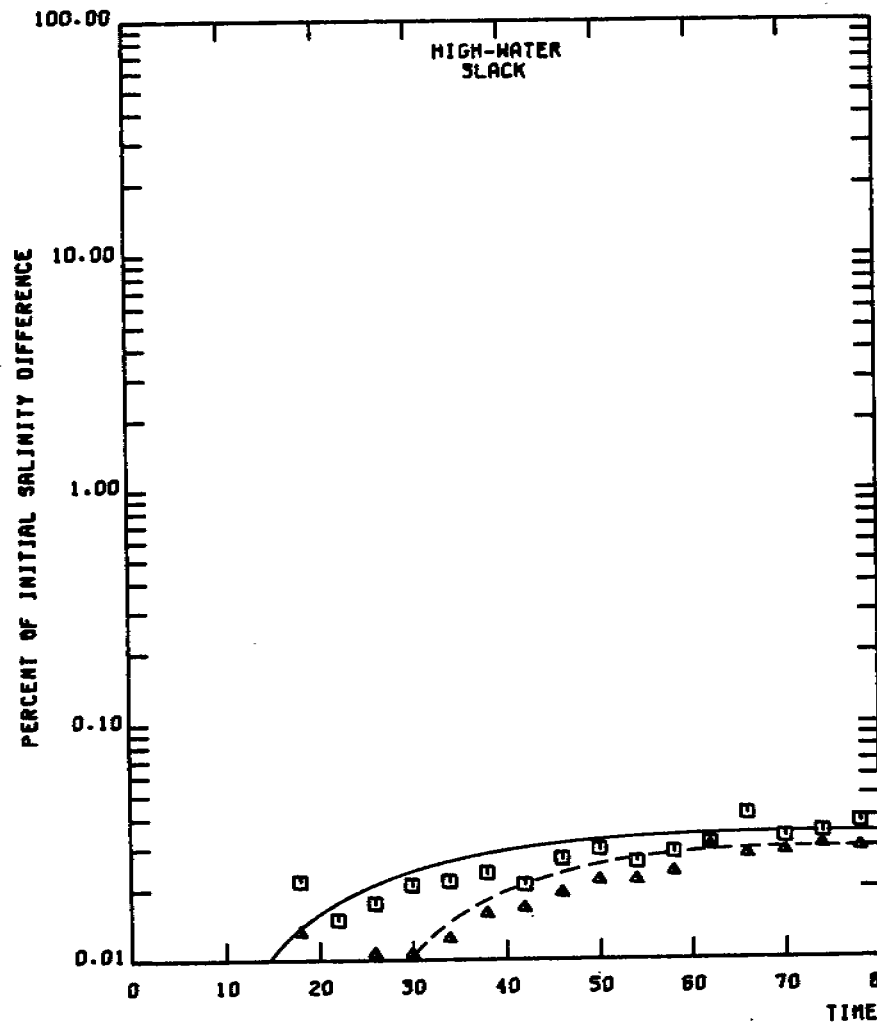
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION LG4

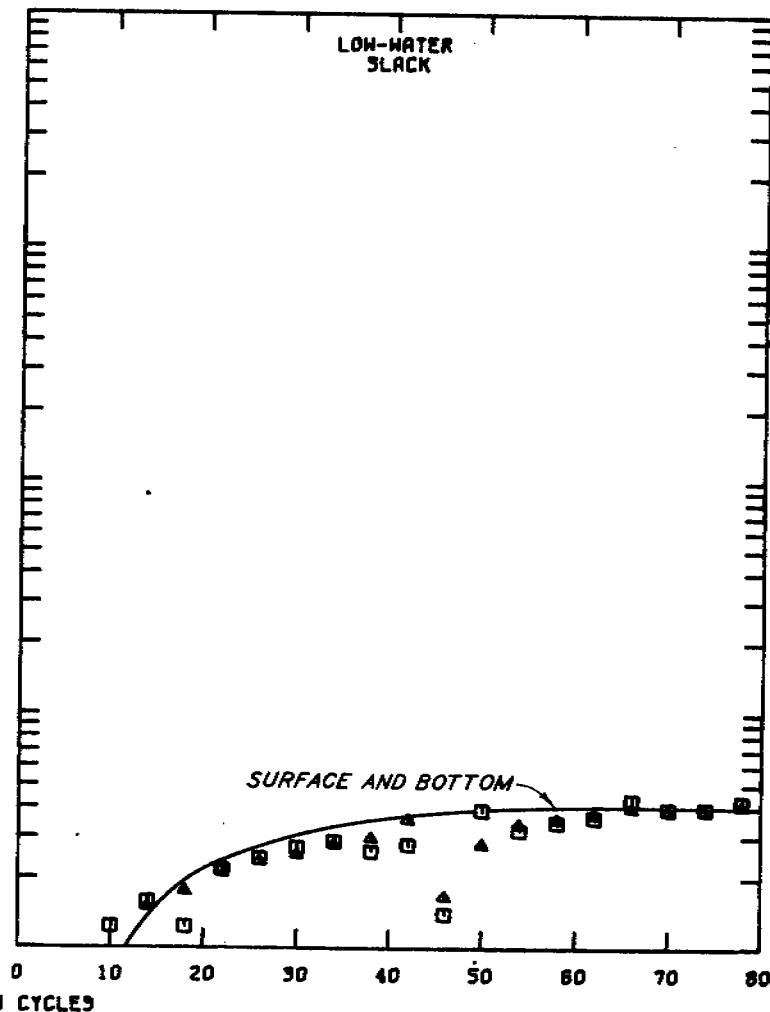
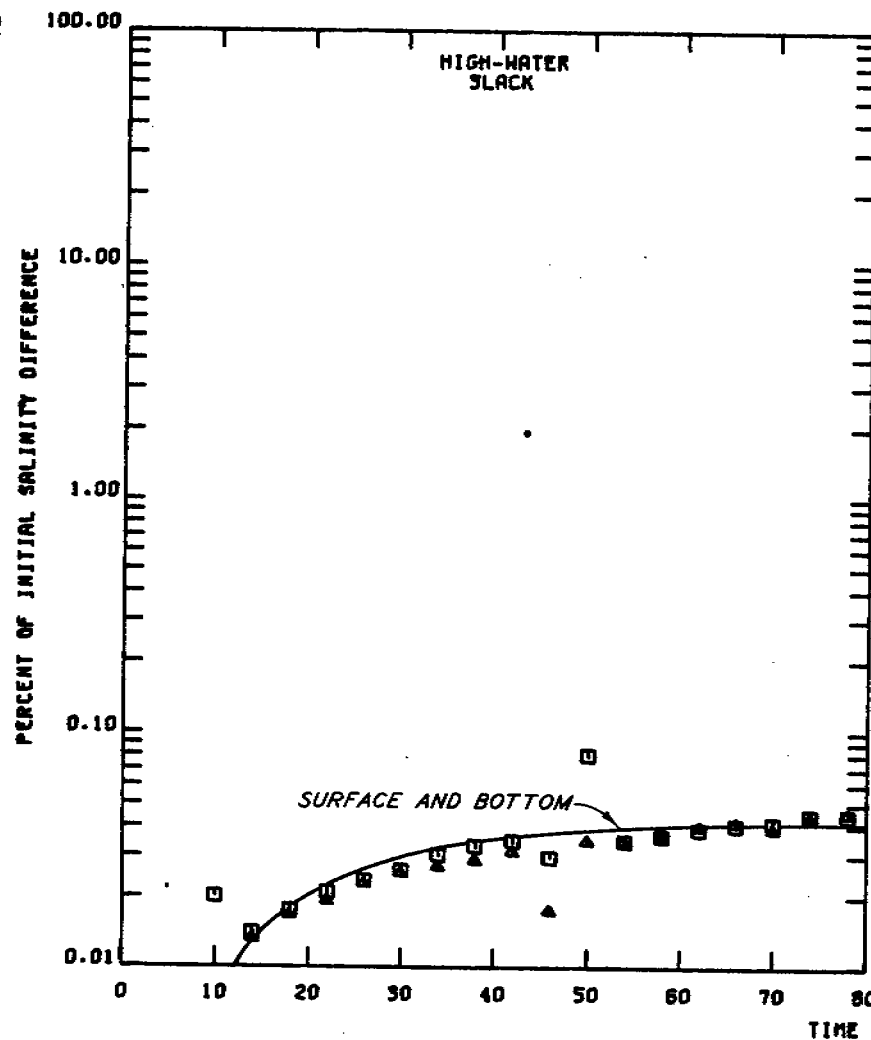


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 △ — — — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION LG5

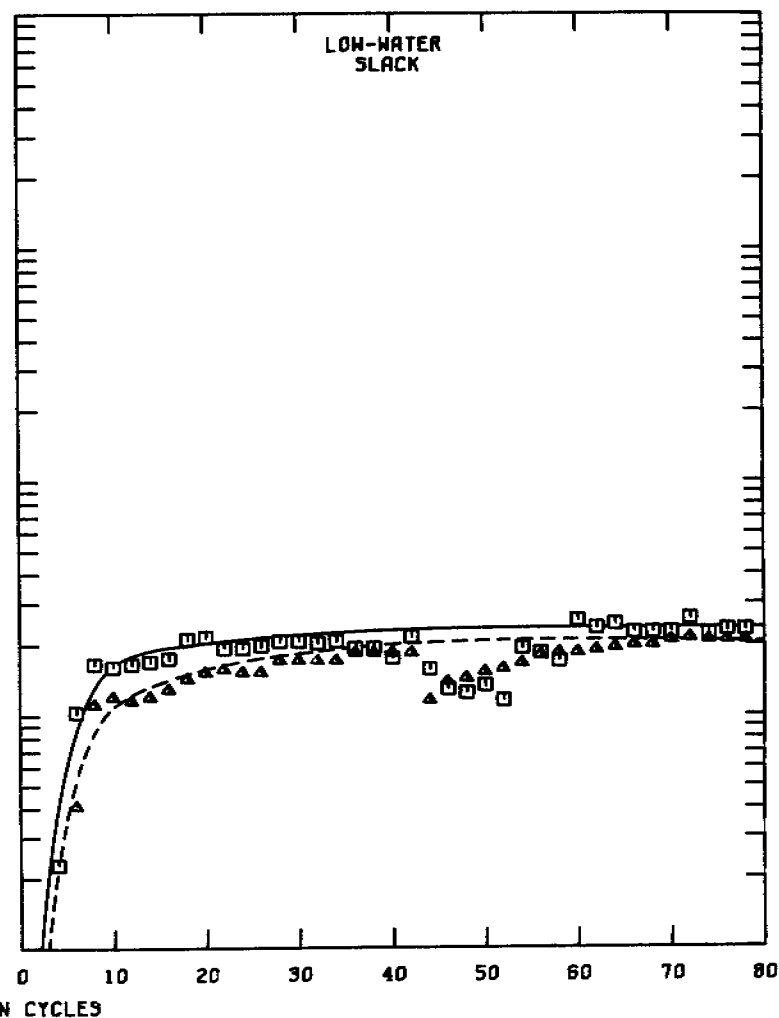
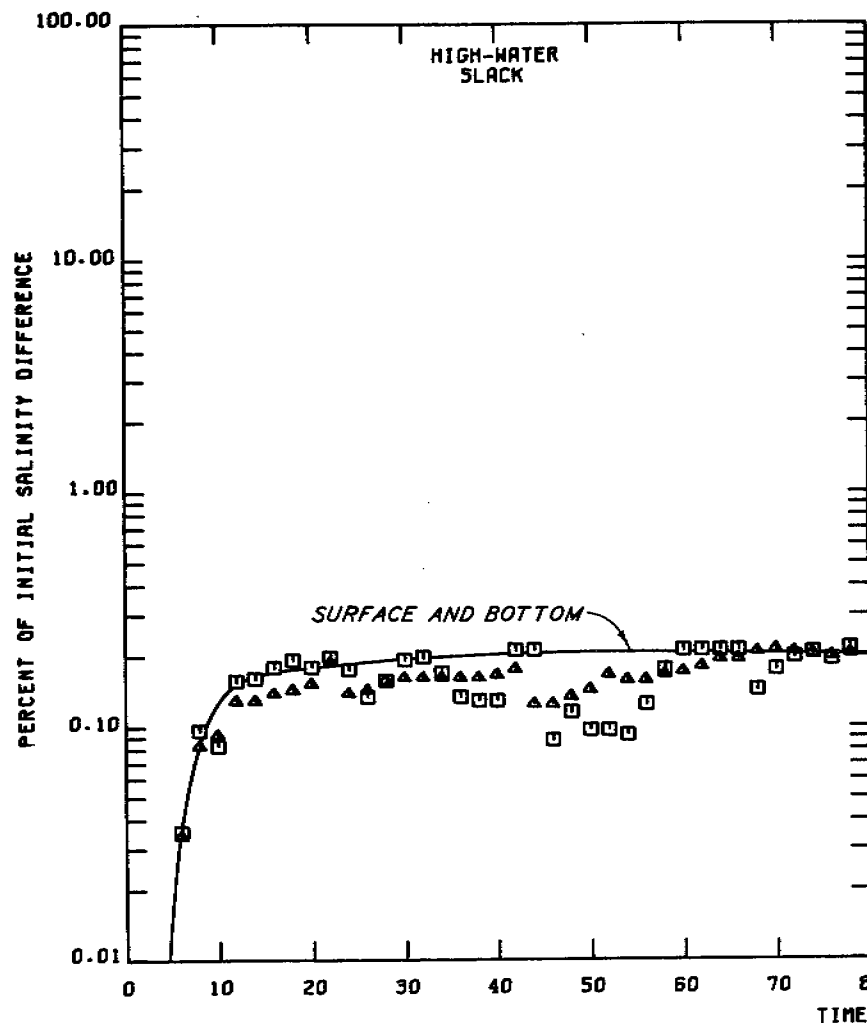


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION L68

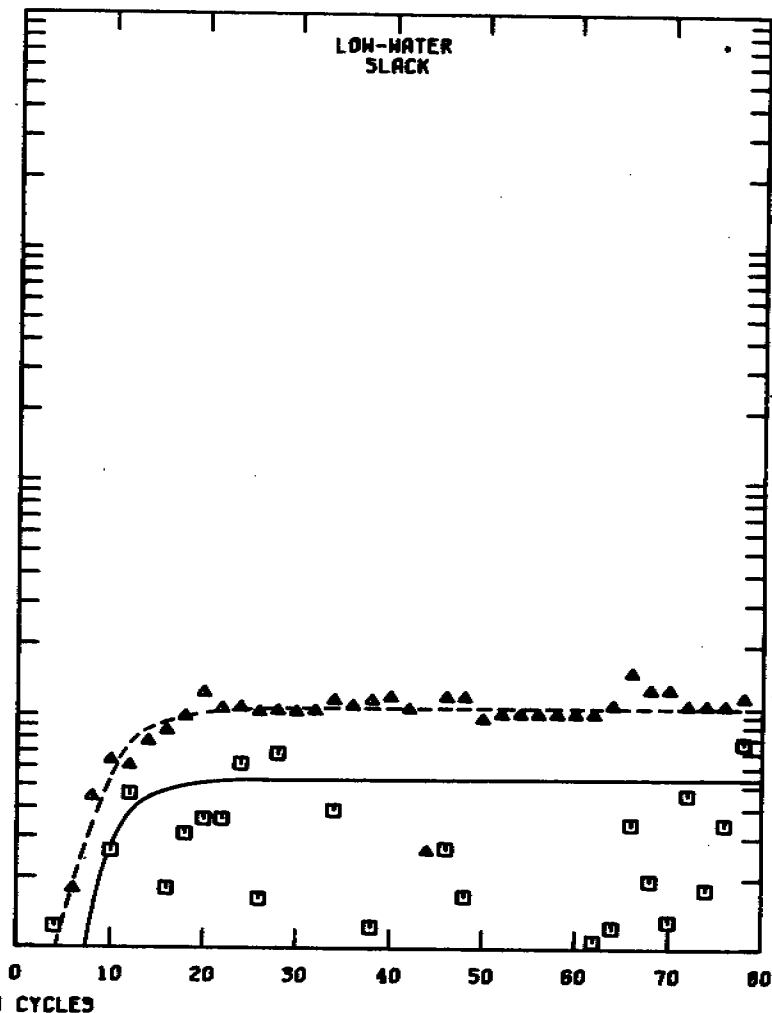
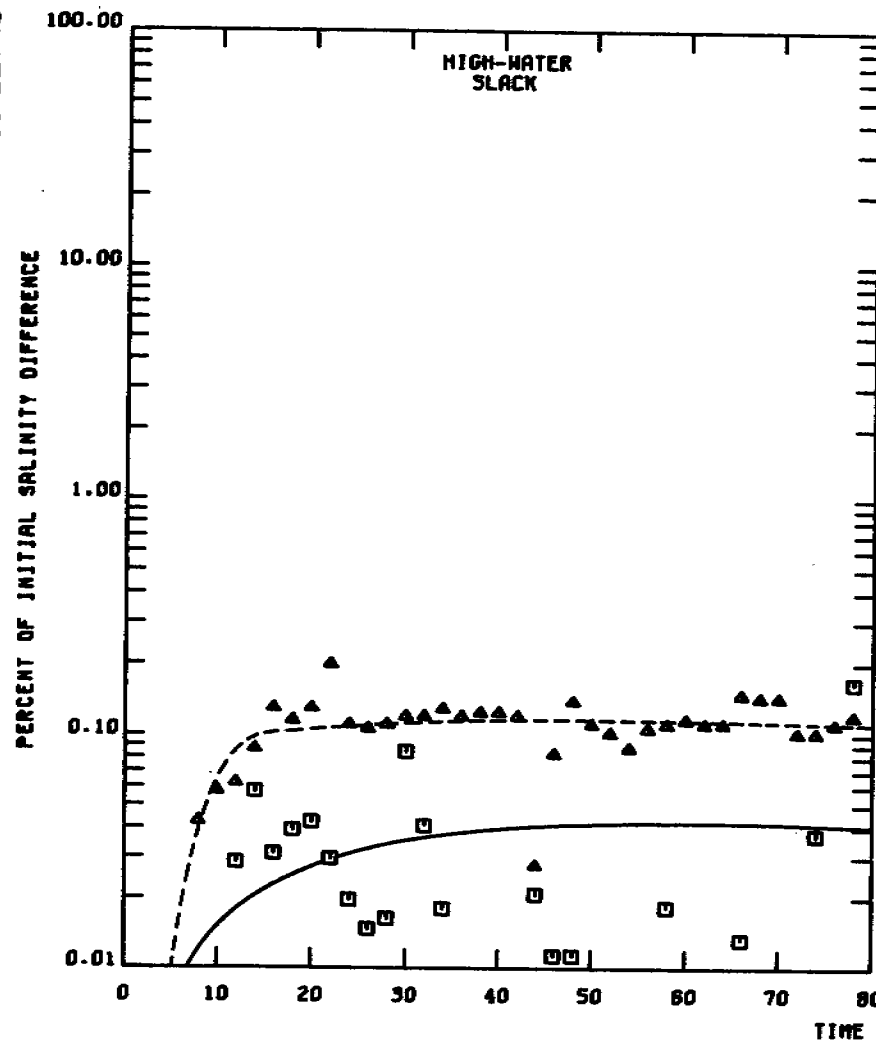


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CF9
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION DB

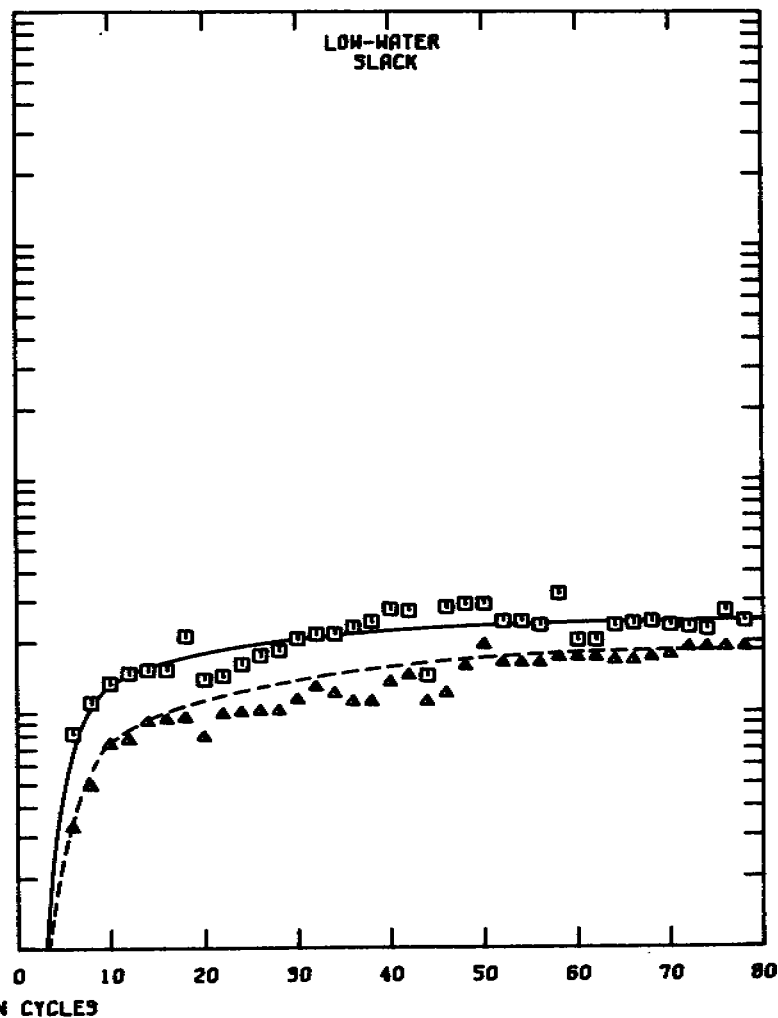
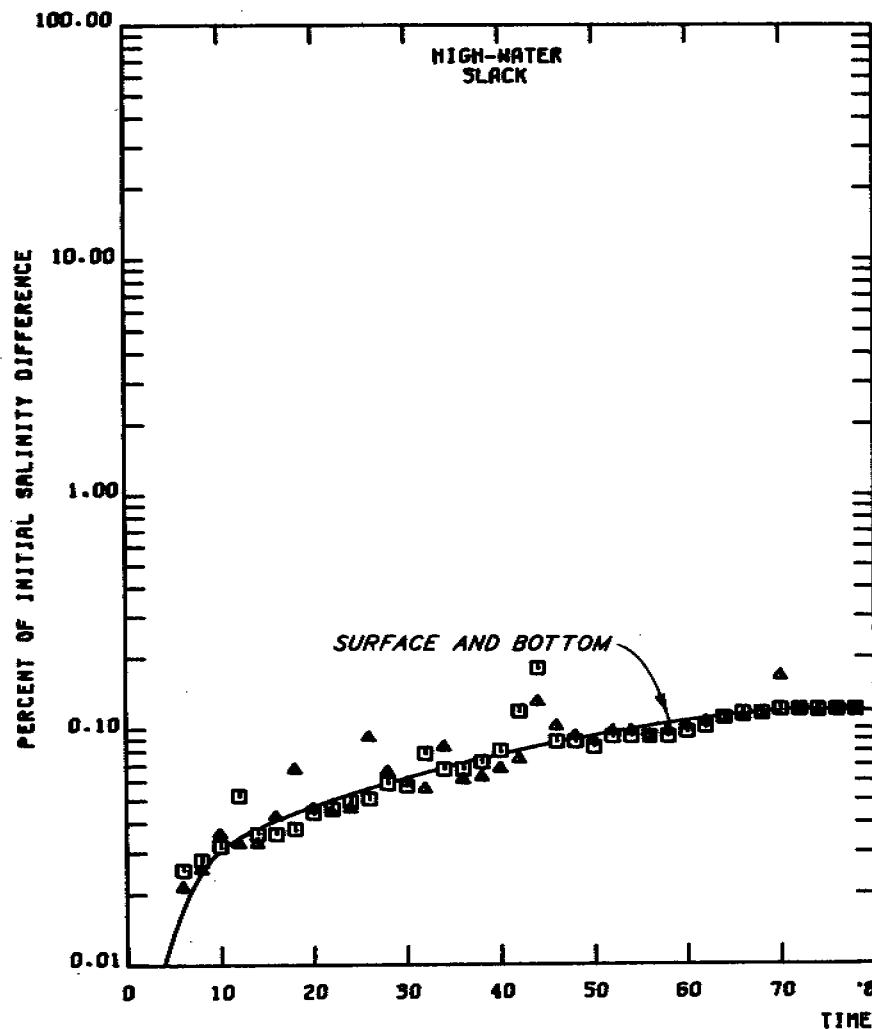


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 △ - - - BOTTOM

**CALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION RIC**



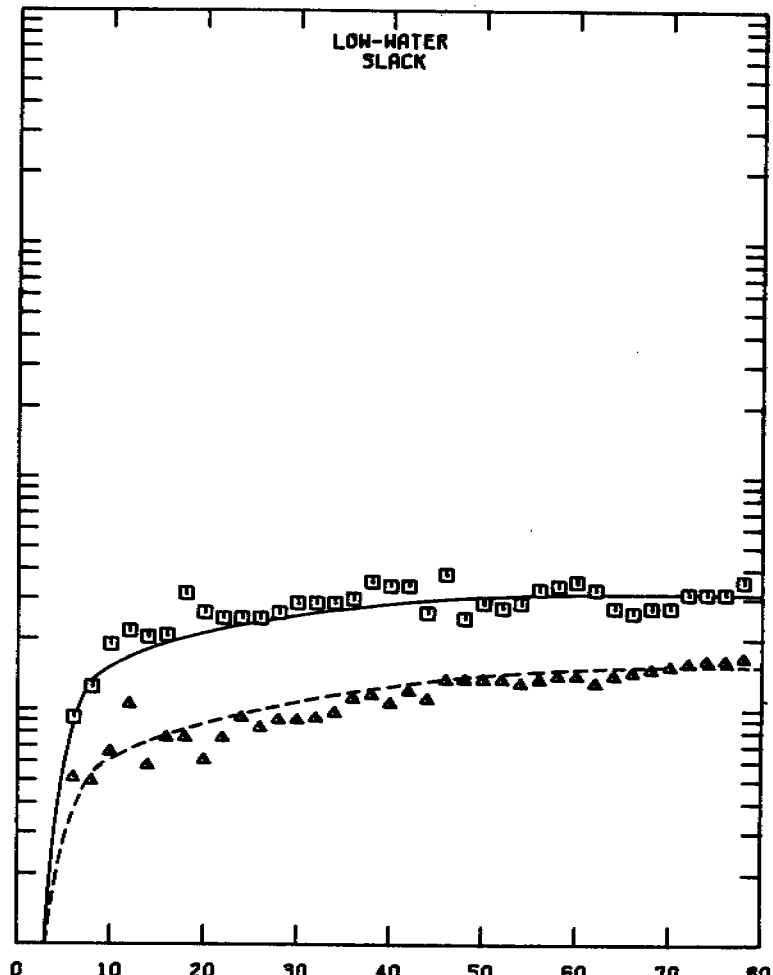
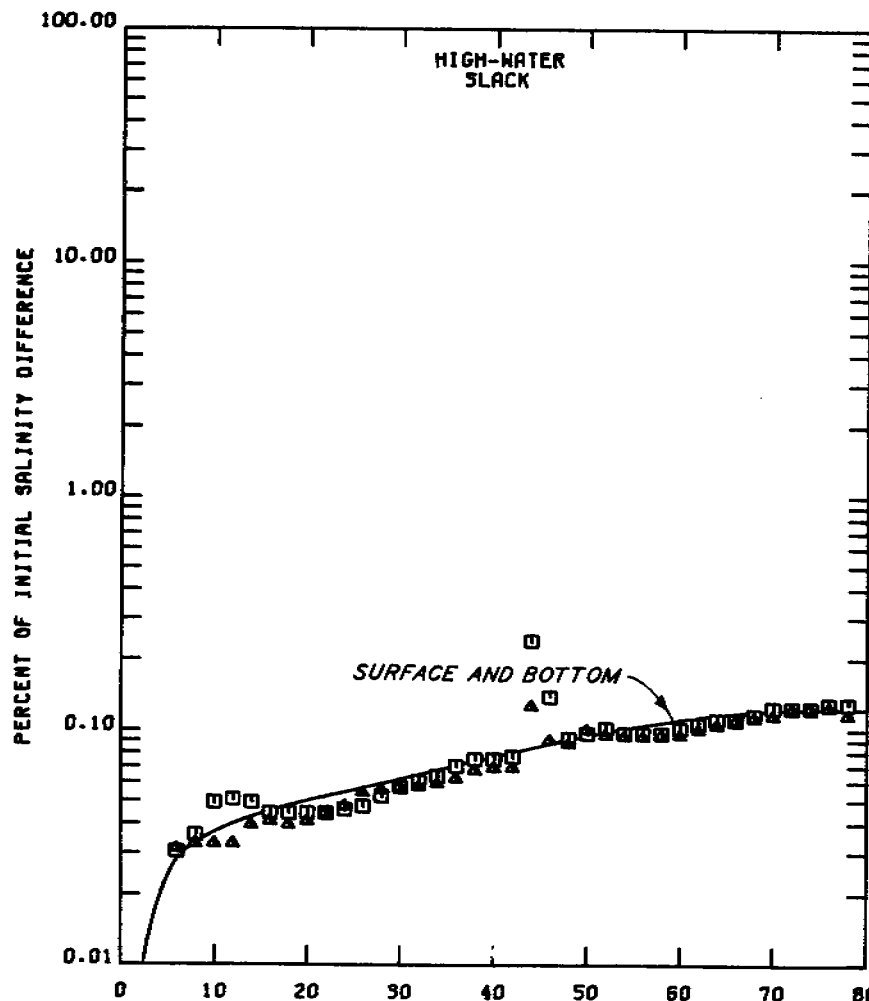
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CF9
 19.6 PPT
 91.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ — SURFACE
 ▲ - - - BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C1**



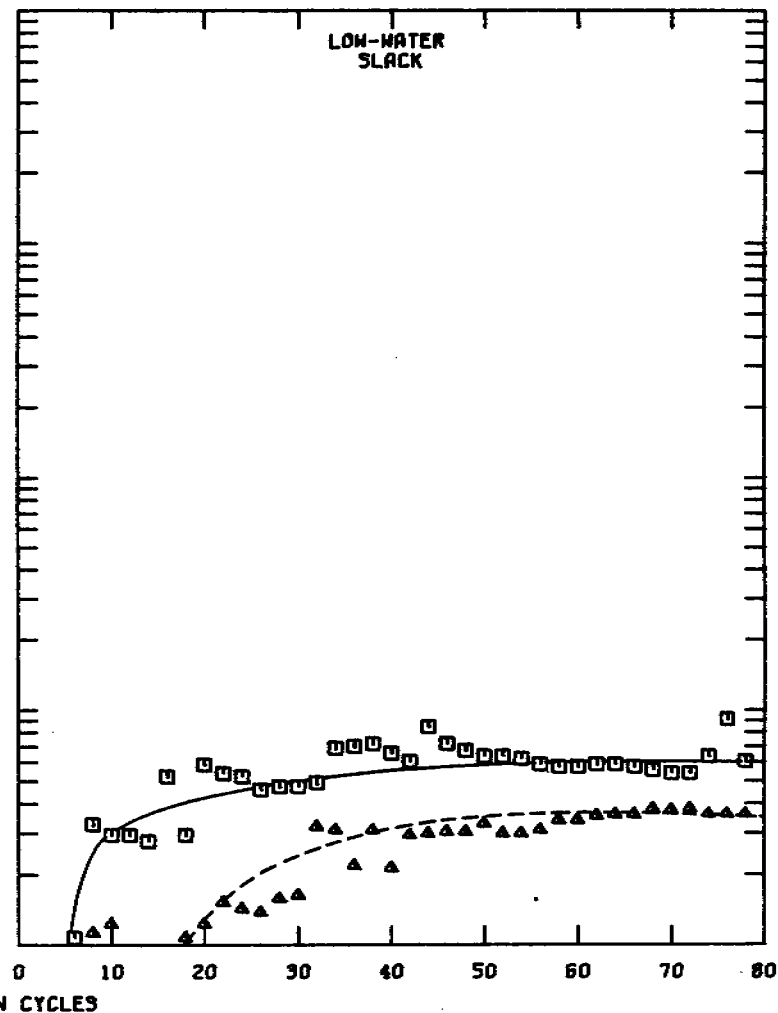
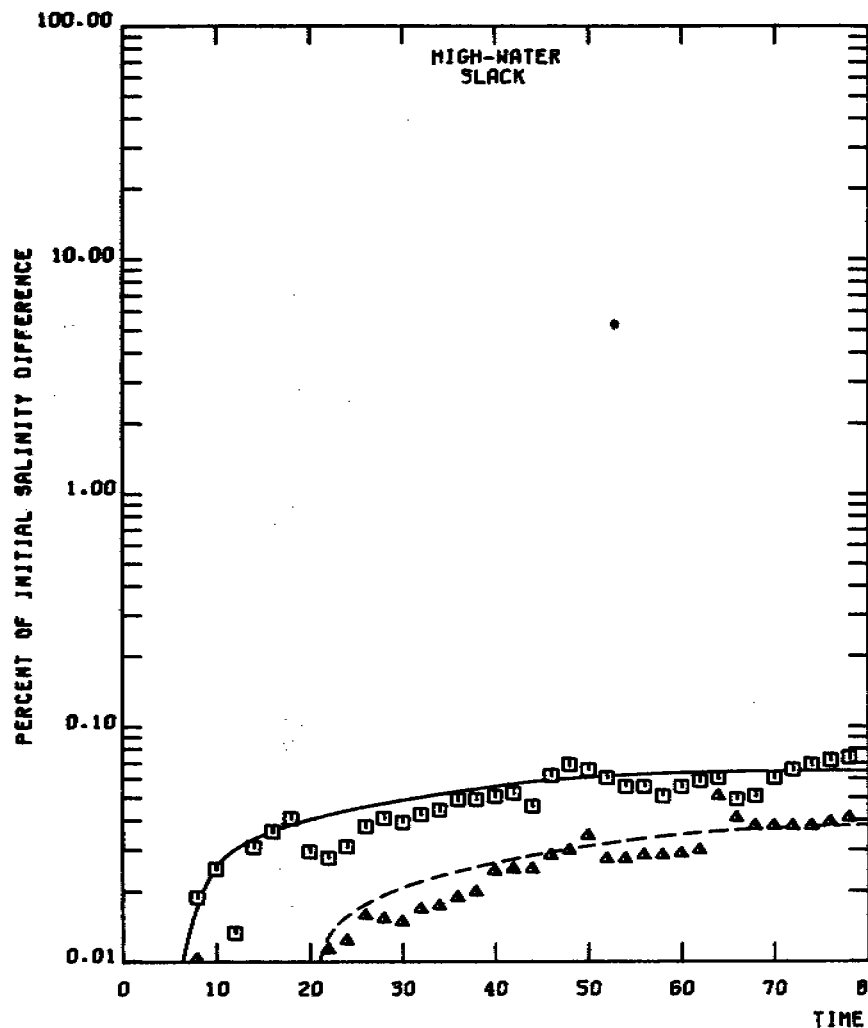
TEST CONDITIONS

FRESH-WATER DISCHARGE	11329 CFS
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ - - -	BOTTOM

GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION C2

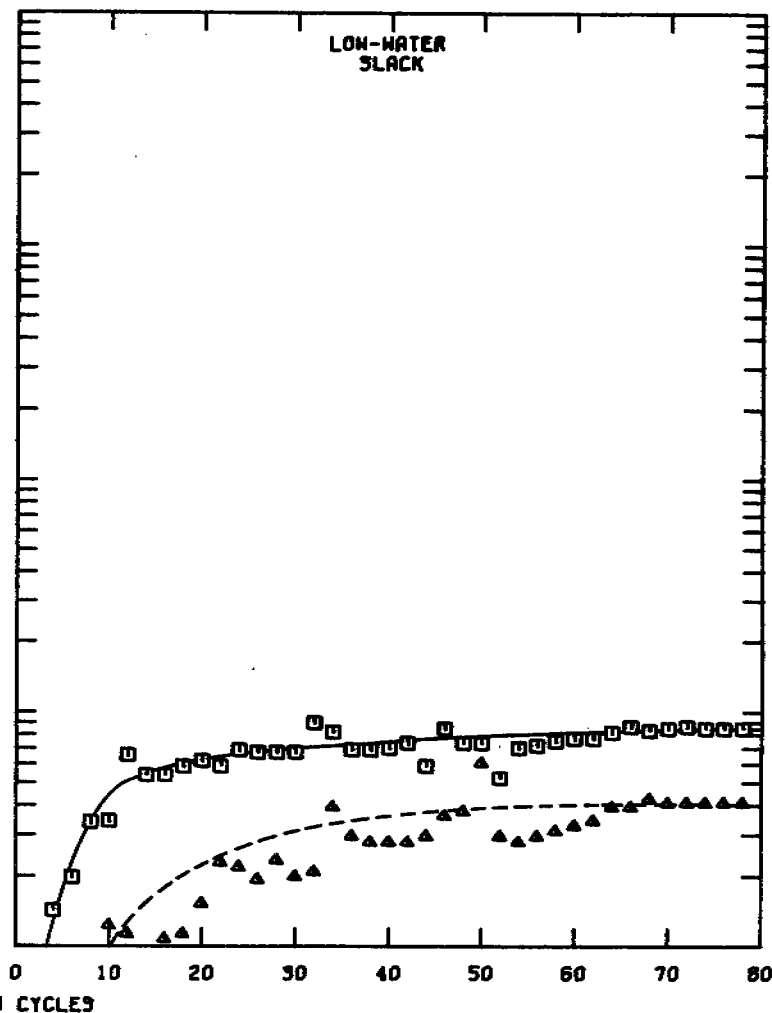
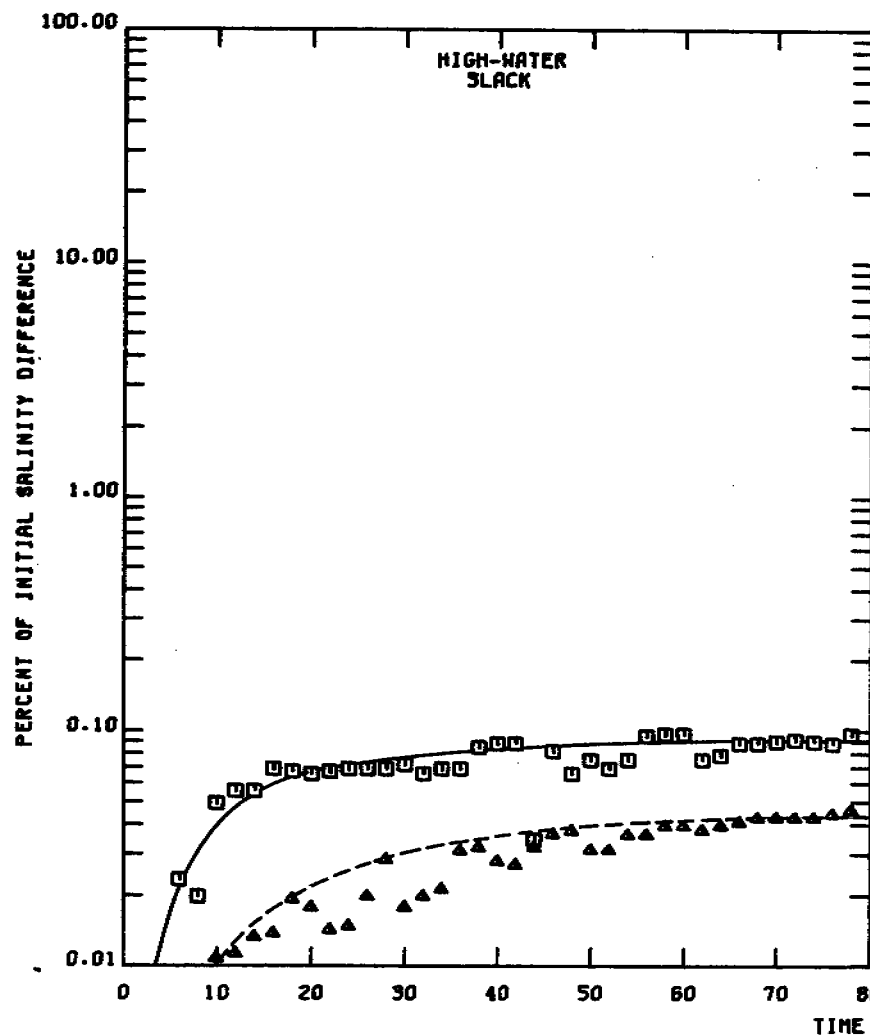


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C3

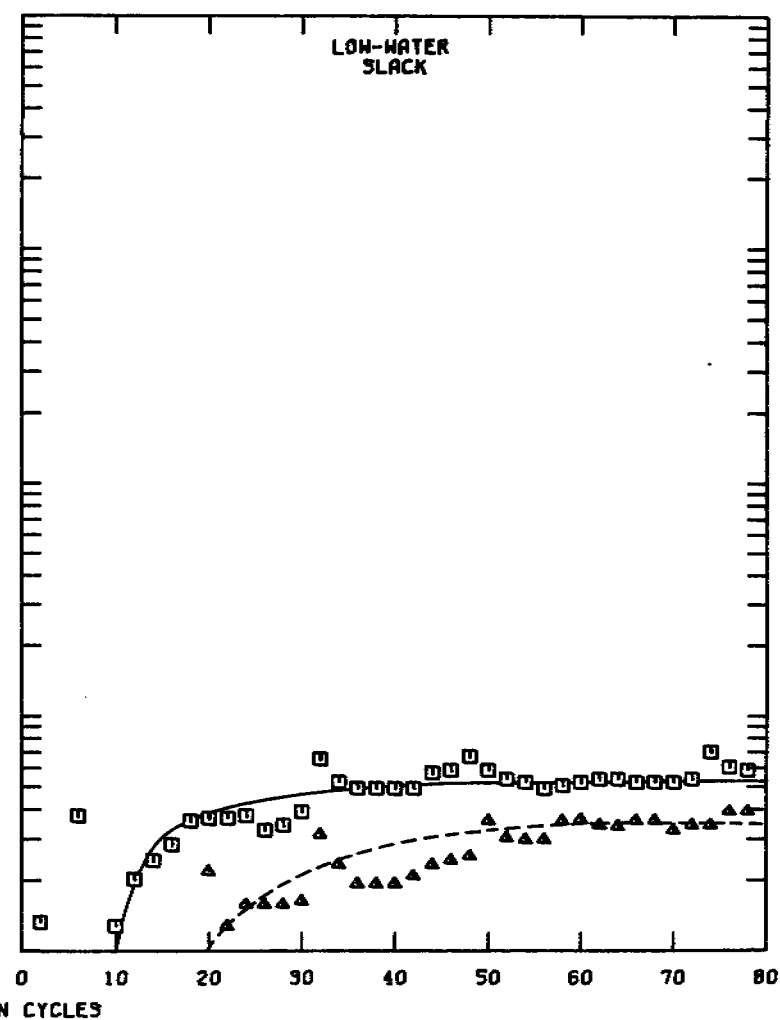
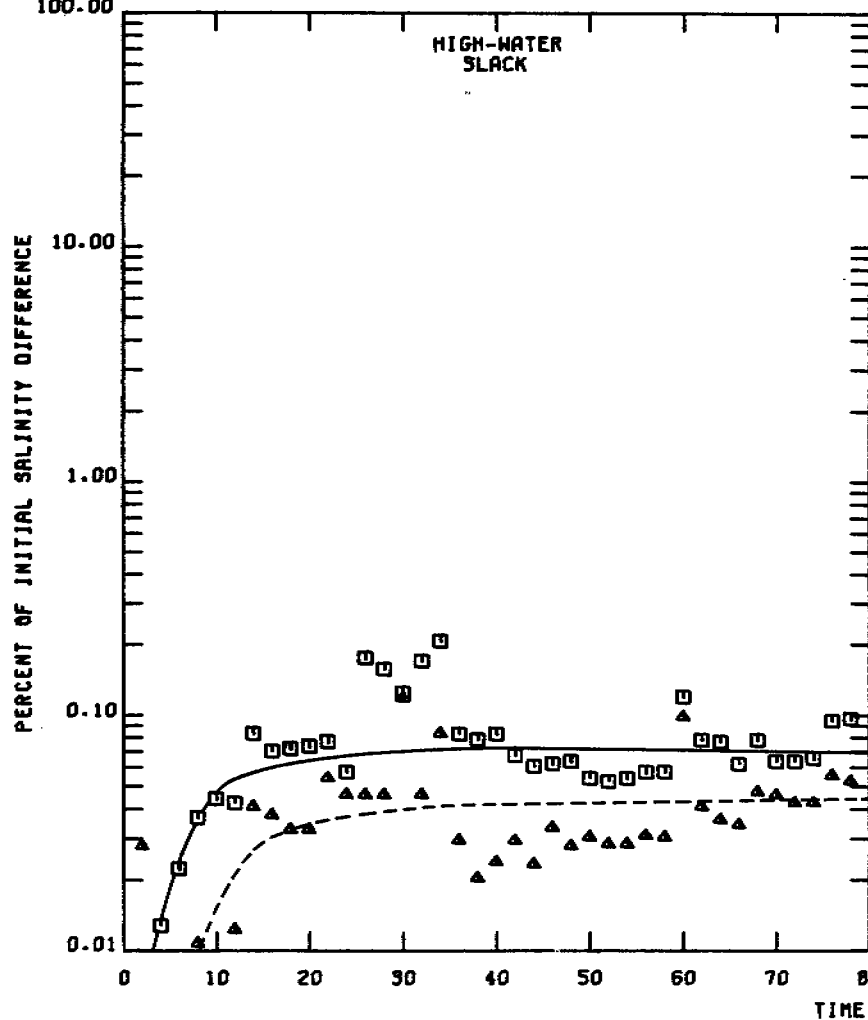


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11329 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C4



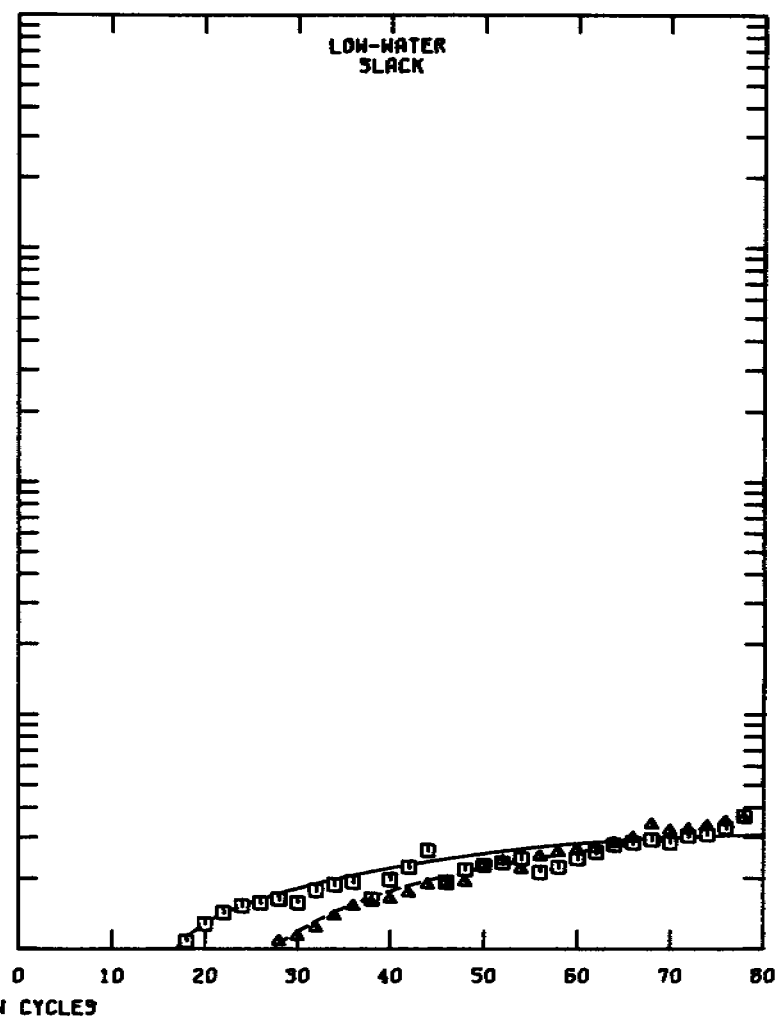
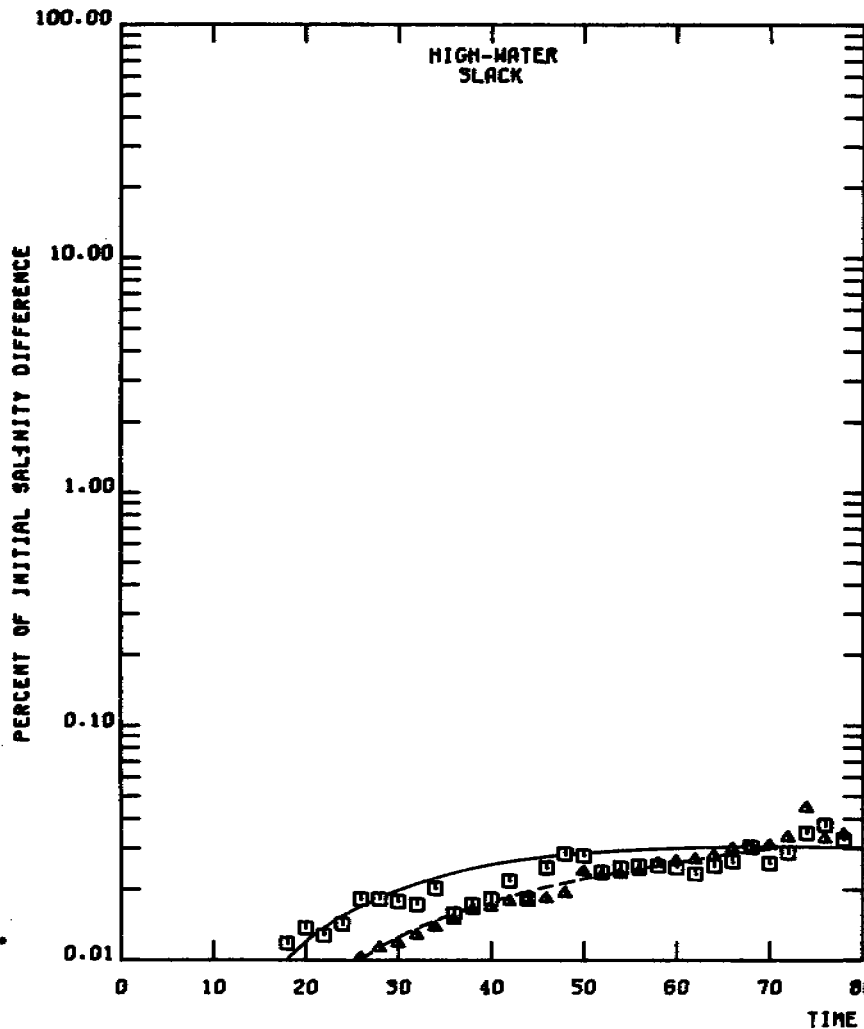
TEST CONDITIONS

FRESH-WATER DISCHARGE	11929 CF3
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ — — —	BOTTOM

GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION C5



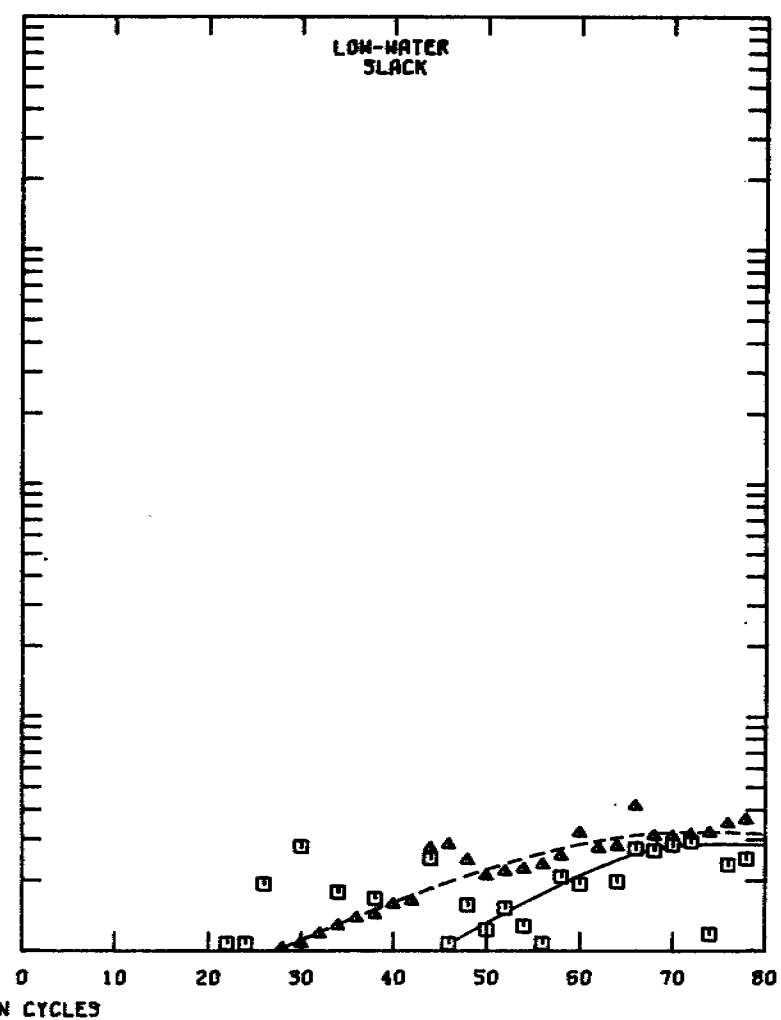
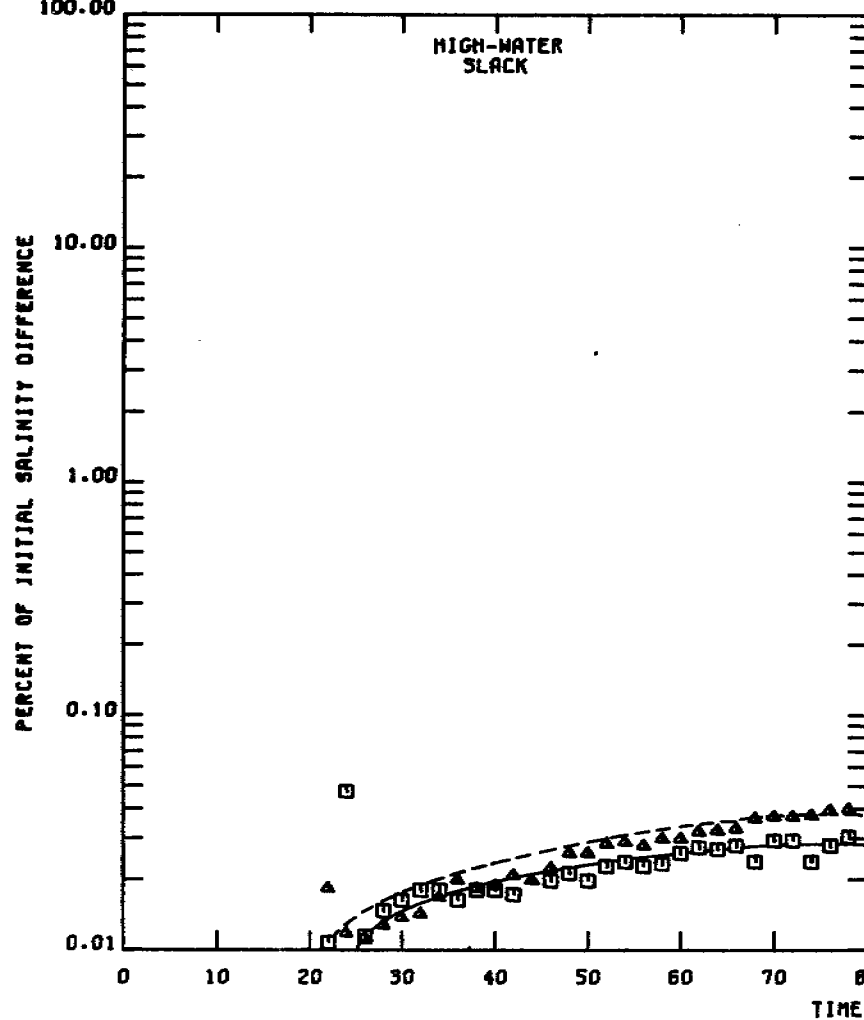
TEST CONDITIONS

FRESH-WATER DISCHARGE	11323 CF3
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ - - -	BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C6



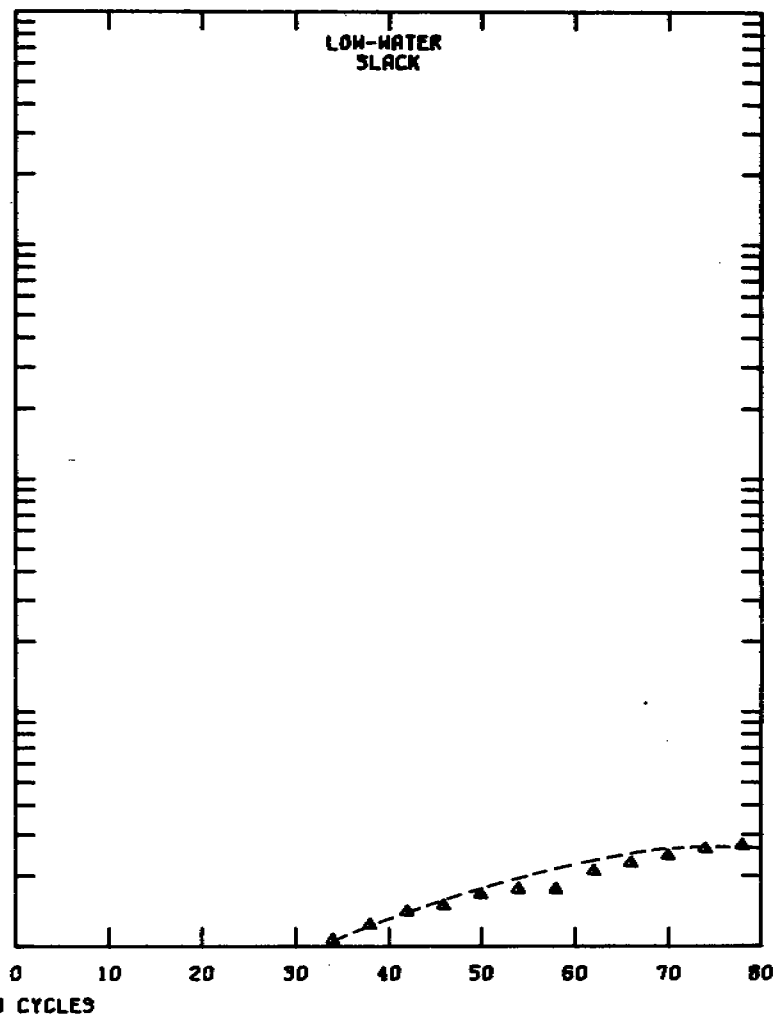
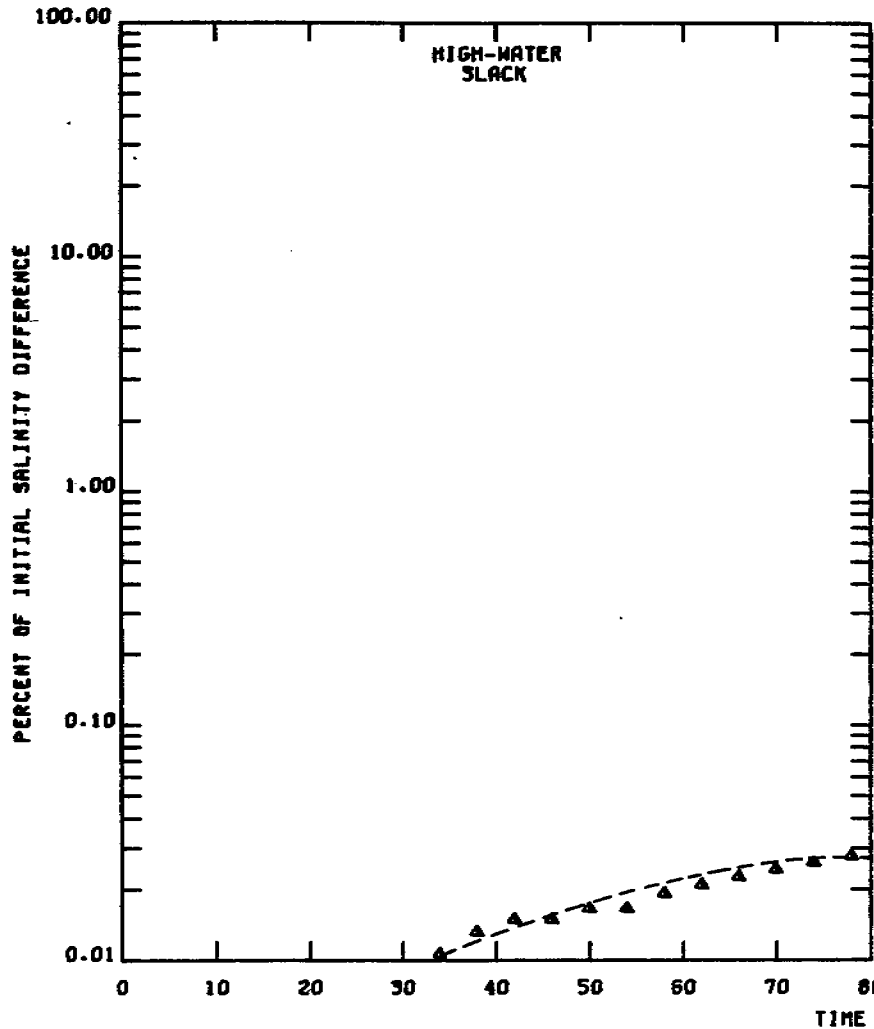
TEST CONDITIONS

FRESH-WATER DISCHARGE	11323 CF3
BASE SALINITY AT DIFFUSER	19.6 PPT
EFFLUENT SALINITY	31.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ — — —	BOTTOM

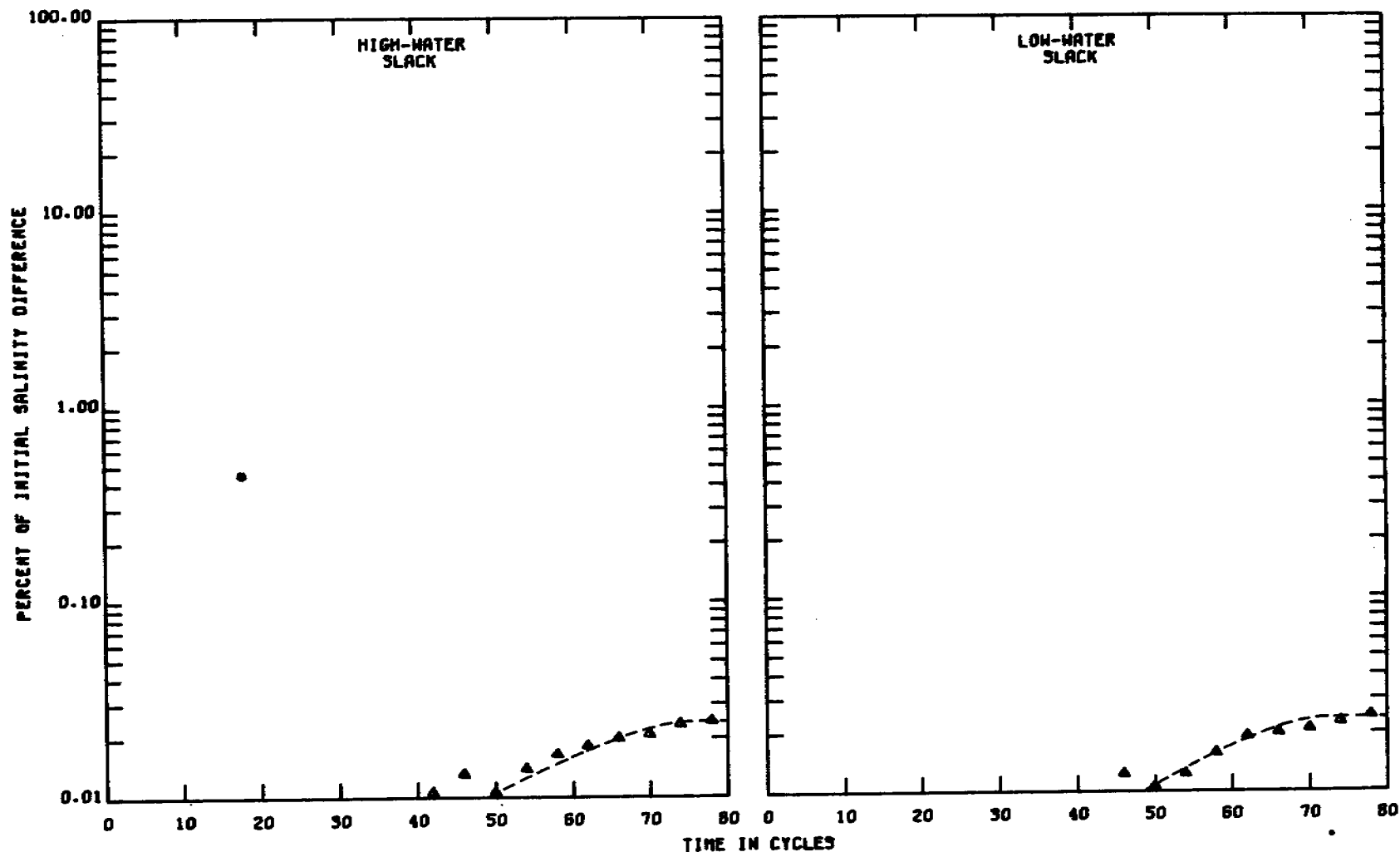
GALVESTON BAY MODEL
SALINE WATER
DISPERSION TEST
10 MGD PLANT
STATION C7



TEST CONDITIONS
 FRESH-WATER DISCHARGE 11929 CF3
 BASE SALINITY AT DIFFUSER 19.6 PPT
 EFFLUENT SALINITY 31.0 PPT
 INITIAL SALINITY DIFFERENCE 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

**GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C8**

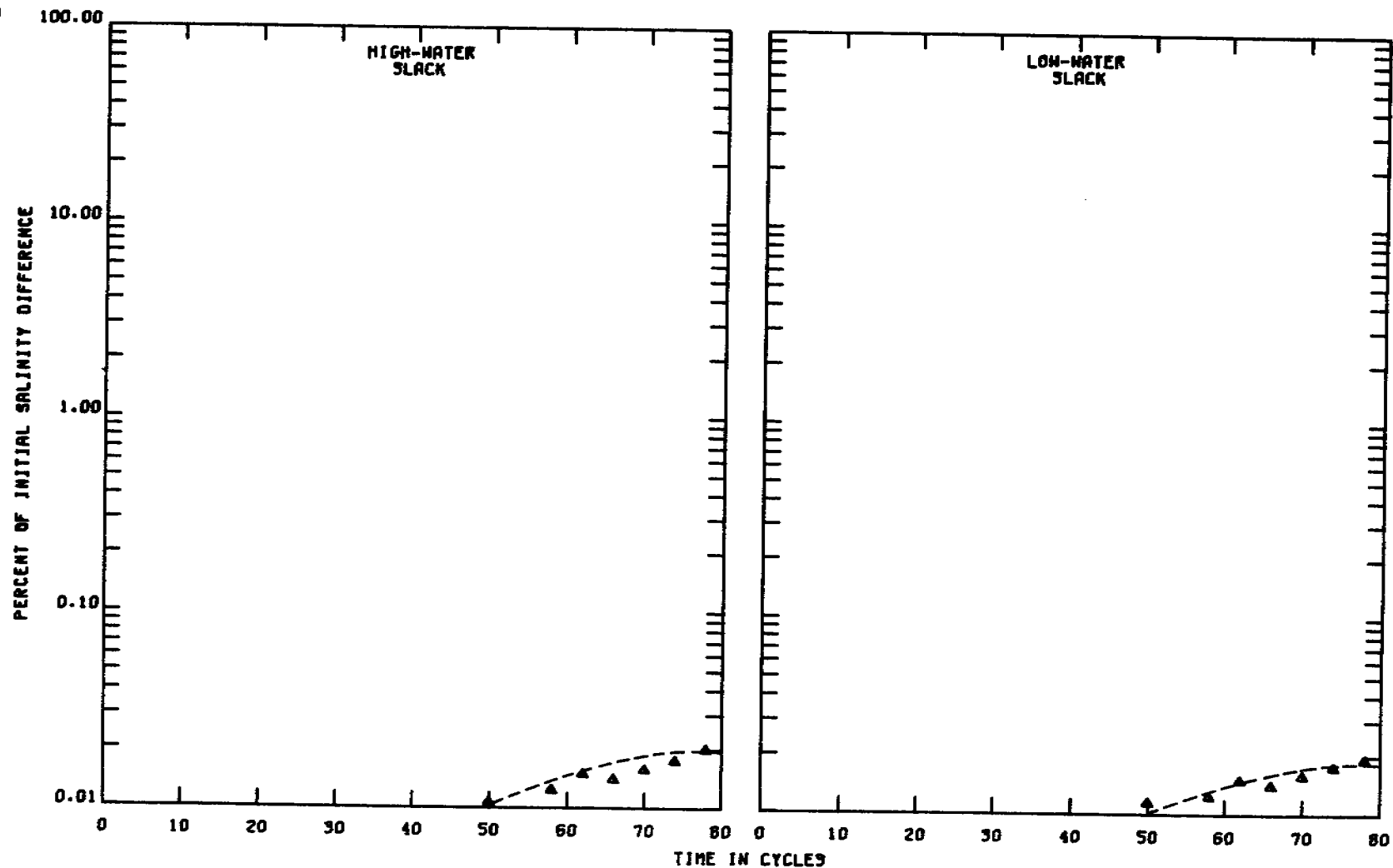


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 91.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C9

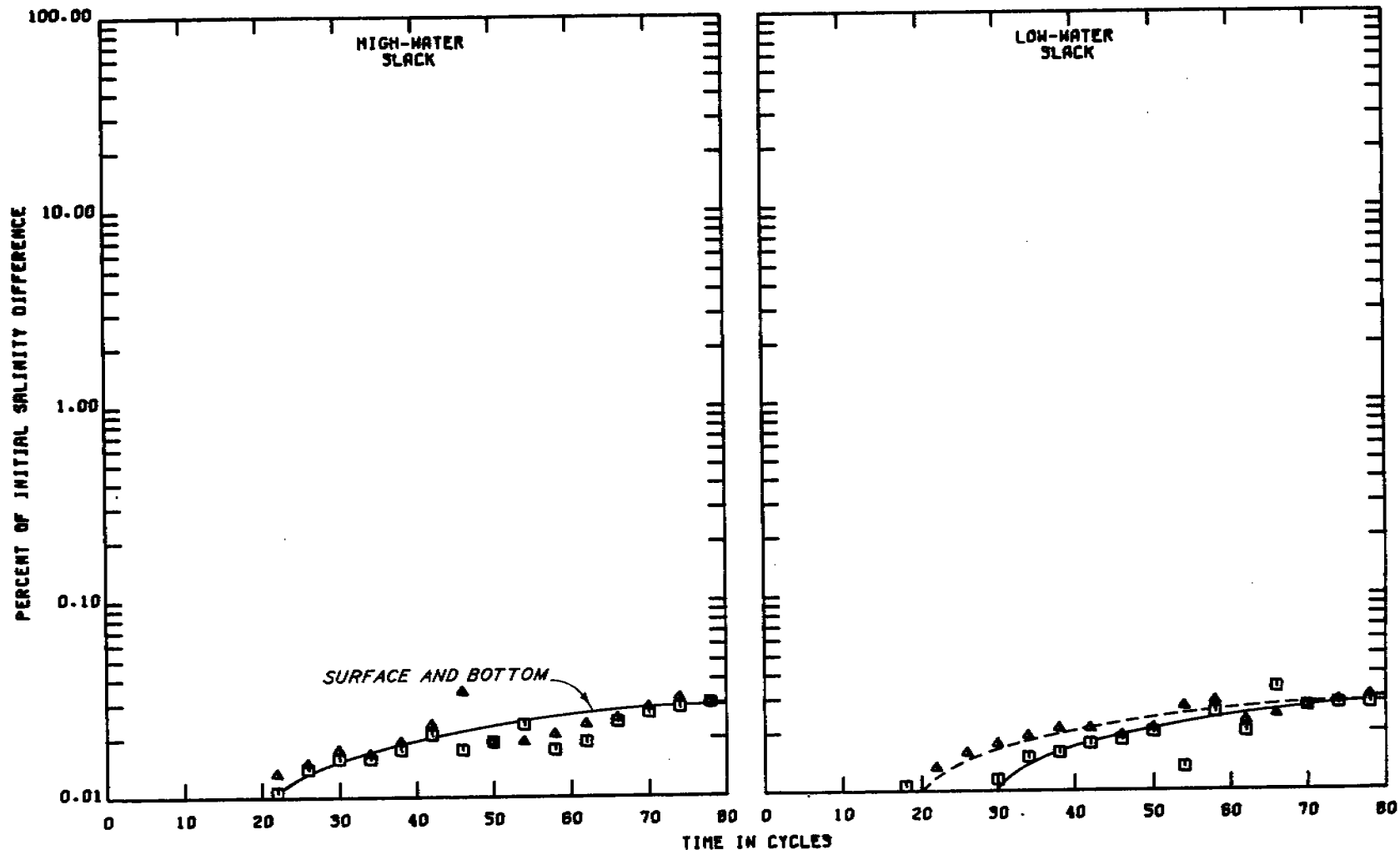


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION C10

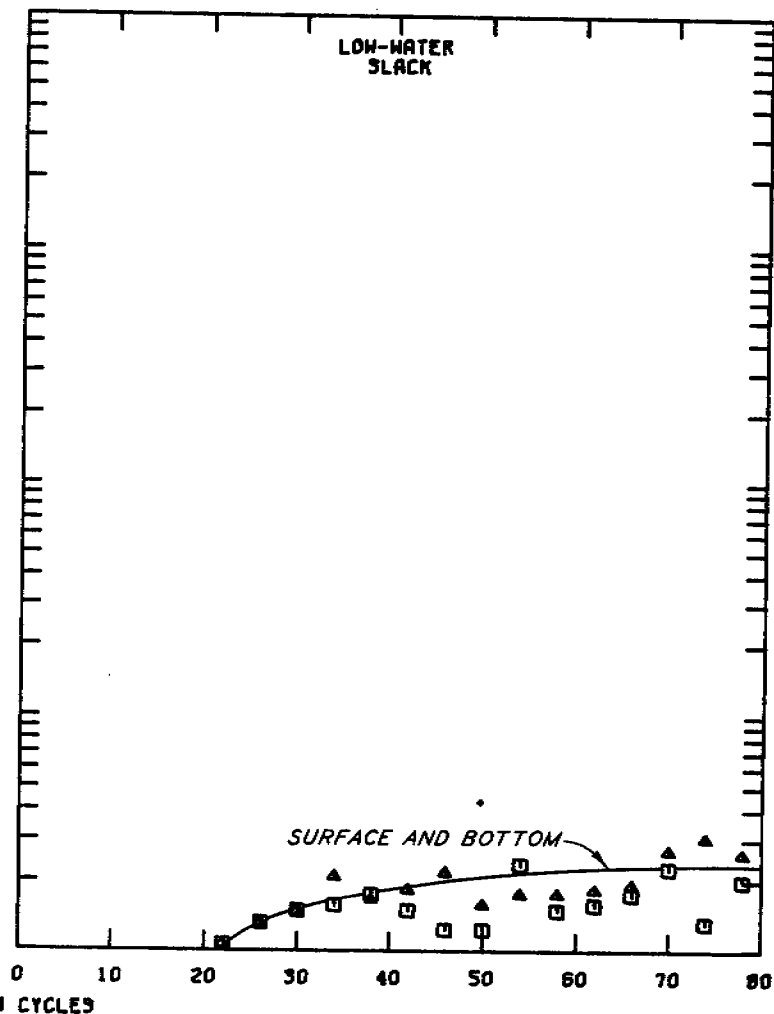
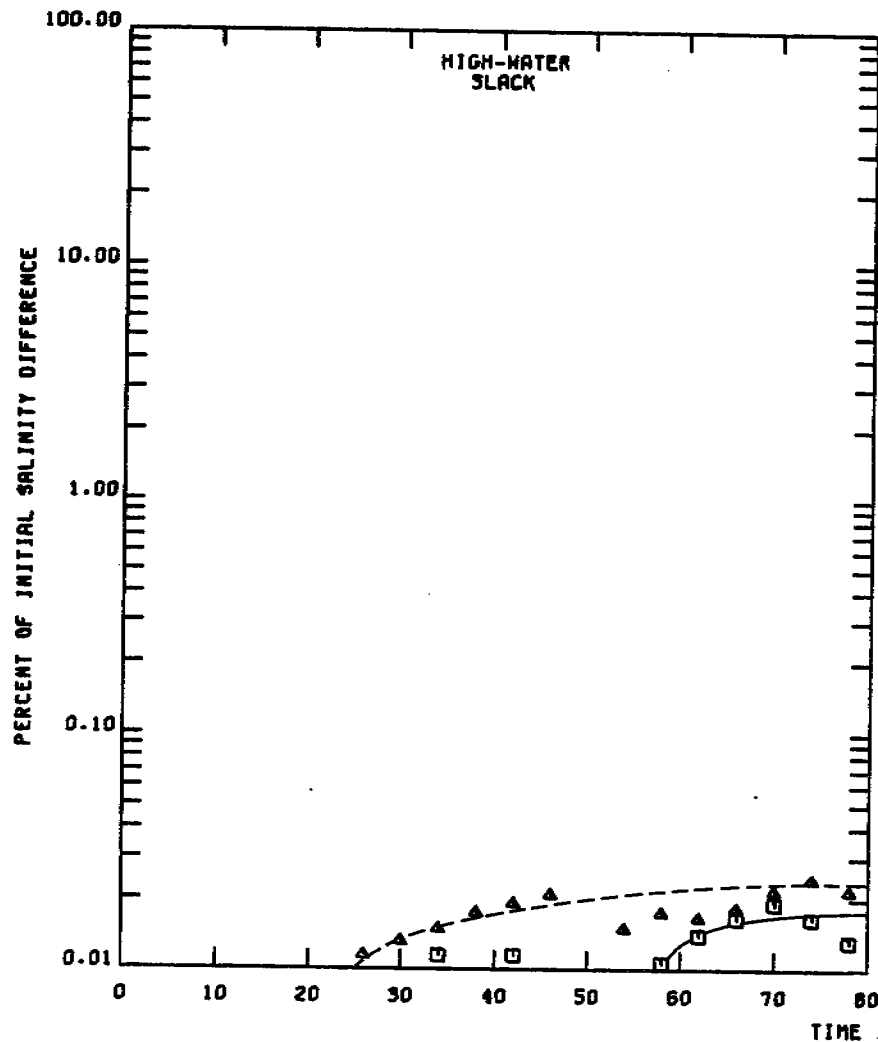


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.8 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ — — — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION T02



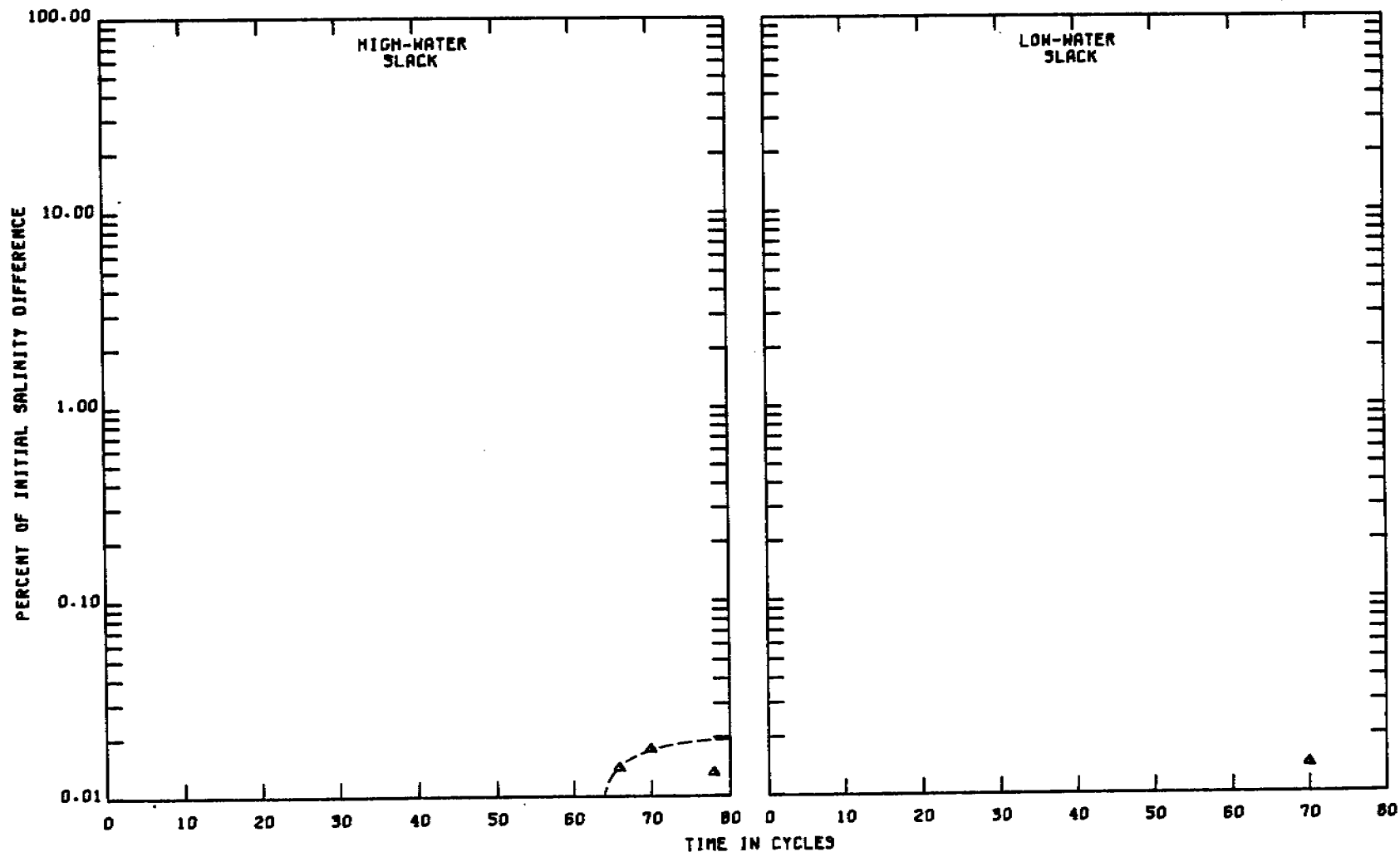
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 91.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION T83

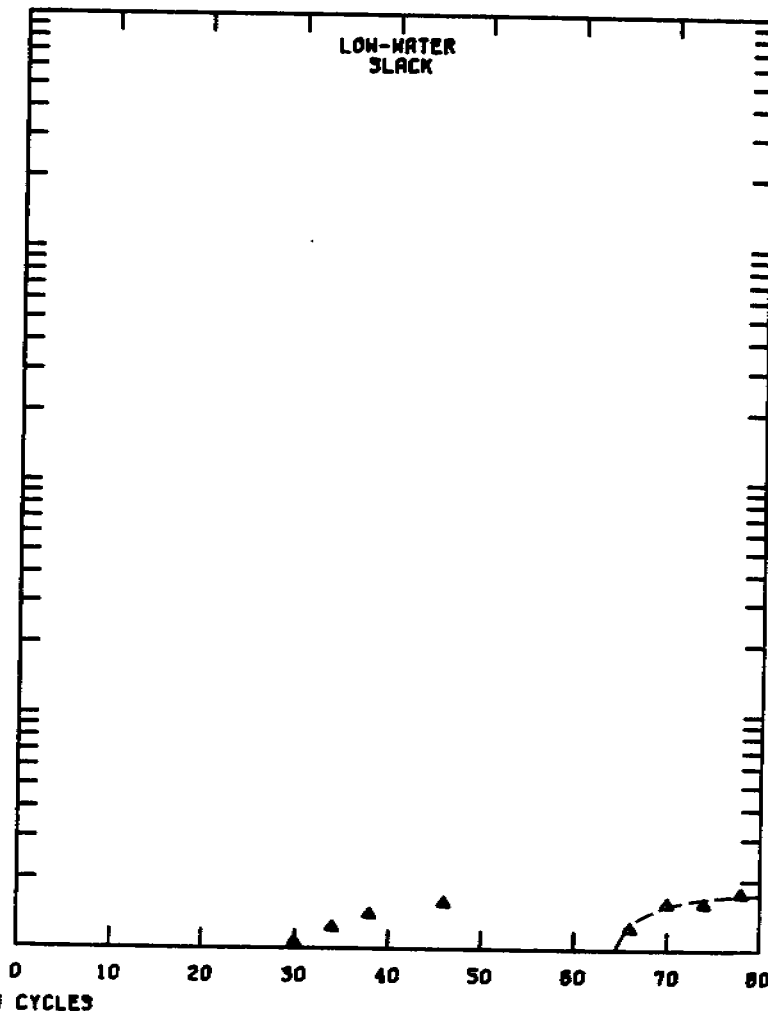
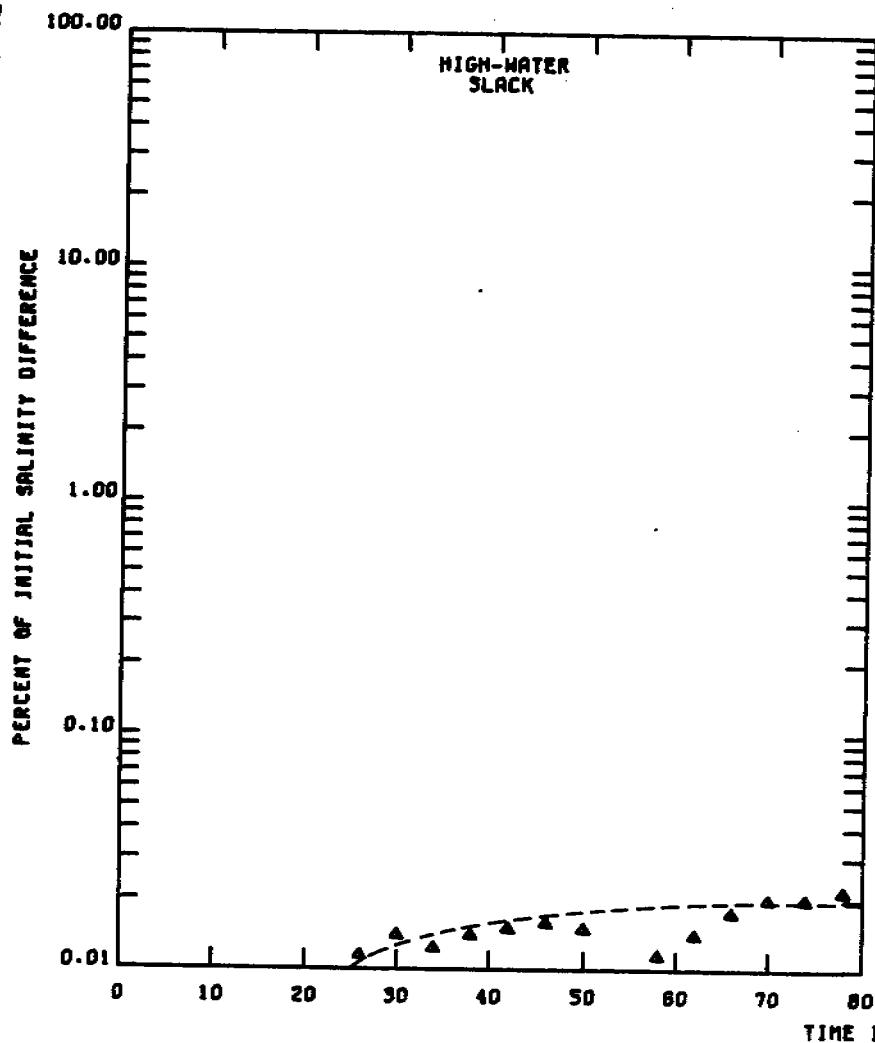


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ — — — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION T84

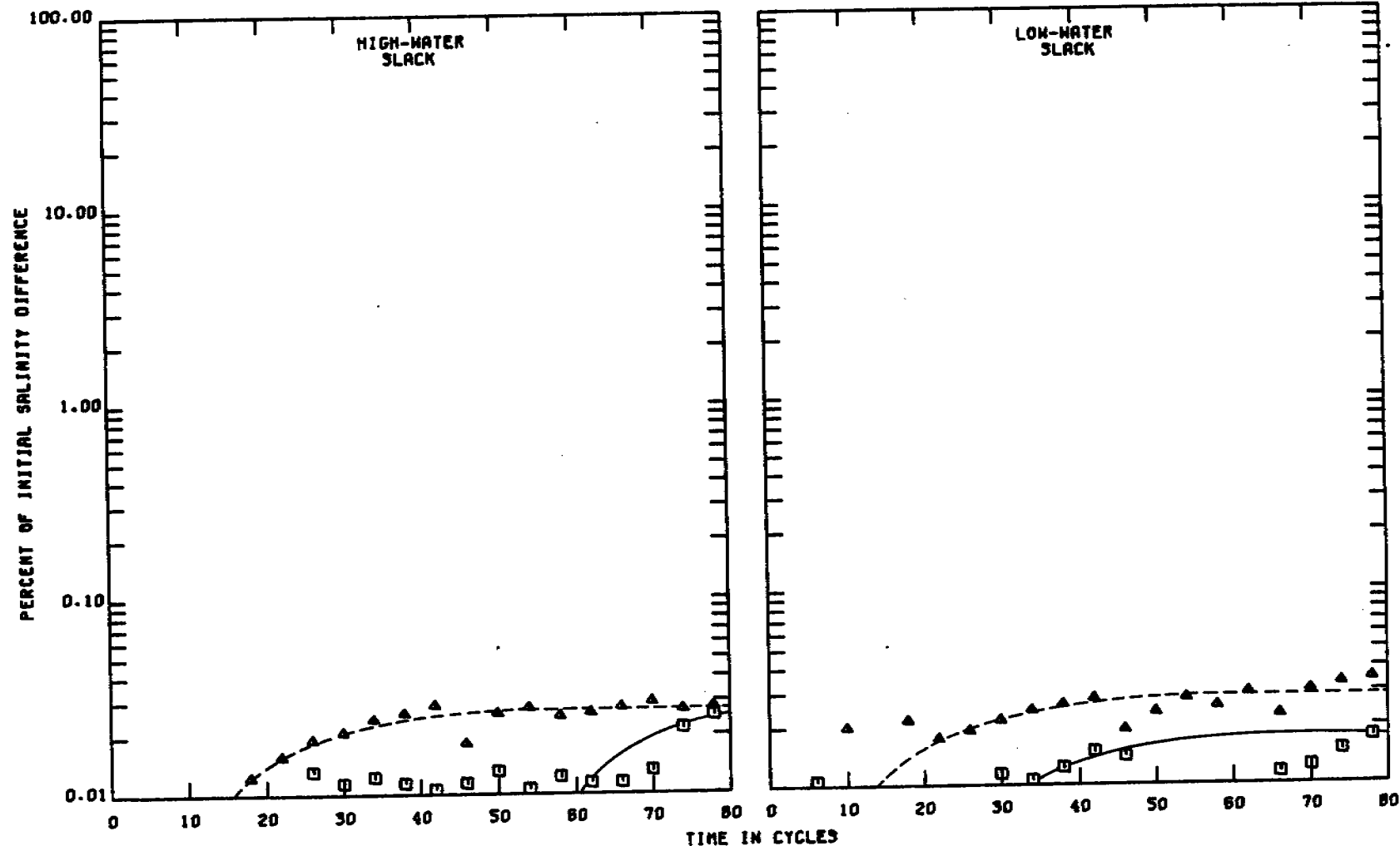


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11929 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 ○ ——— SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION T05

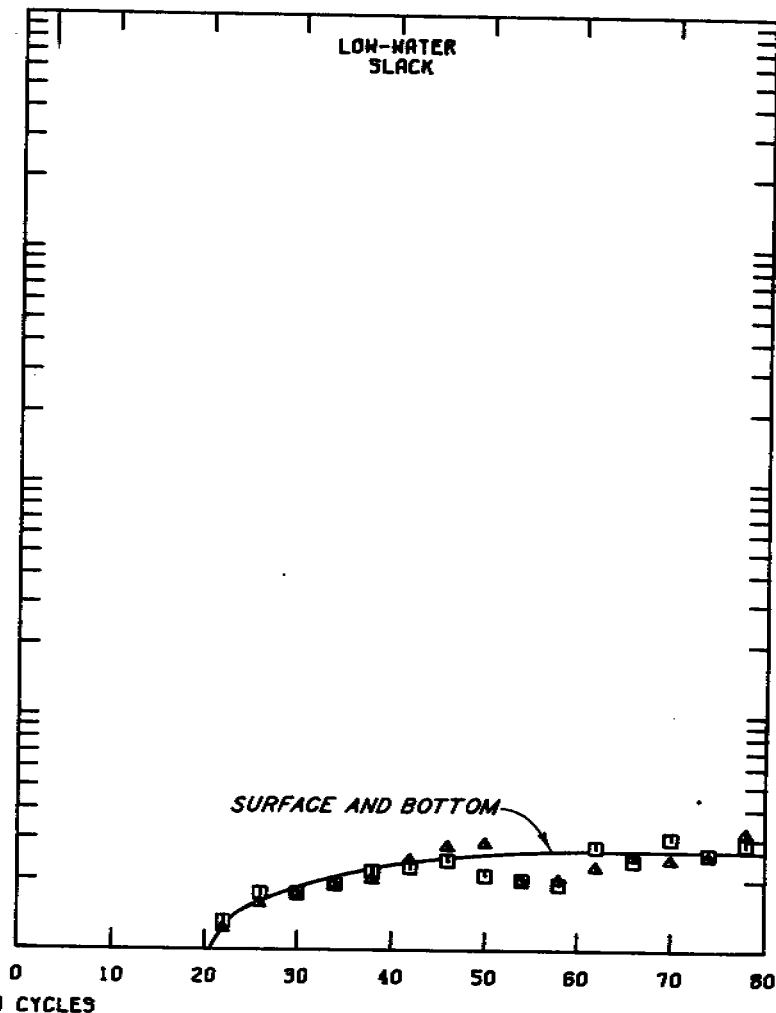
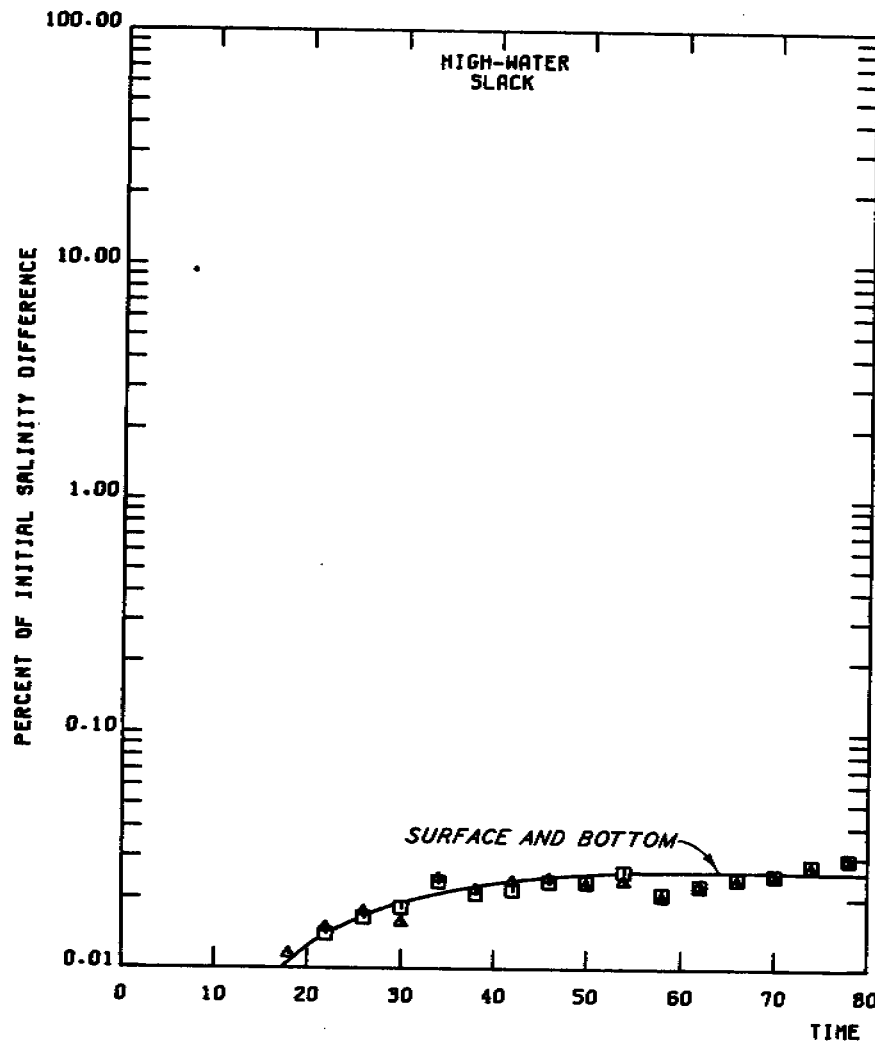


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION T86



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

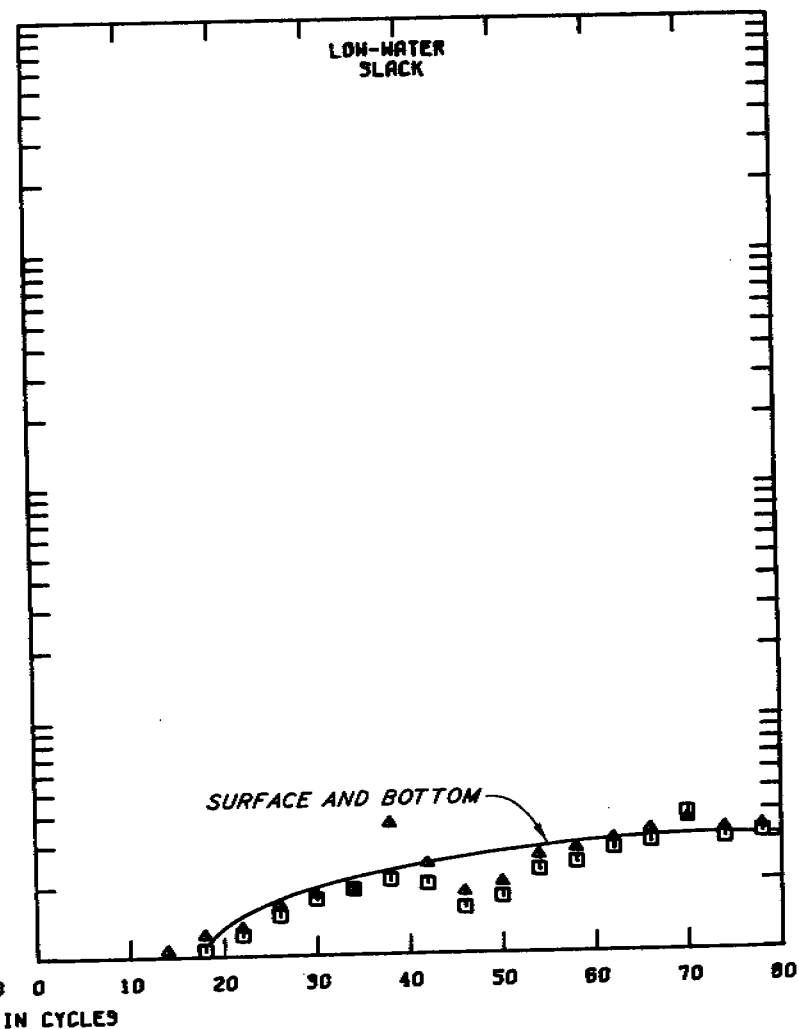
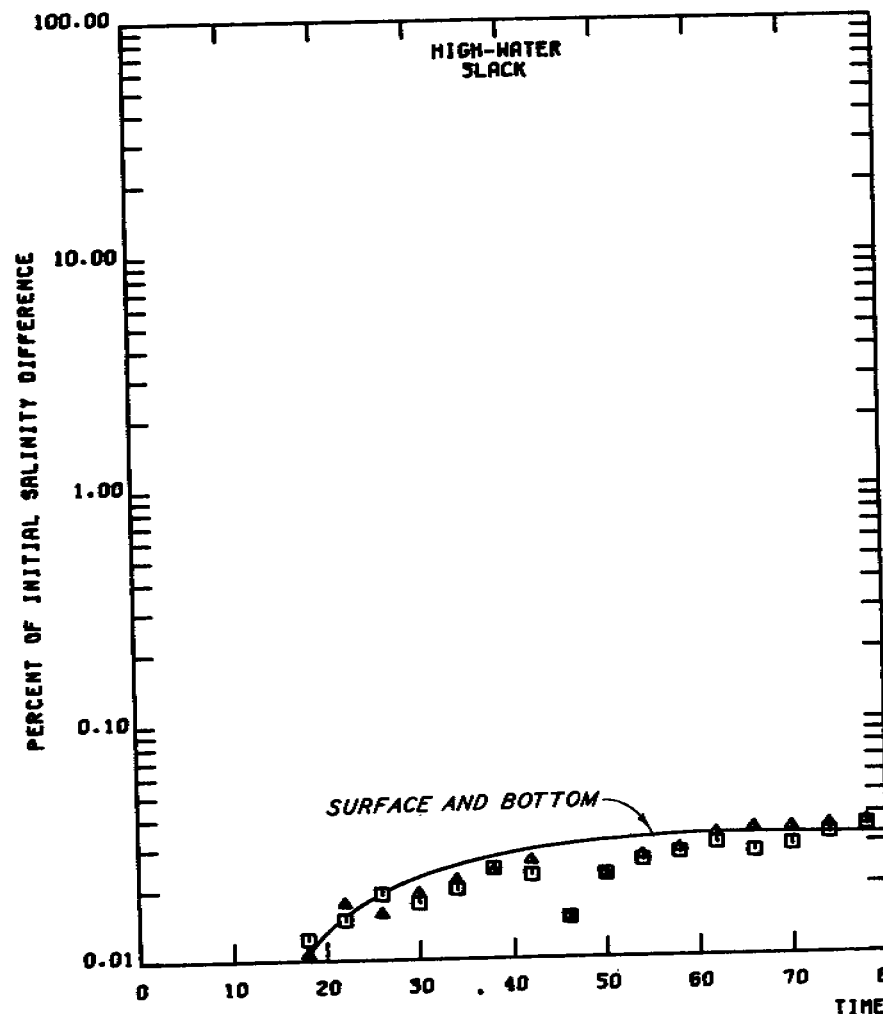
11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ — SURFACE
 ▲ - - - BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT

STATION M33

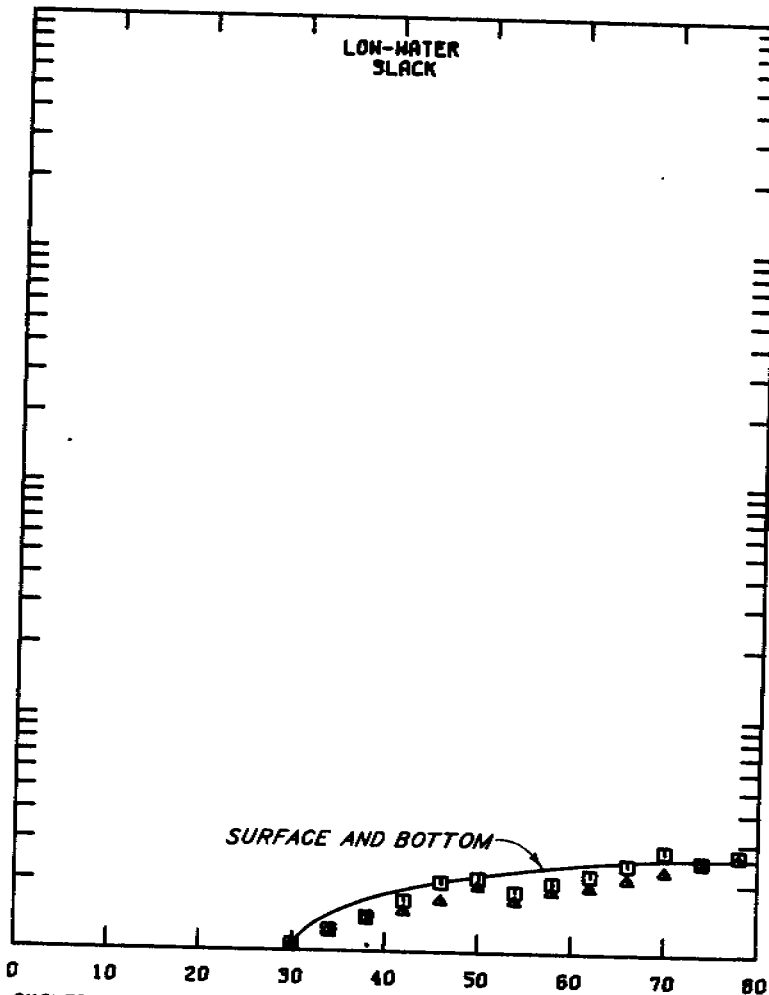
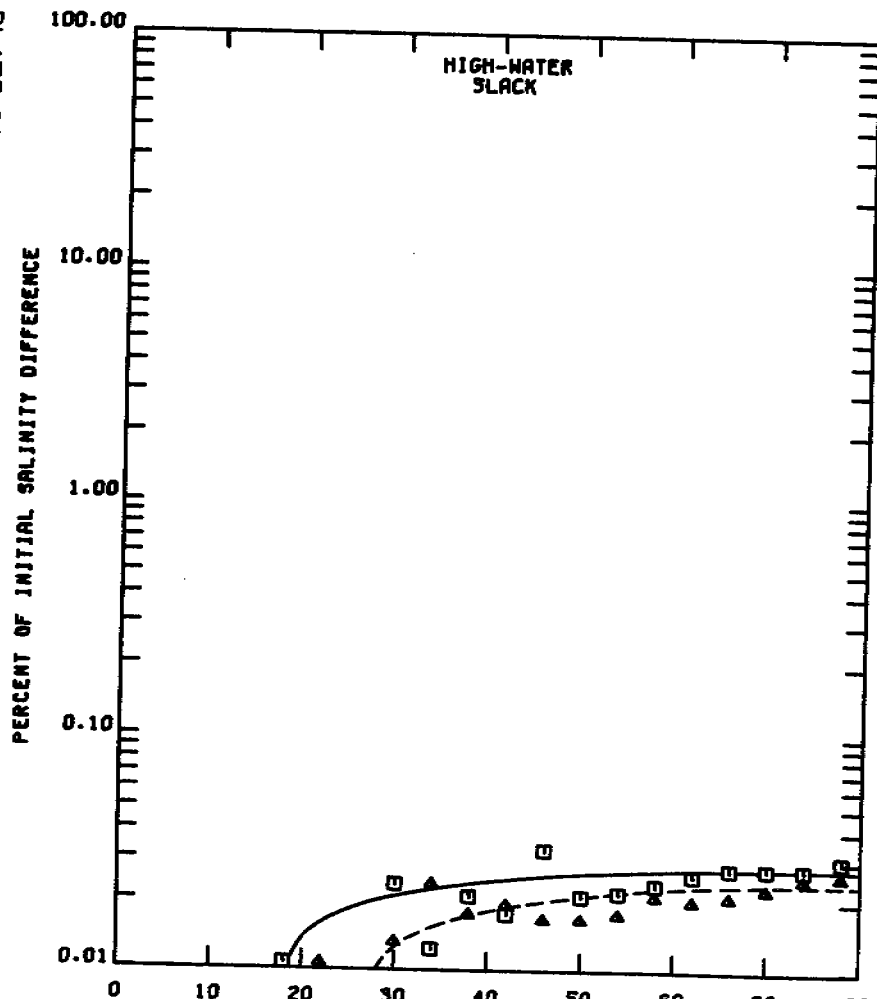


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11323 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ — BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION E01

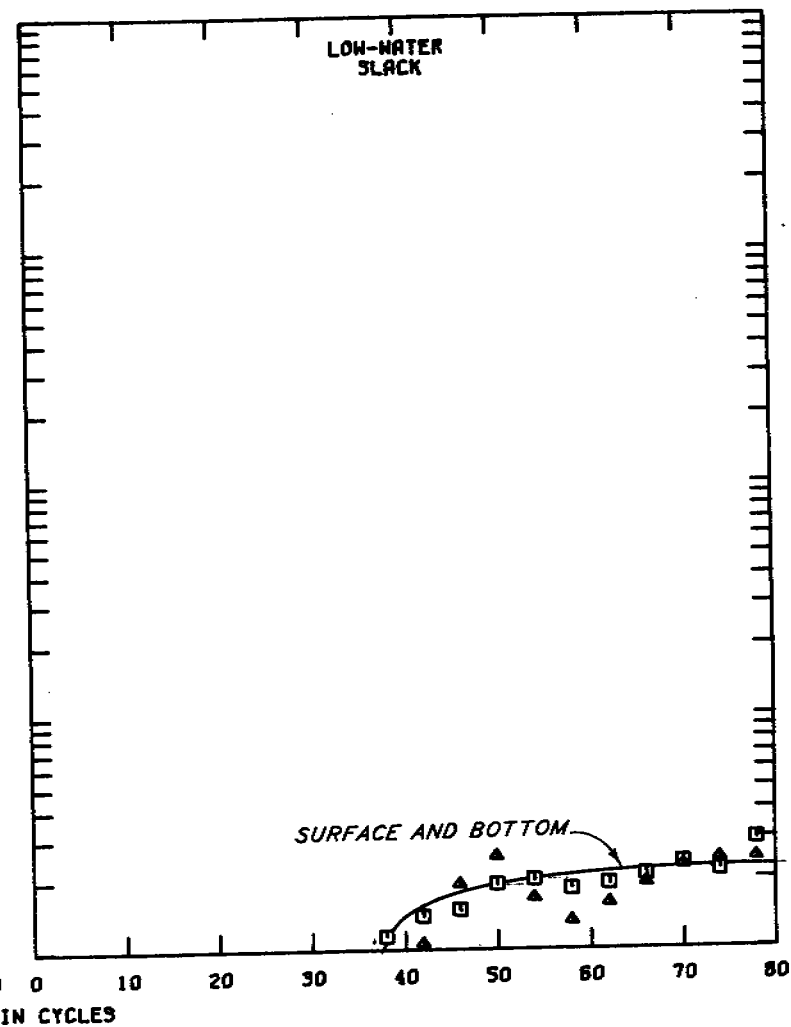
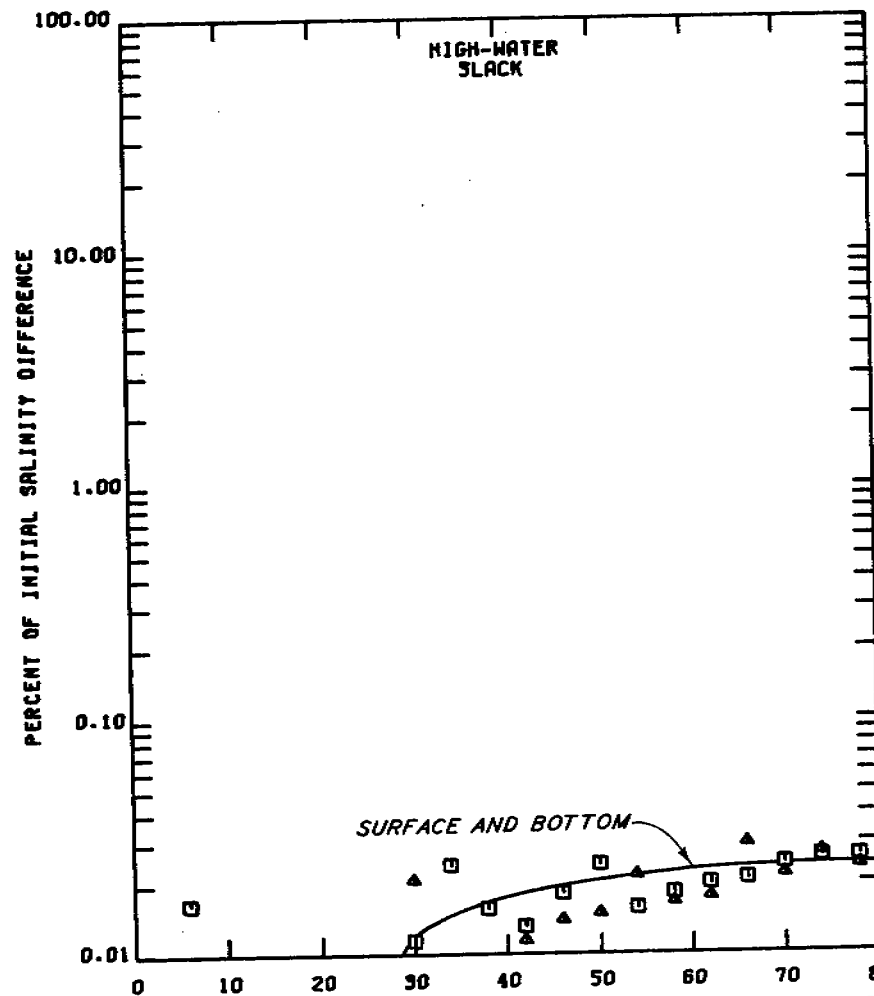


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

11923 CFS
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION E82

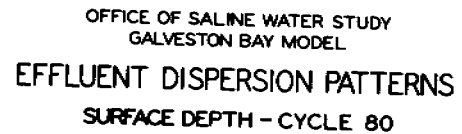


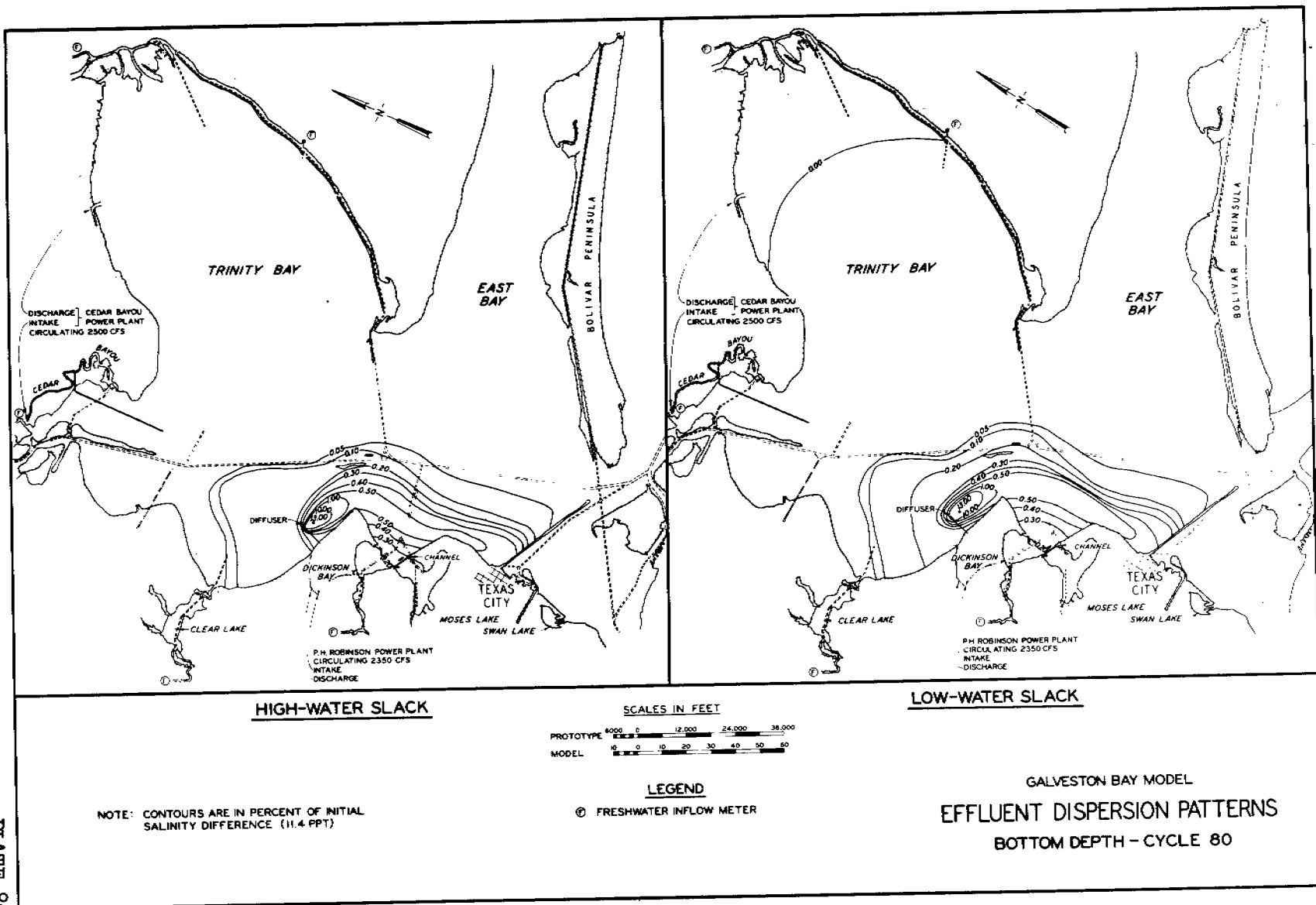
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

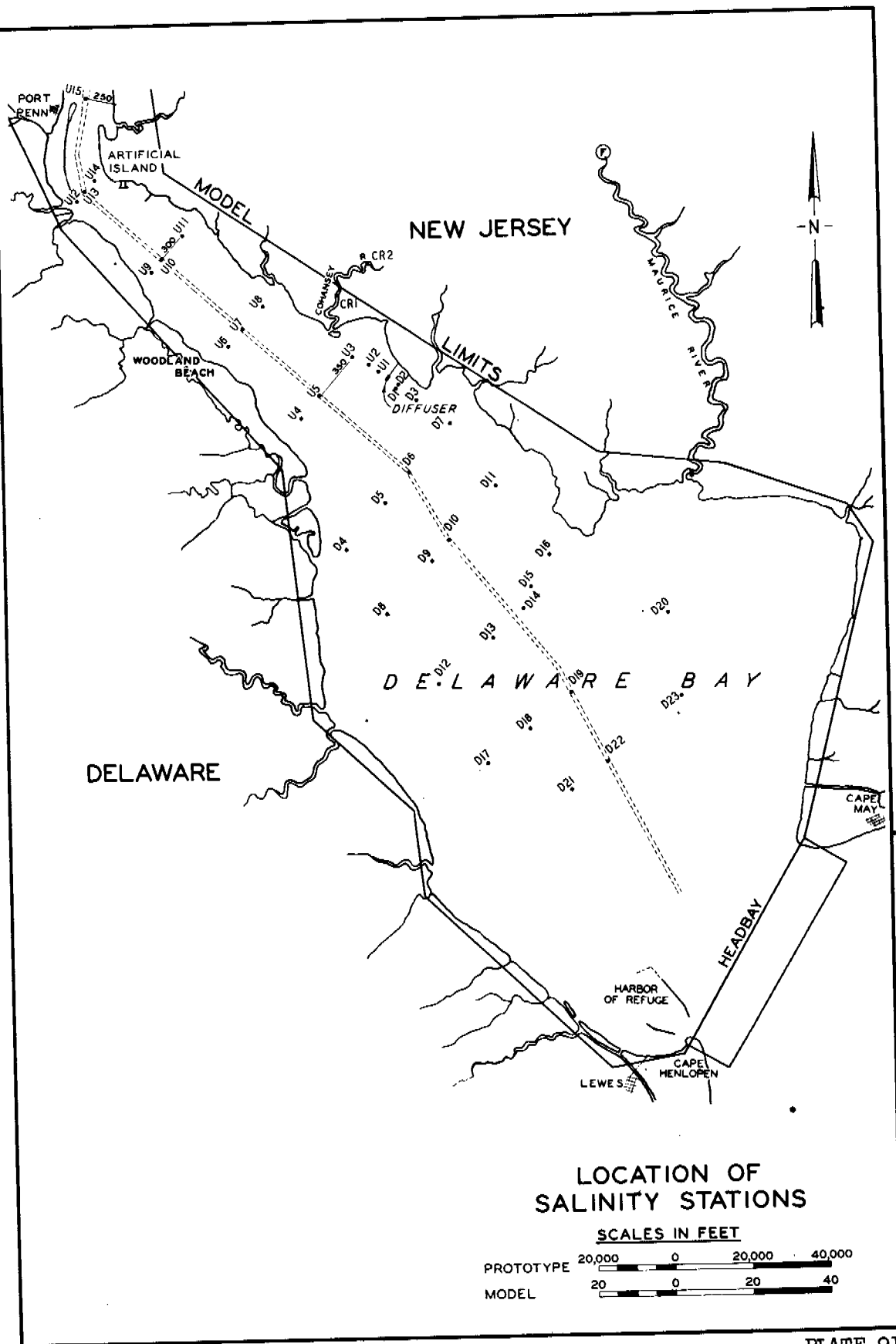
11529 CF3
 19.6 PPT
 31.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

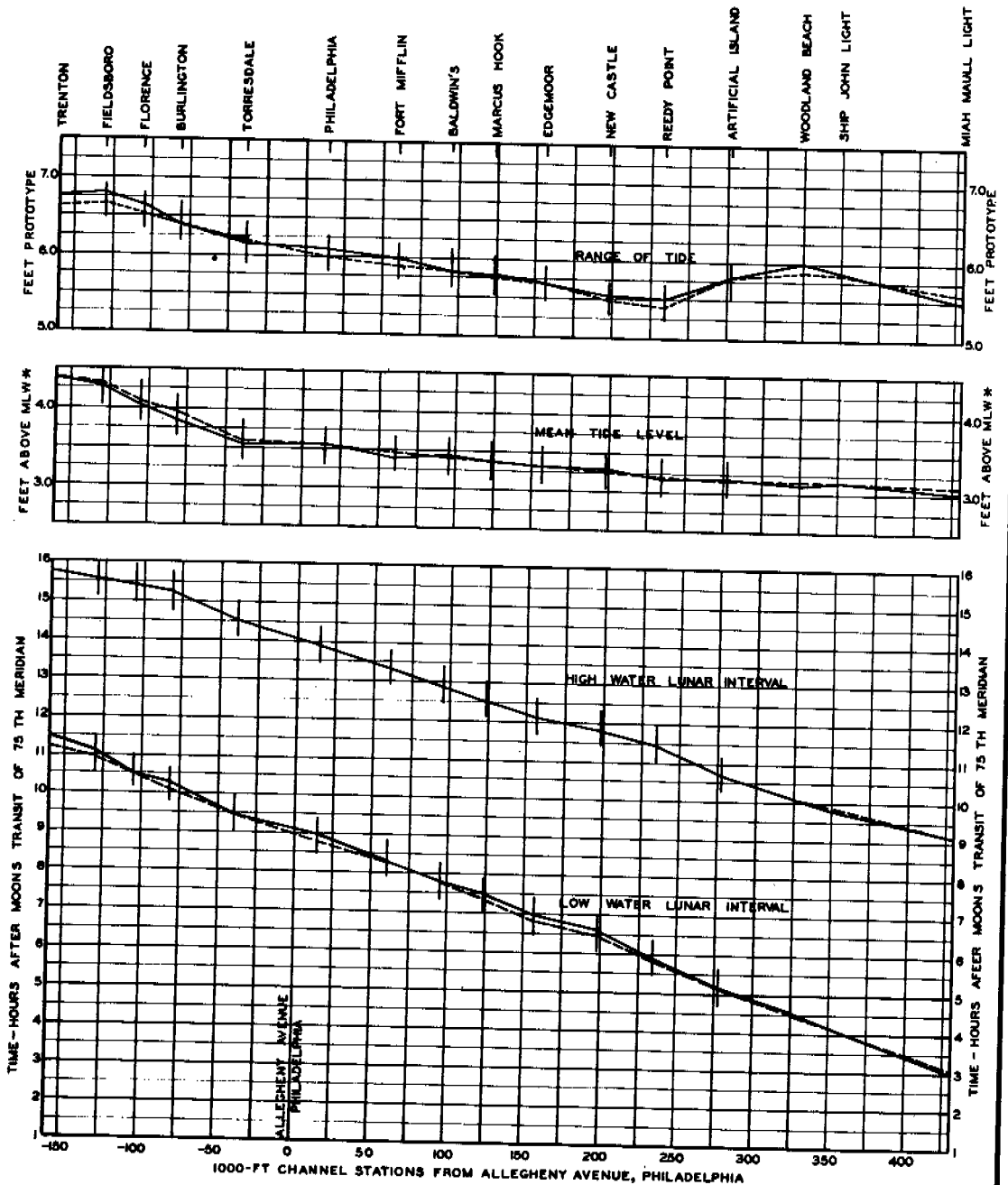
GALVESTON BAY MODEL
 SALINE WATER
 DISPERSION TEST
 10 MGD PLANT
 STATION E83







TIDE STATIONS

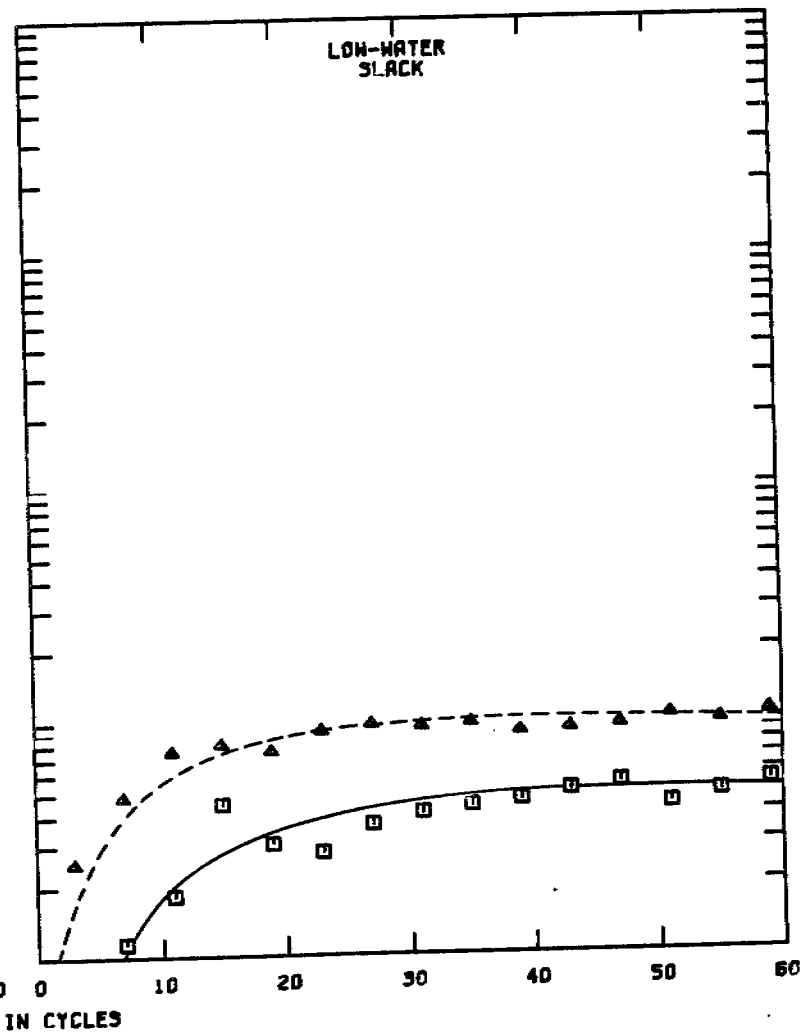
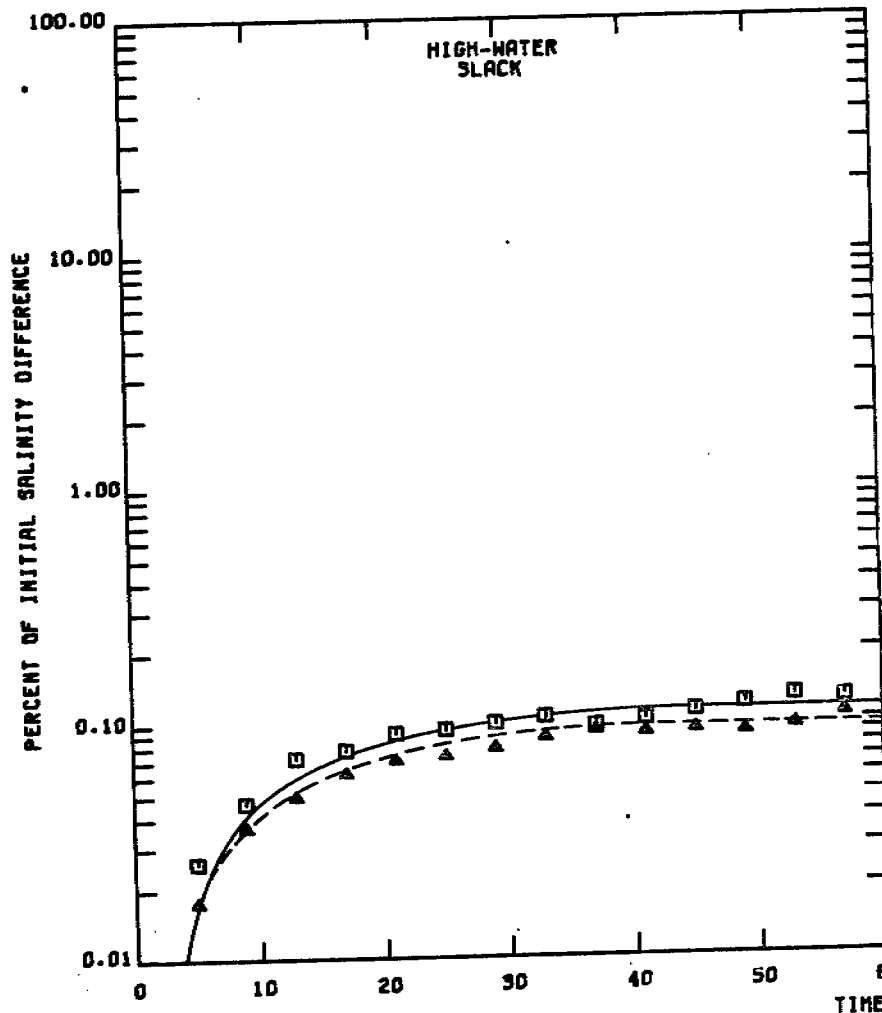


MODEL TEST DATA
 TIDE MEAN
 FRESH WATER DISCHARGE 20,200 CFS (MEAN AT CAPES)
 OCEAN SALINITY 31,000 PPM

LEGEND
 ——— MODEL
 - - - - - PROTOTYPE

* HEIGHTS REFER TO DELAWARE RIVER DATUM WHICH IS 2.90 FEET BELOW MEAN SEA LEVEL SANDY HOOK, 1929 ADJUSTMENT.

DELAWARE RIVER MODEL
 TIDAL OBSERVATIONS

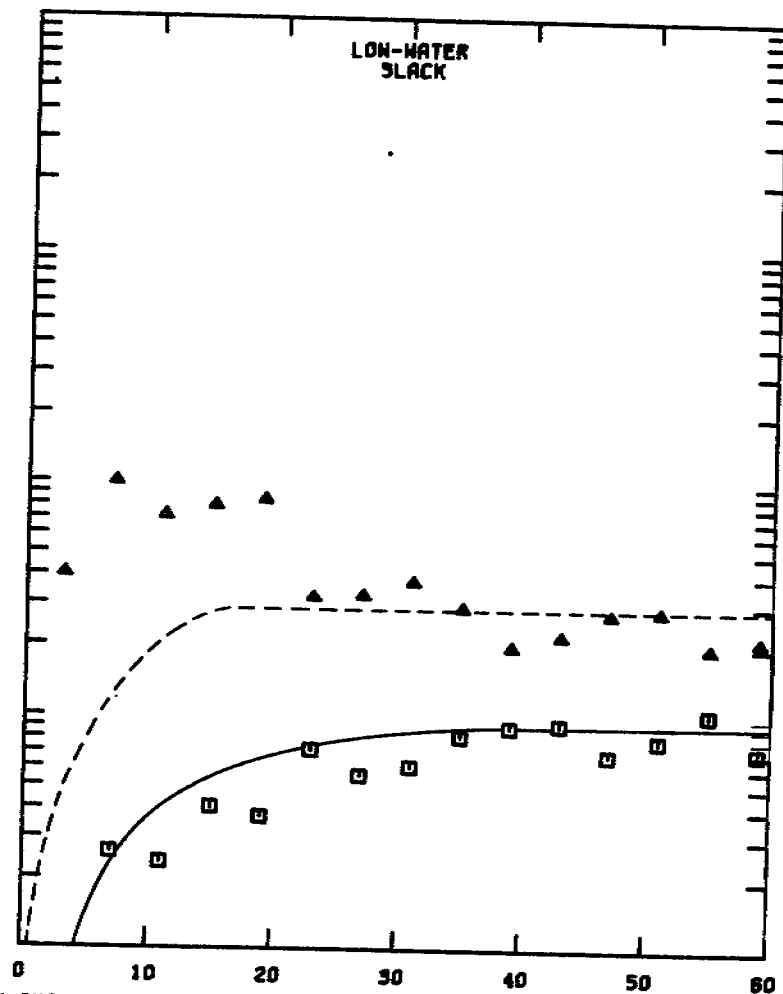
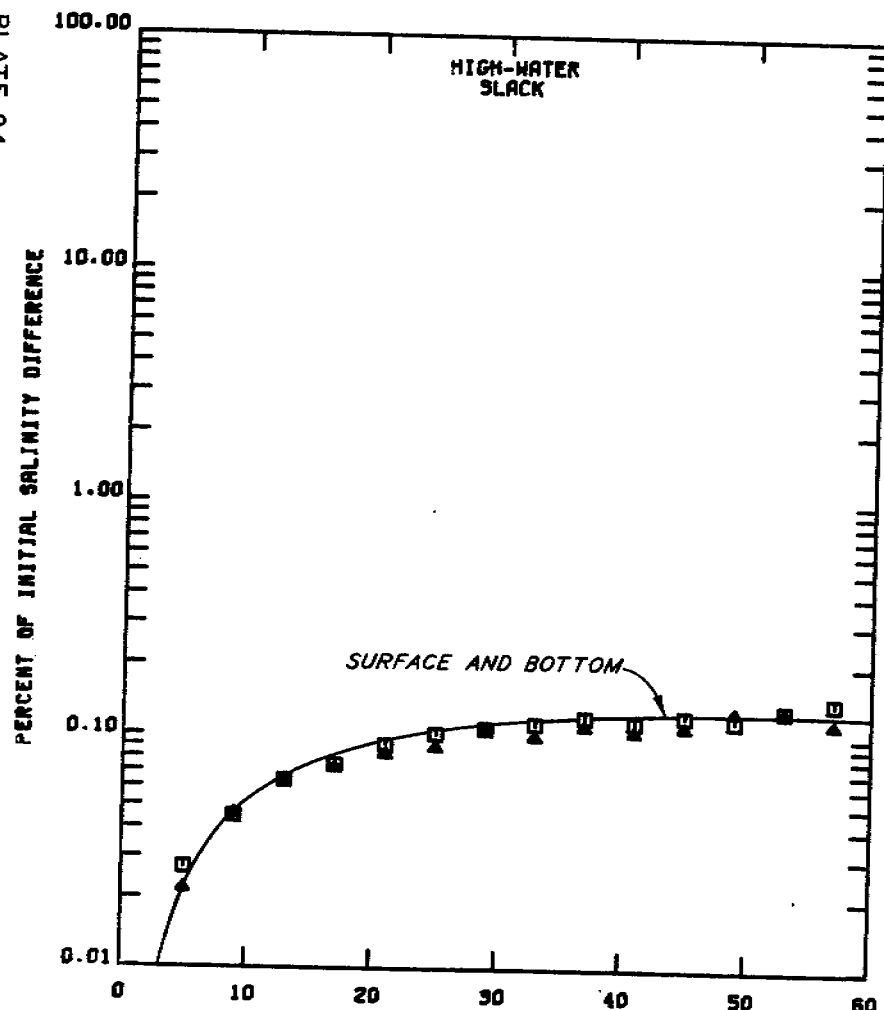


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D1

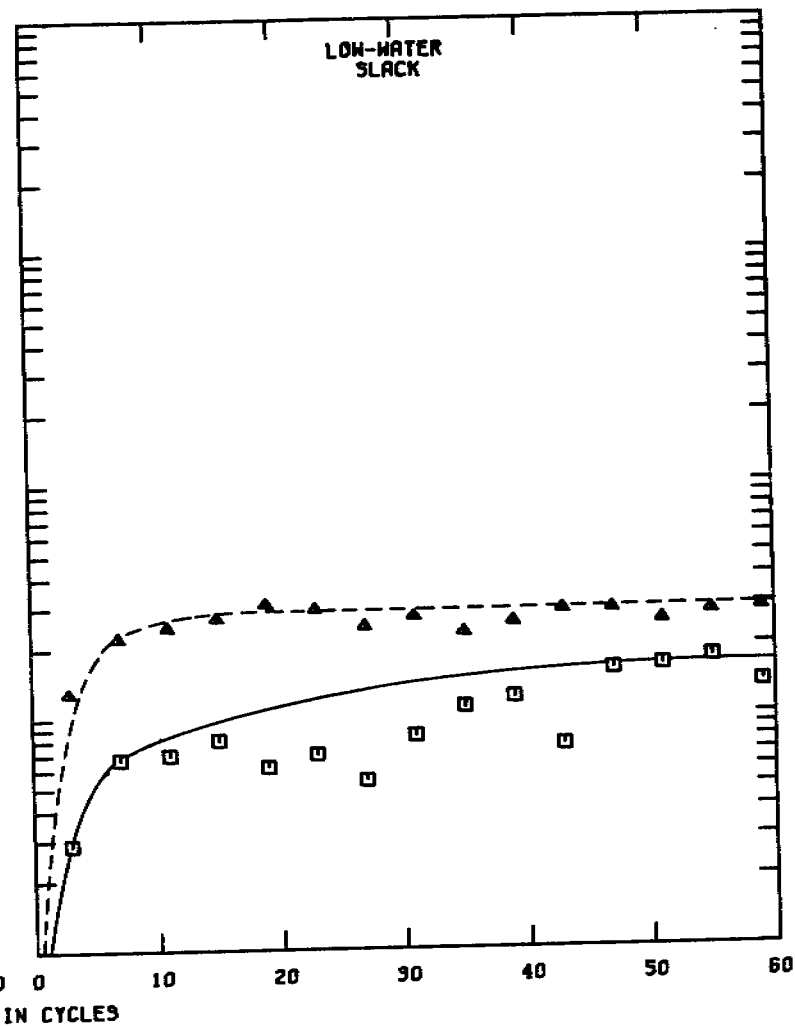
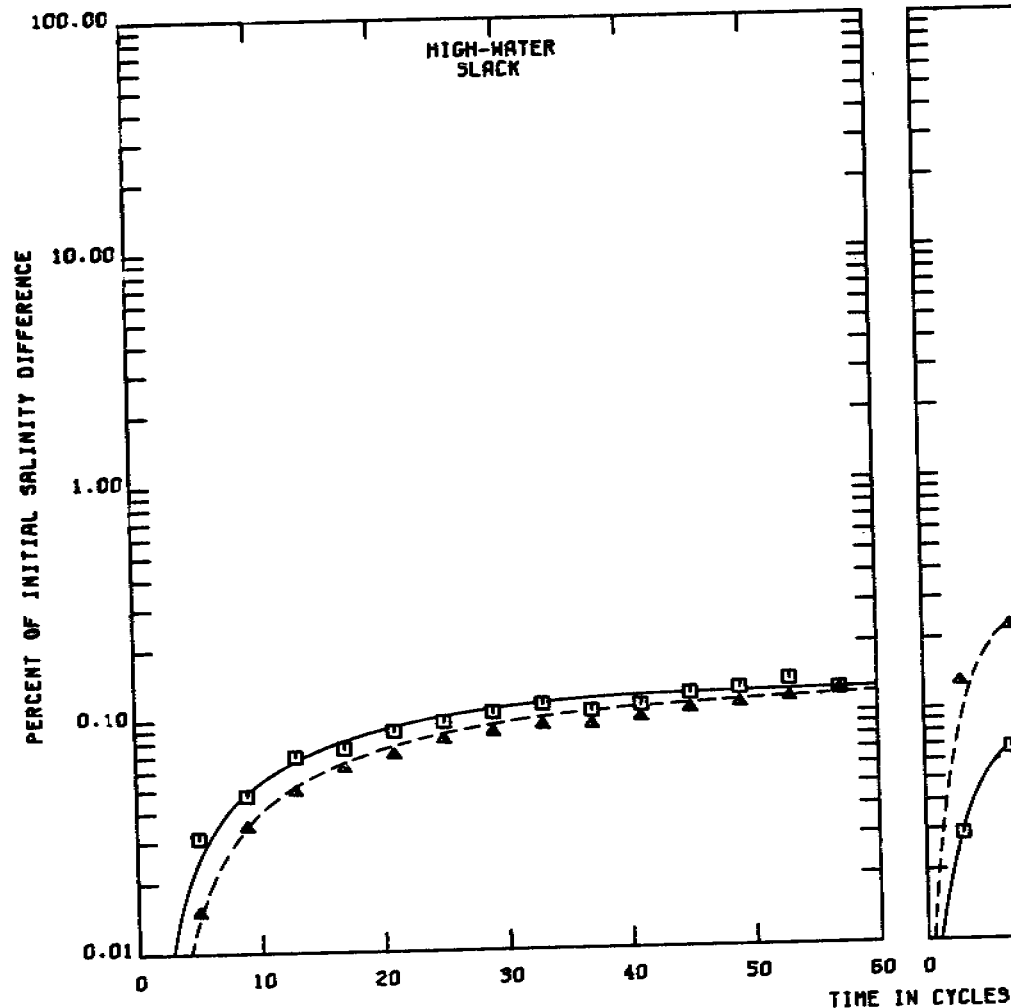


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D2



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

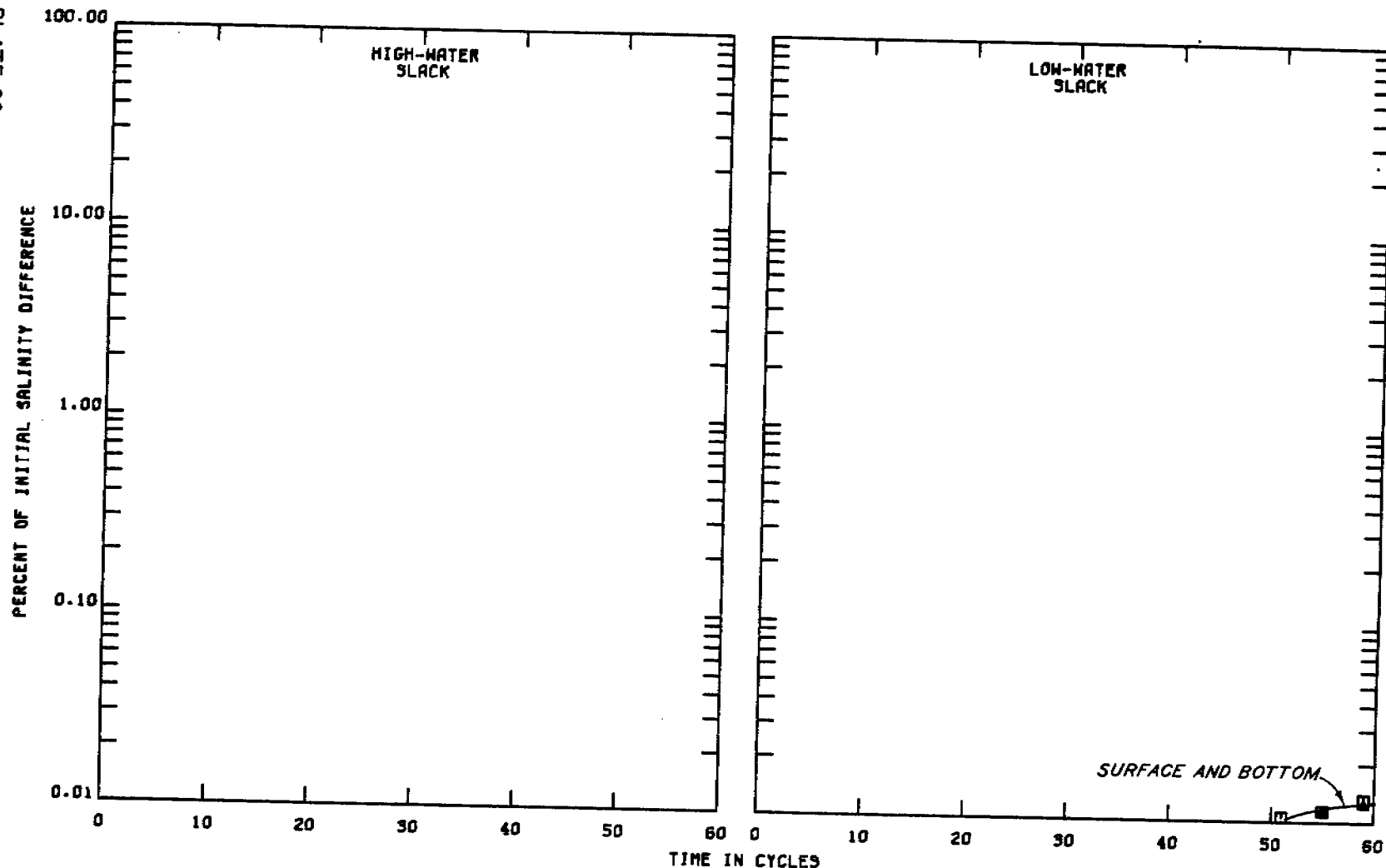
6542 CF3
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D3

PLATE 96

110



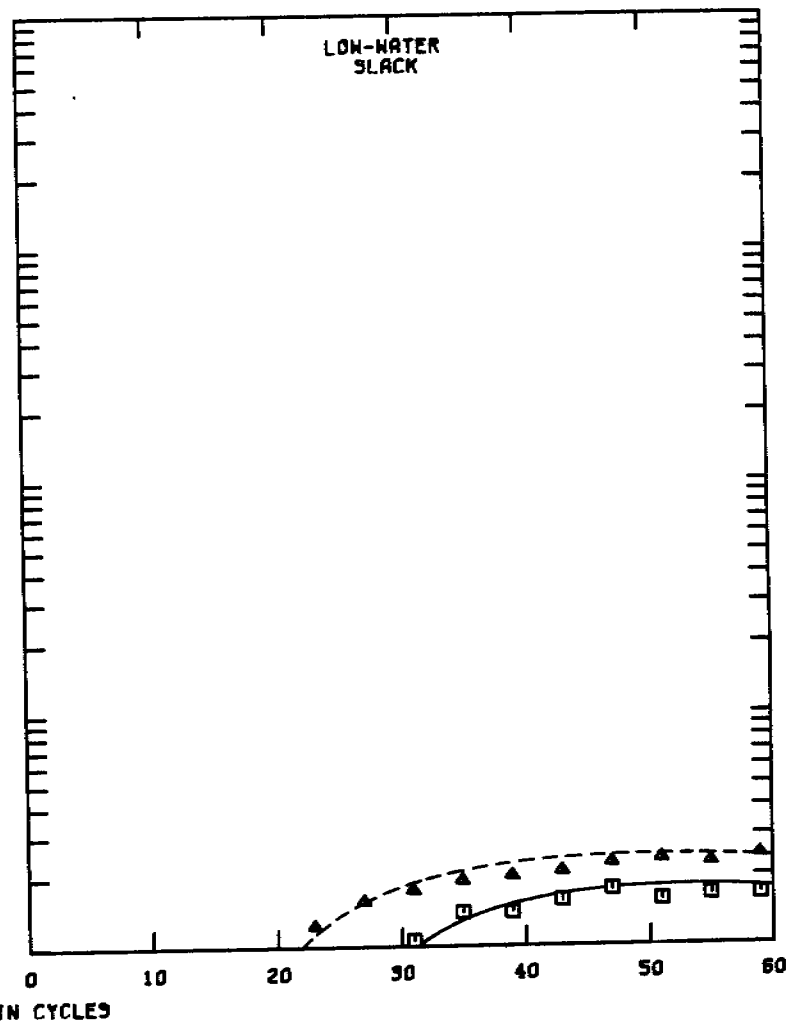
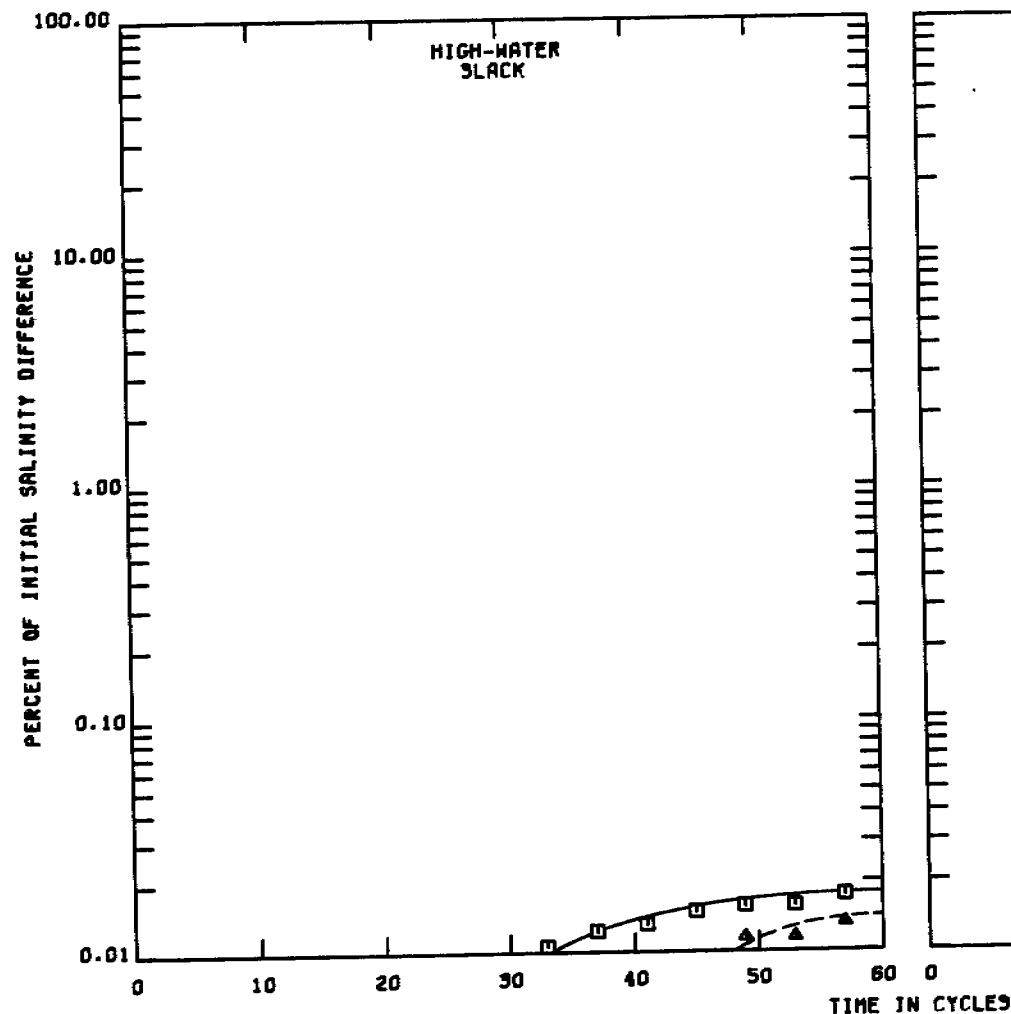
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D4

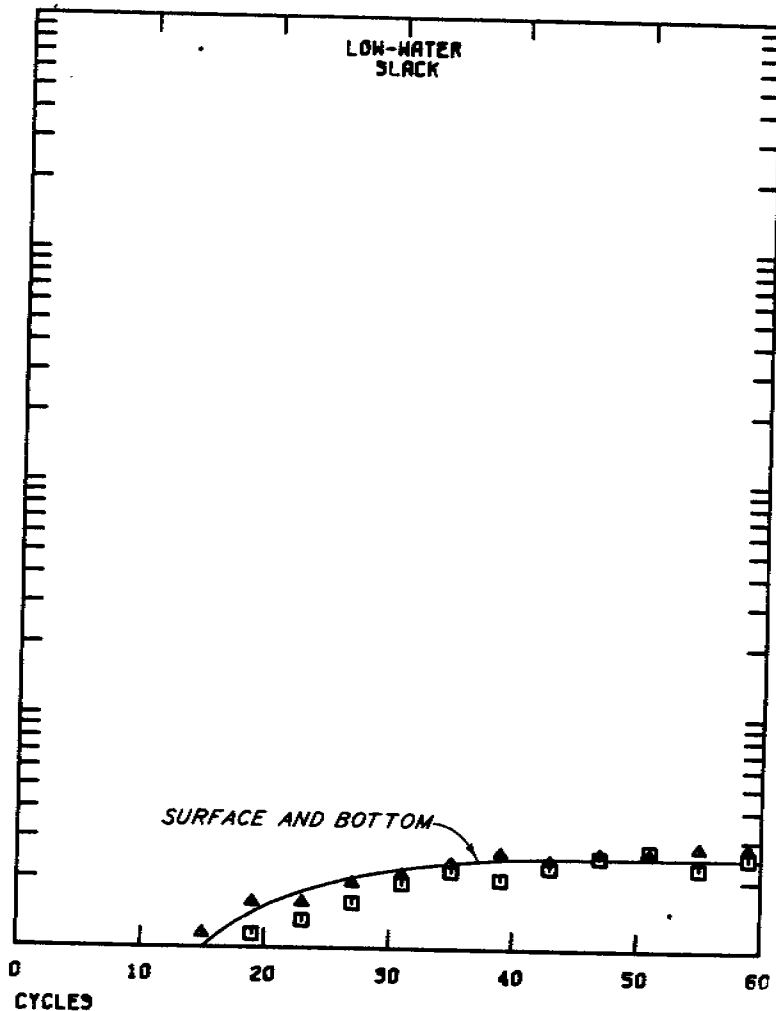
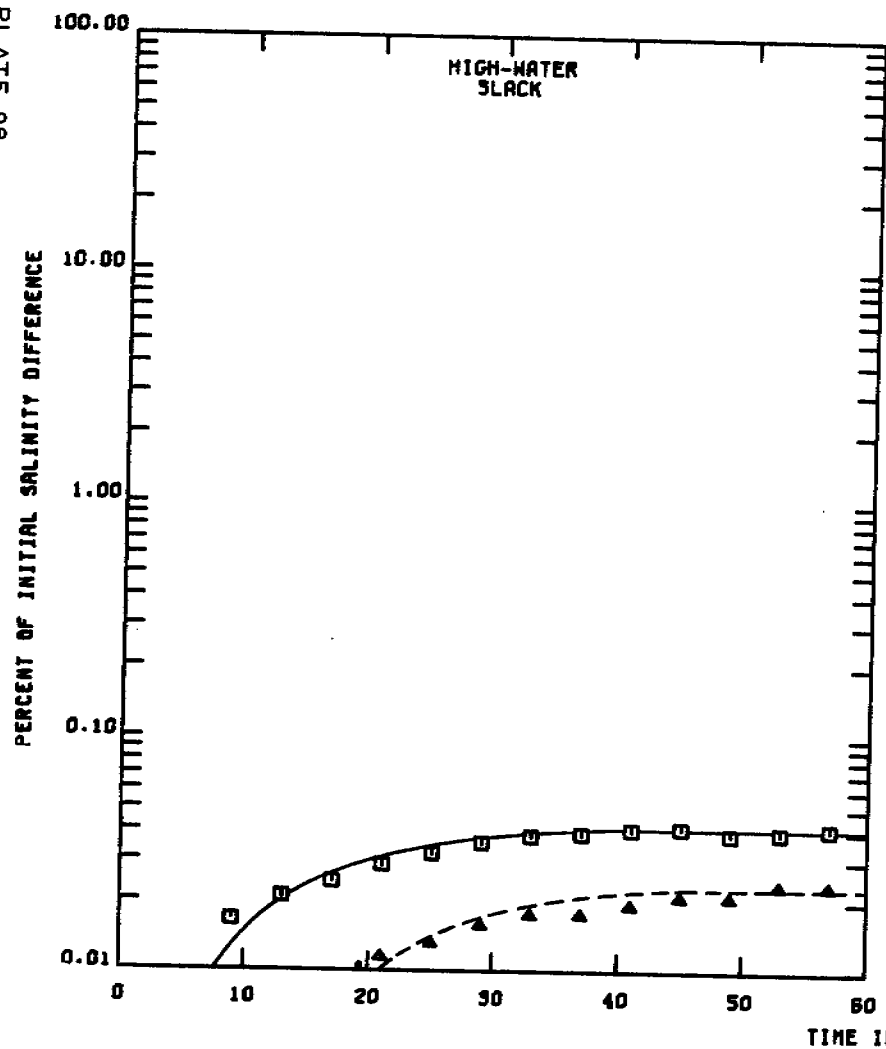


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D5

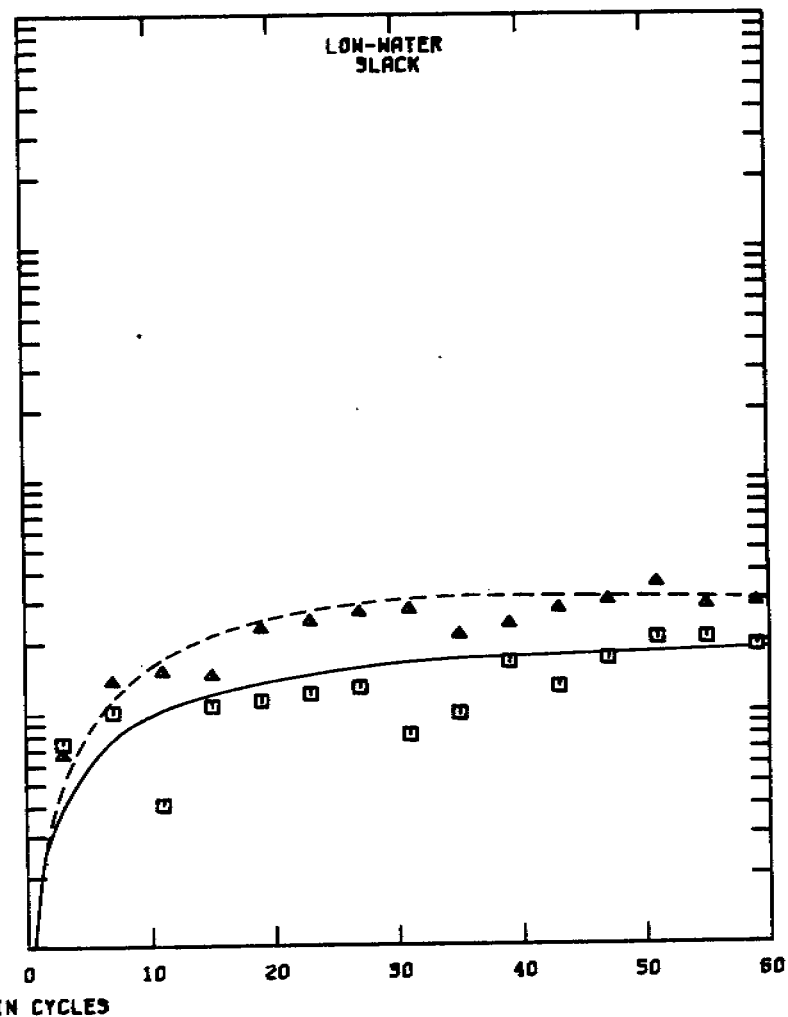
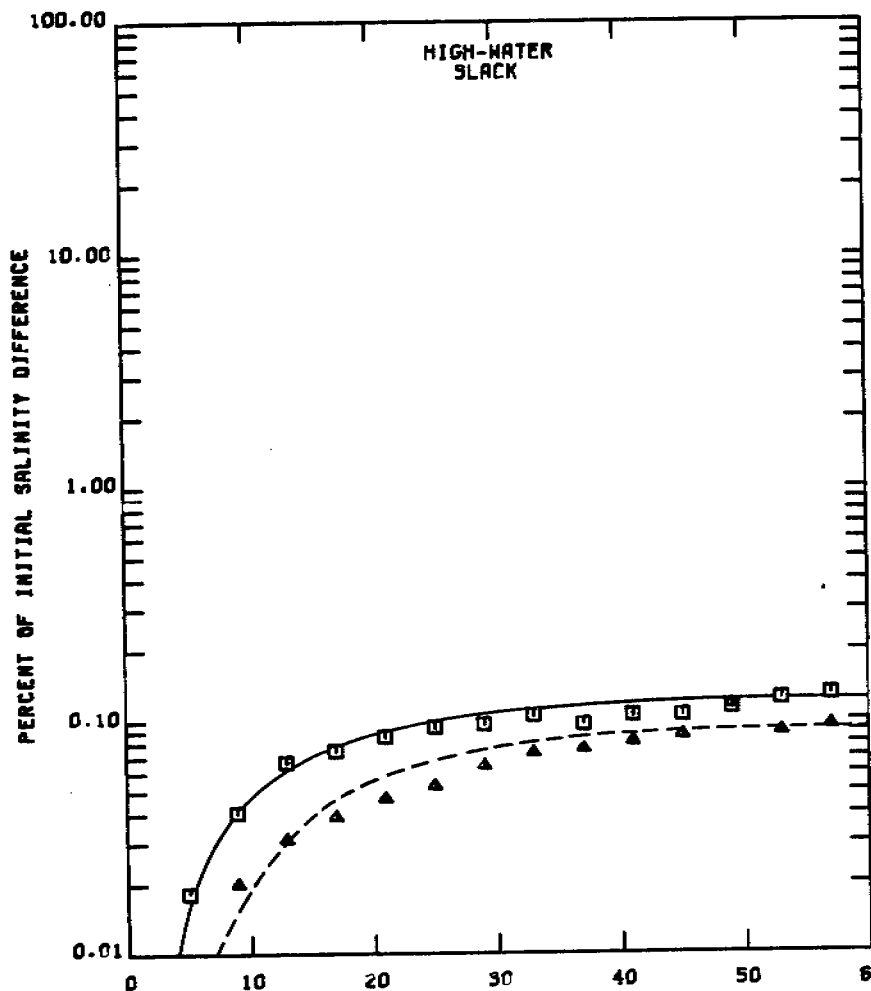


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D6



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

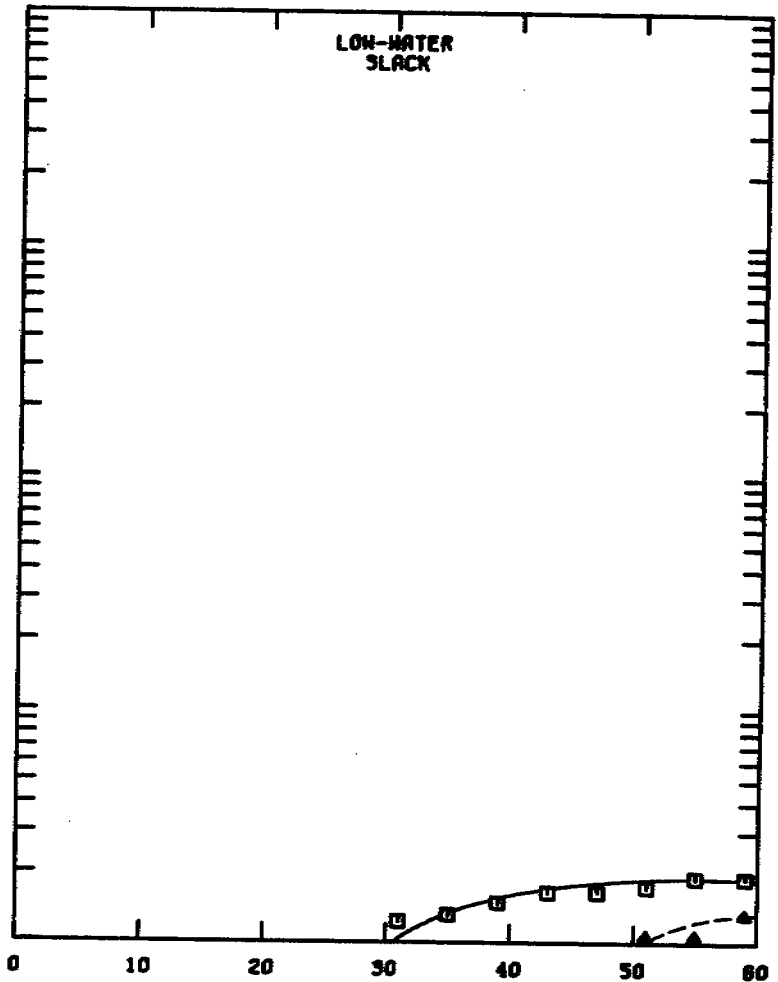
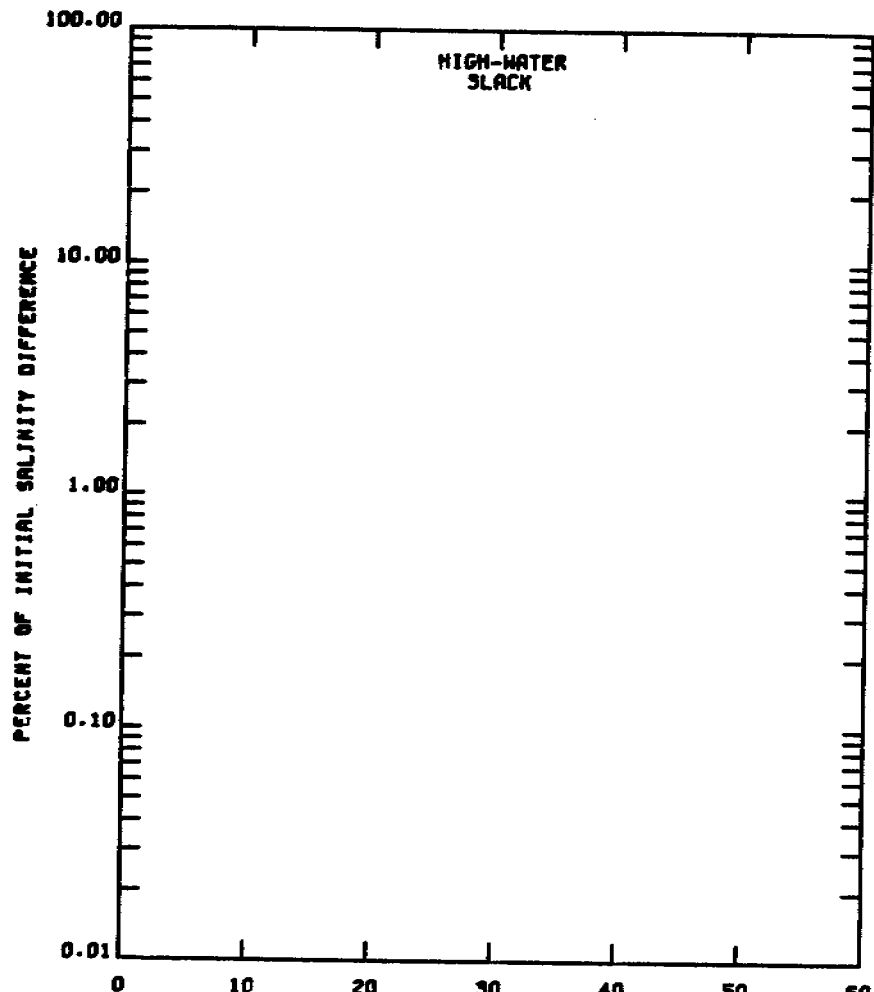
LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D7

PLATE 100

124

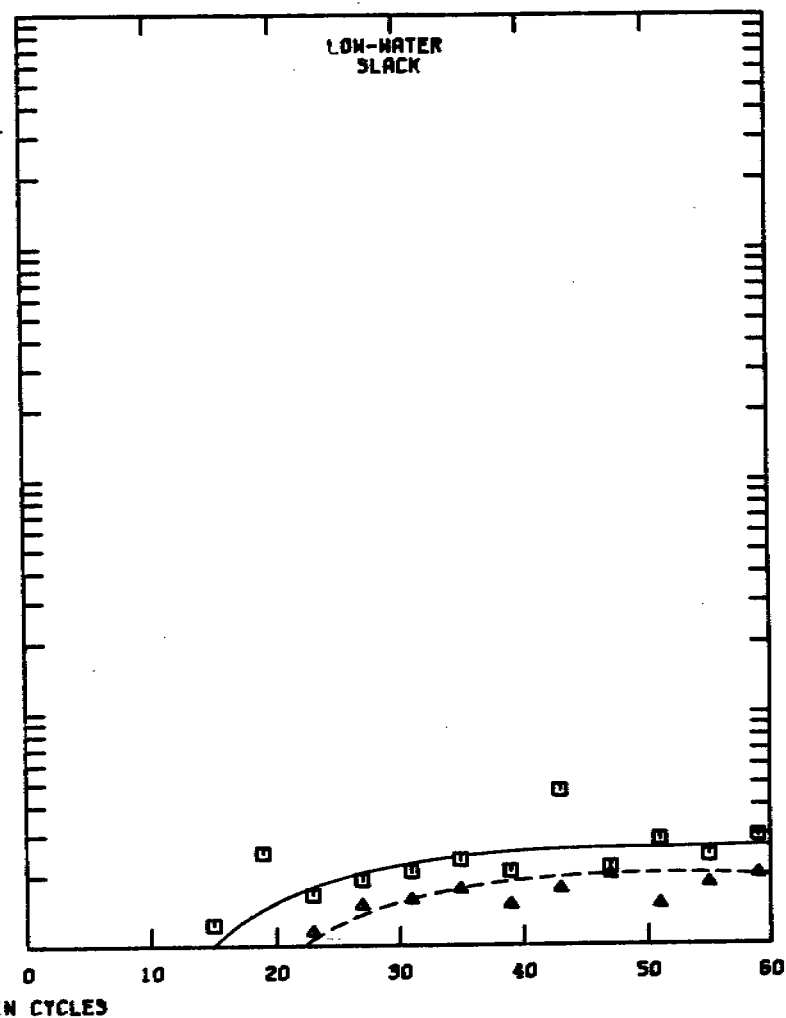
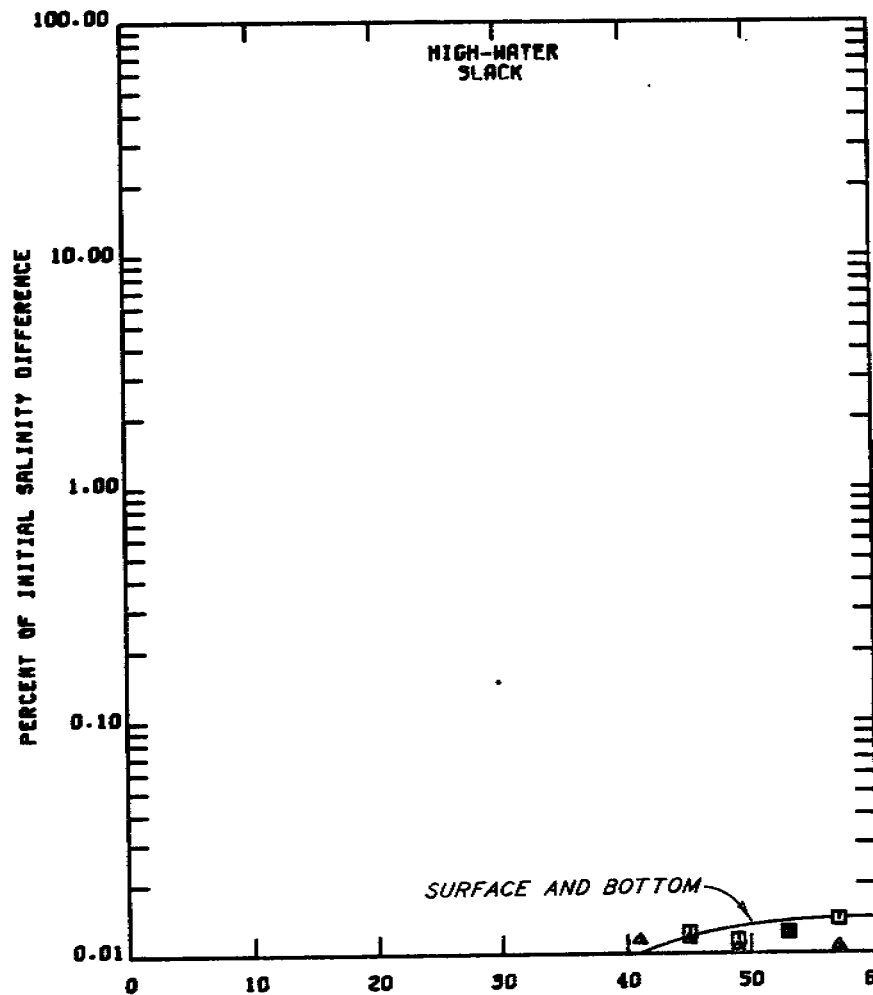


TIME IN CYCLES

TEST CONDITIONS
 FRESH-WATER DISCHARGE 6542 CFS
 BASE SALINITY AT DIFFUSER 21.0 PPT
 EFFLUENT SALINITY 32.4 PPT
 INITIAL SALINITY DIFFERENCE 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION D9



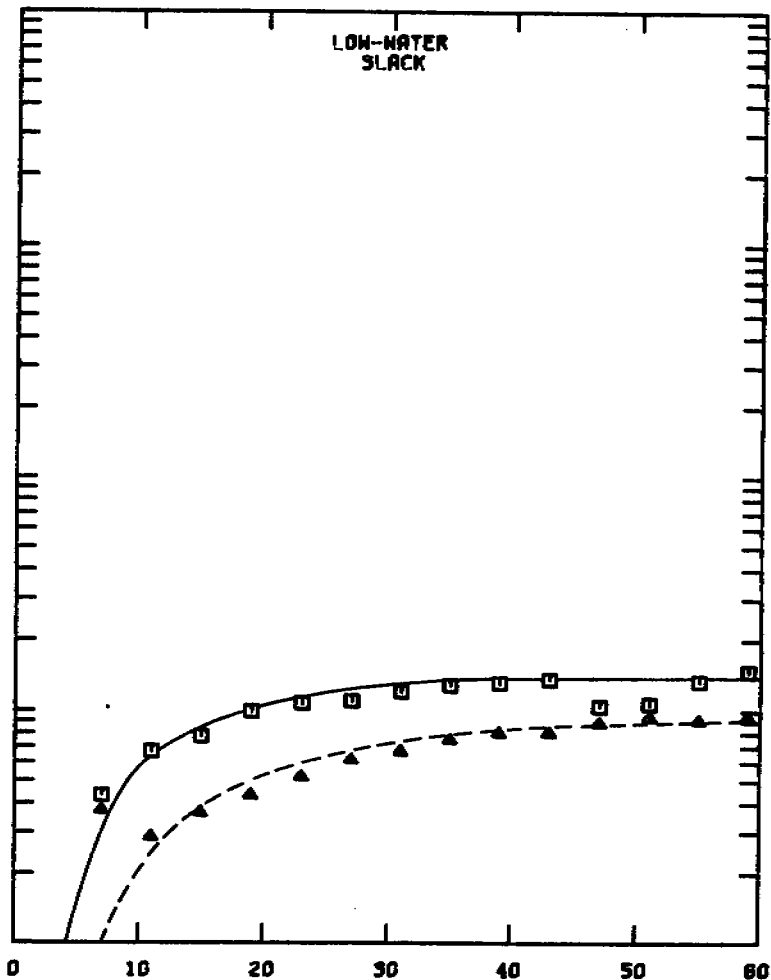
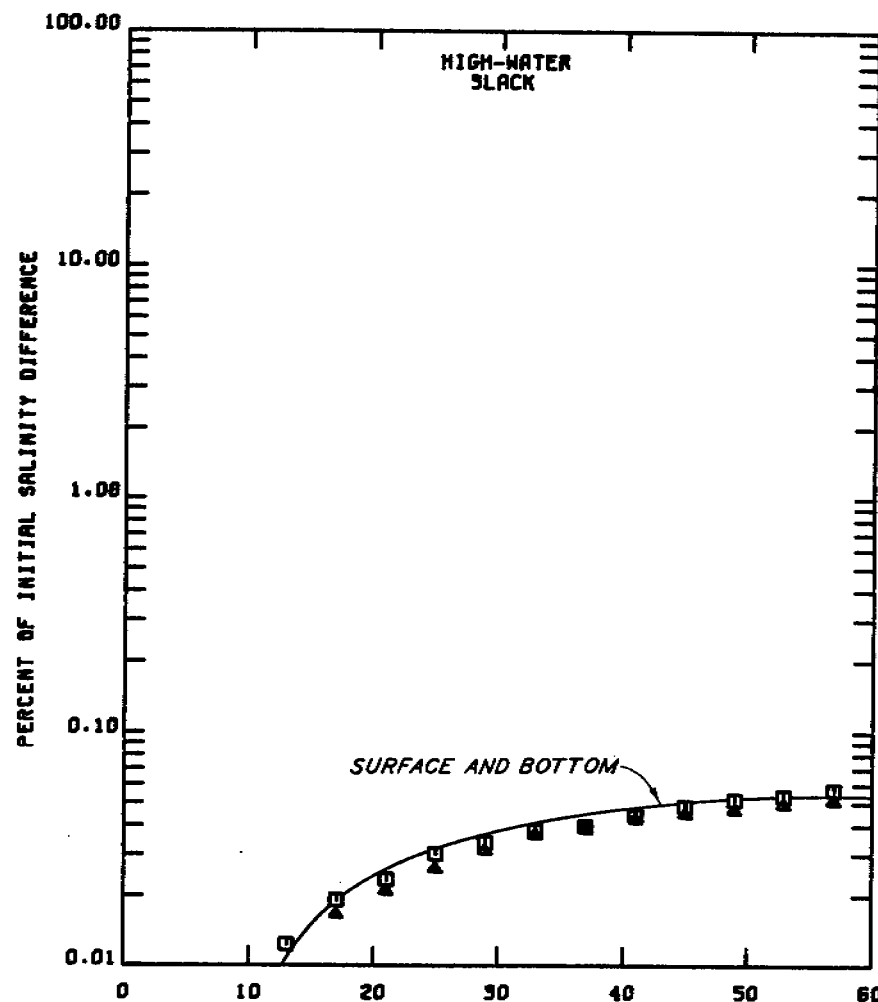
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD**

STATION D10



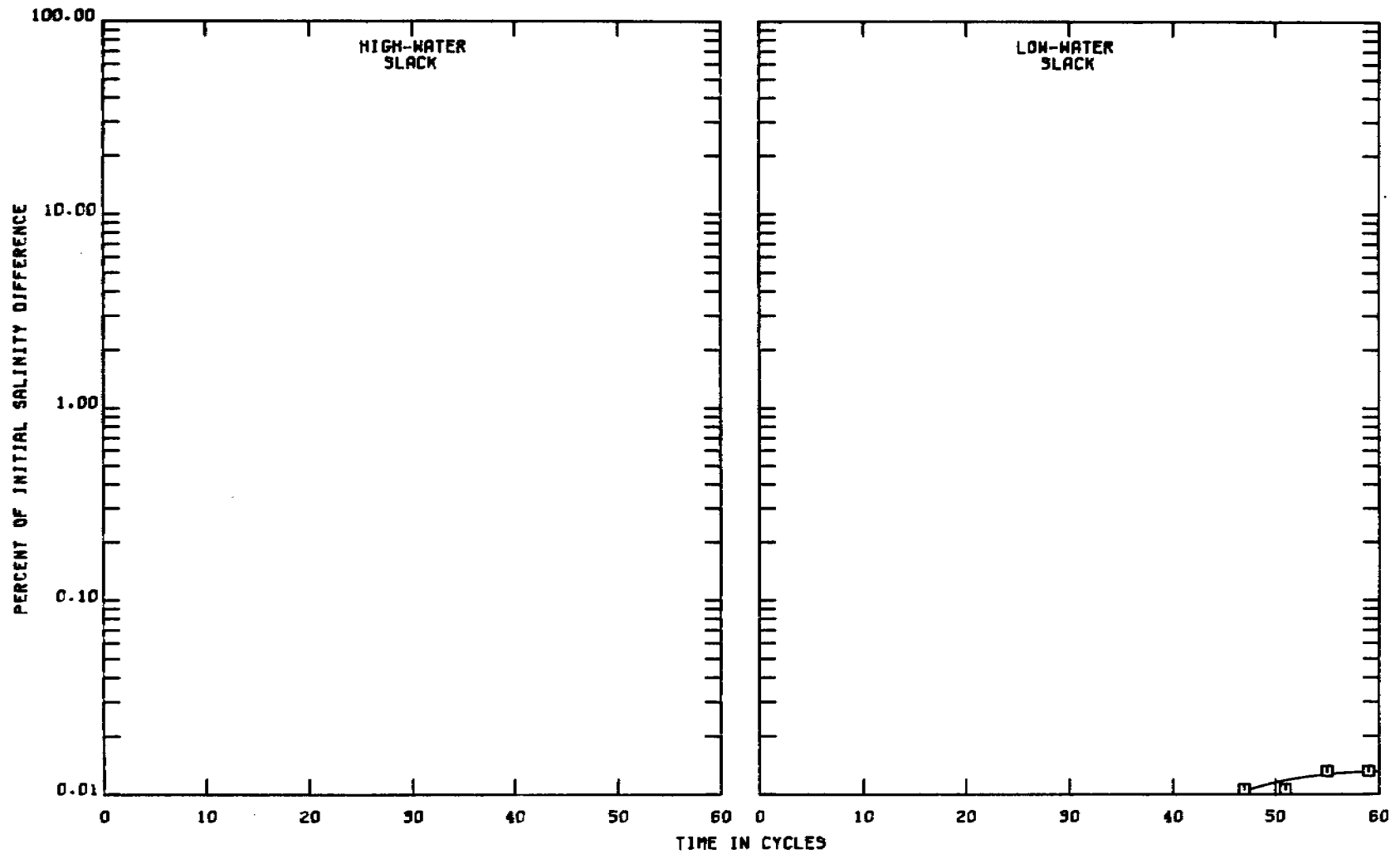
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 LONGO PLANT-LOW FLOW PERIOD**

STATION D11



TEST CONDITIONS

FRESH-WATER DISCHARGE	6542 CFS
BASE SALINITY AT DIFFUSER	21.0 PPT
EFFLUENT SALINITY	32.4 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
▲ - - -	BOTTOM

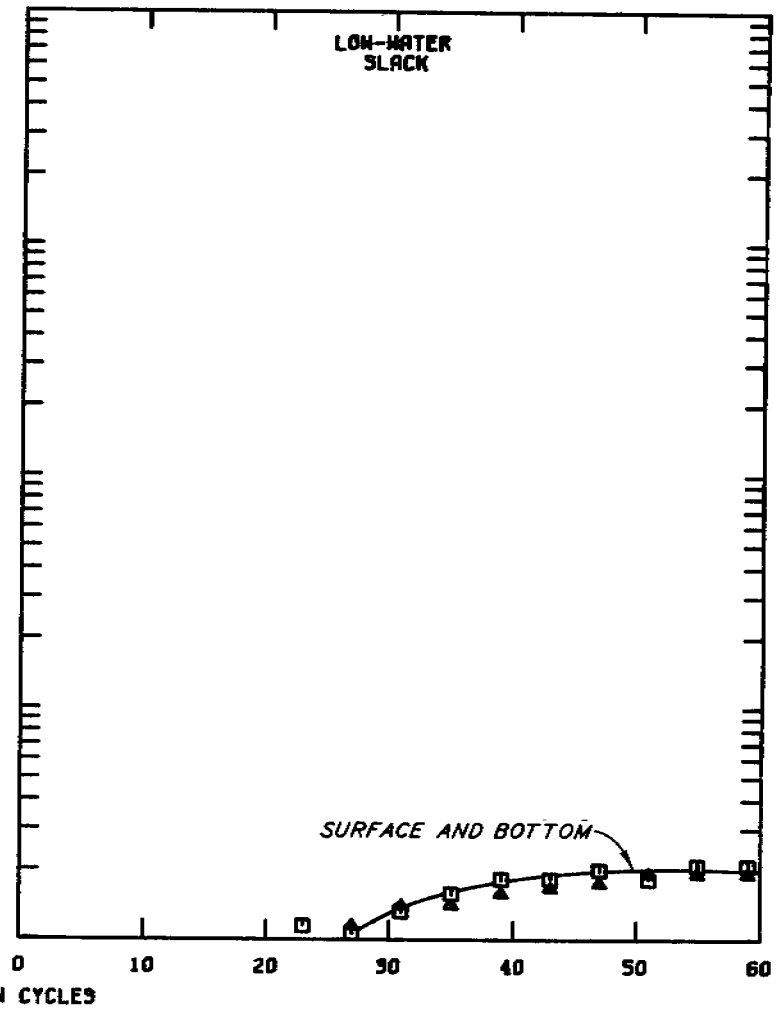
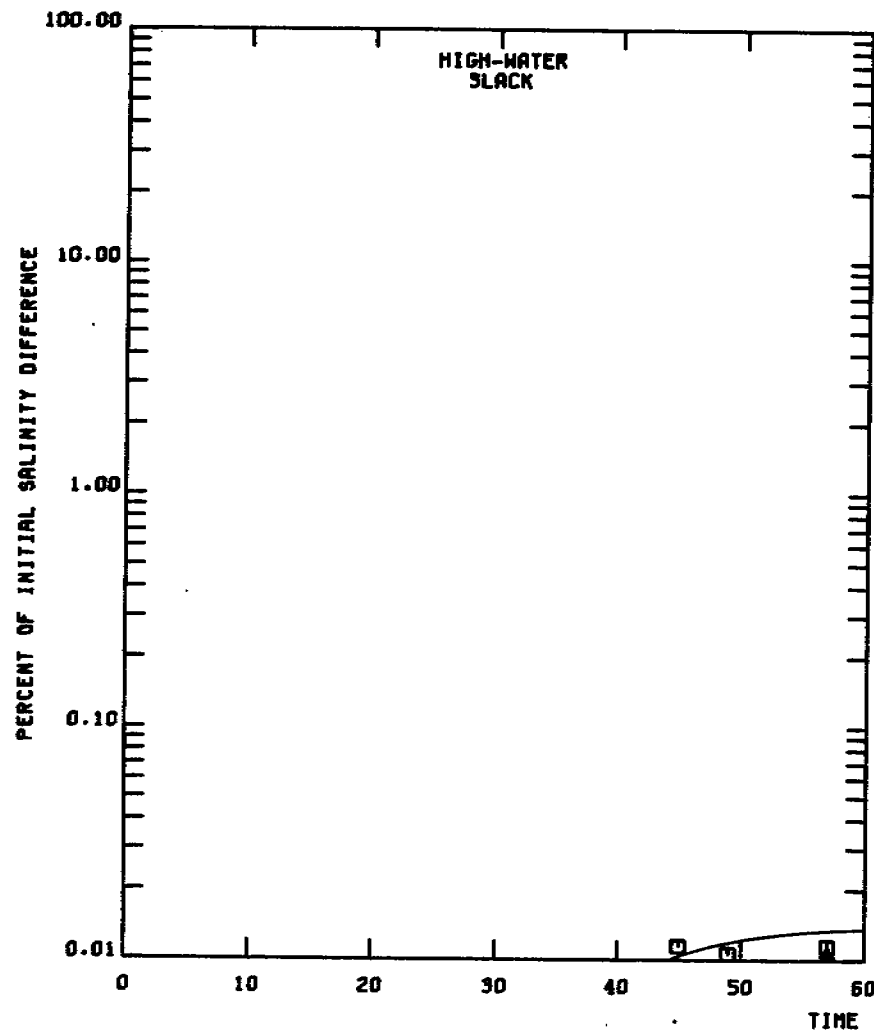
DELAWARE RIVER MODEL

SALINE WATER

DISPERSION TEST

10MGD PLANT-LOW FLOW PERIOD

STATION D13



TEST CONDITIONS

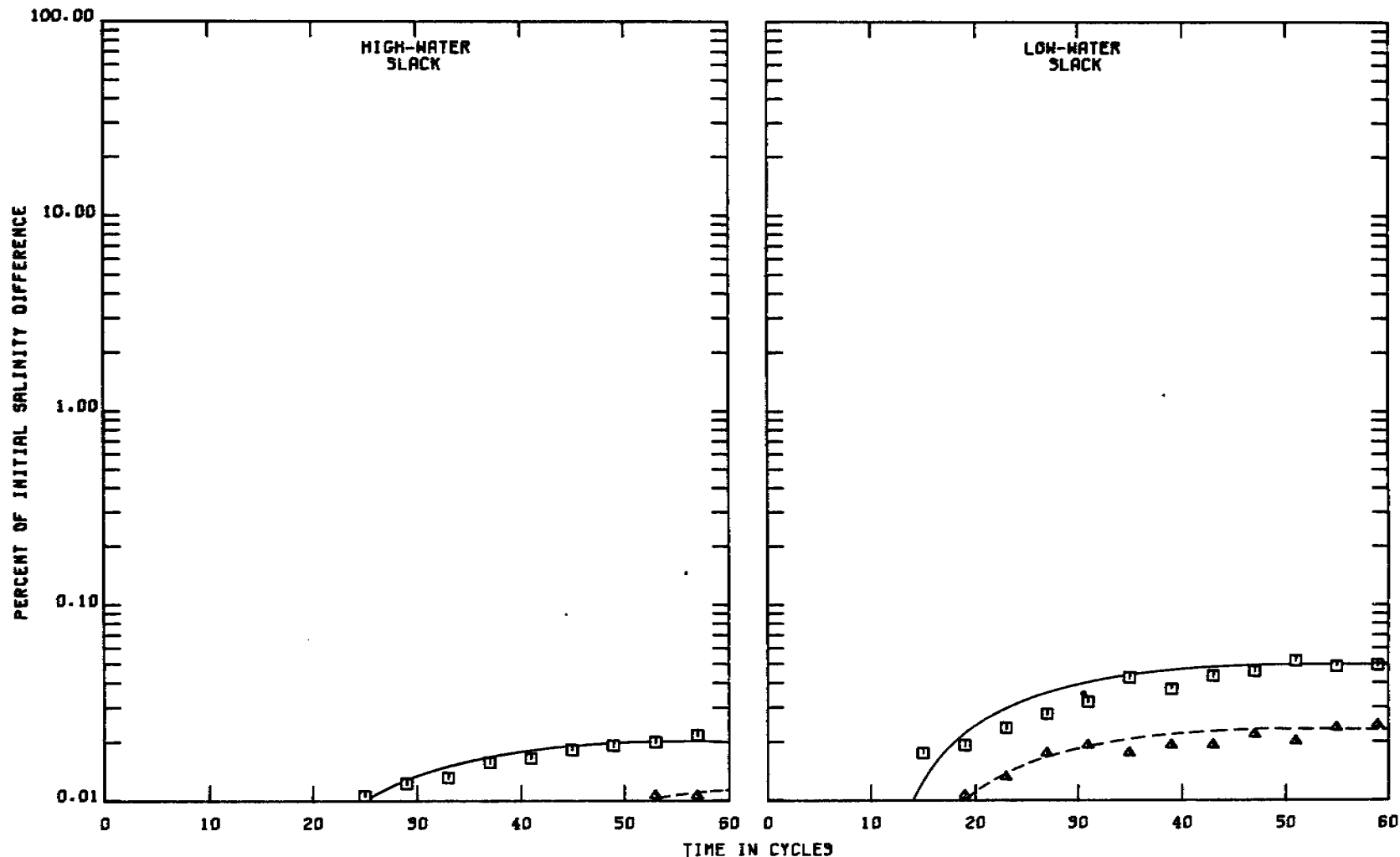
FRESH-WATER DISCHARGE	6542 CFS
BASE SALINITY AT DIFFUSER	21.0 PPT
EFFLUENT SALINITY	32.4 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
▲ — — —	BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-LOW FLOW PERIOD

STATION D14



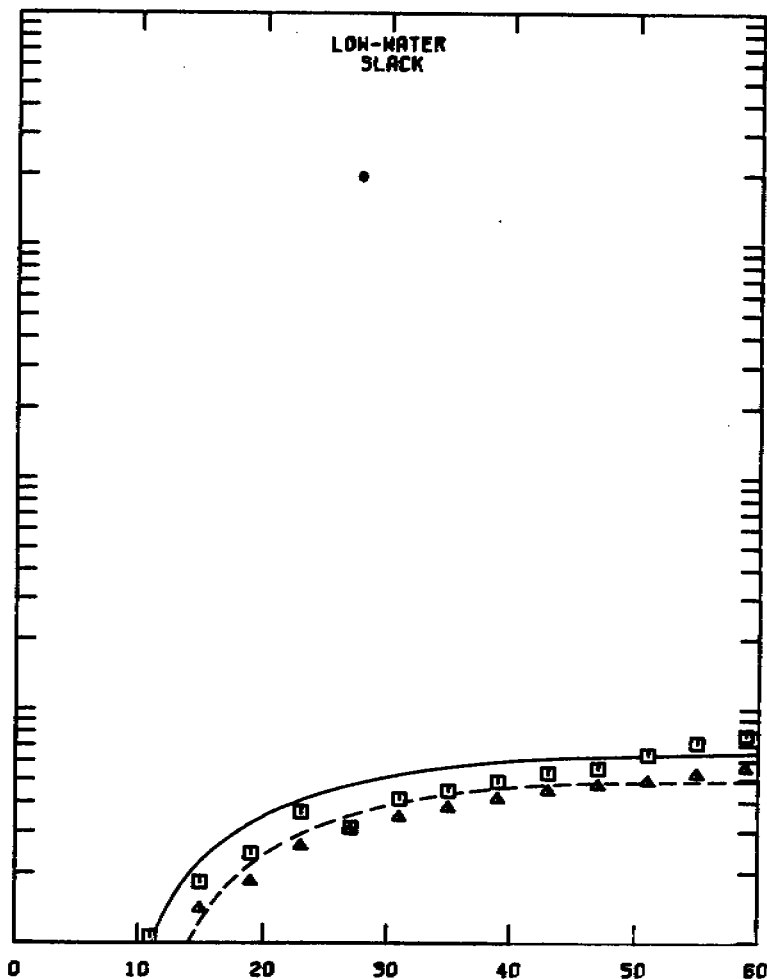
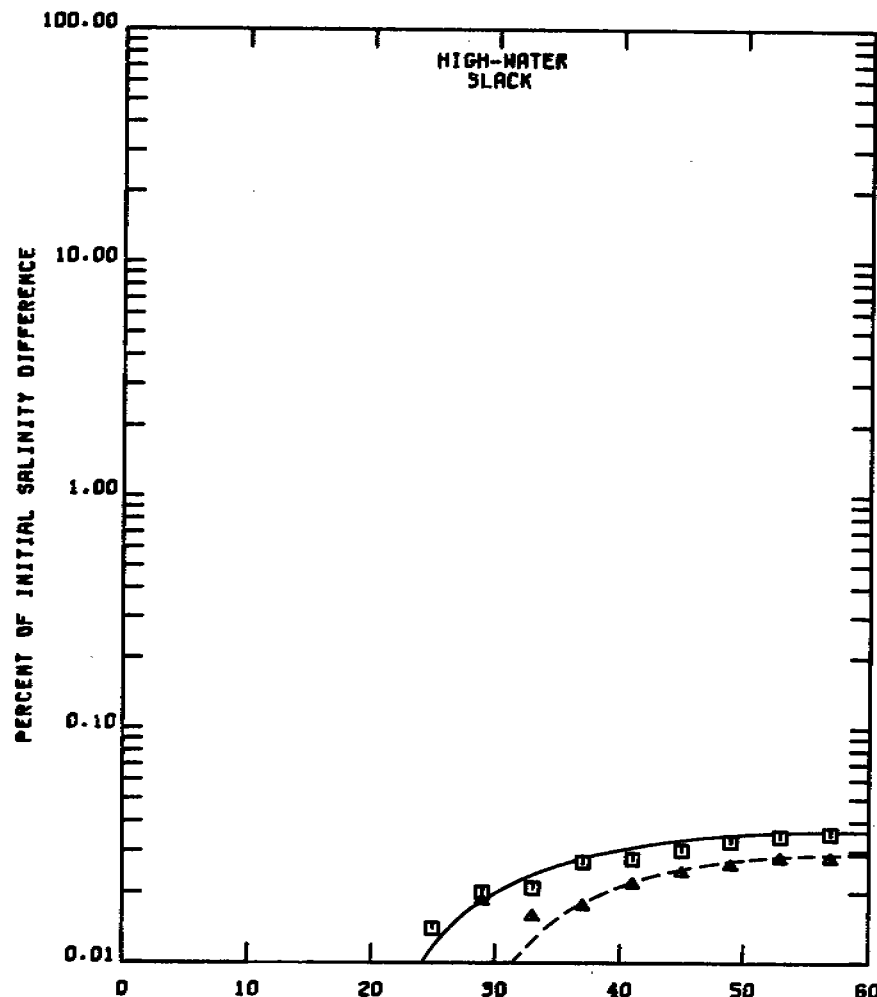
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D15

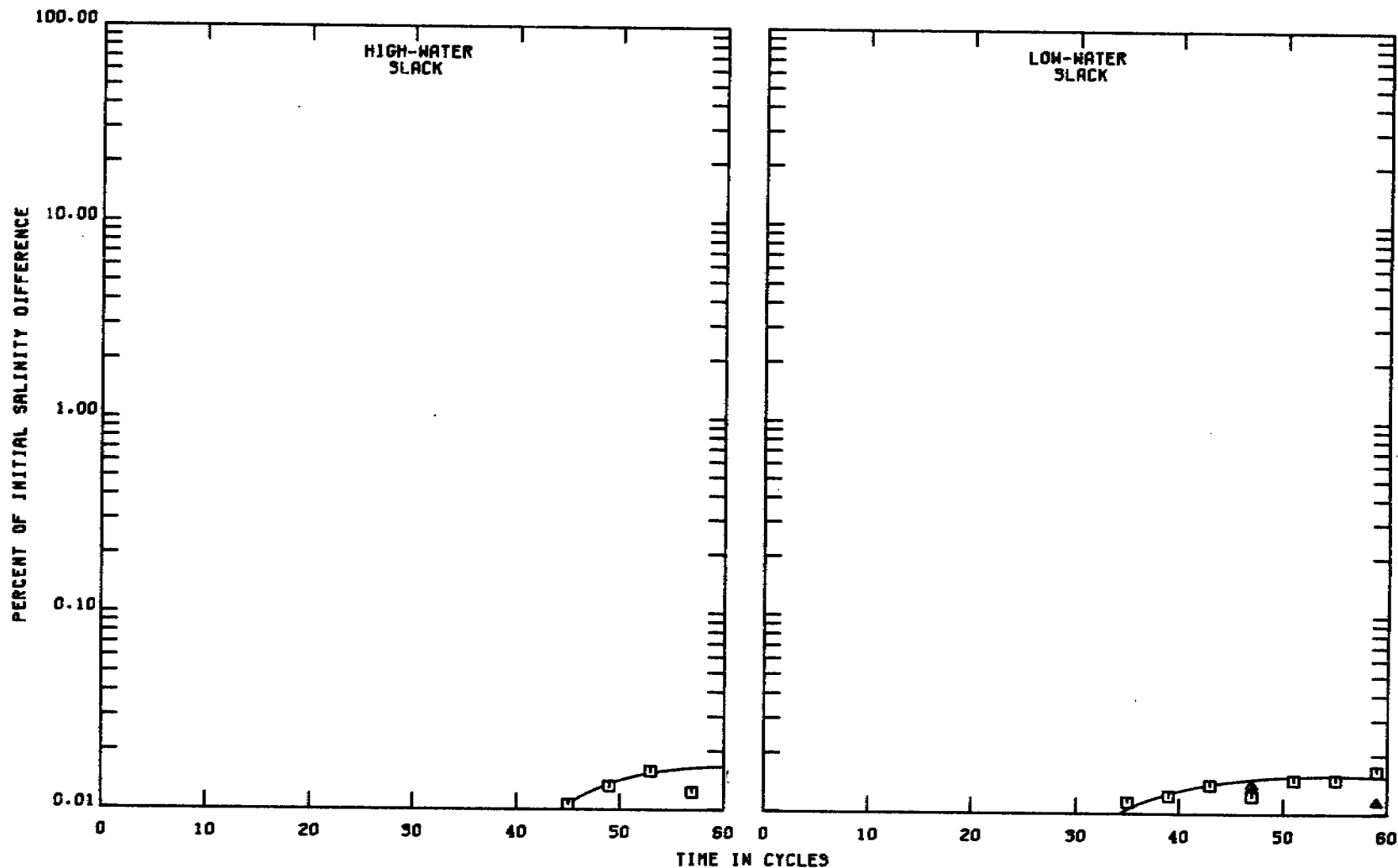


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CF9
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD**



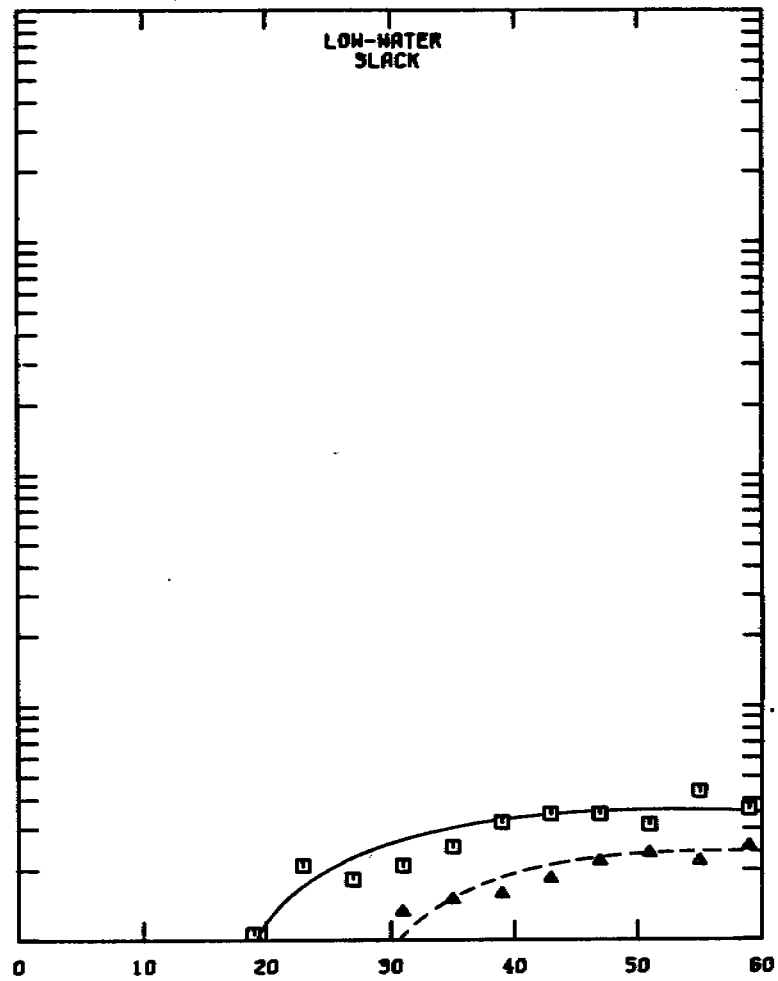
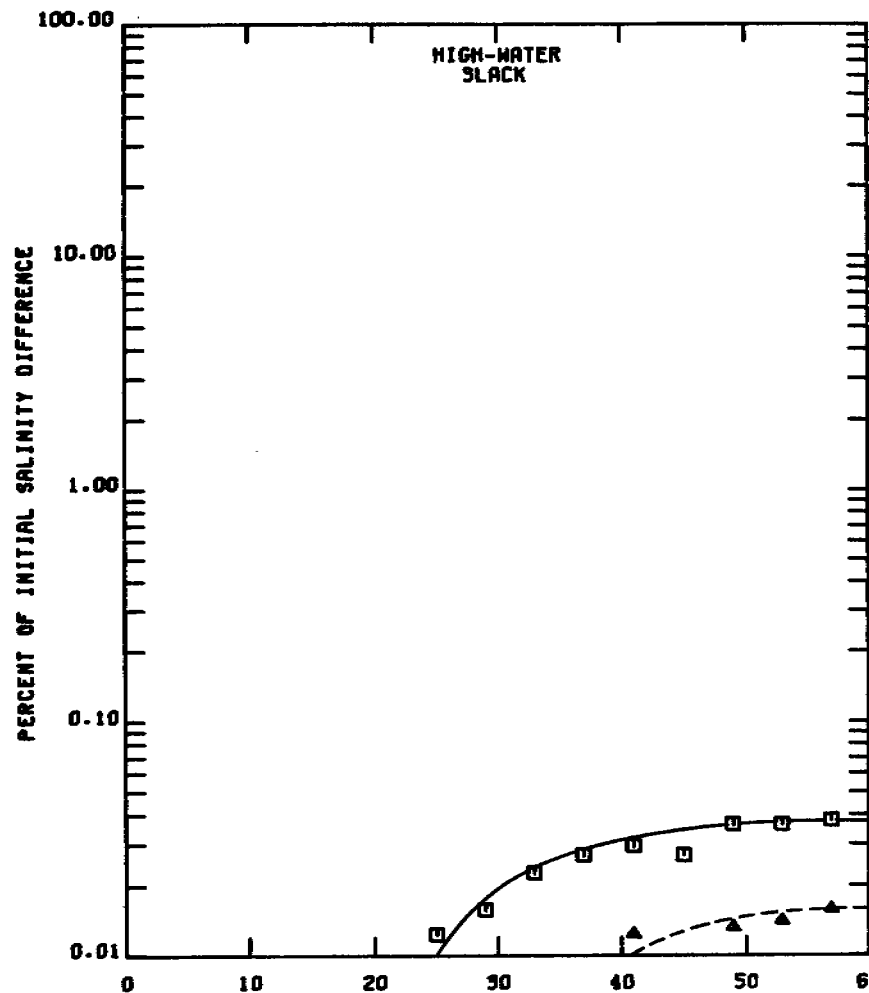
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D19



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

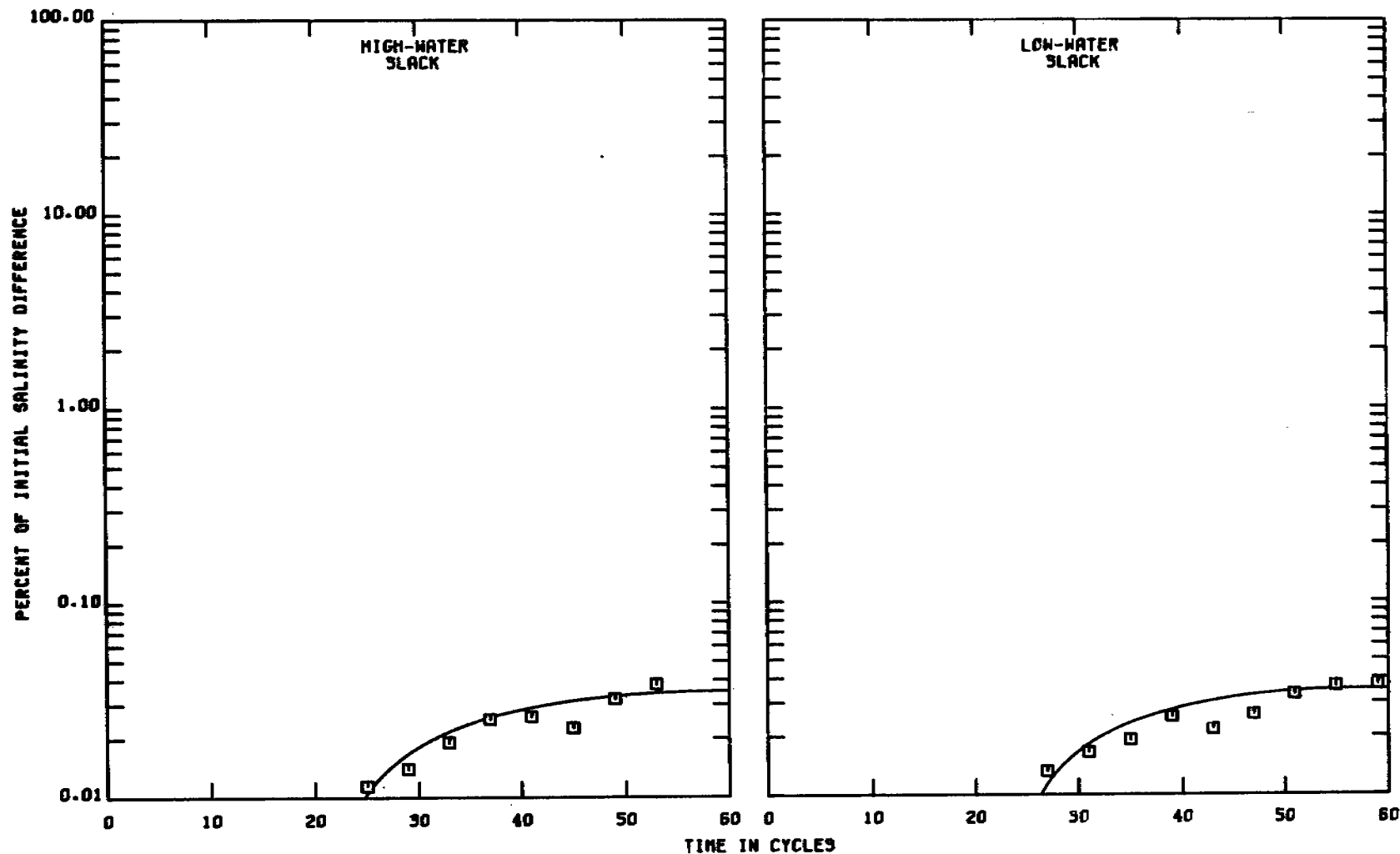
6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D20



TEST CONDITIONS

FRESH-WATER DISCHARGE 6542 CFS

BASE SALINITY AT DIFFUSER 21.0 PPT

EFFLUENT SALINITY 32.4 PPT

INITIAL SALINITY DIFFERENCE 11.4 PPT

EFFLUENT INJECTION RATE 21.2 MGD

LEGEND

□ ——— SURFACE

▲ — — — BOTTOM

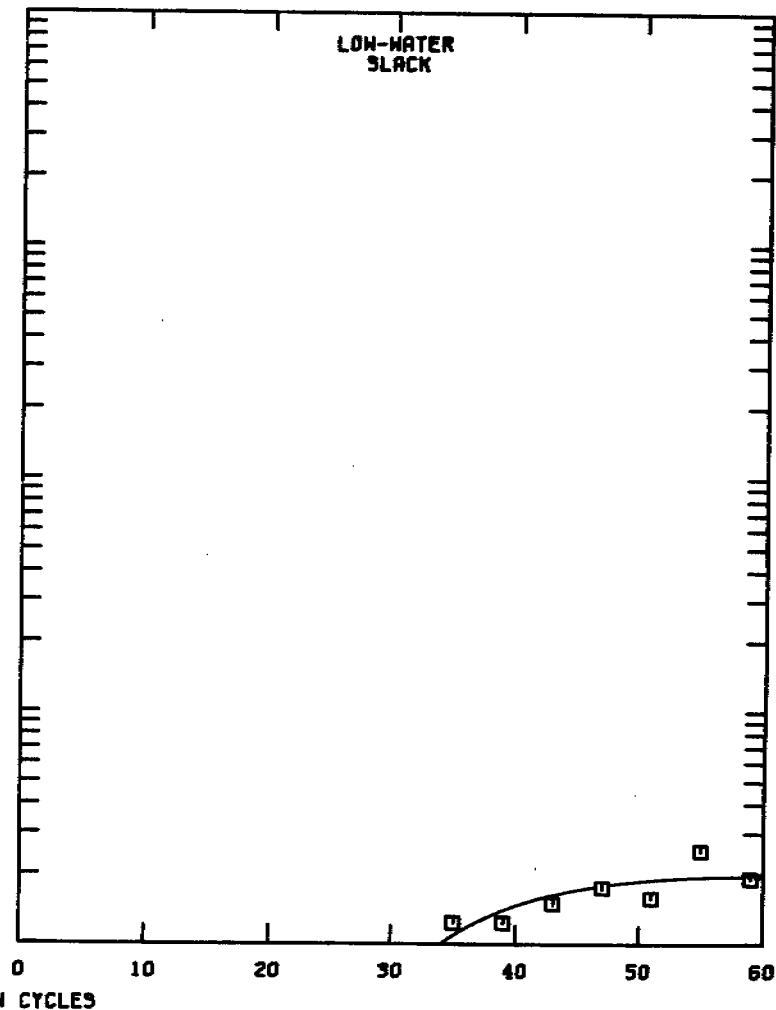
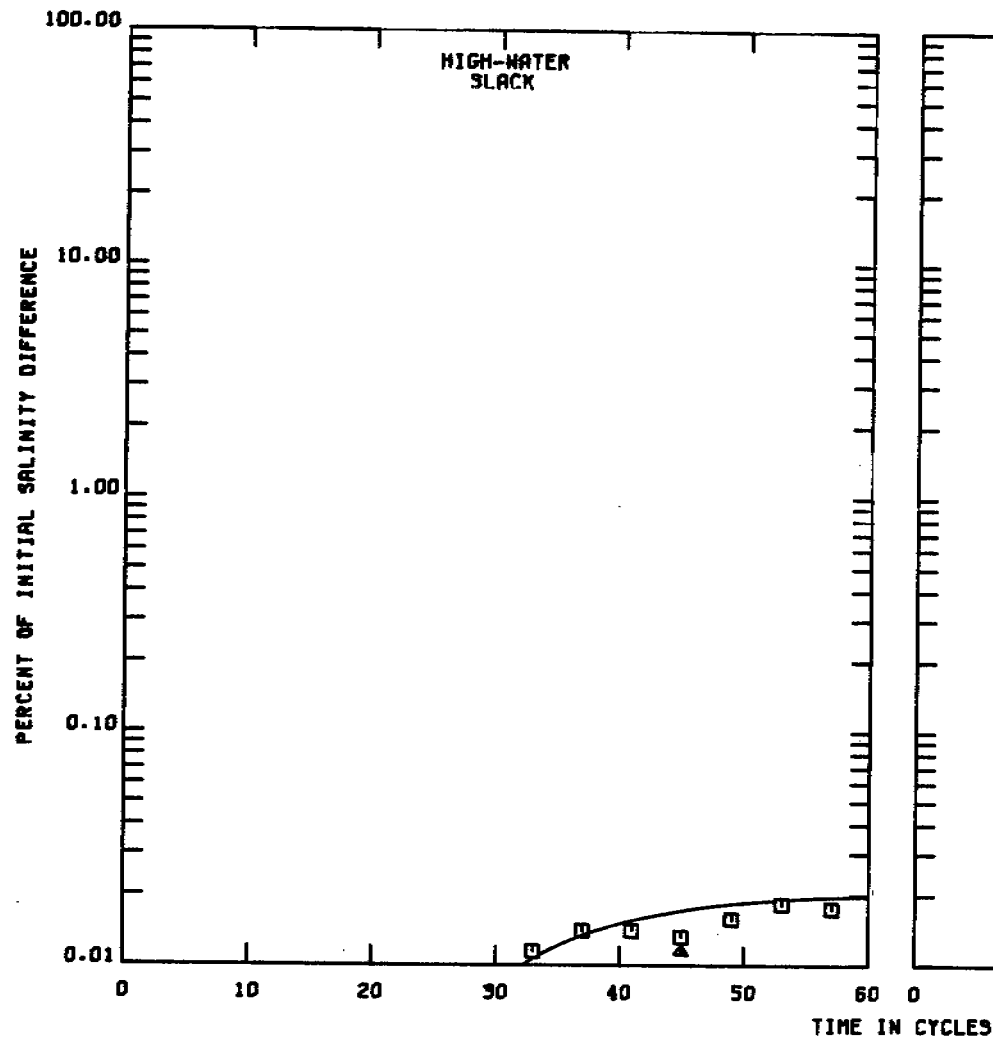
DELAWARE RIVER MODEL

SALINE WATER

DISPERSION TEST

10MGD PLANT-LOW FLOW PERIOD

STATION D21



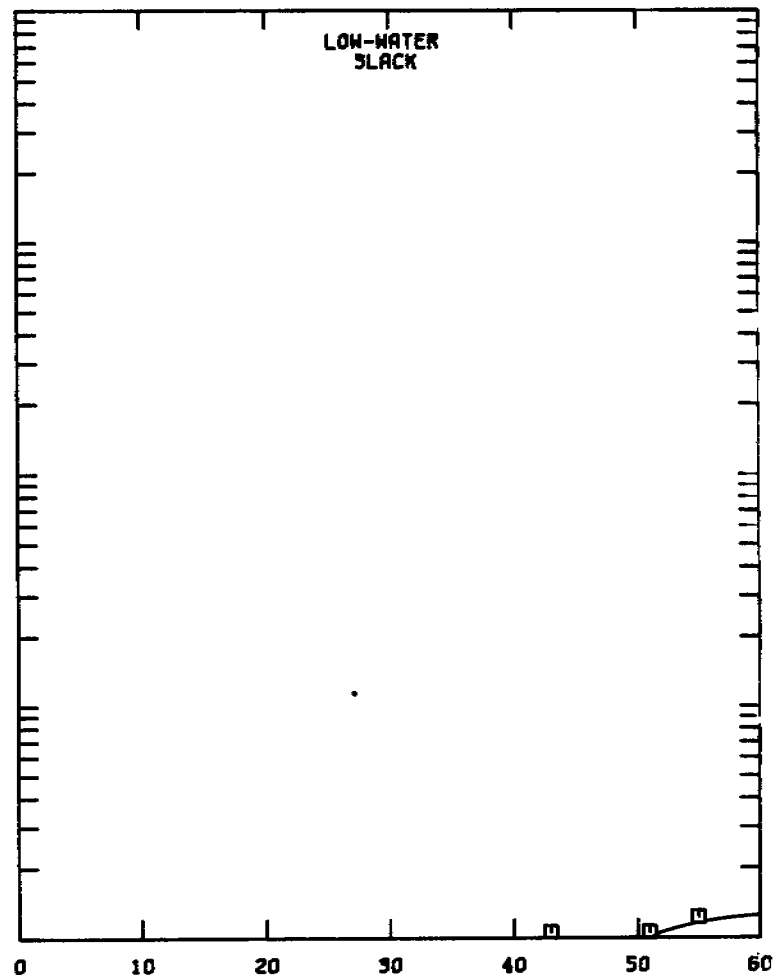
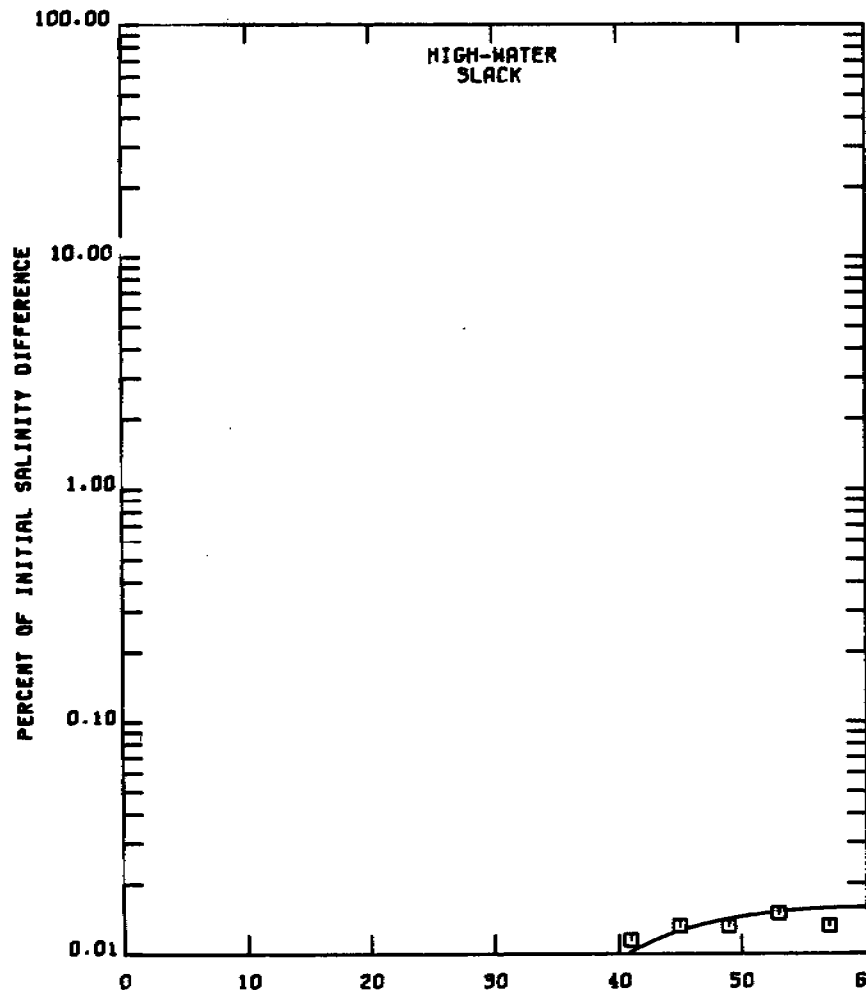
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D22



TIME IN CYCLES

TEST CONDITIONS

FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

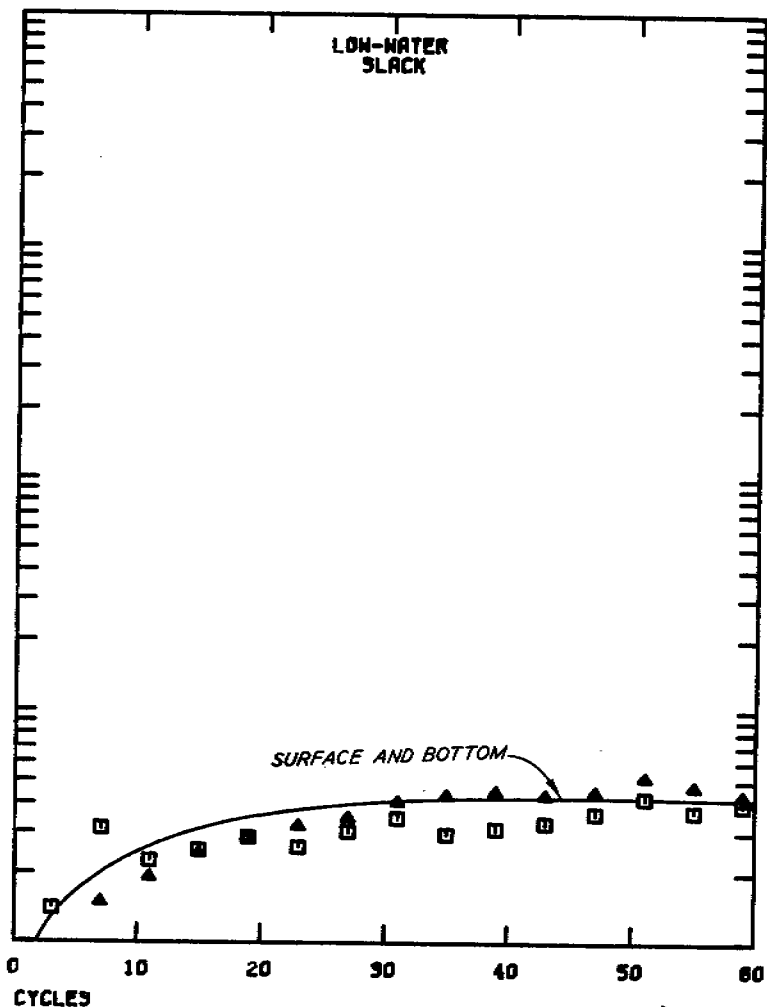
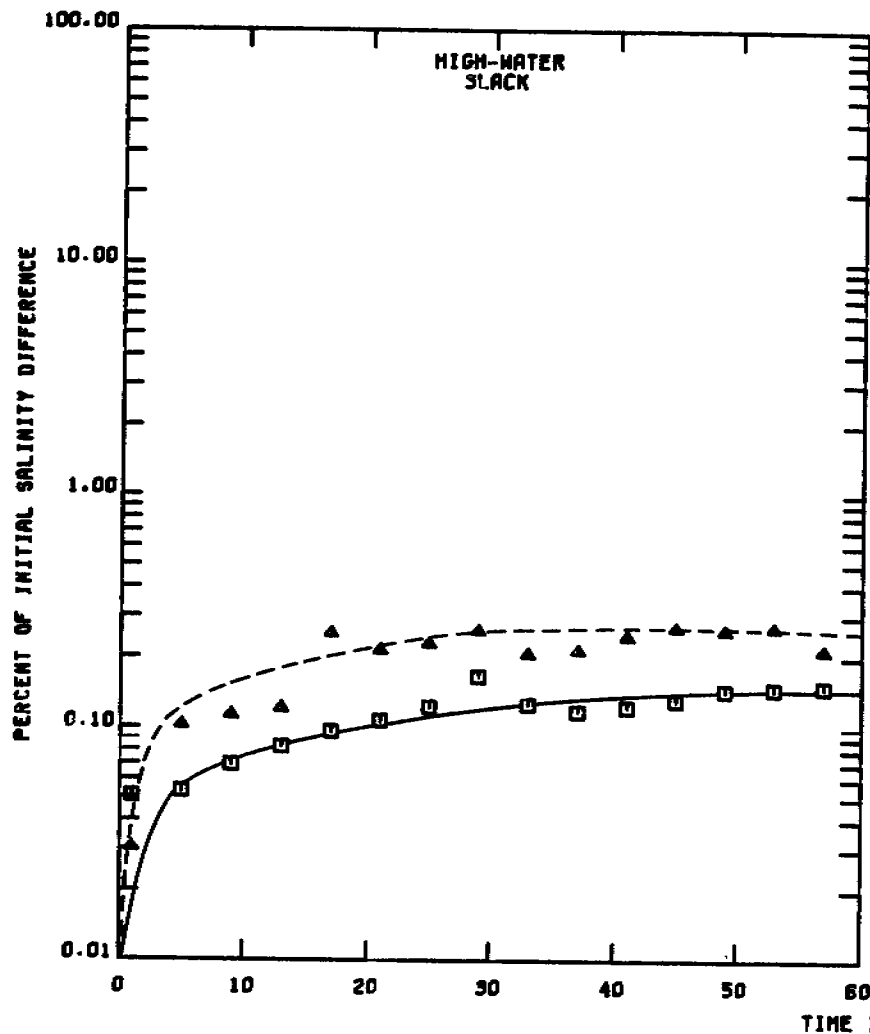
6542 CF3
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ ——— SURFACE
 ▲ - - - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION D23



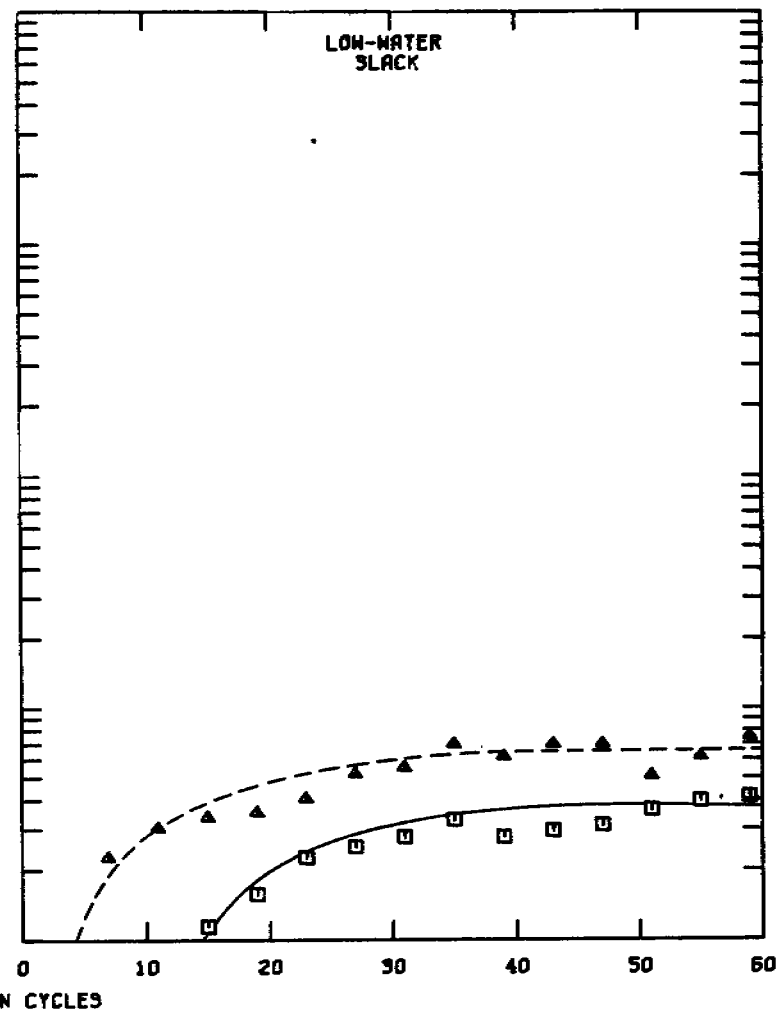
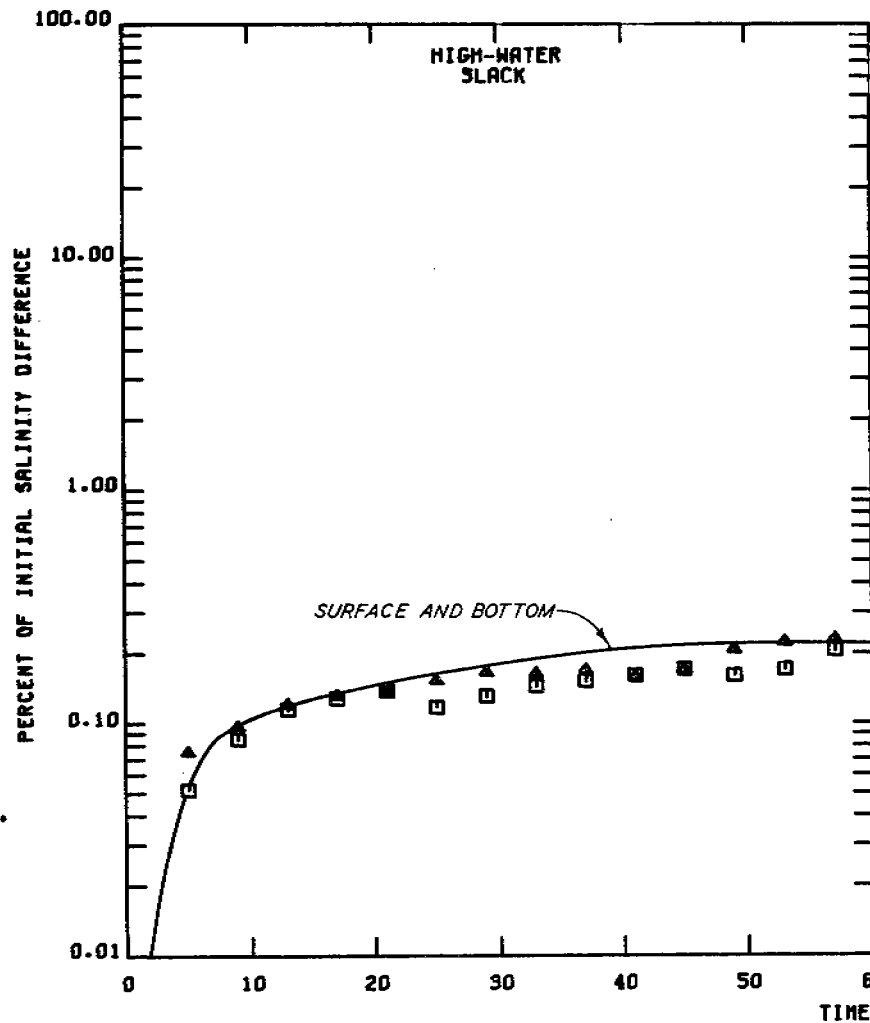
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD**

STATION U1



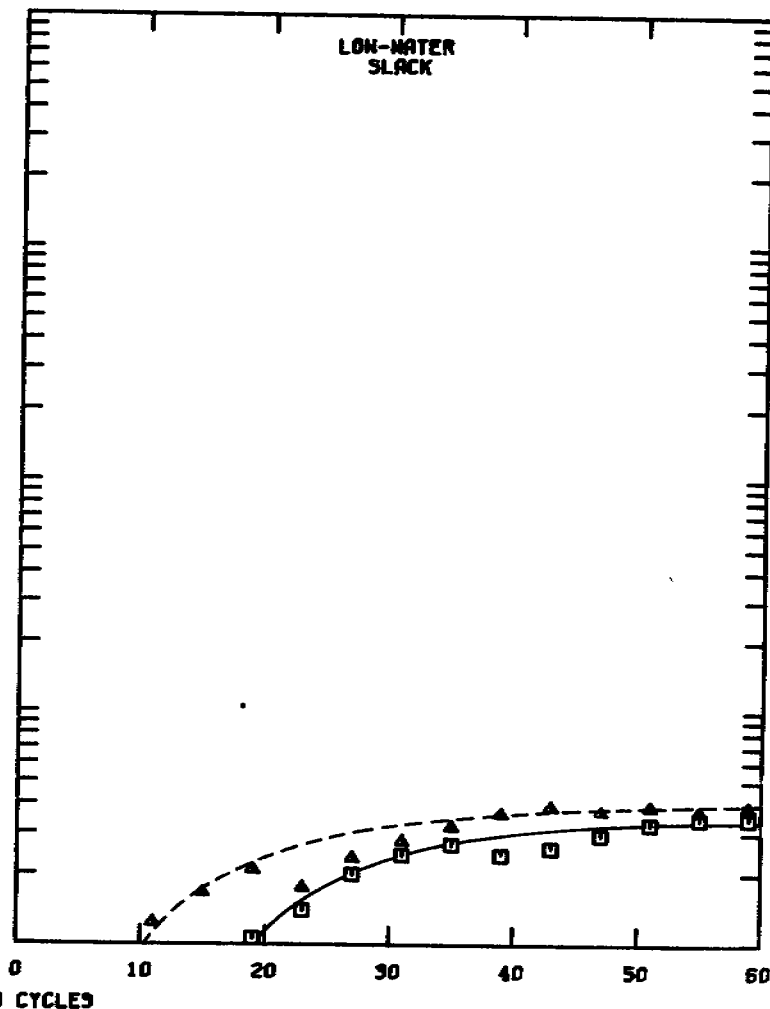
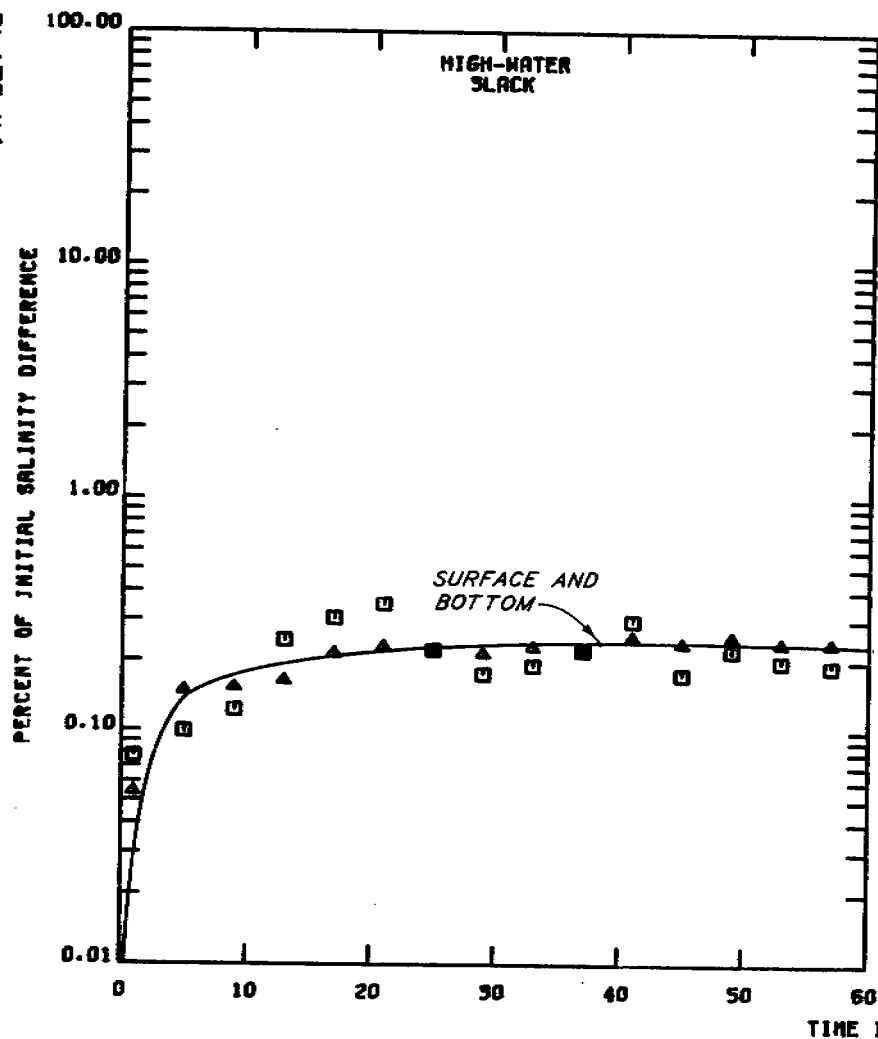
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 AGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-LOW FLOW PERIOD

STATION U2



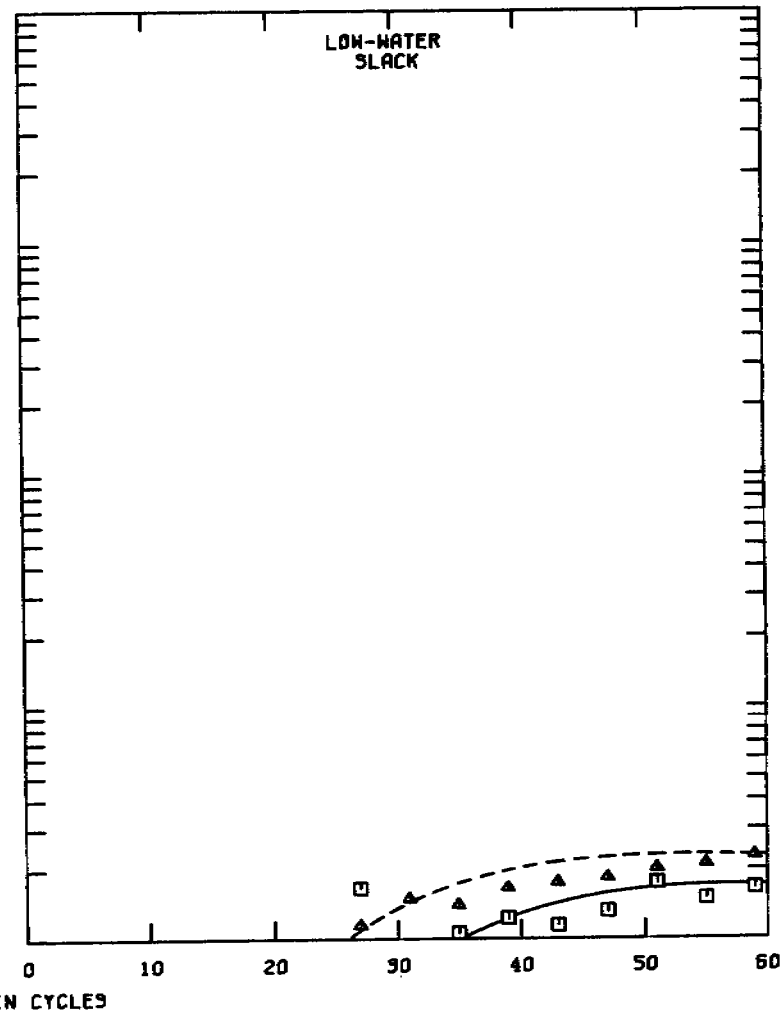
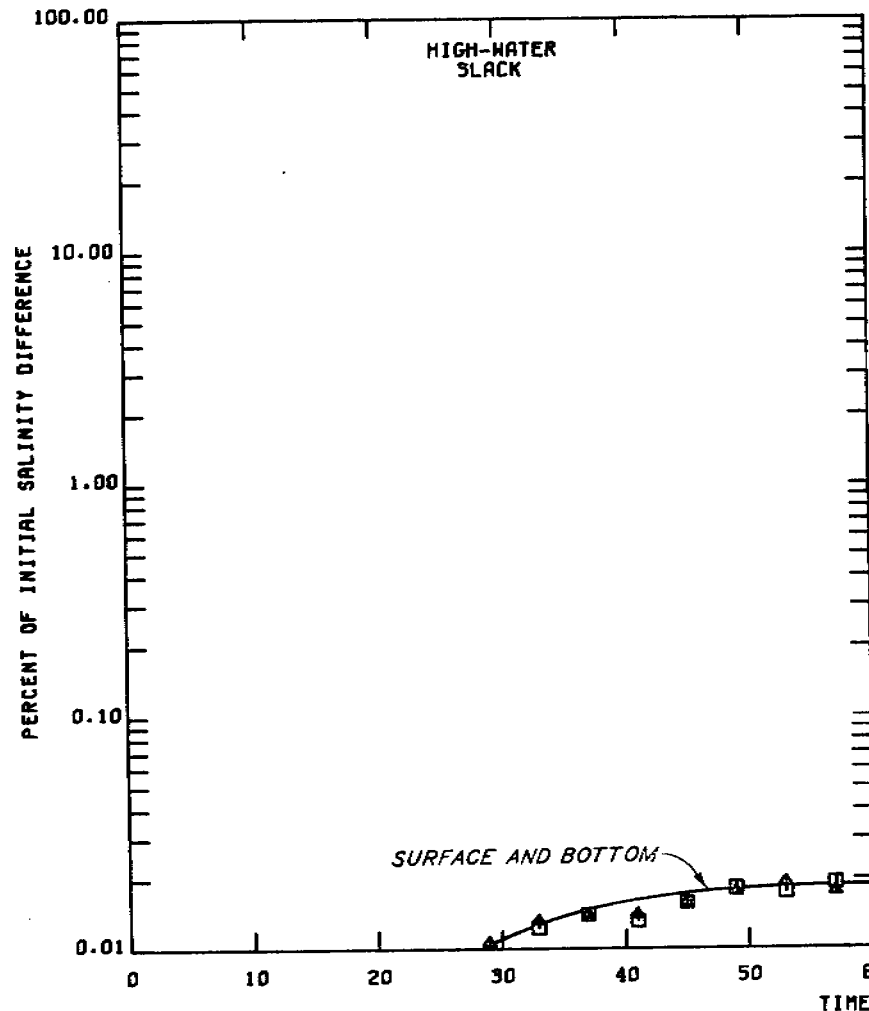
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 AGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION U3

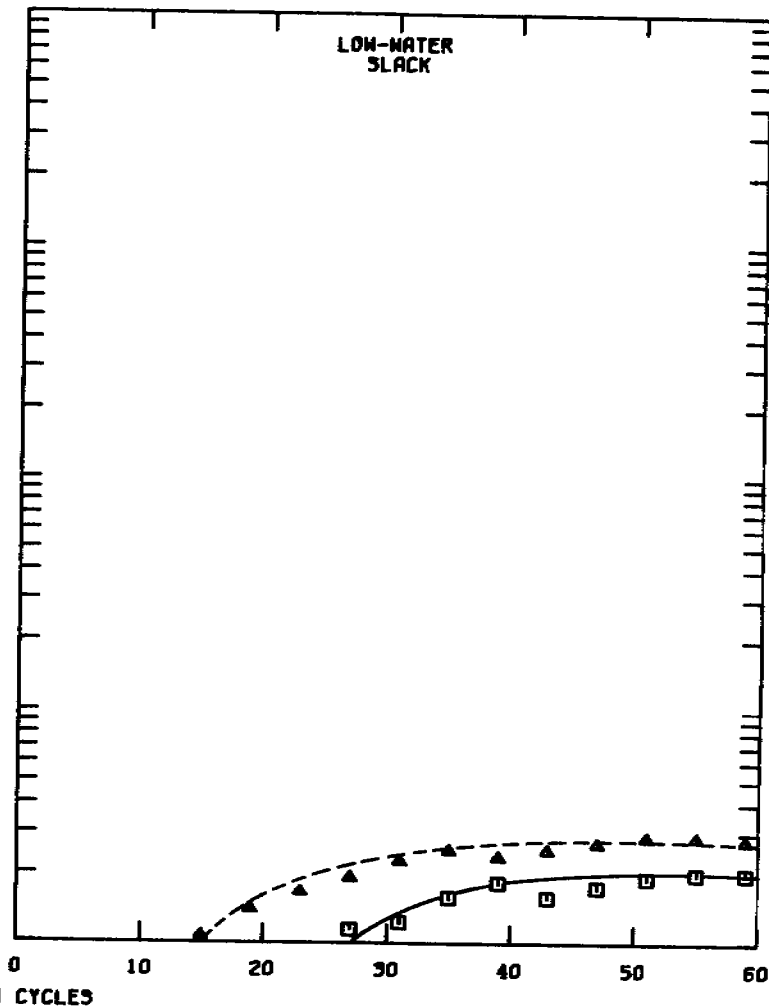
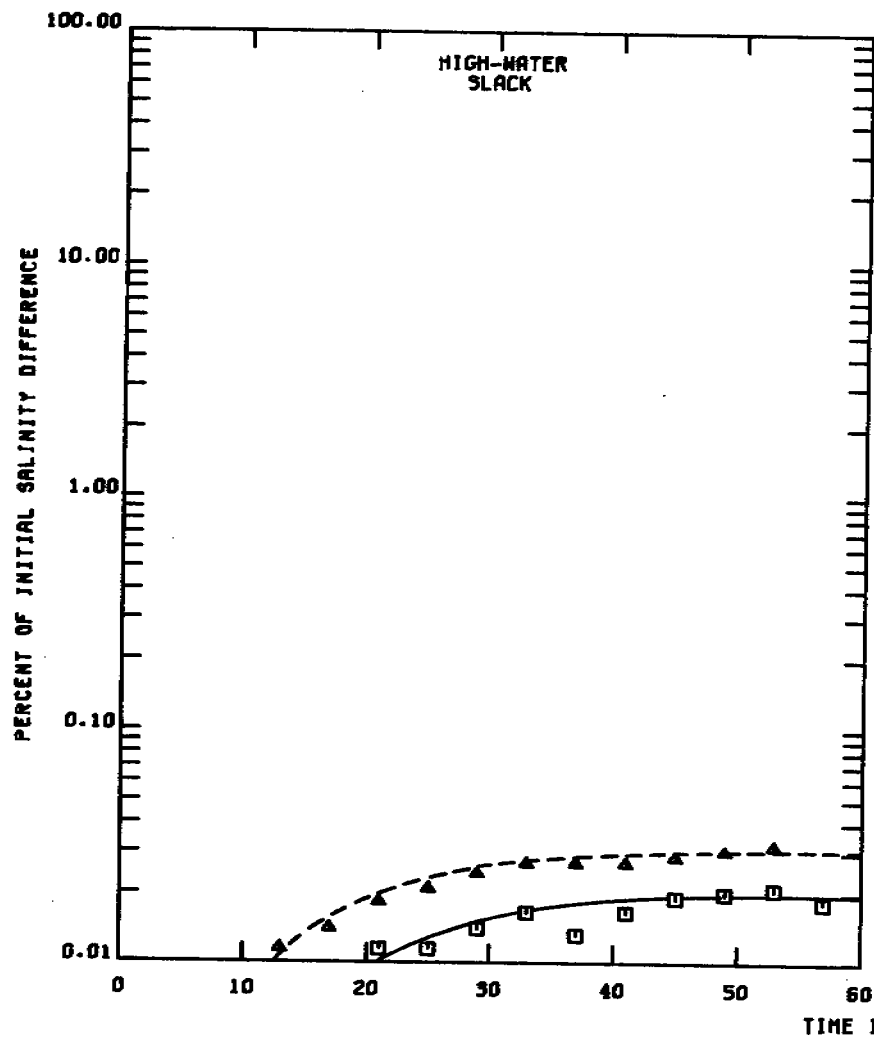


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CF9
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION U4



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ — — — BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION U5

PERCENT OF INITIAL SALINITY DIFFERENCE

100.00

10.00

1.00

0.10

0.01

0

10

20

30

40

50

60

HIGH-WATER
SLACK

TIME IN CYCLES

LOW-WATER
SLACK

0

10

20

30

40

50

60

TEST CONDITIONS

FRESH-WATER DISCHARGE
BASE SALINITY AT DIFFUSER
EFFLUENT SALINITY
INITIAL SALINITY DIFFERENCE
EFFLUENT INJECTION RATE

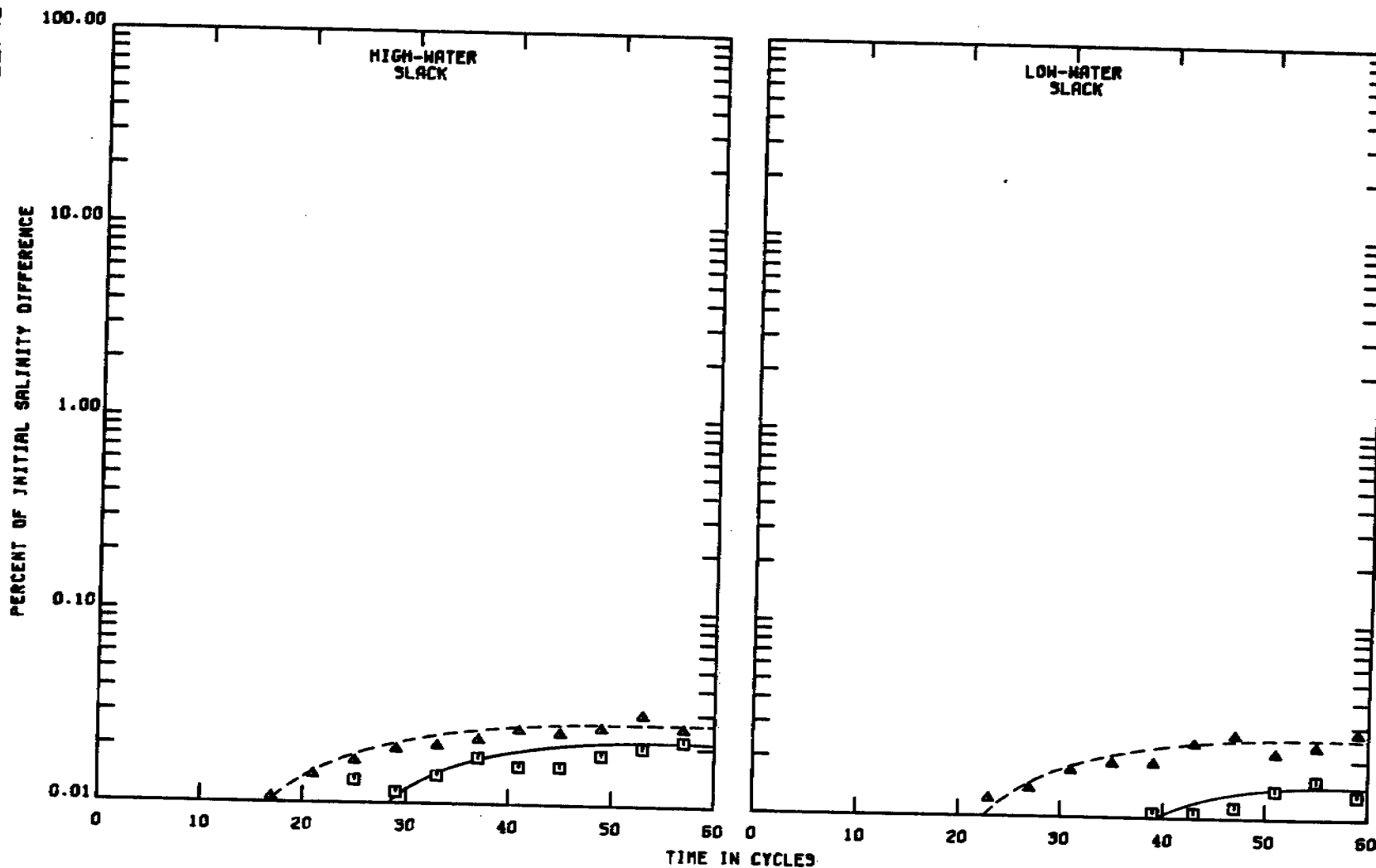
6542 CF3
21.0 PPT
32.4 PPT
11.4 PPT
21.2 AGD

LEGEND

□ — SURFACE
▲ — — — BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-LOW FLOW PERIOD

STATION U6



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION U7

PERCENT OF INITIAL SALINITY DIFFERENCE

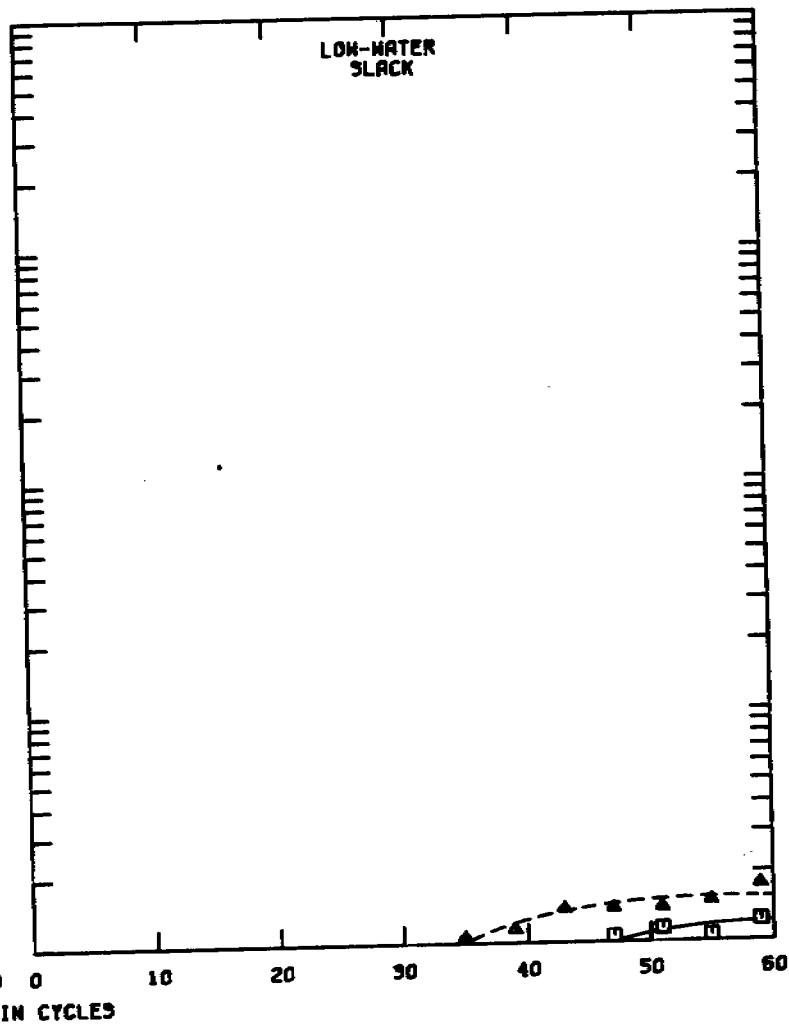
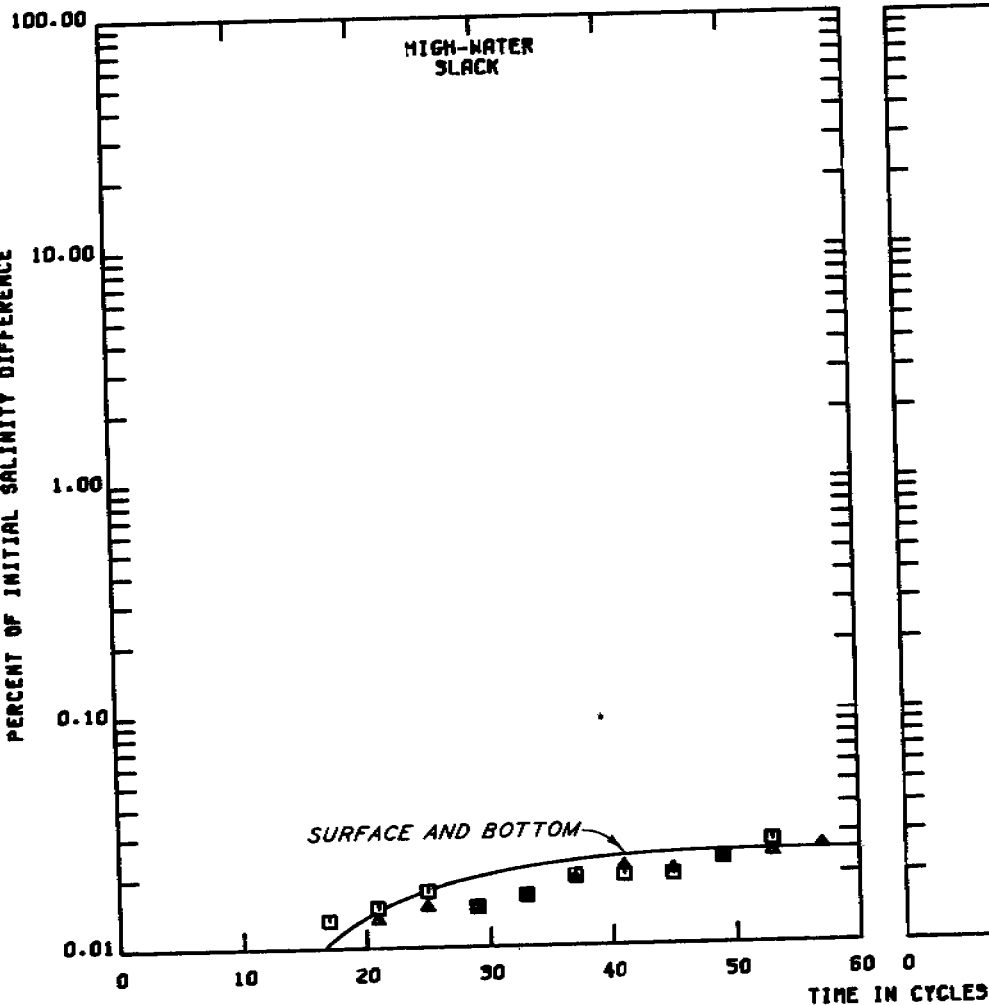


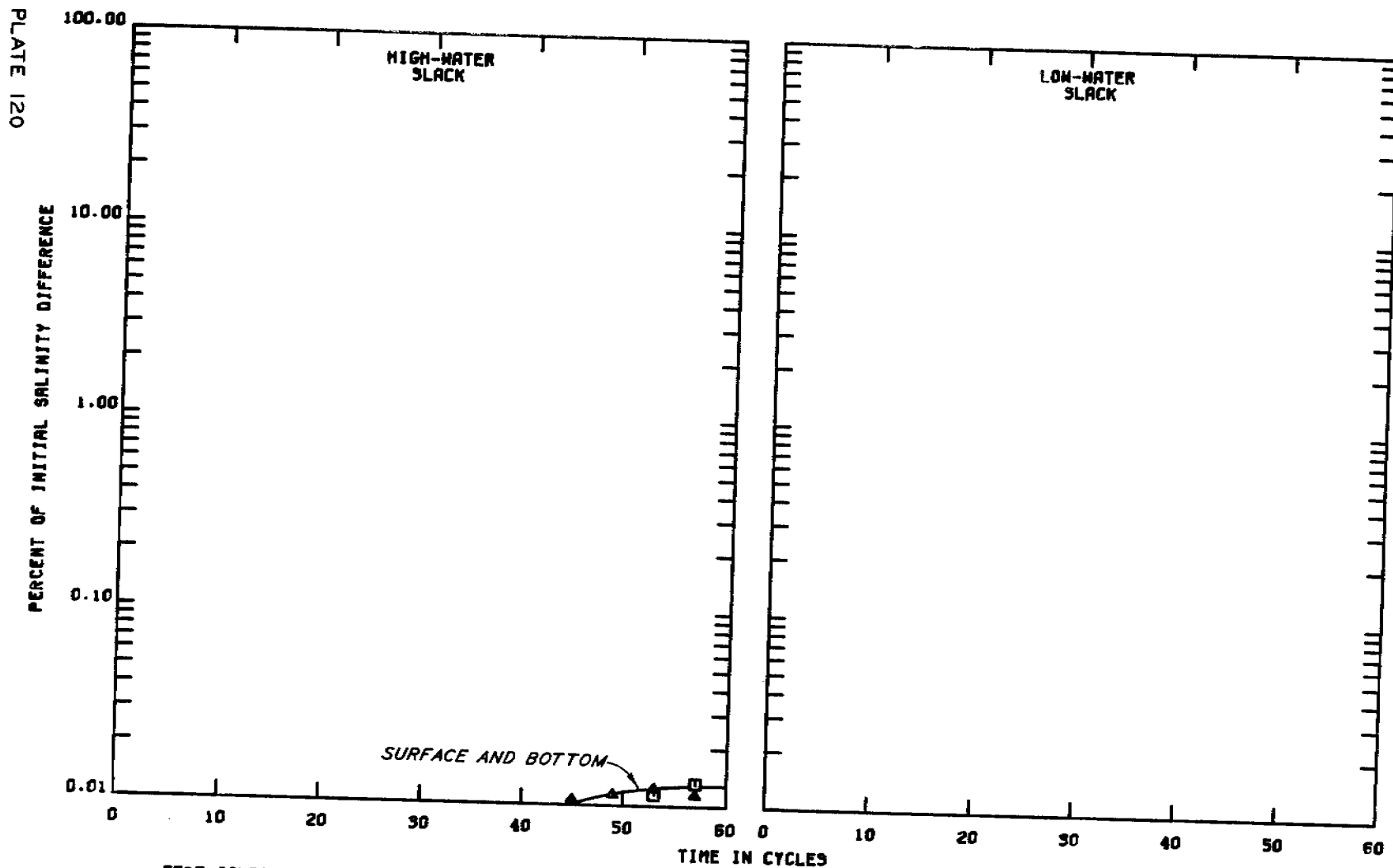
PLATE 119

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION U8



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION U9

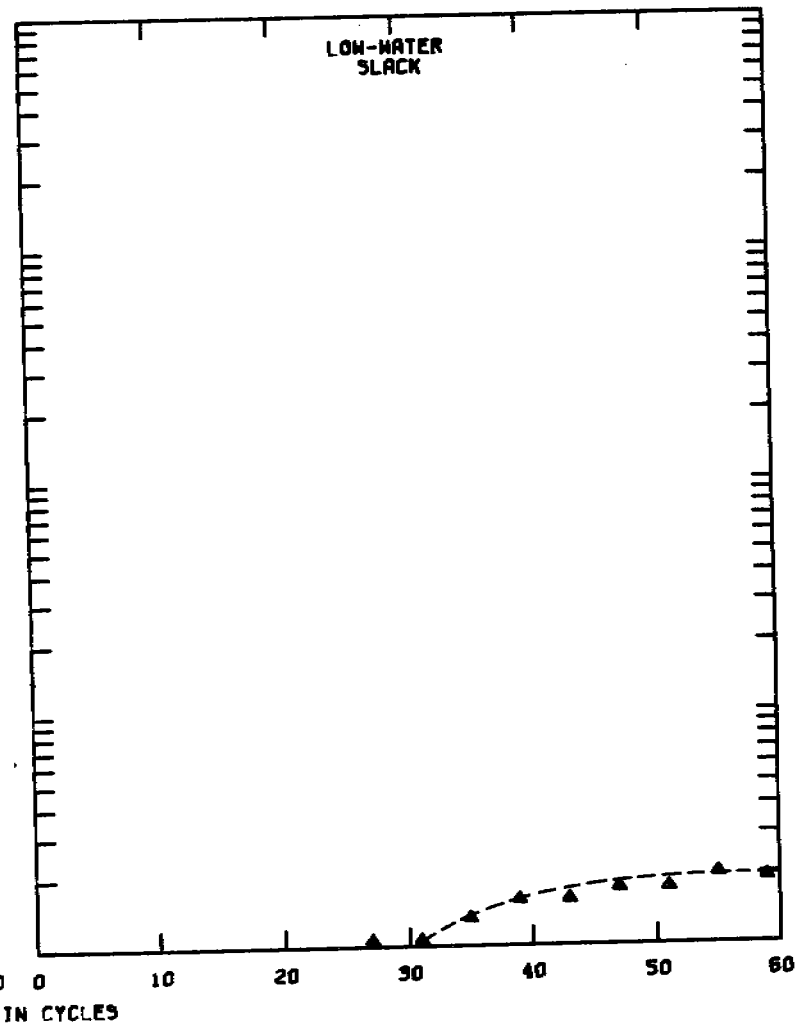
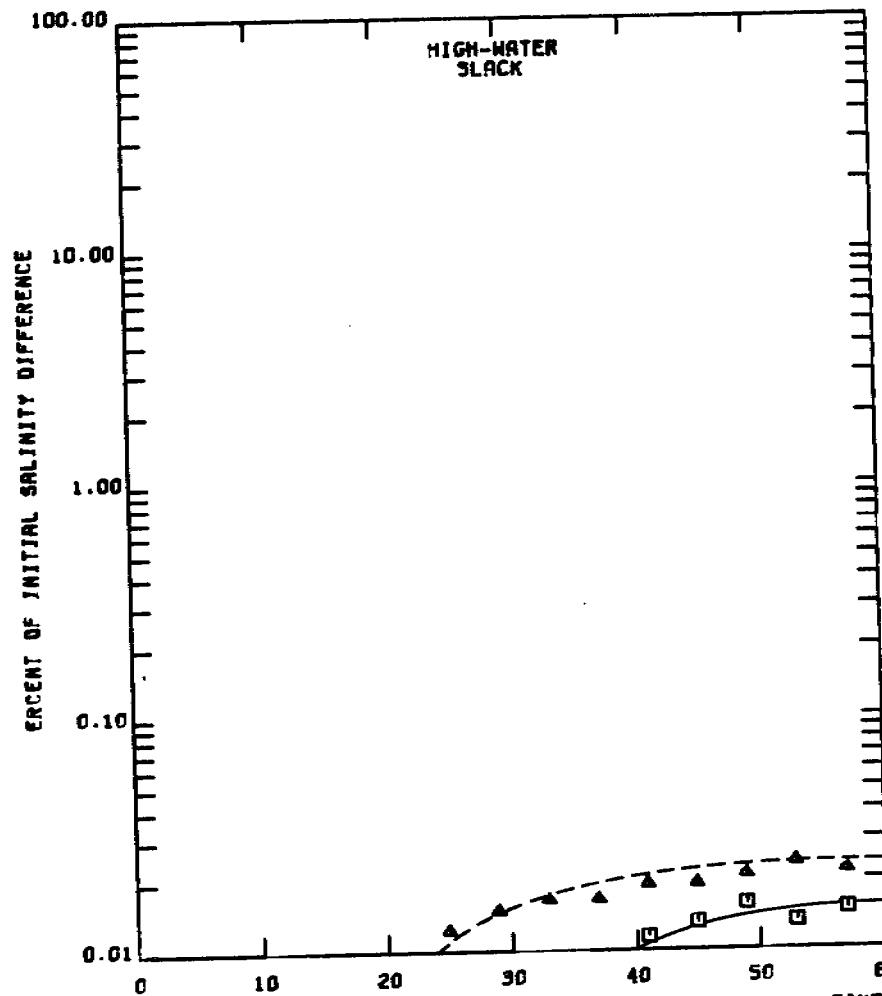


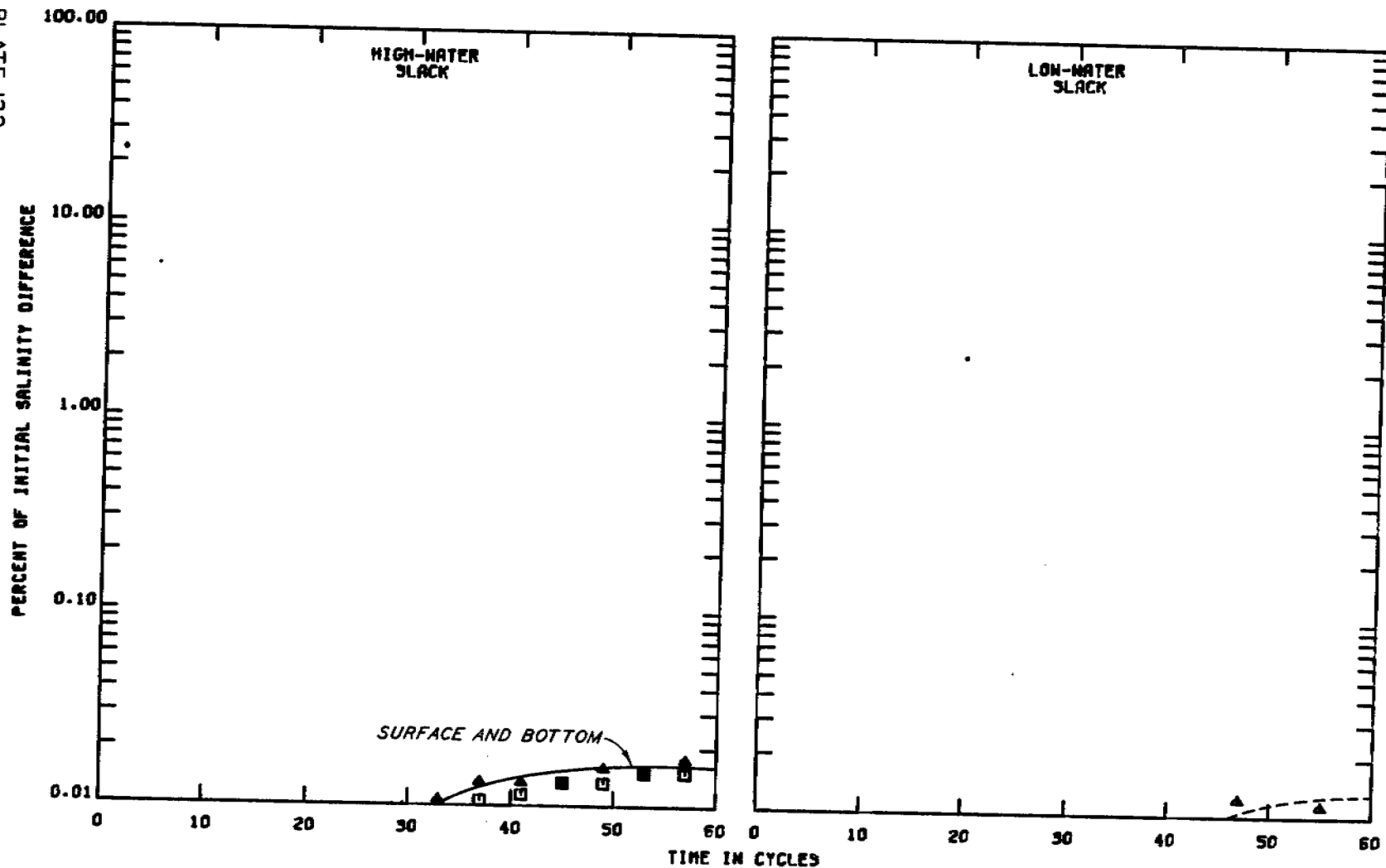
PLATE 121

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 △ — — — BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD
 STATION U10



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE.

6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD

STATION U11

PERCENT OF INITIAL SALINITY DIFFERENCE

HIGH-WATER
SLACKLOW-WATER
SLACK100.00
10.00
1.00
0.10
0.01

0

10

20

30

40

50

60

TIME IN CYCLES

0

10

20

30

40

50

60

TEST CONDITIONS

FRESH-WATER DISCHARGE
BASE SALINITY AT DIFFUSER
EFFLUENT SALINITY
INITIAL SALINITY DIFFERENCE
EFFLUENT INJECTION RATE

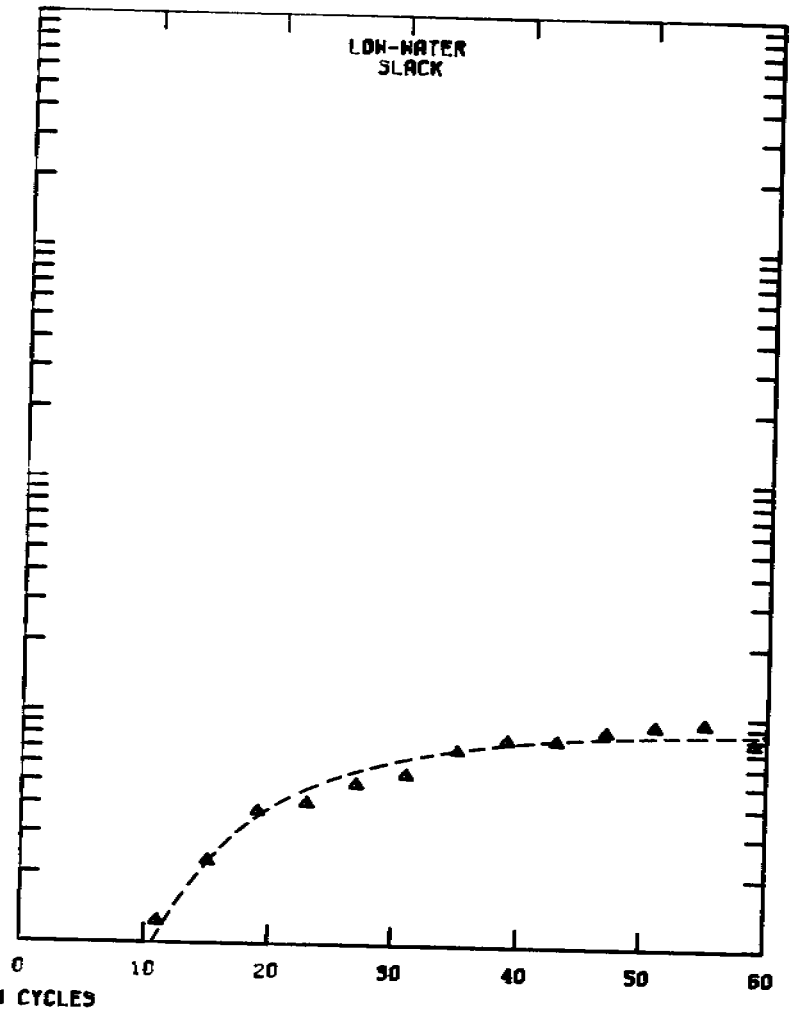
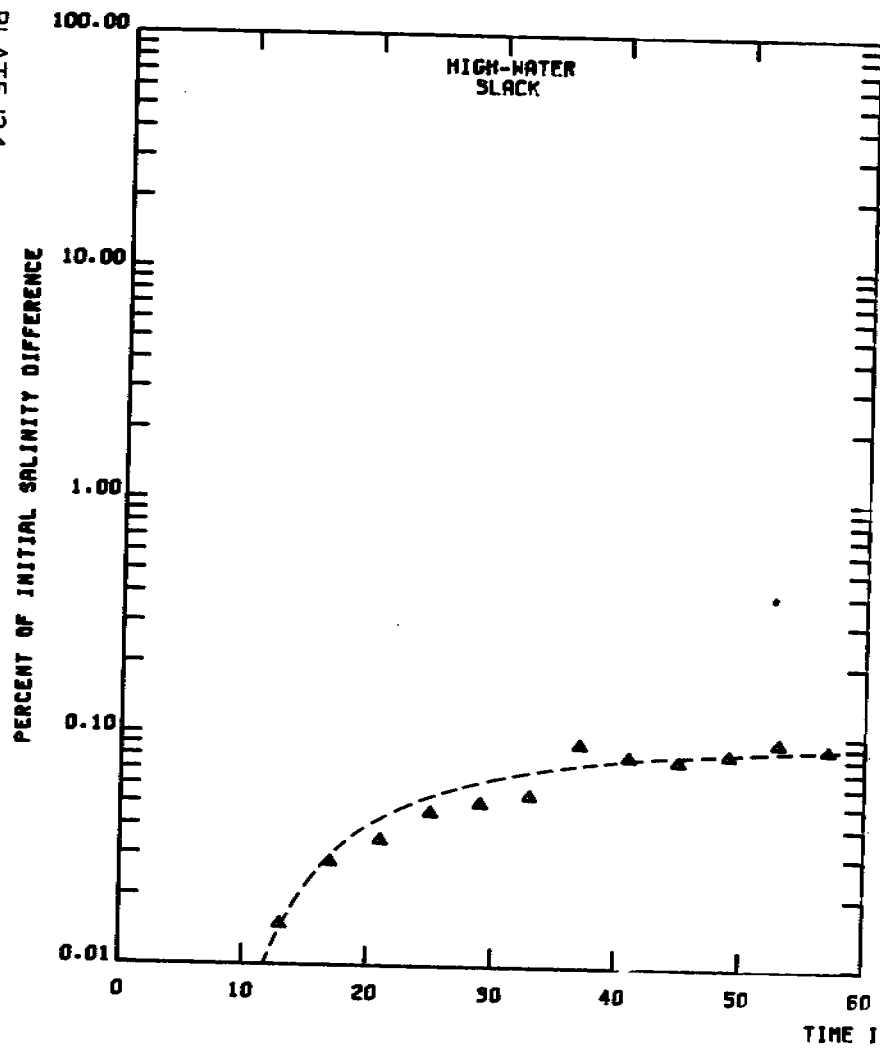
6542 CFS
21.0 PPT
32.4 PPT
11.4 PPT
21.2 MGD

LEGEND

□ ——— SURFACE
▲ - - - BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-LOW FLOW PERIOD

STATION CRI

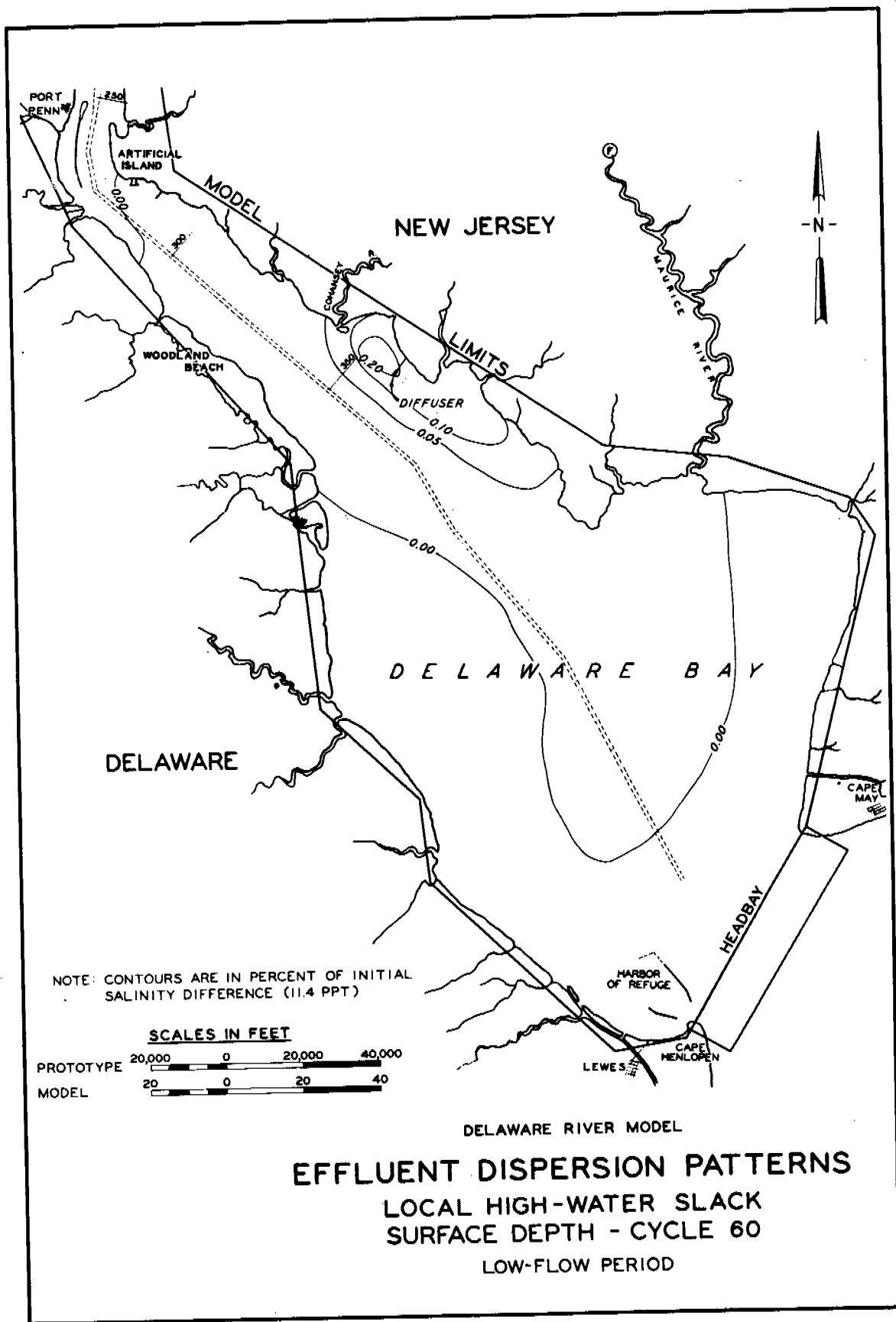


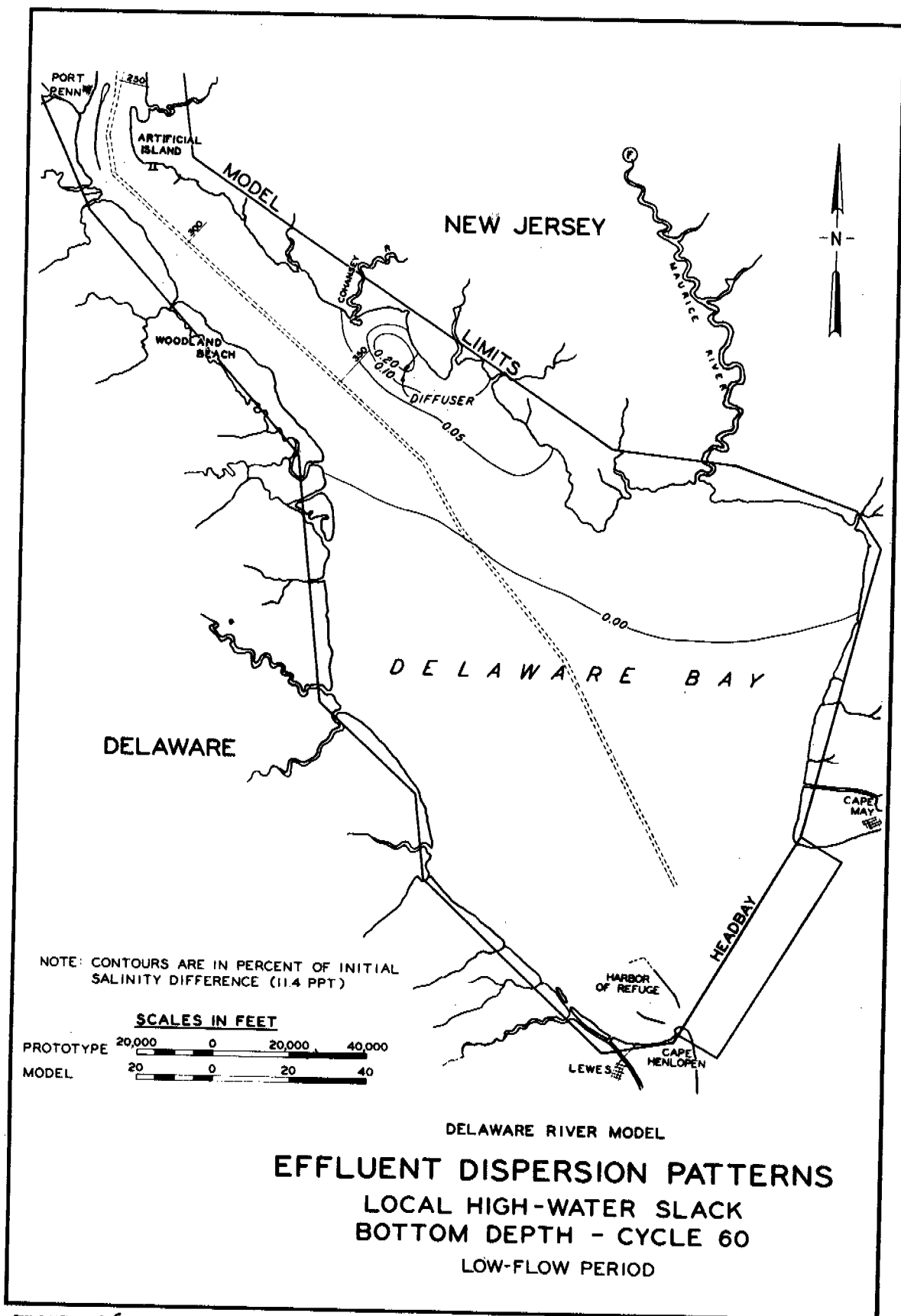
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

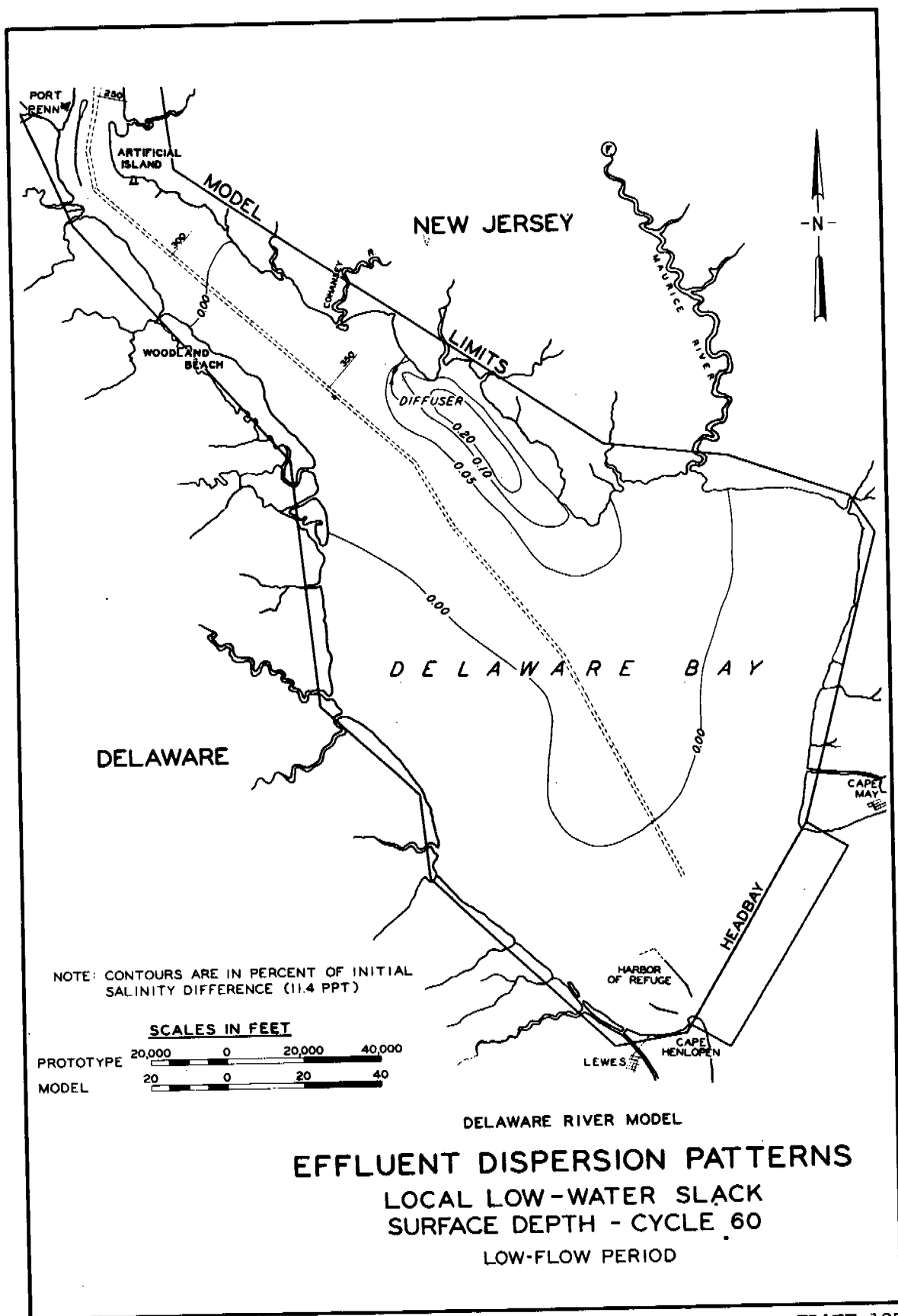
6542 CFS
 21.0 PPT
 32.4 PPT
 11.4 PPT
 21.2 MGD

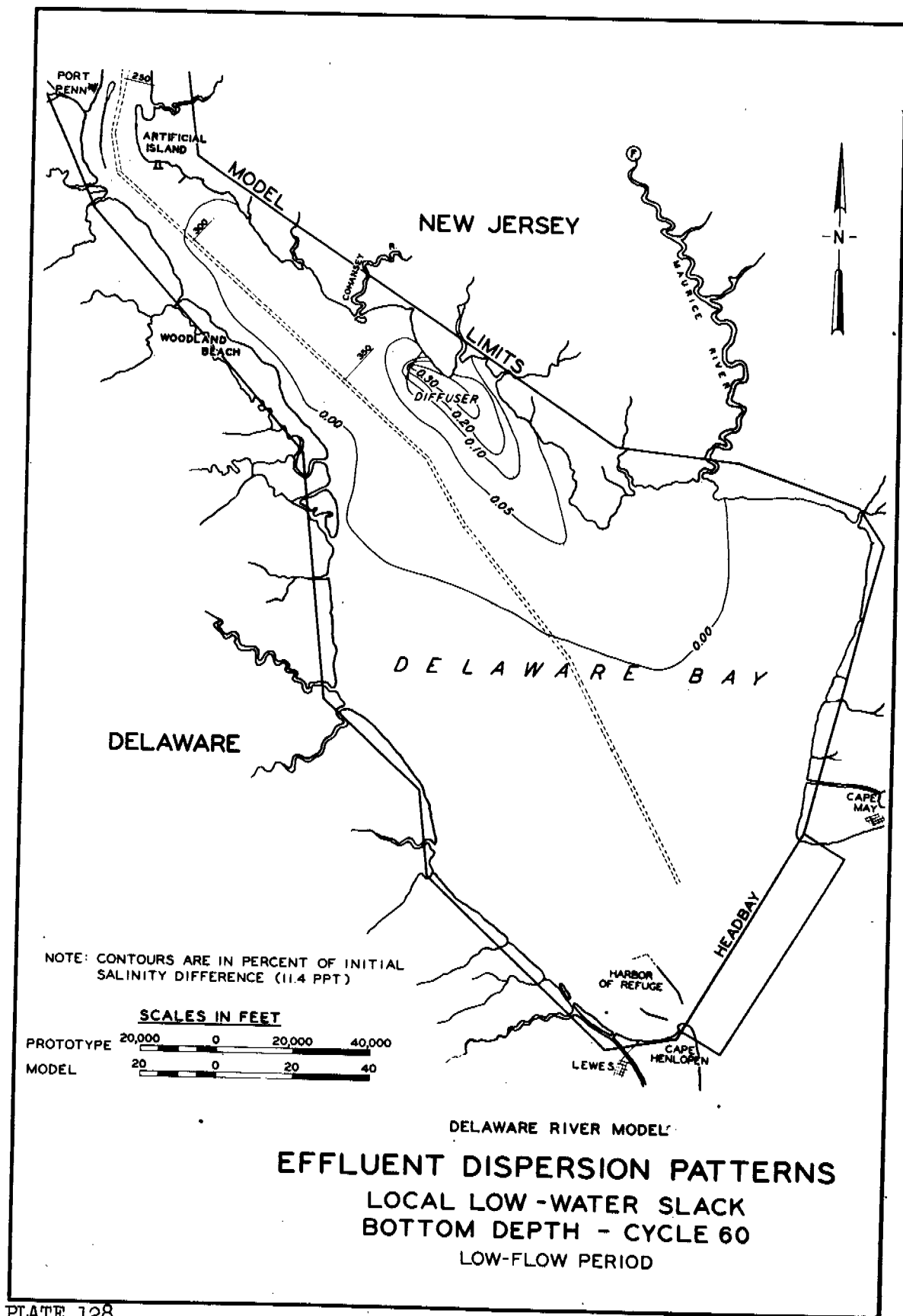
LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

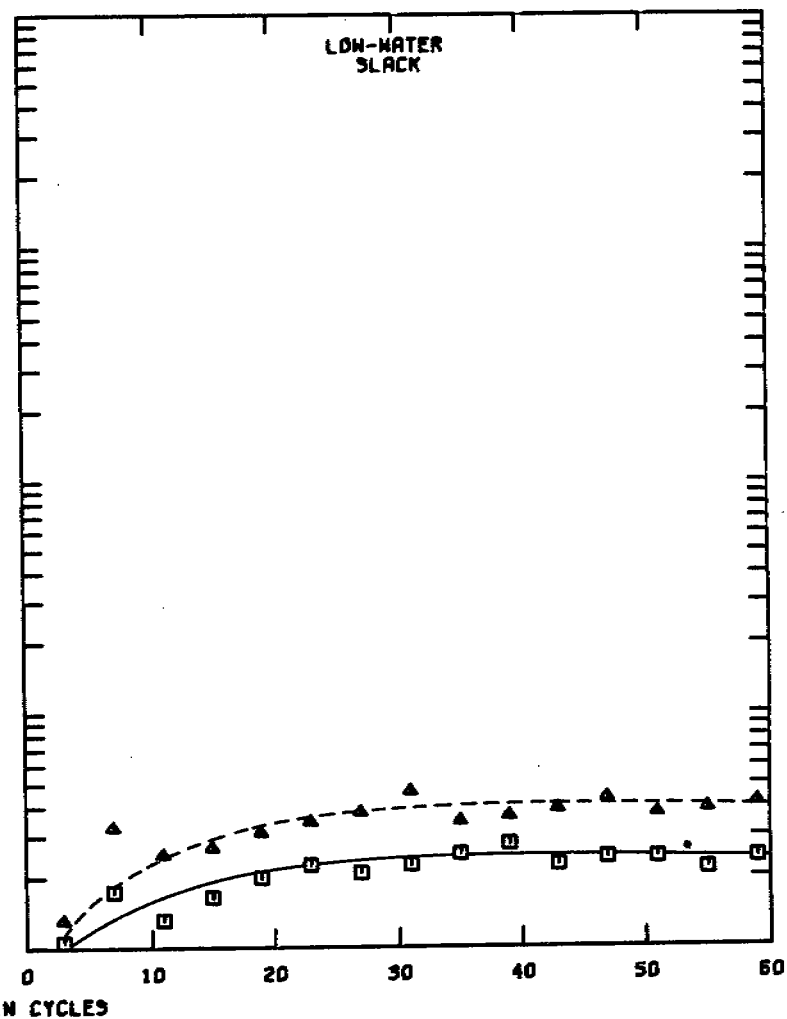
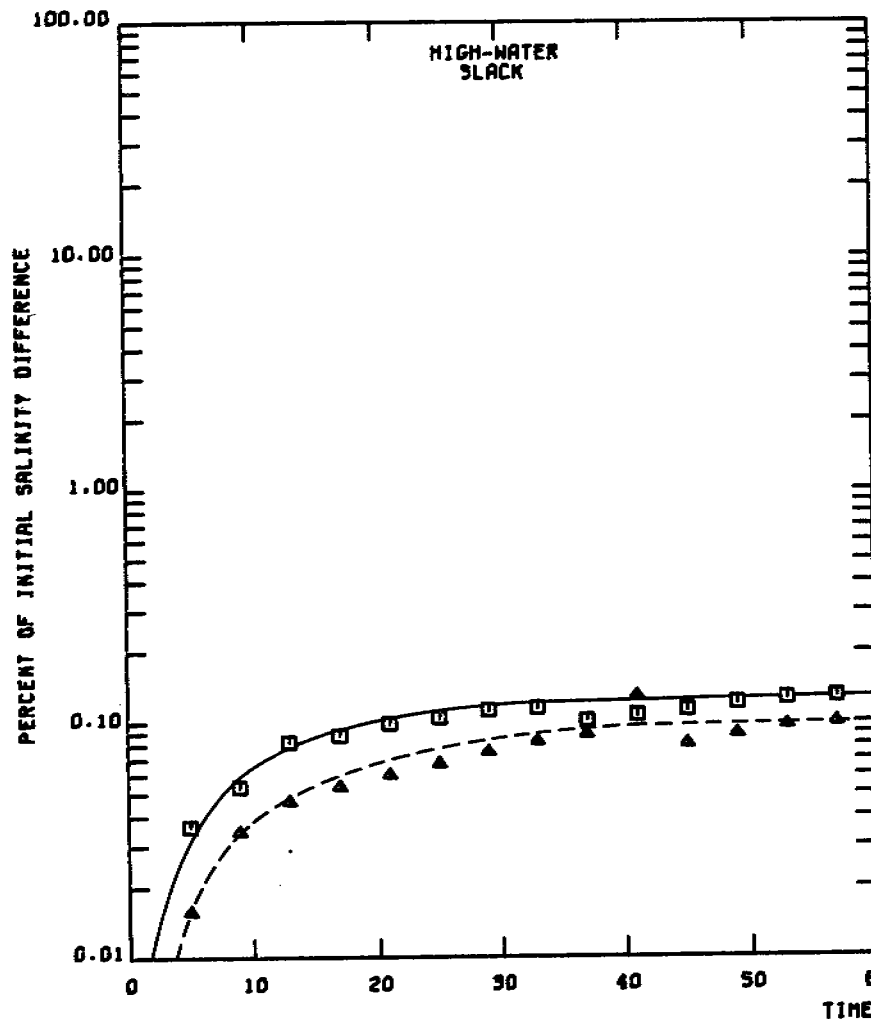
DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-LOW FLOW PERIOD











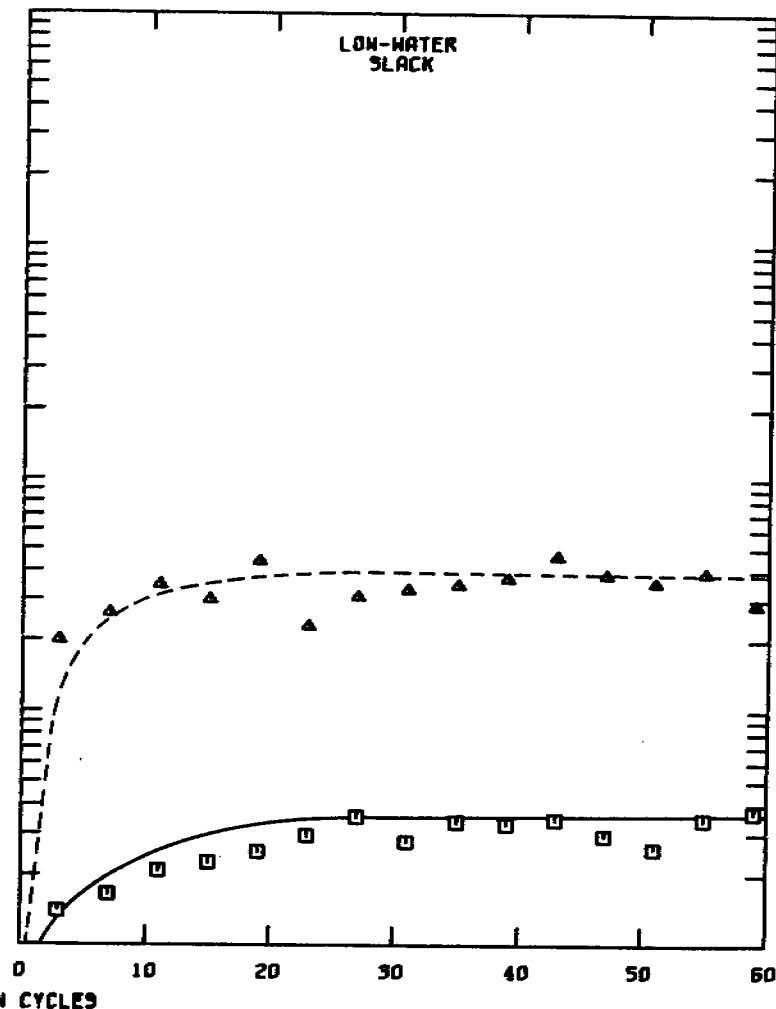
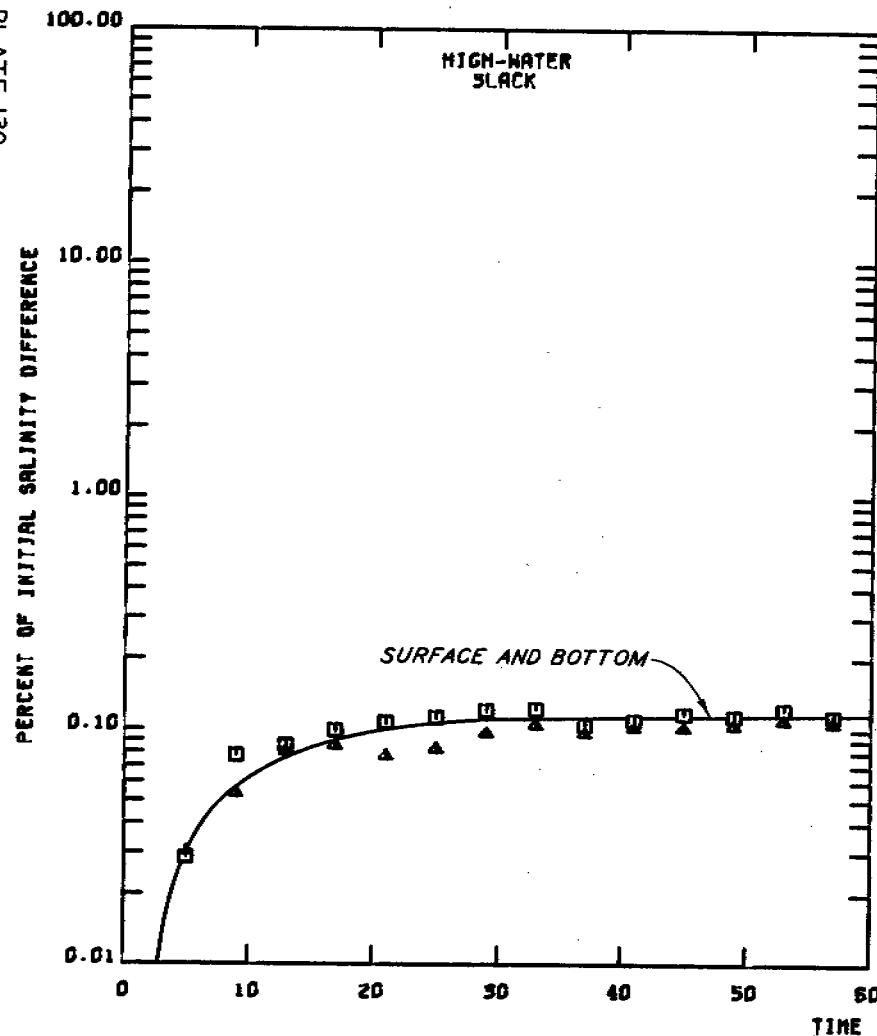
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION DI



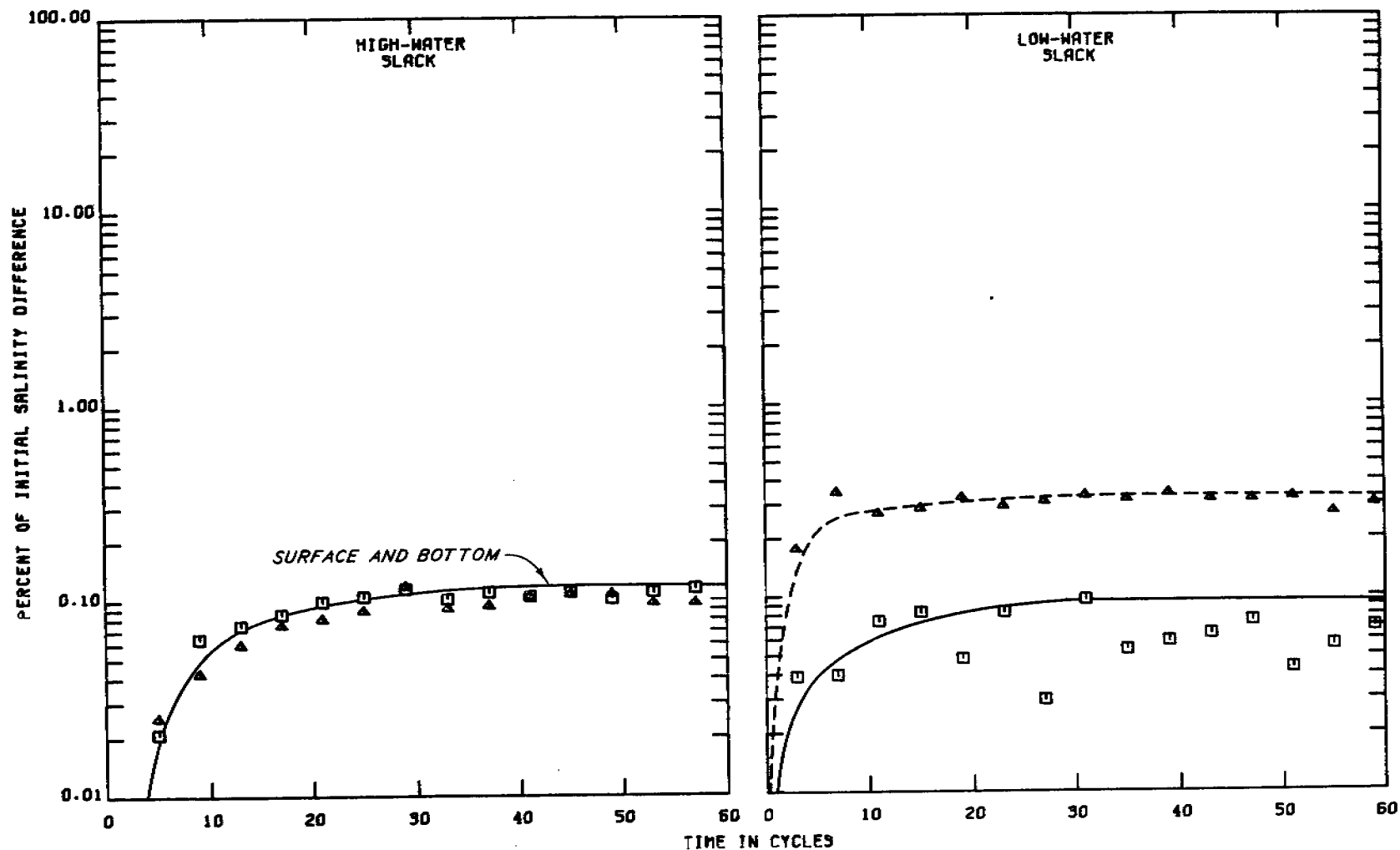
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.8 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD**

STATION 02

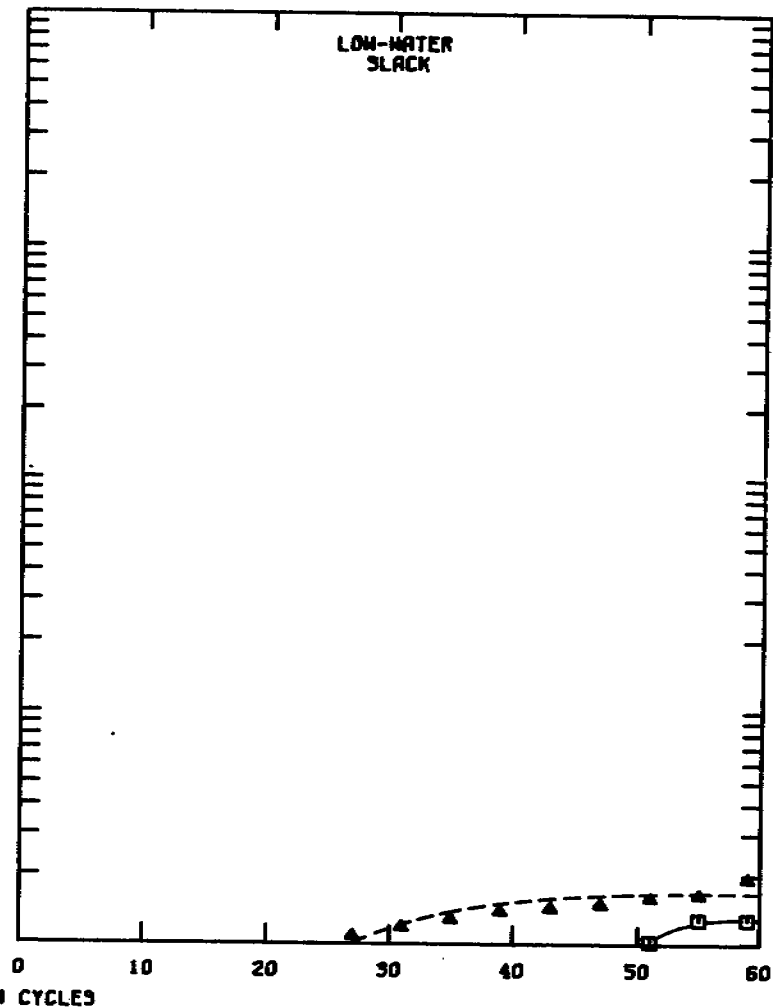
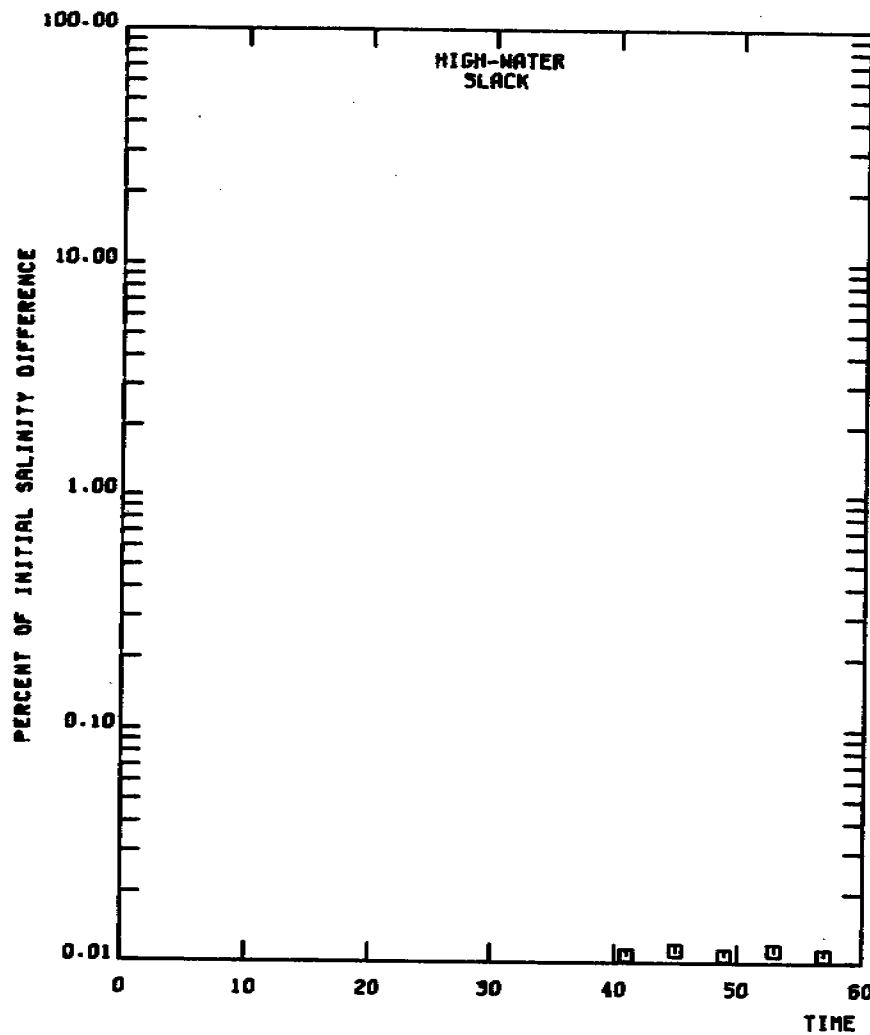


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D3



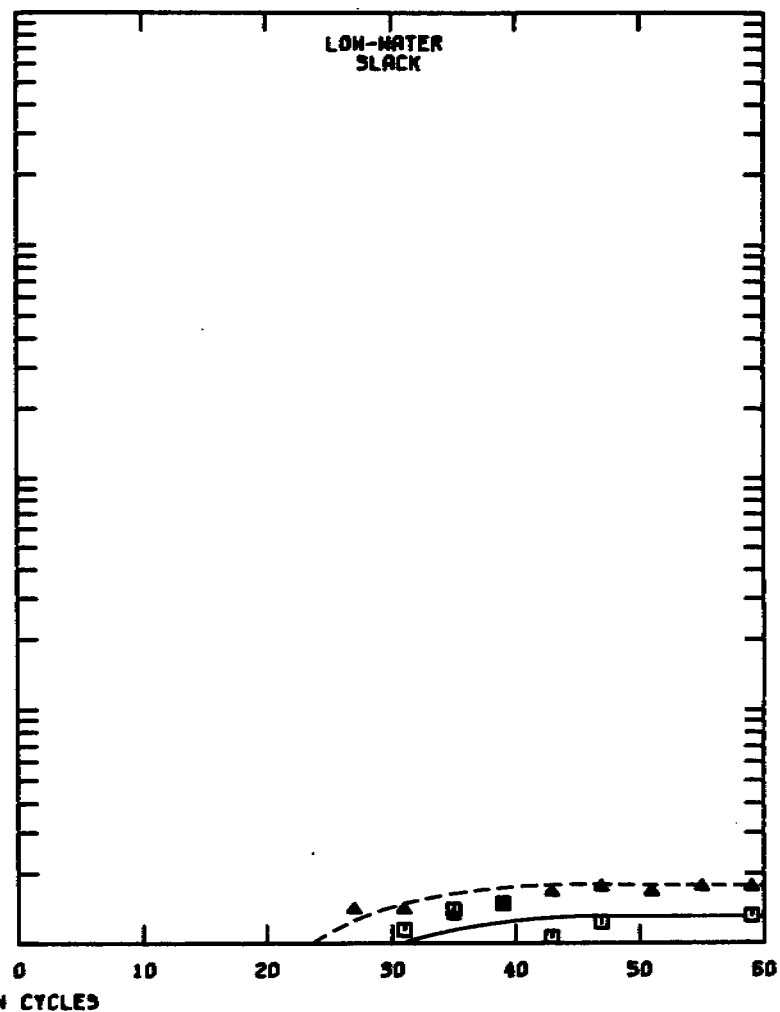
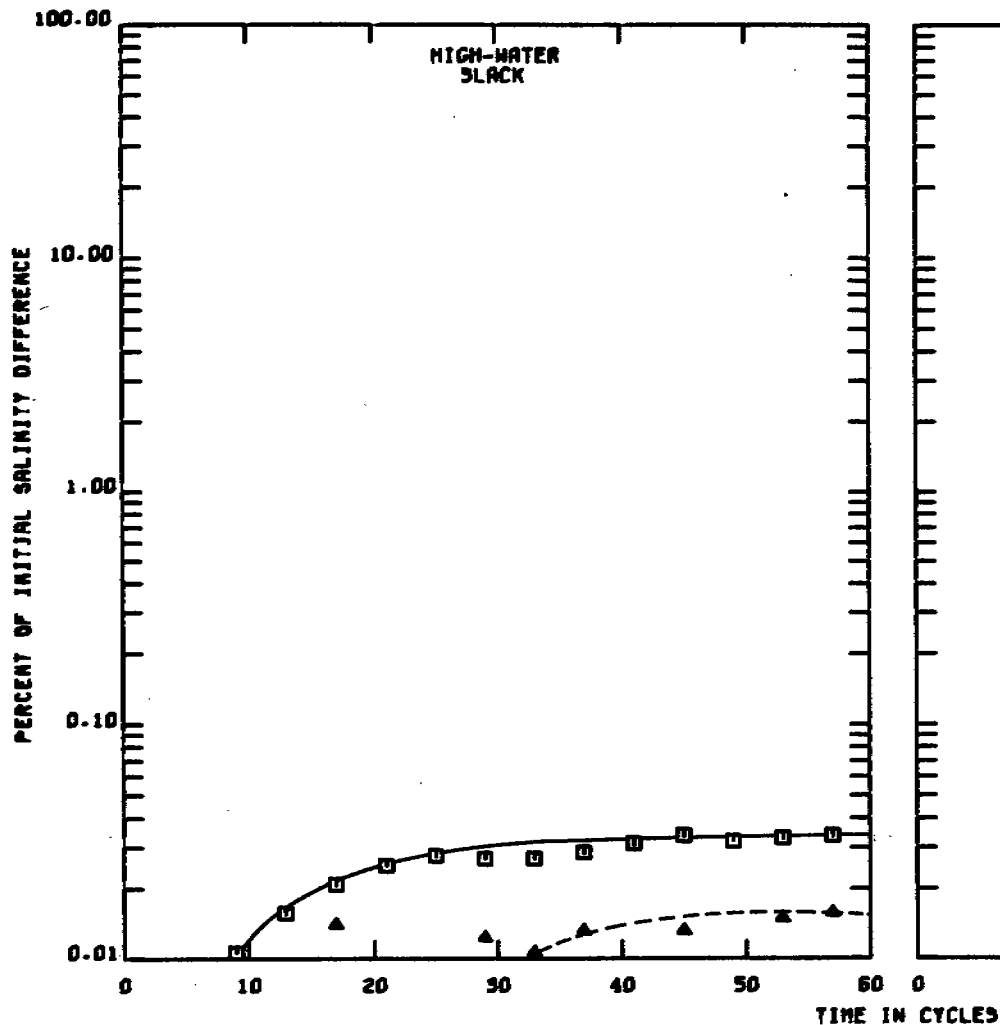
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 NGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D5



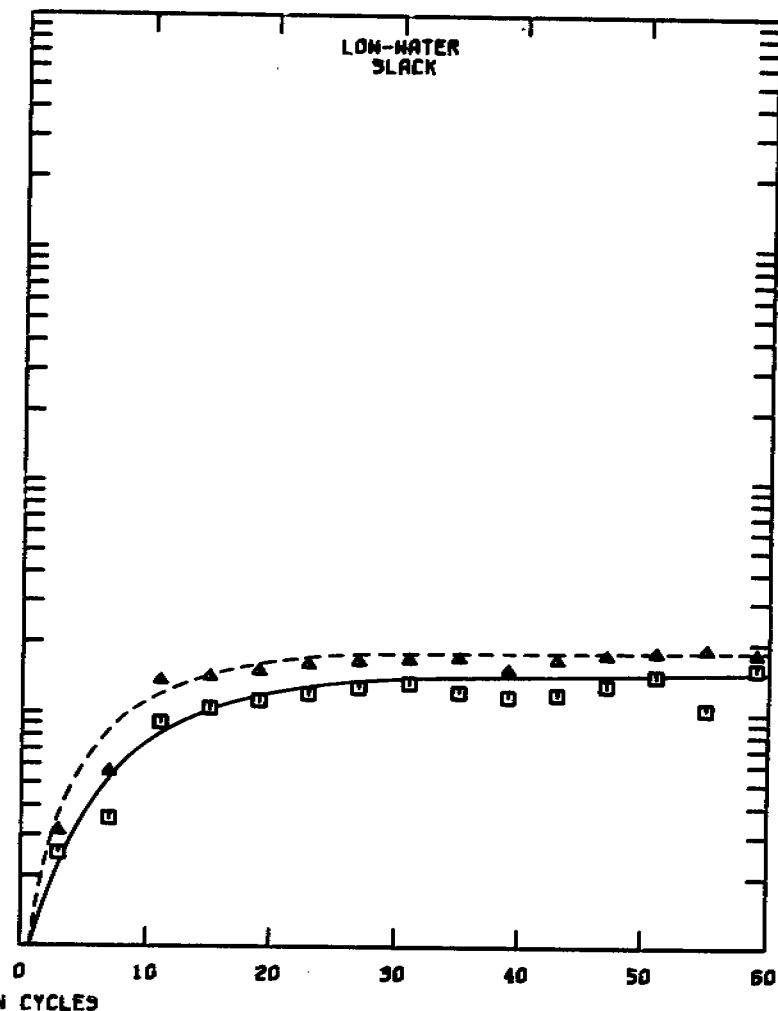
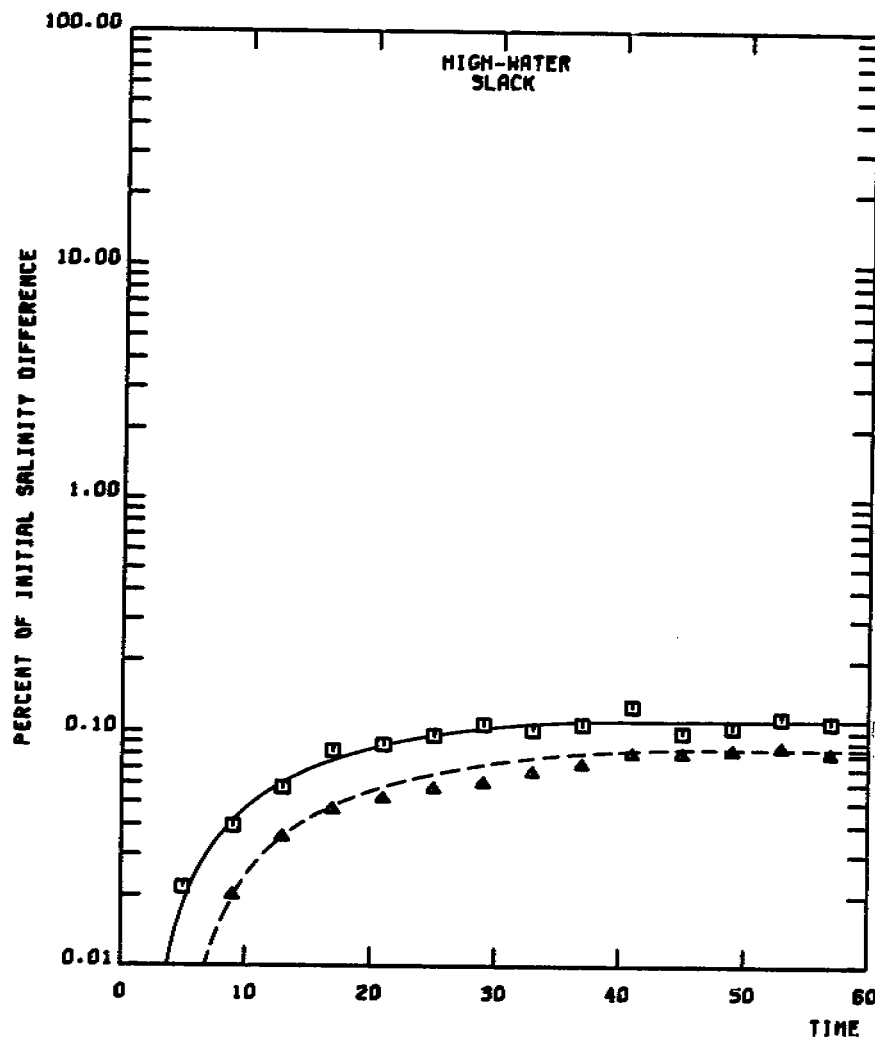
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD**

STATION D6



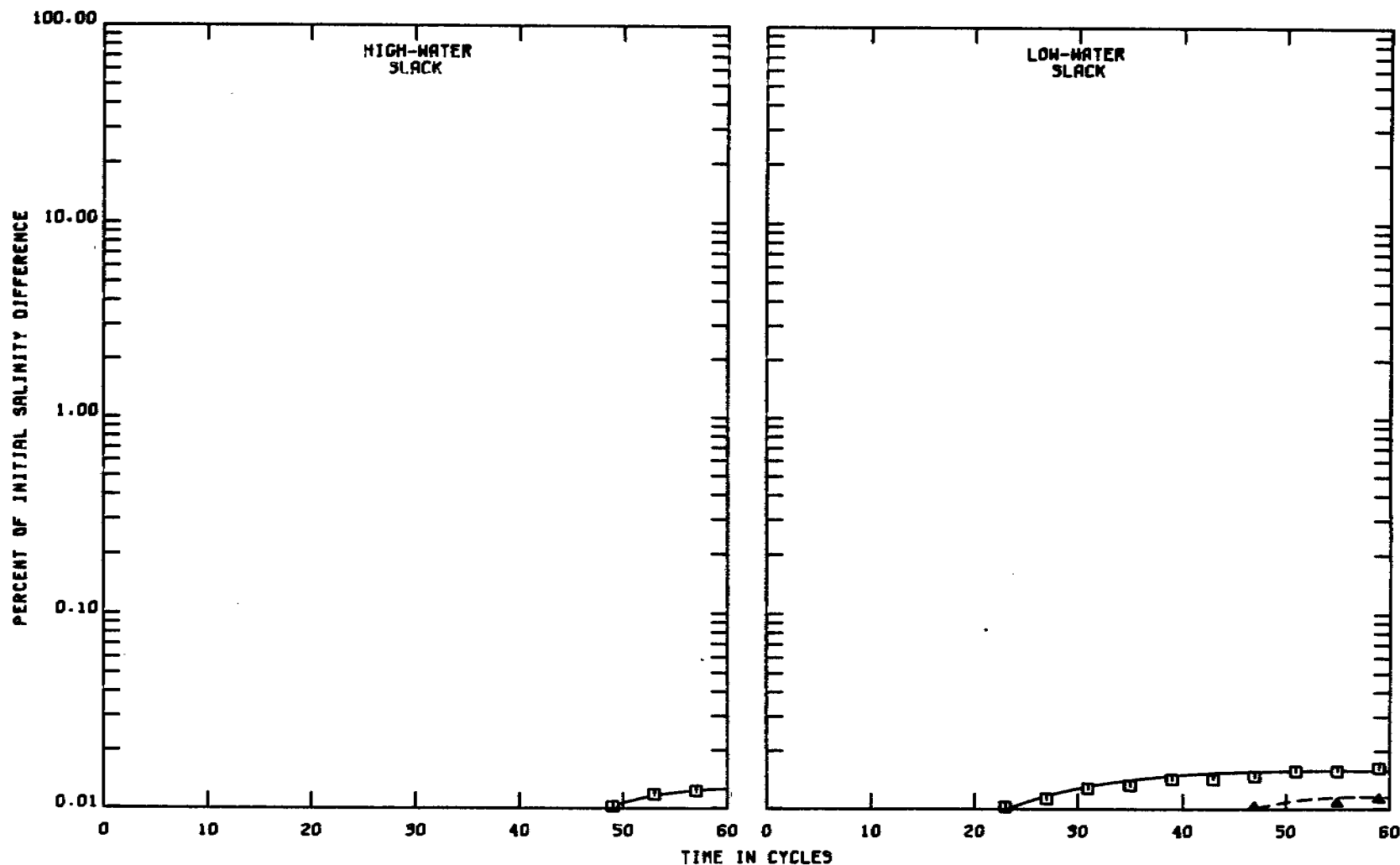
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD**

STATION D7



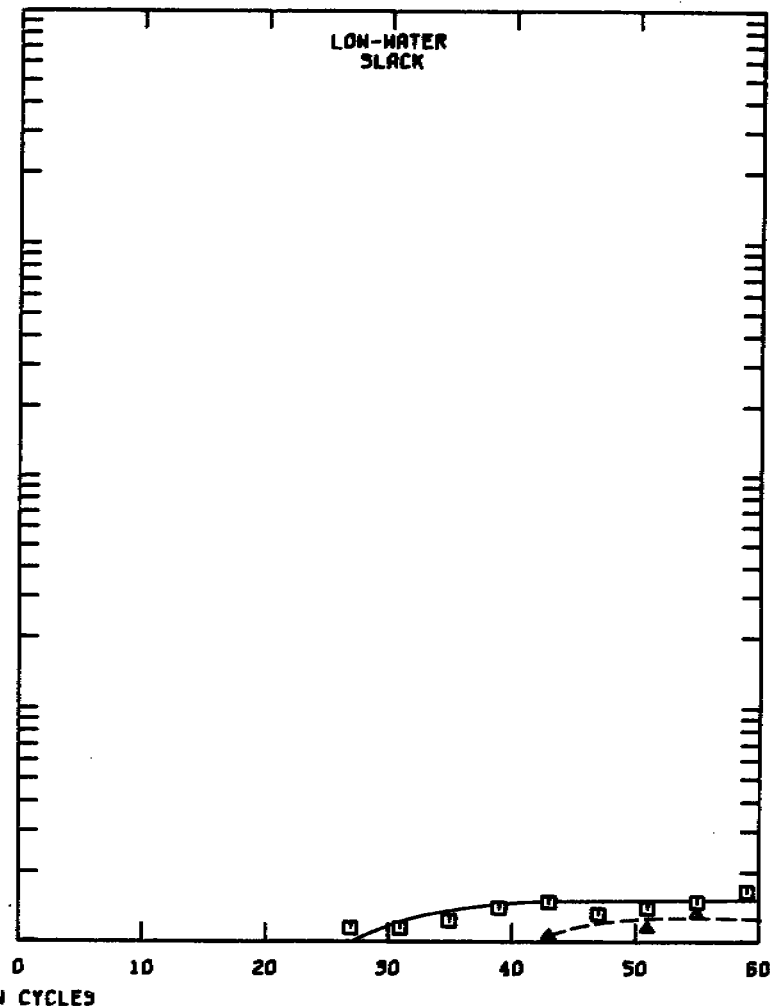
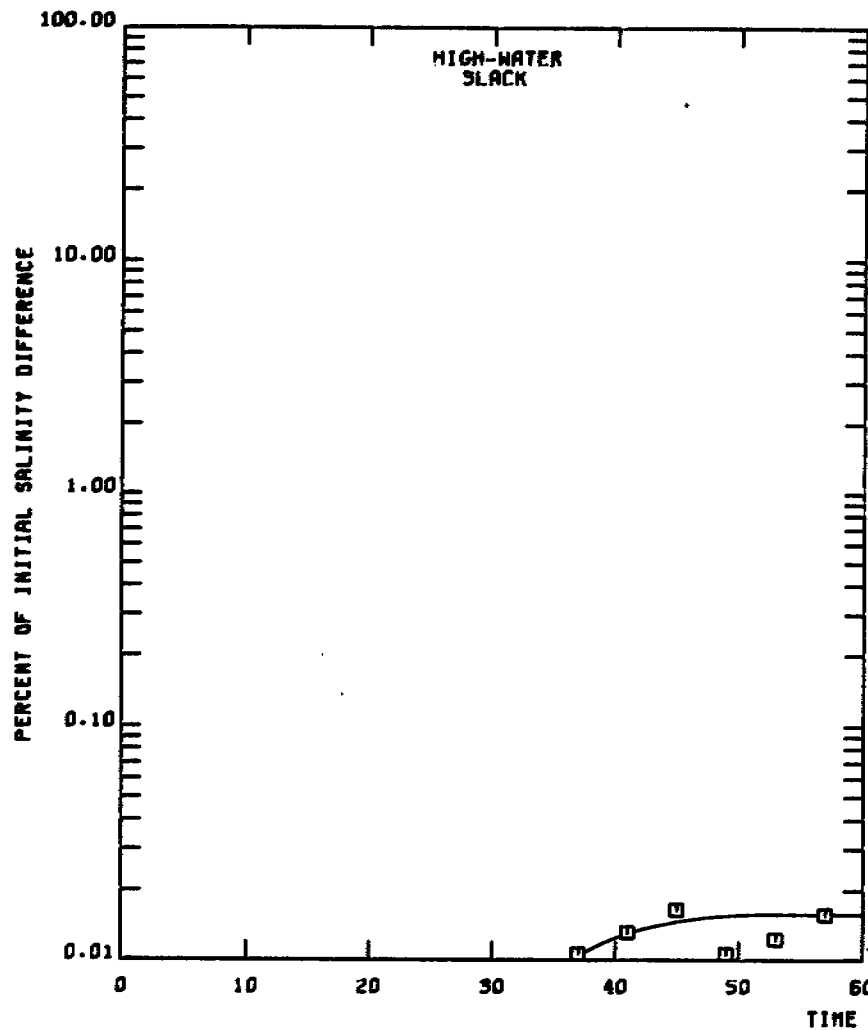
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D9



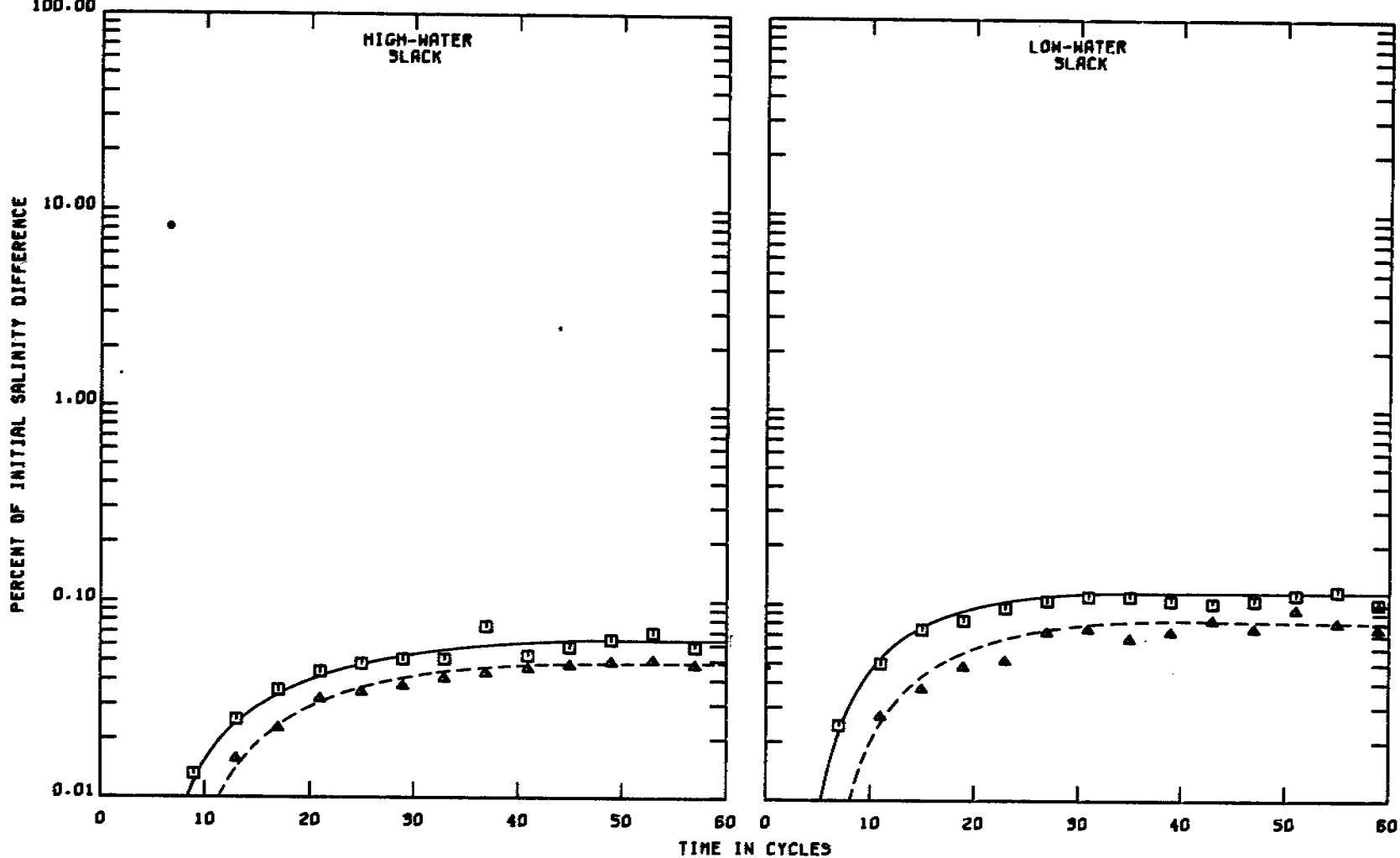
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D10



TEST CONDITIONS

FRESH-WATER DISCHARGE

BASE SALINITY AT DIFFUSER

EFFLUENT SALINITY

INITIAL SALINITY DIFFERENCE

EFFLUENT INJECTION RATE

20200 CFS

17.6 PPT

29.0 PPT

11.4 PPT

21.2 MGD

LEGEND

□ — SURFACE

▲ - - - BOTTOM

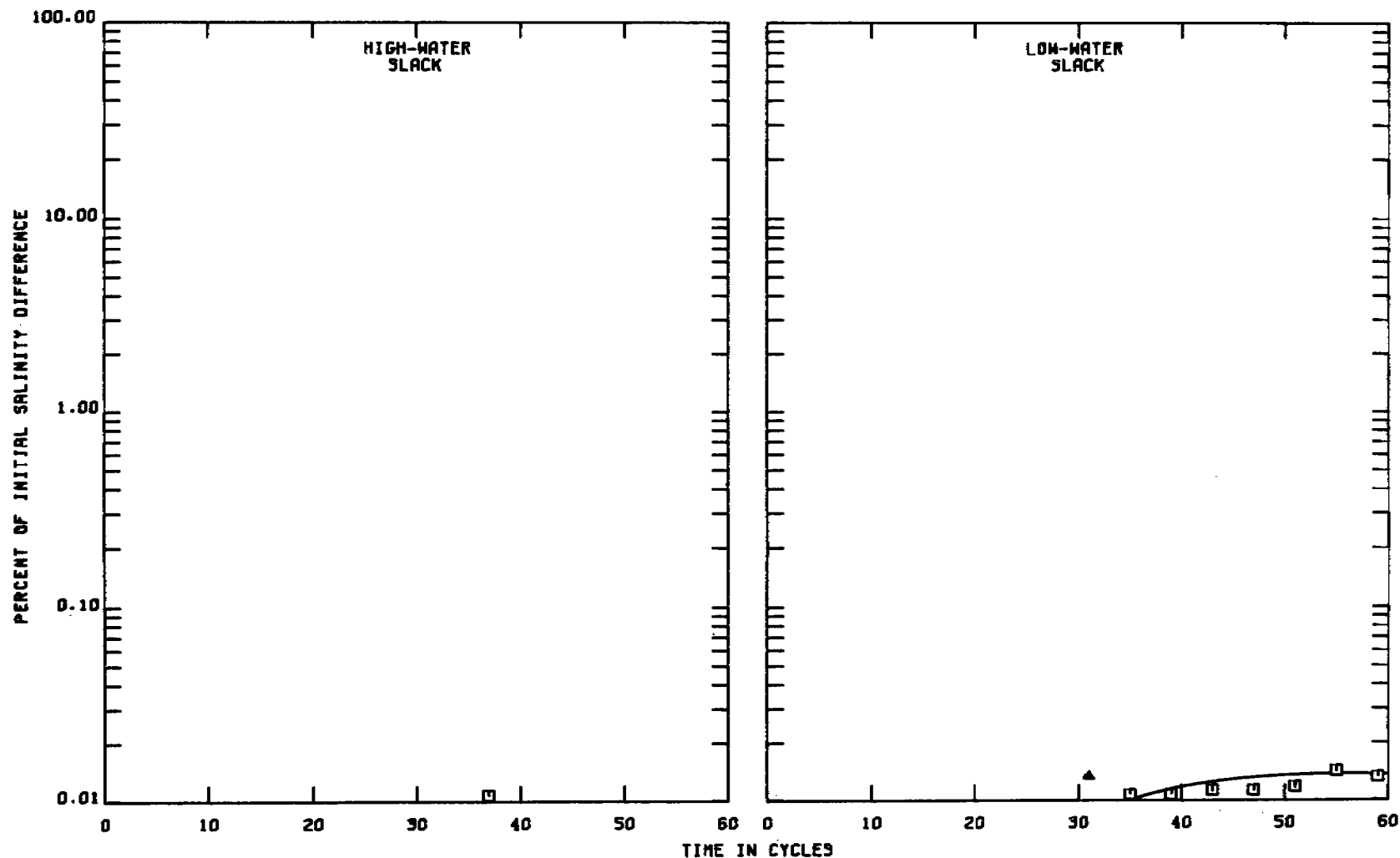
DELAWARE RIVER MODEL

SALINE WATER

DISPERSION TEST

10MGD PLANT-MEAN FLOW PERIOD

STATION DII



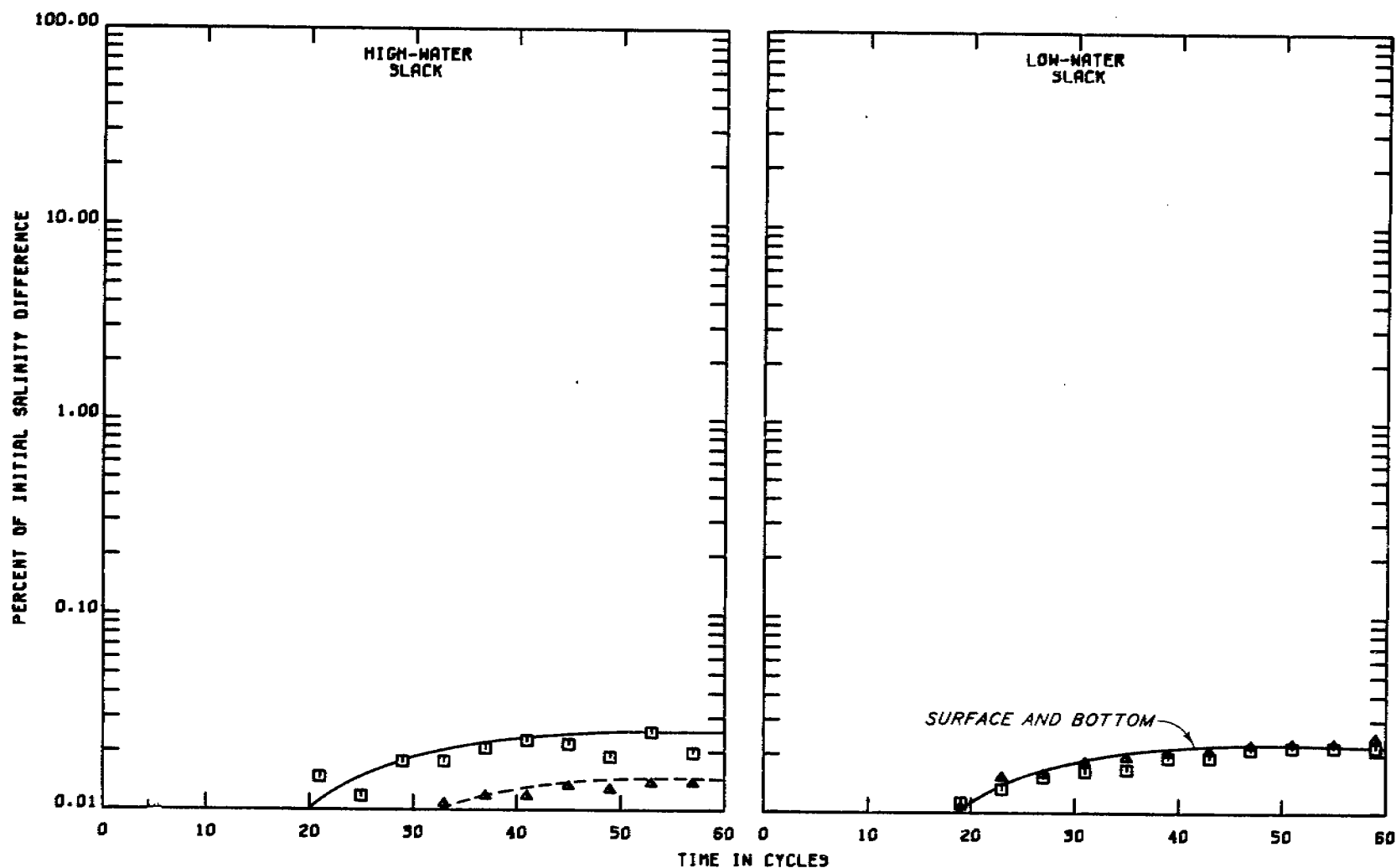
TEST CONDITIONS

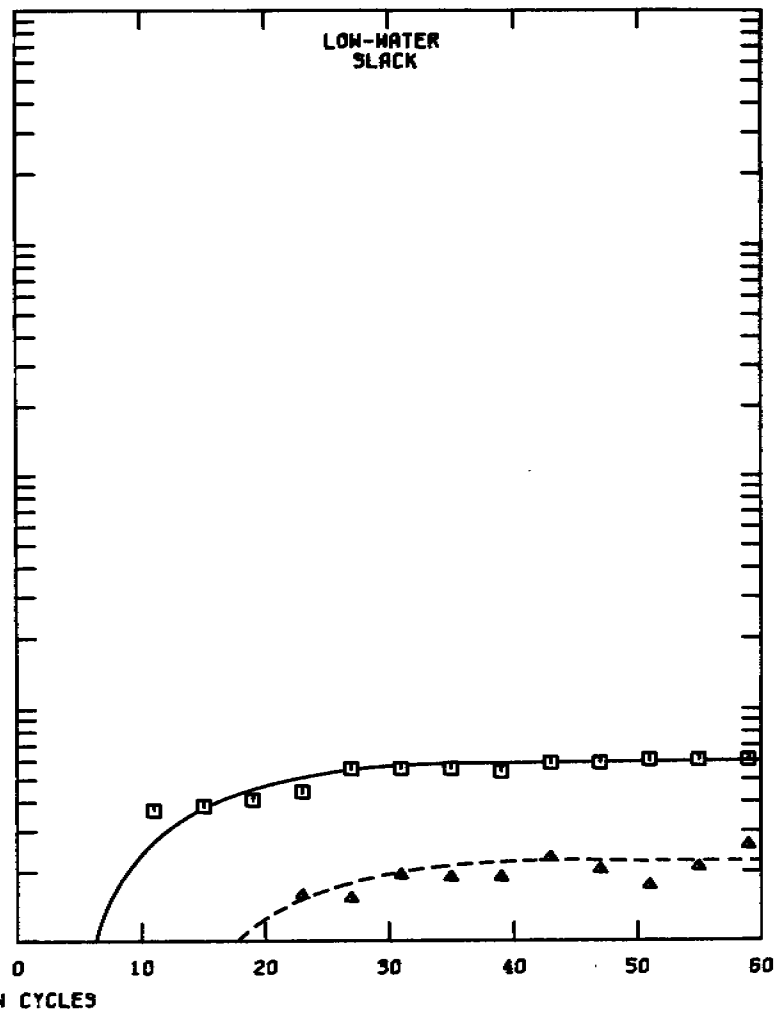
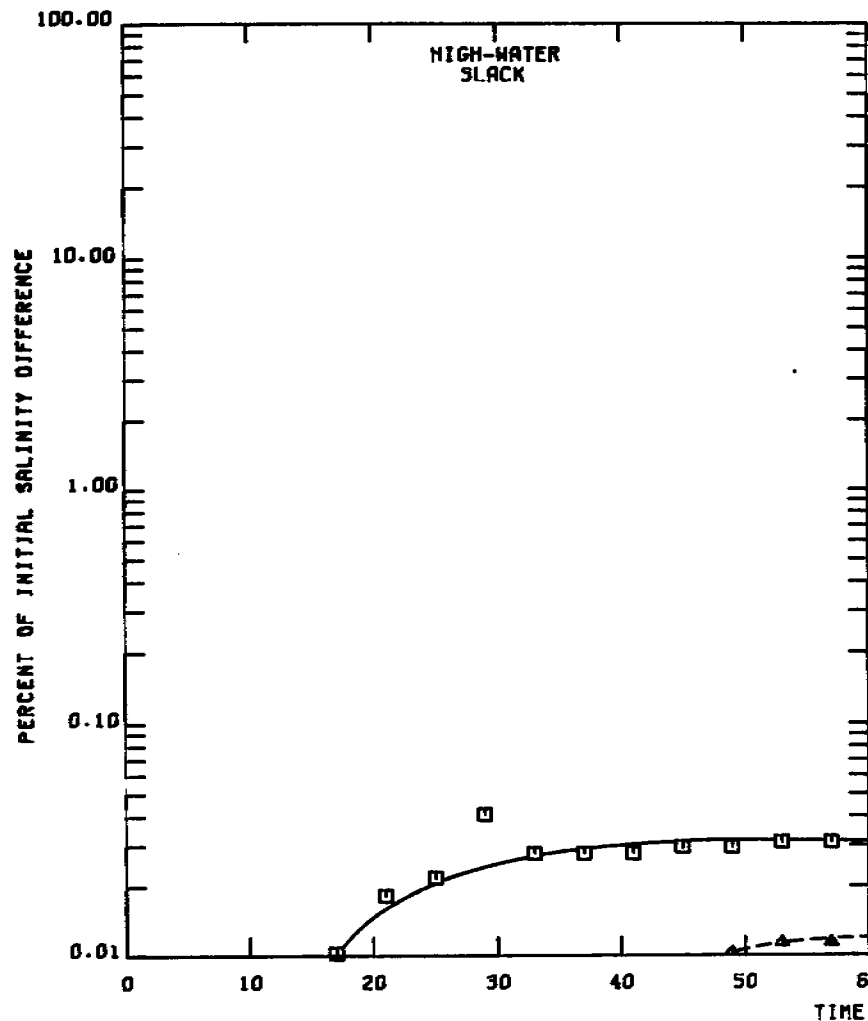
FRESH-WATER DISCHARGE	20200 CFS
BASE SALINITY AT DIFFUSER	17.6 PPT
EFFLUENT SALINITY	29.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
▲ - - -	BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-MEAN FLOW PERIOD
STATION D13

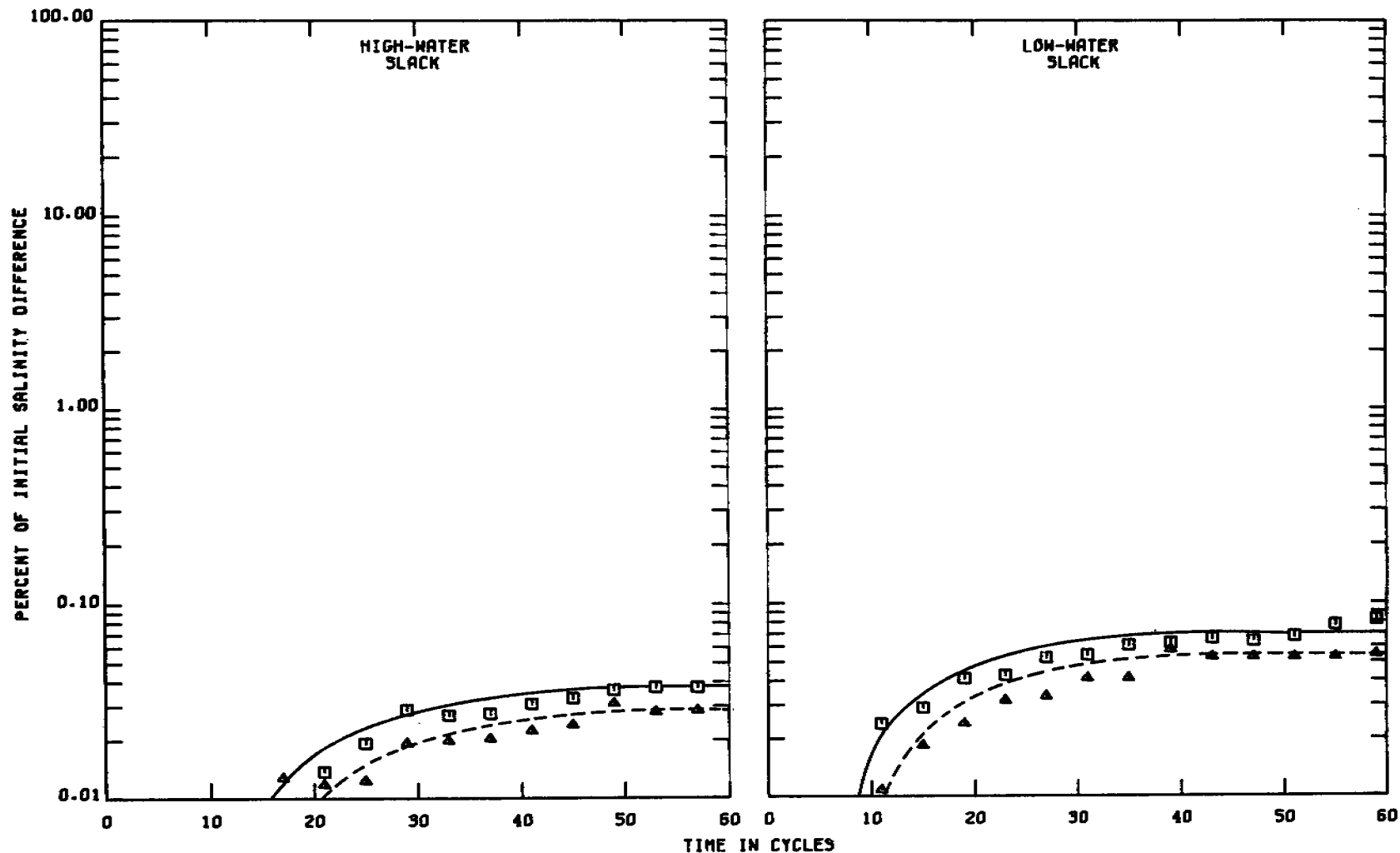




TEST CONDITIONS
 FRESH-WATER DISCHARGE 20200 CF3
 BASE SALINITY AT DIFFUSER 17.6 PPT
 EFFLUENT SALINITY 29.0 PPT
 INITIAL SALINITY DIFFERENCE 11.4 PPT
 EFFLUENT INJECTION RATE 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION D15



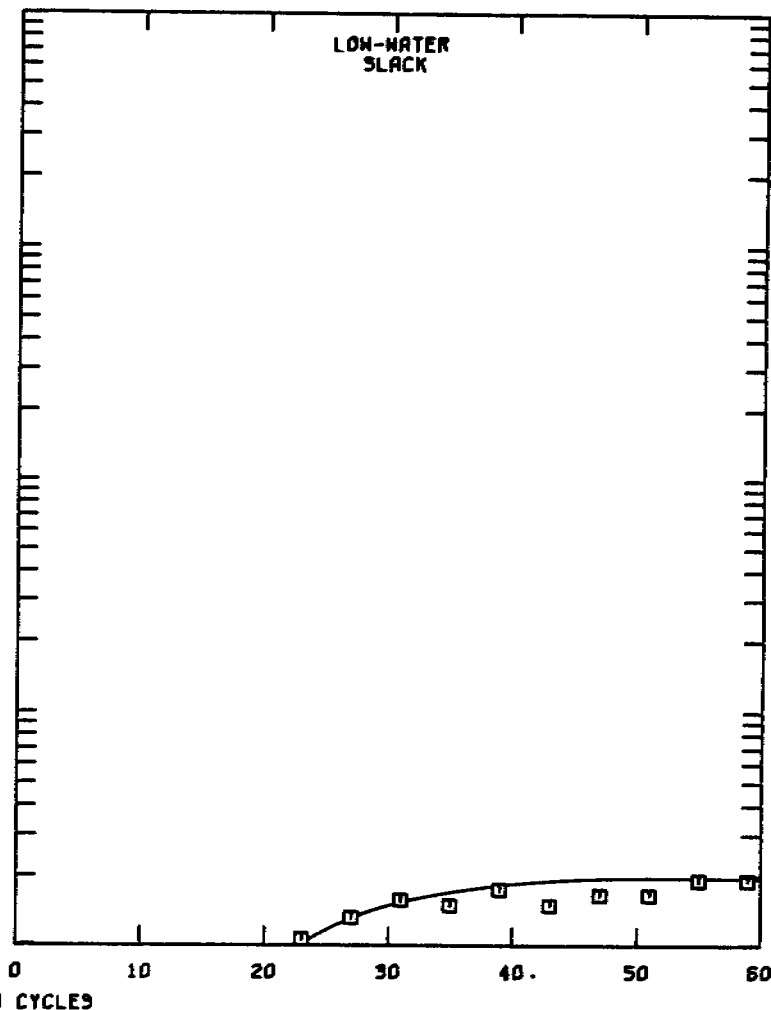
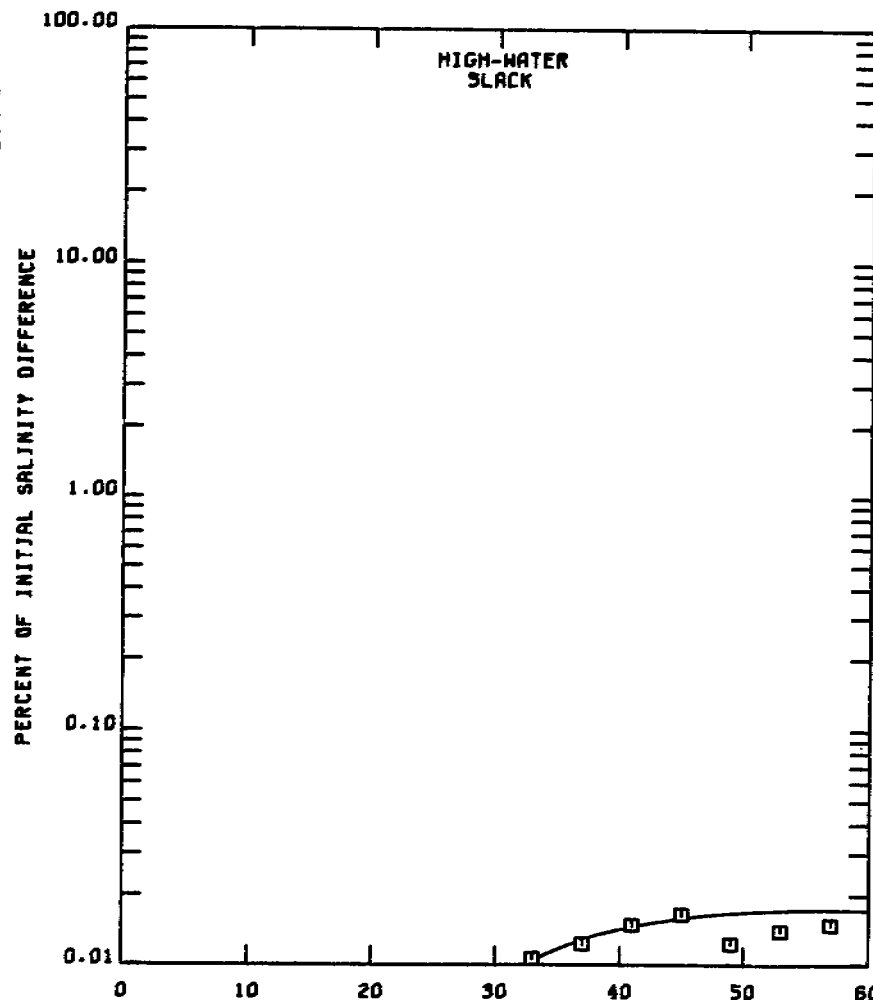
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D16



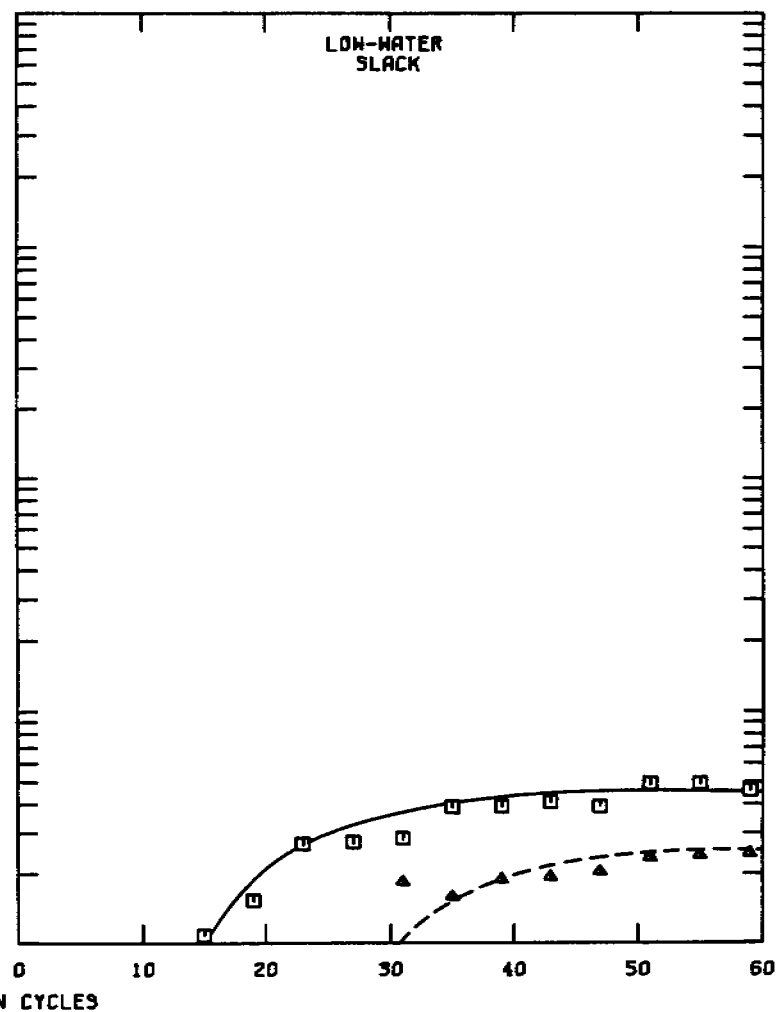
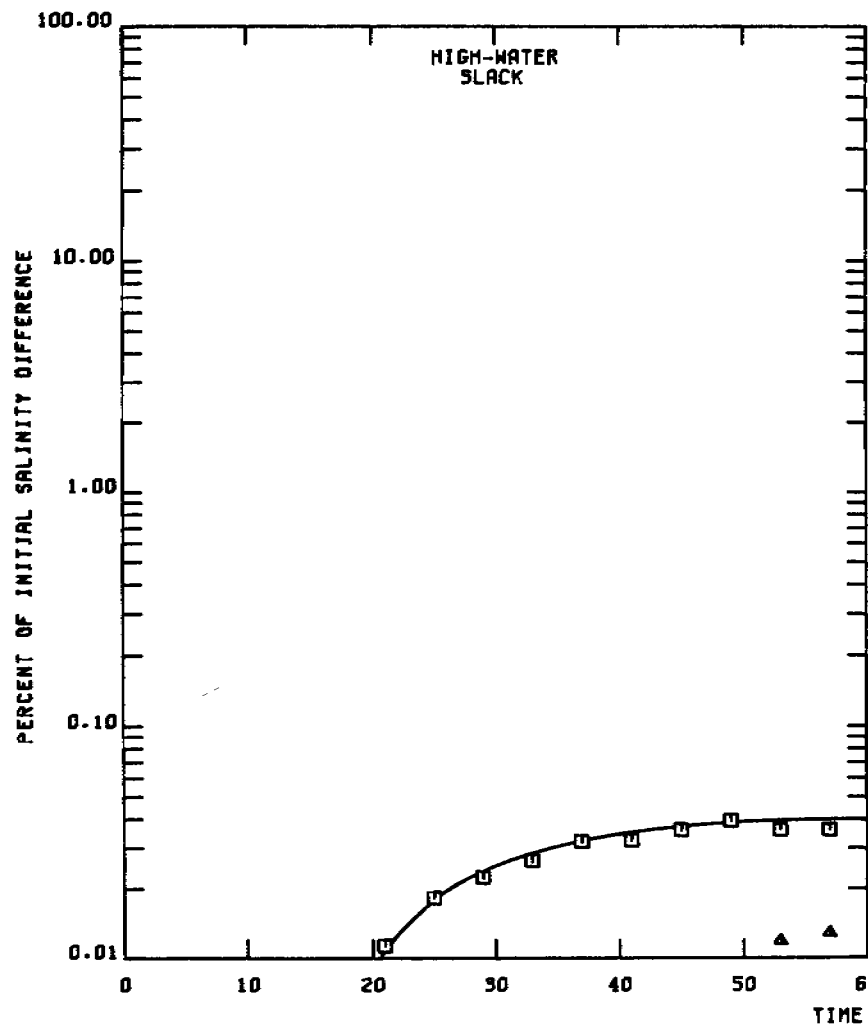
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF9
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D19



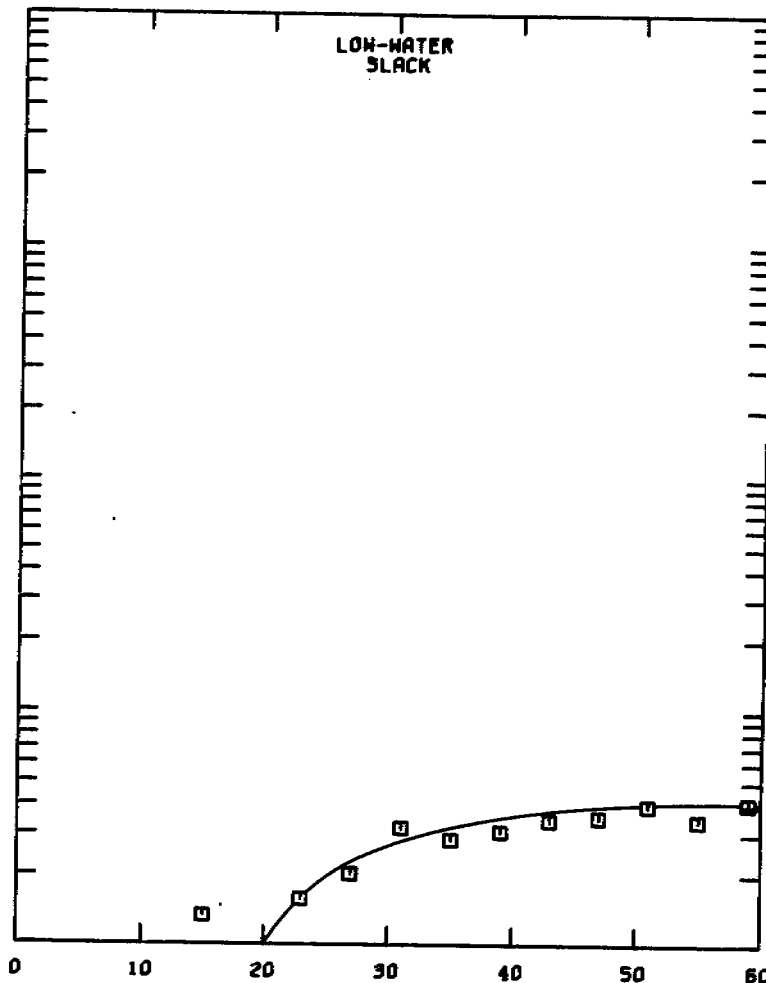
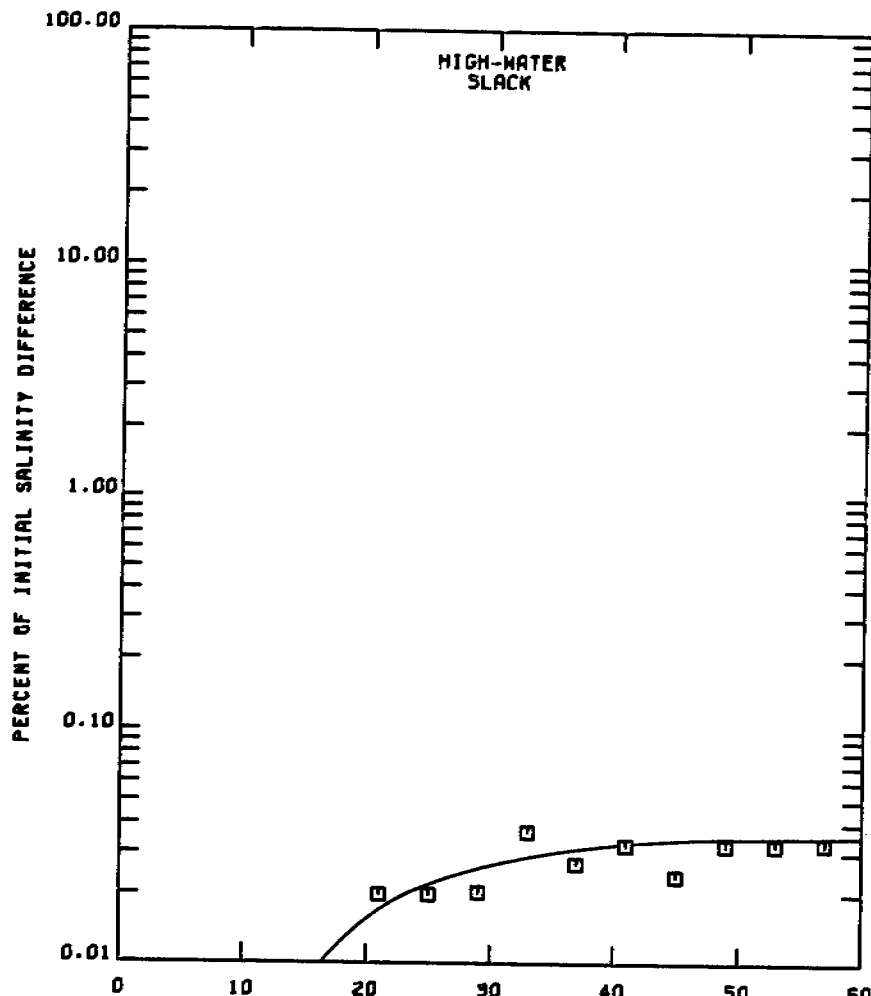
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF3
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION D20



TIME IN CYCLES

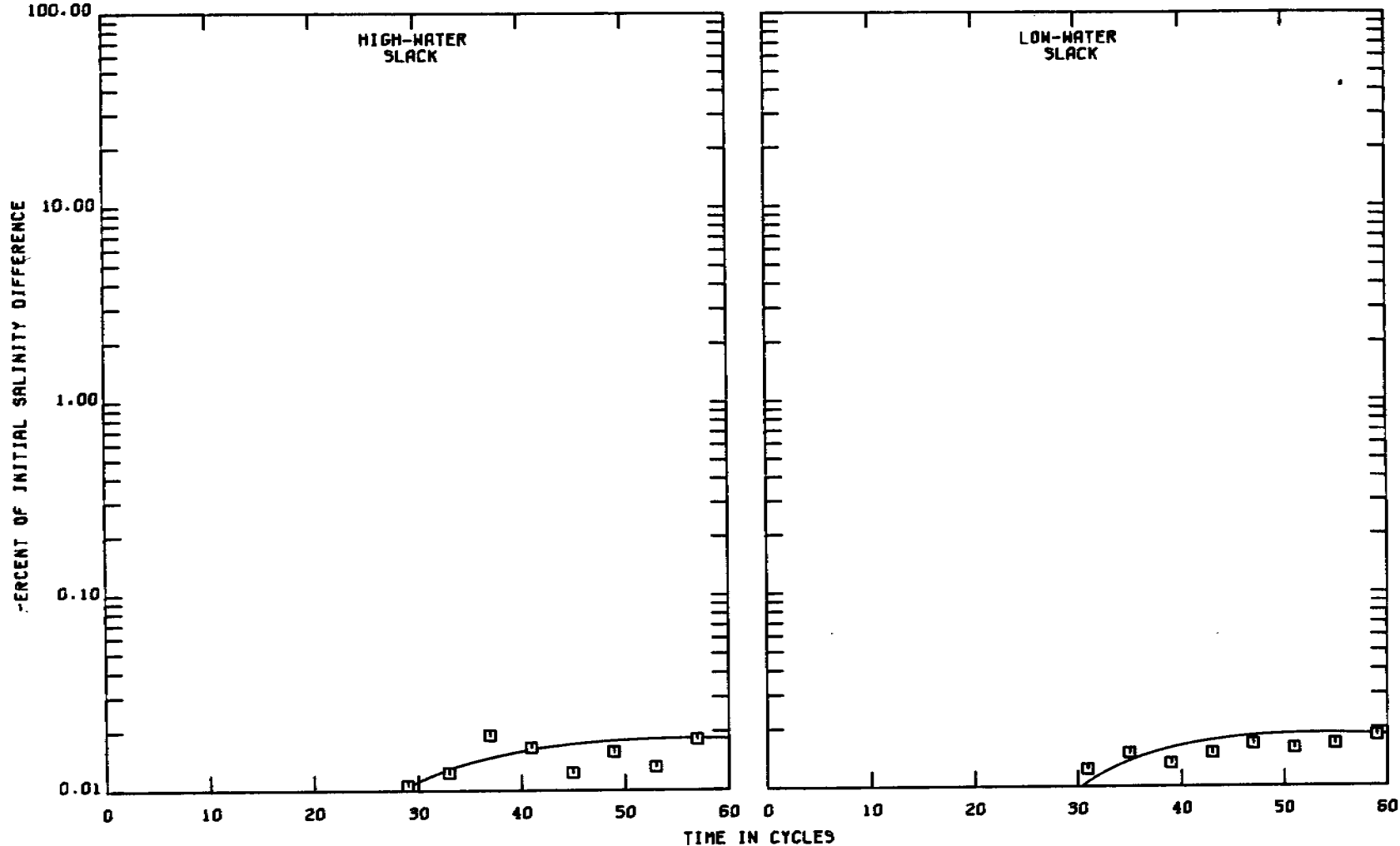
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D2I



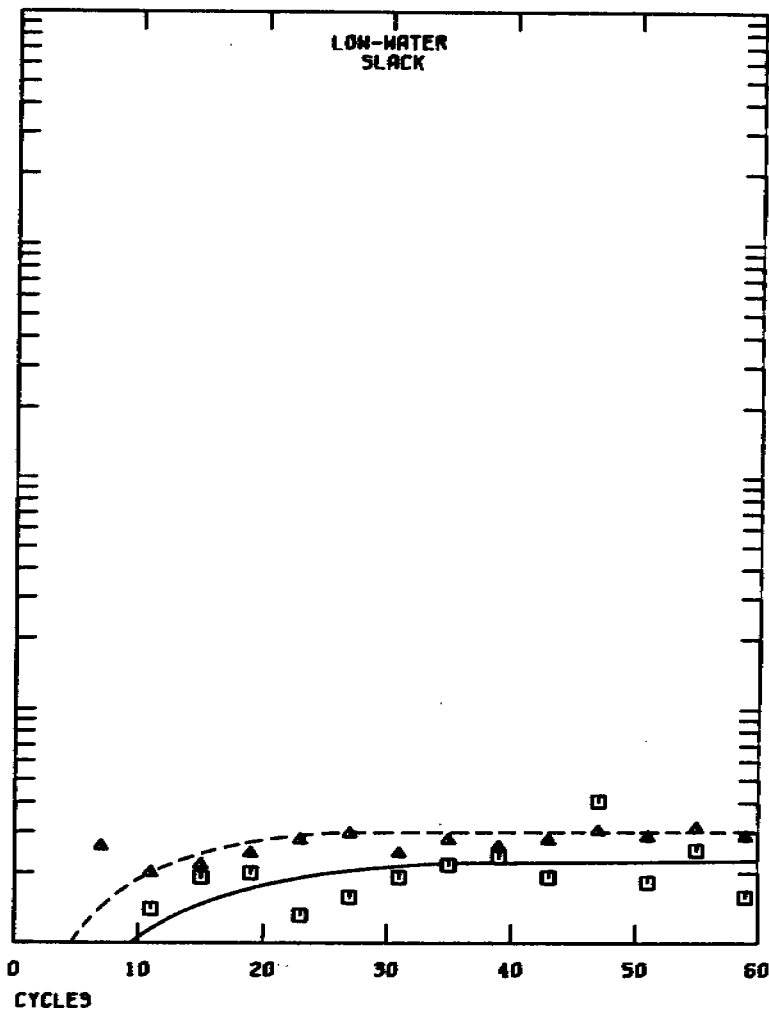
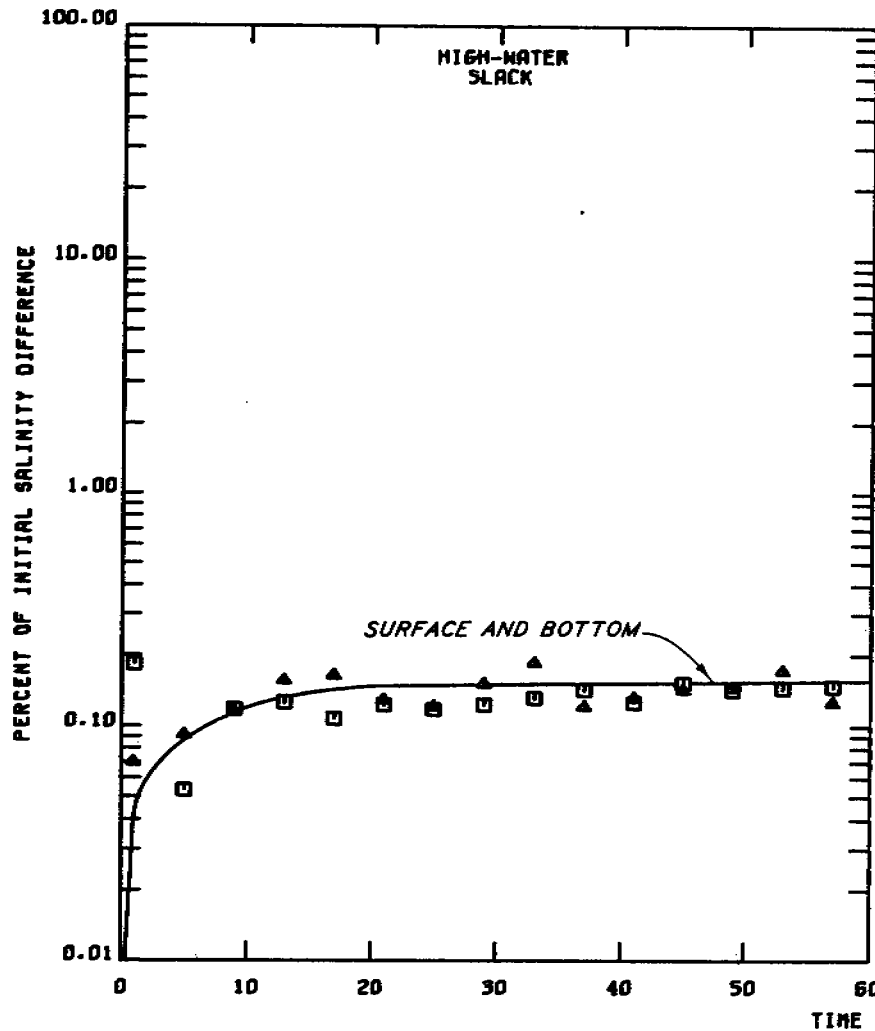
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF3
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION D22



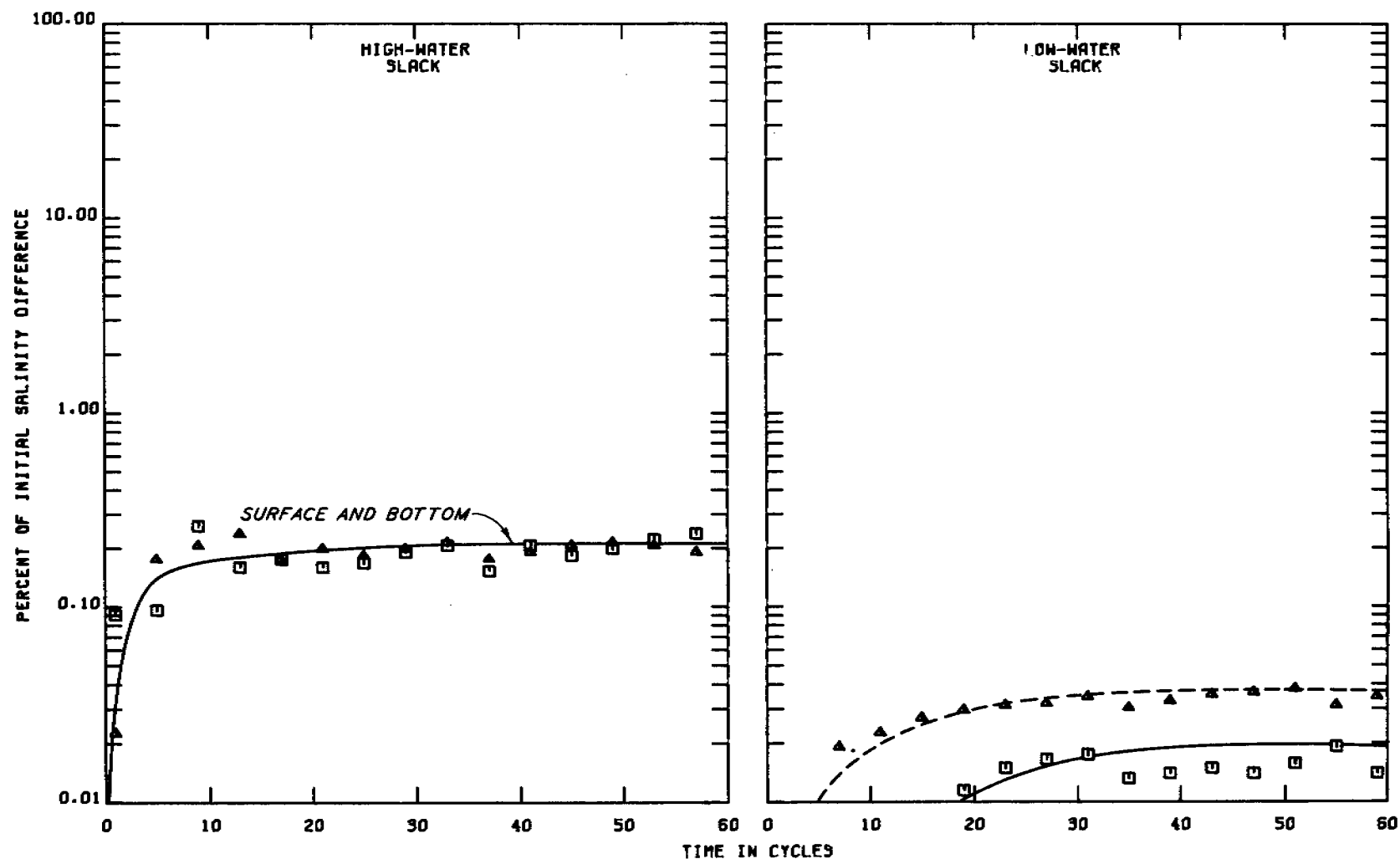
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF3
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

STATION III

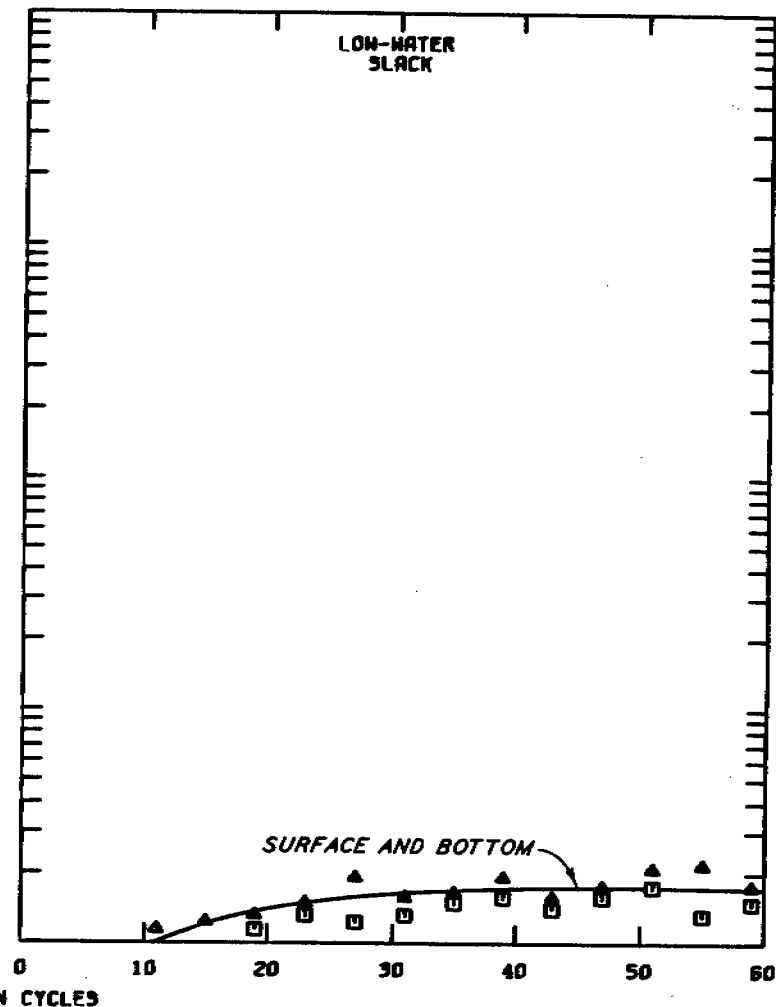
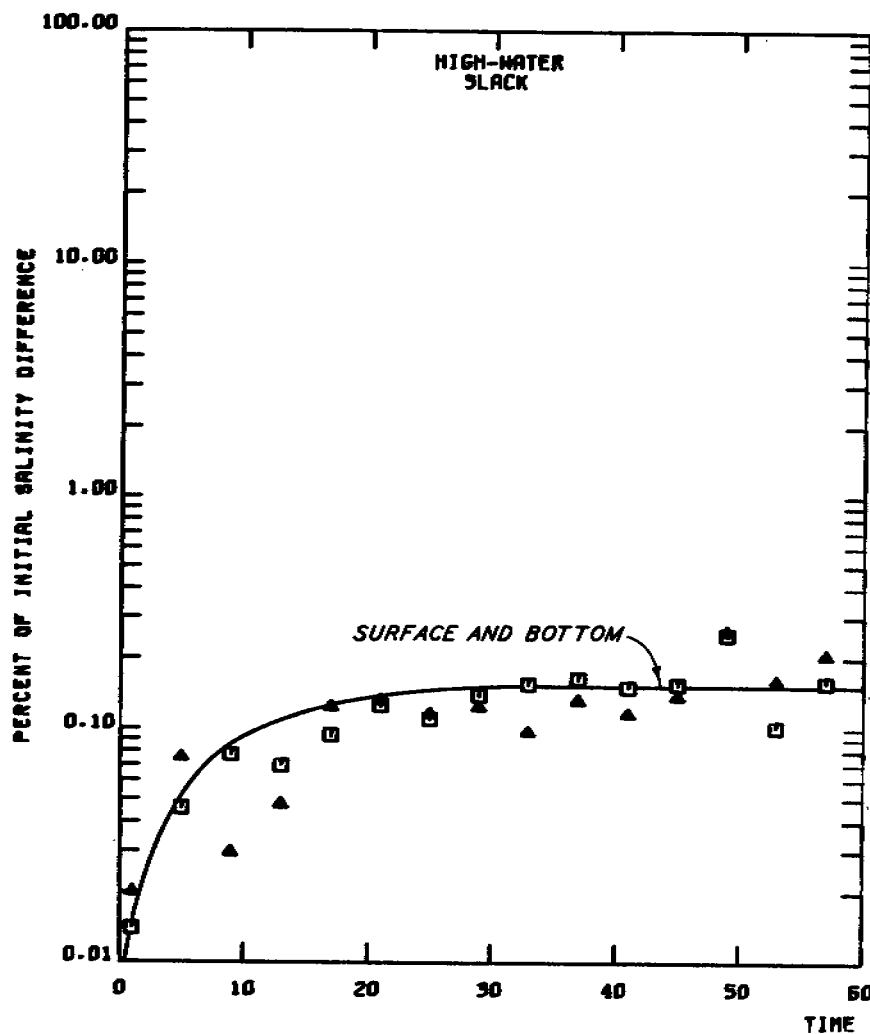


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 △ — BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION U2



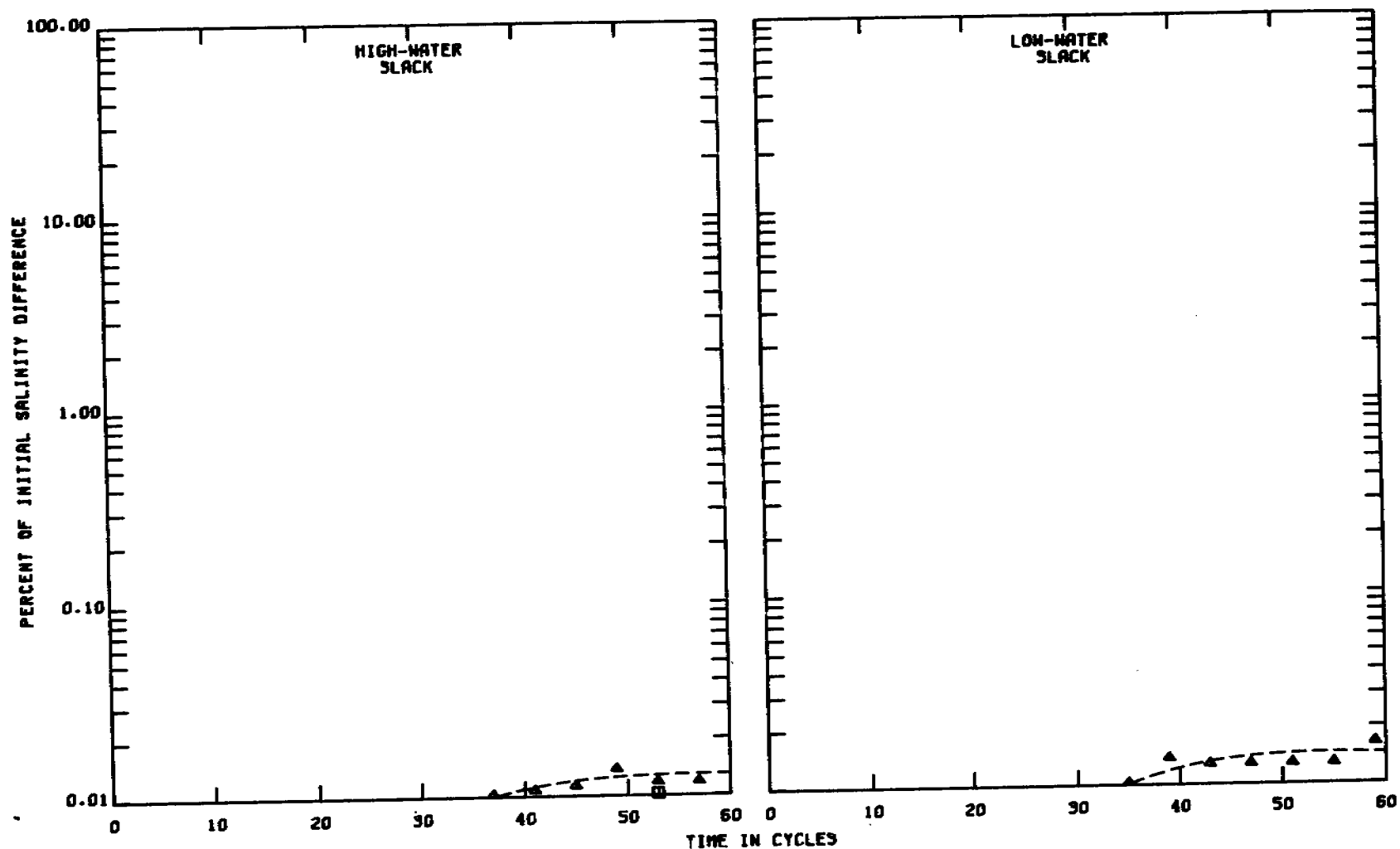
TEST CONDITIONS

FRESH-WATER DISCHARGE	20200 CF9
BASE SALINITY AT DIFFUSER	17.6 PPT
EFFLUENT SALINITY	29.0 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ - - -	BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-MEAN FLOW PERIOD
STATION U3

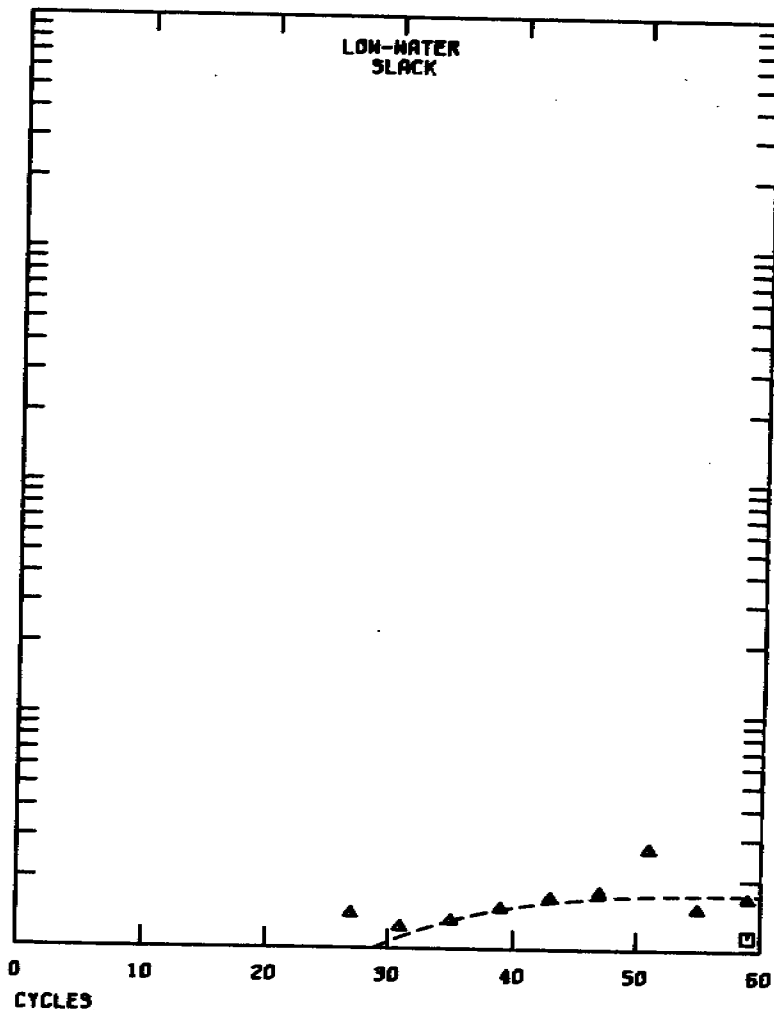
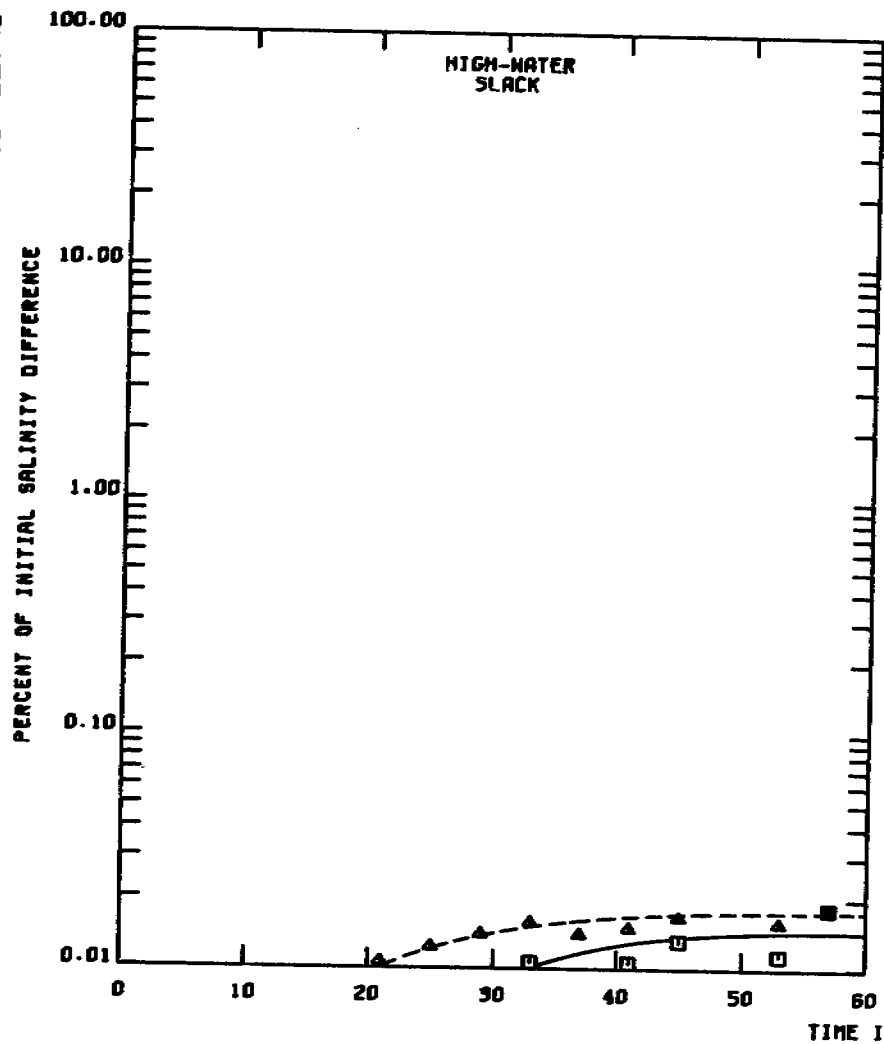


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ — — — BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION U4

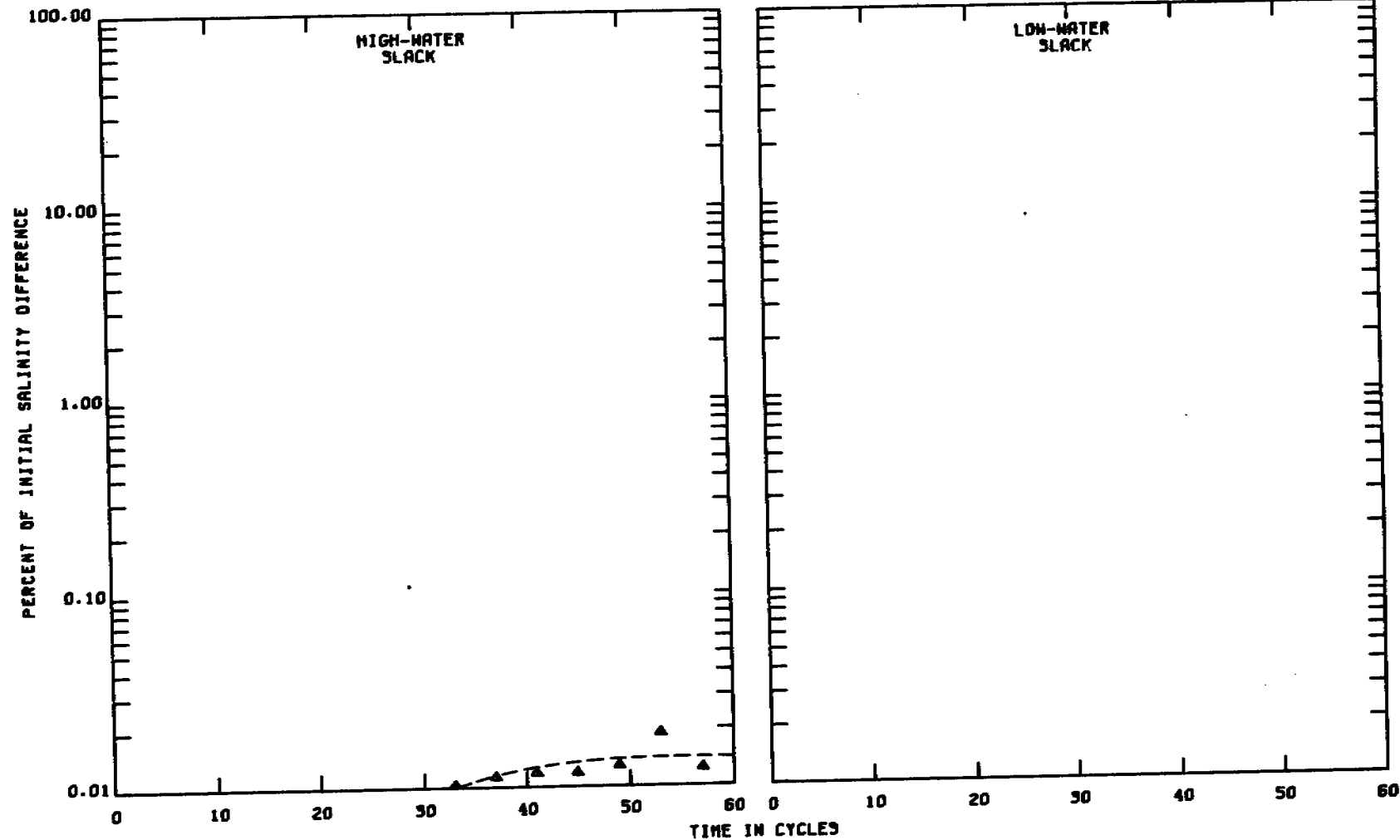


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION US

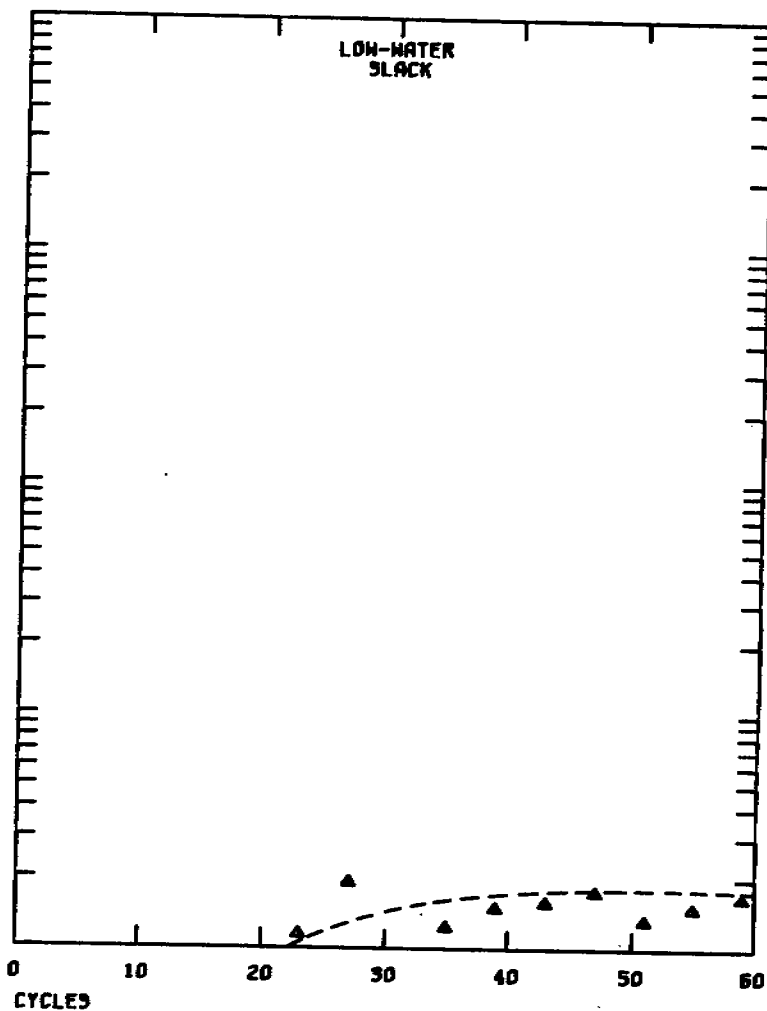
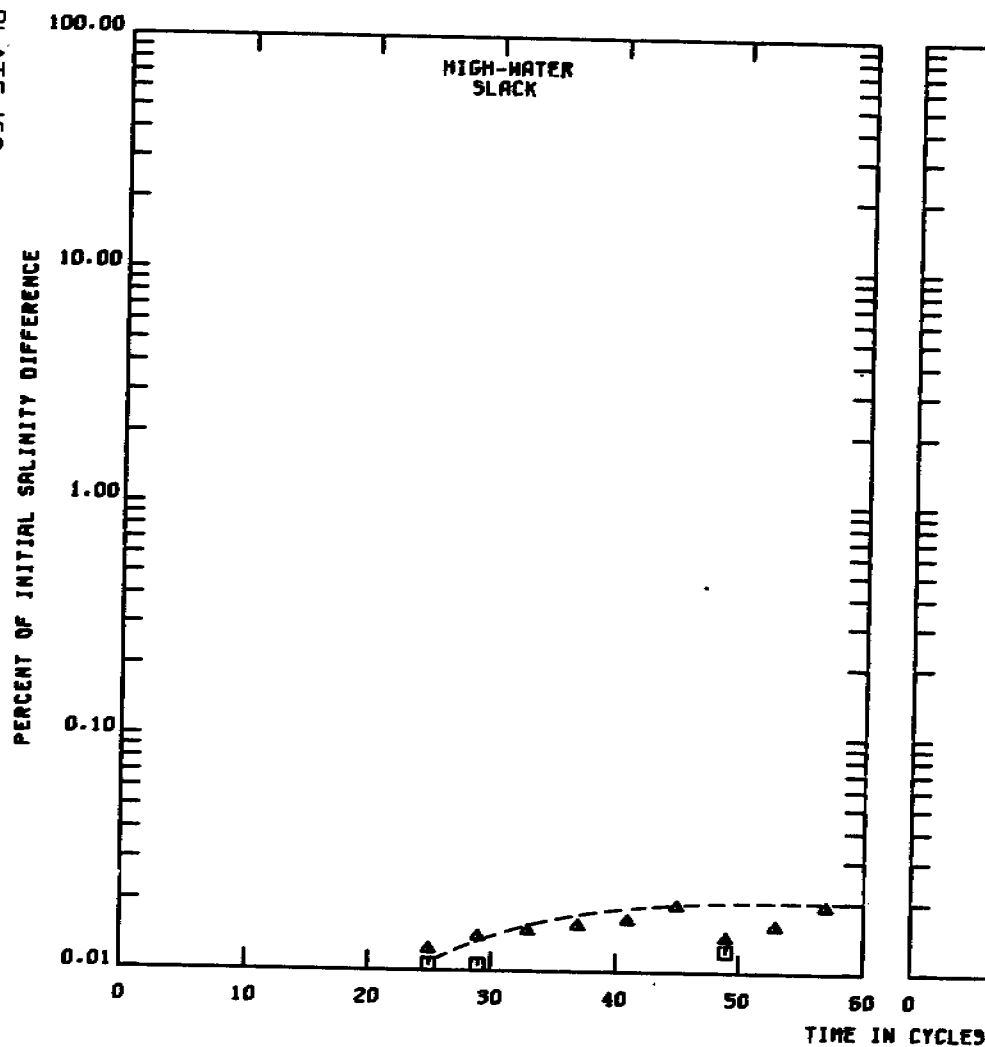


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF3
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION U6**

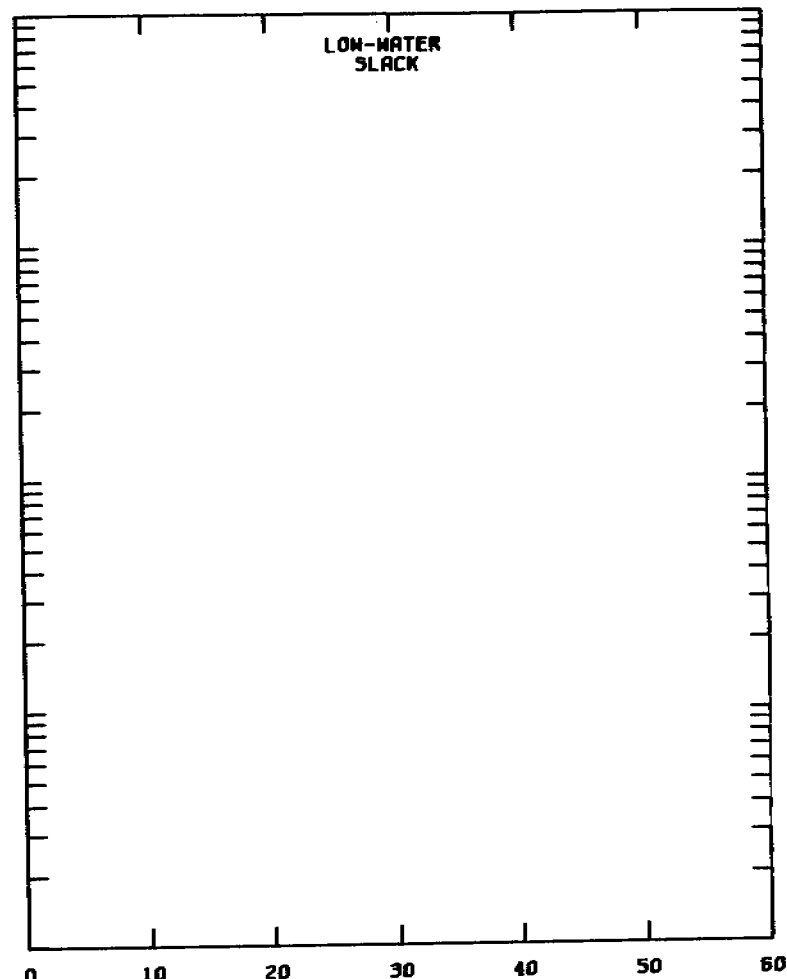
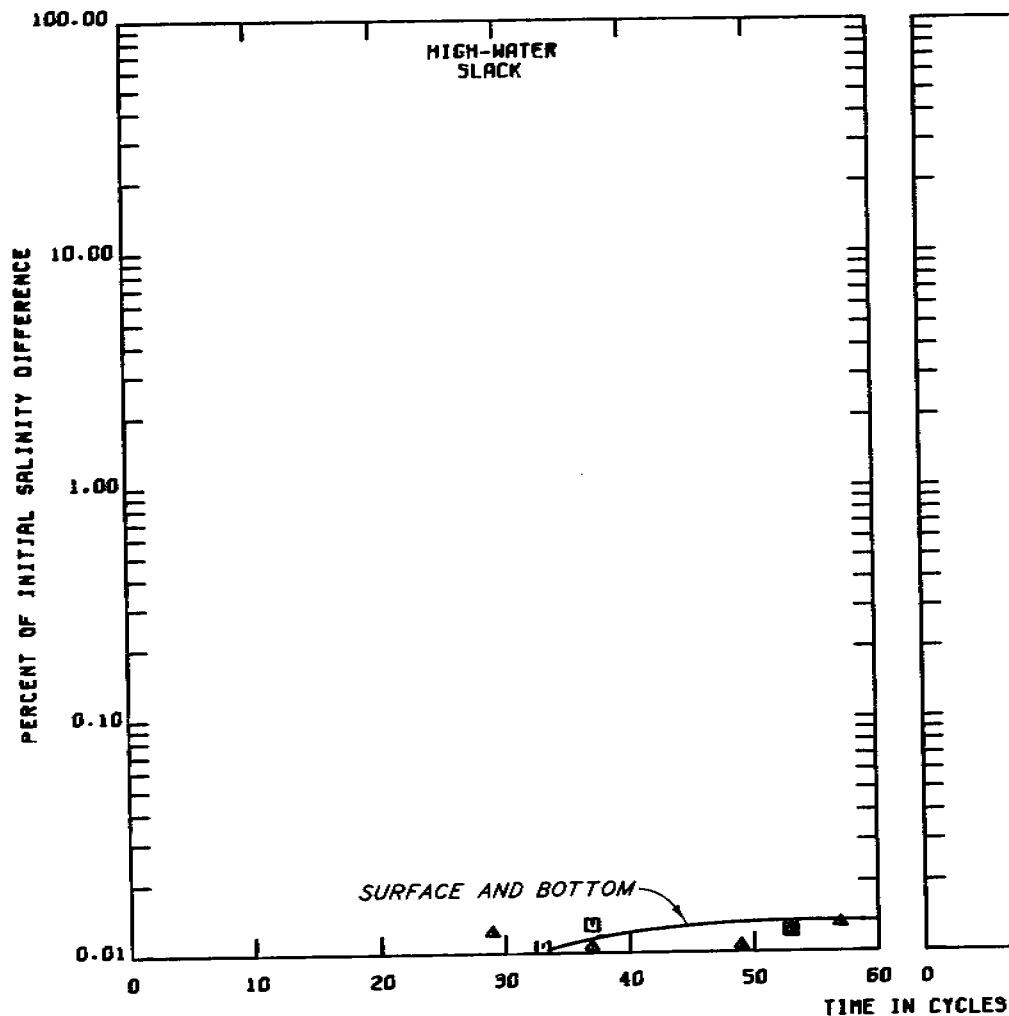


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ — BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION 17



TEST CONDITIONS

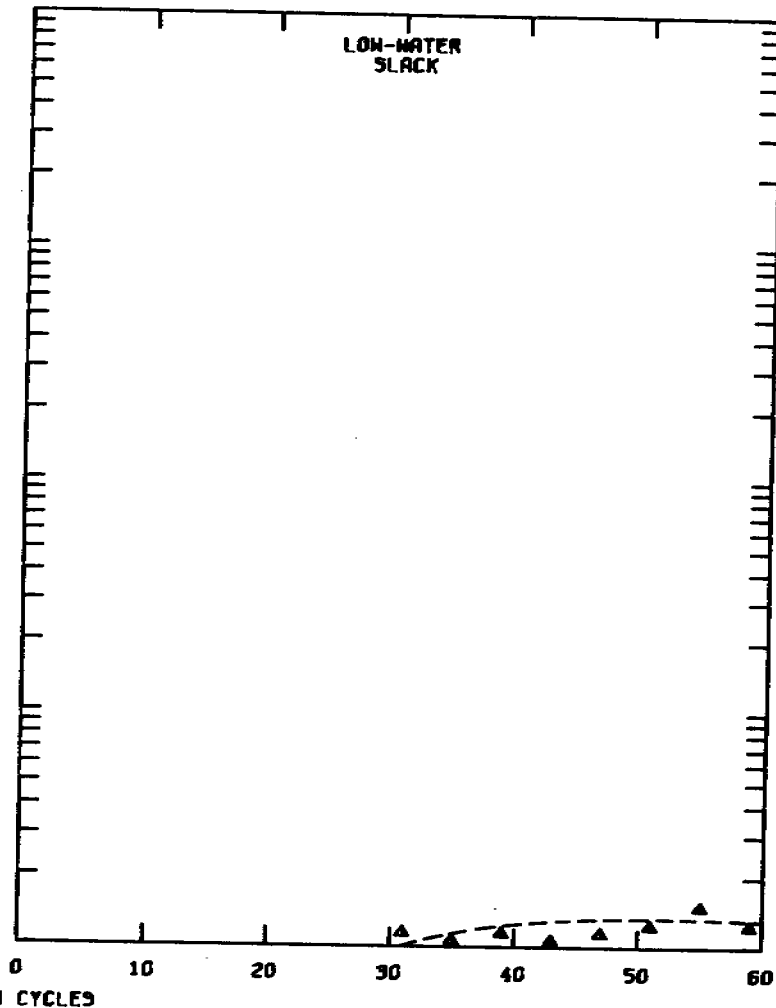
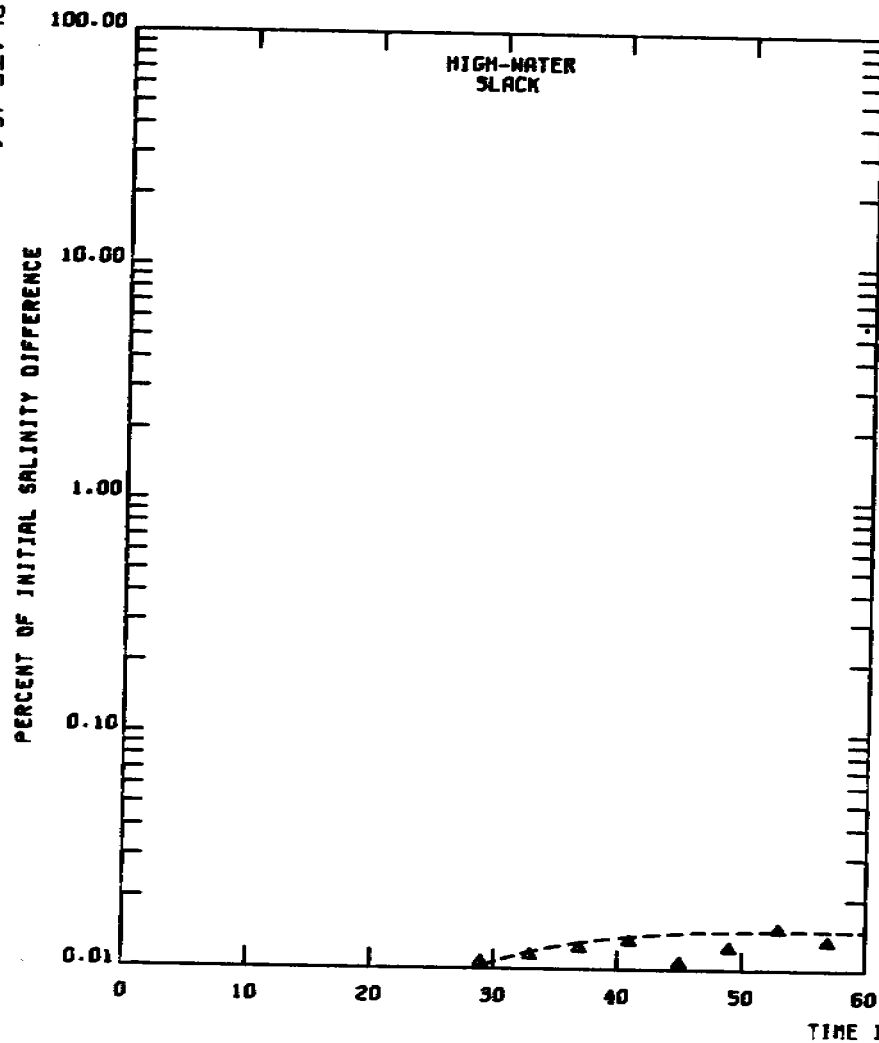
FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ — SURFACE
 △ — — — BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION U8

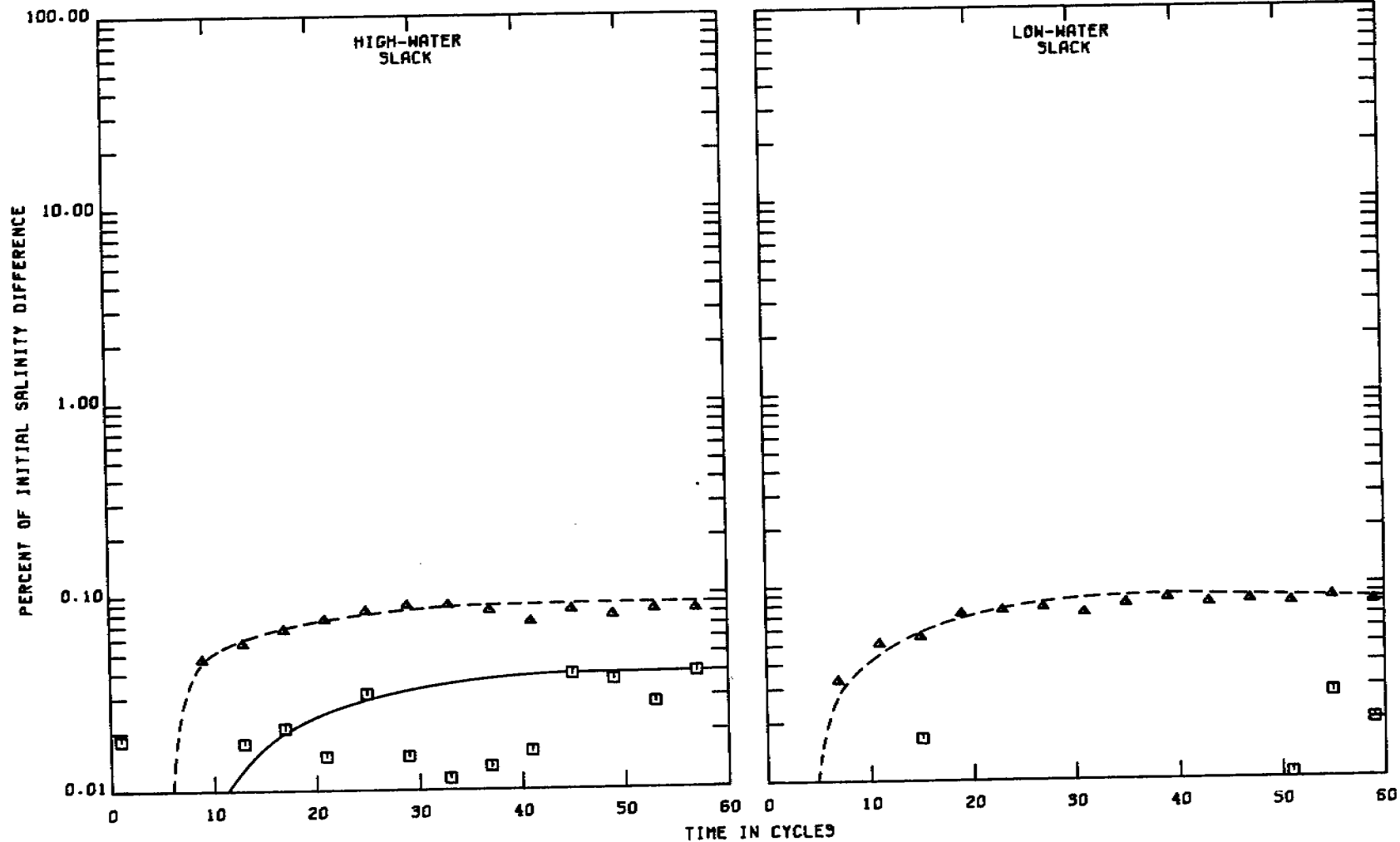


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION U10



TEST CONDITIONS

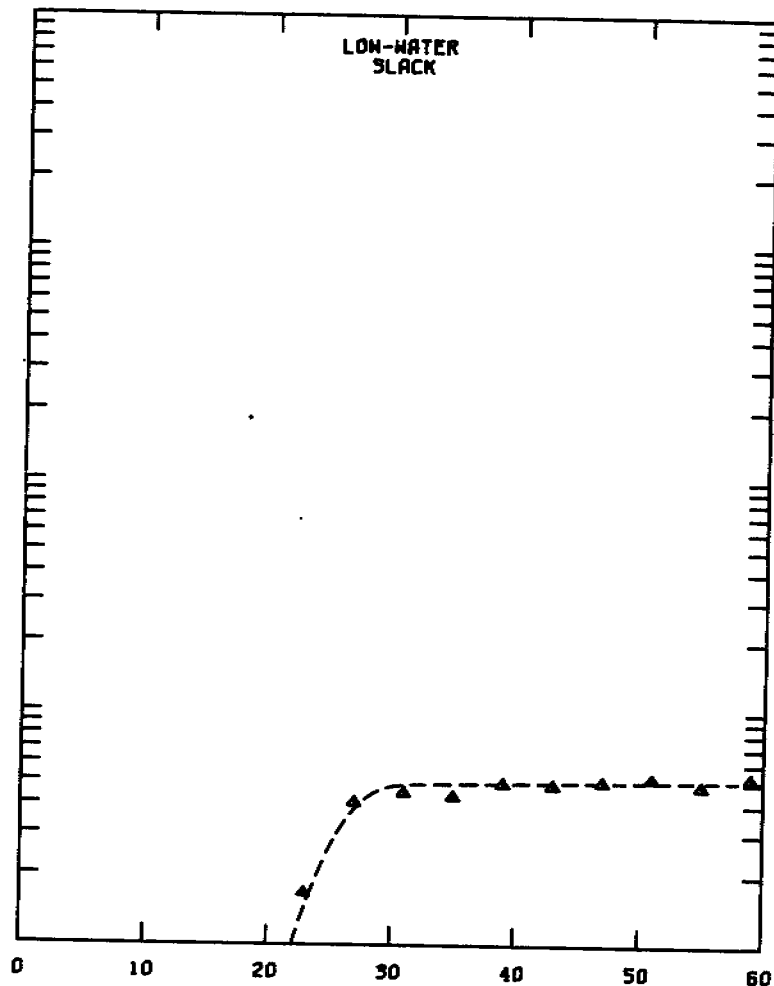
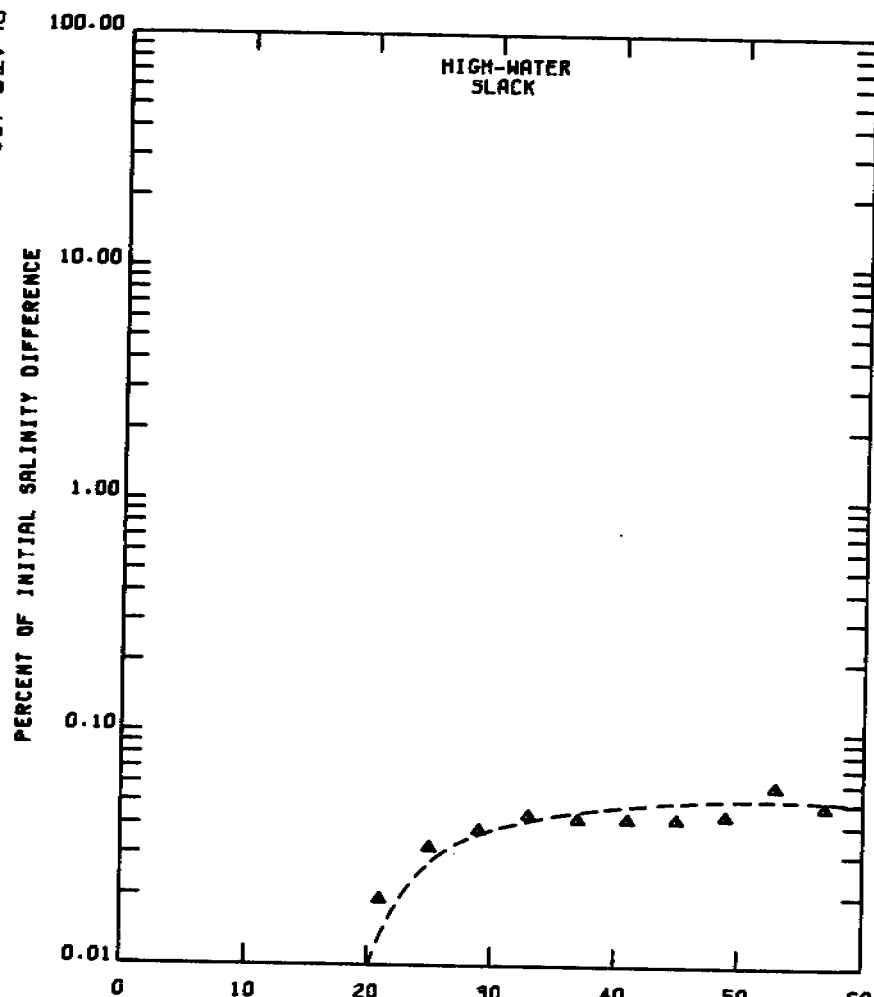
FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

20200 CF3
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

LEGEND

□ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD
 STATION CR I



TIME IN CYCLES

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

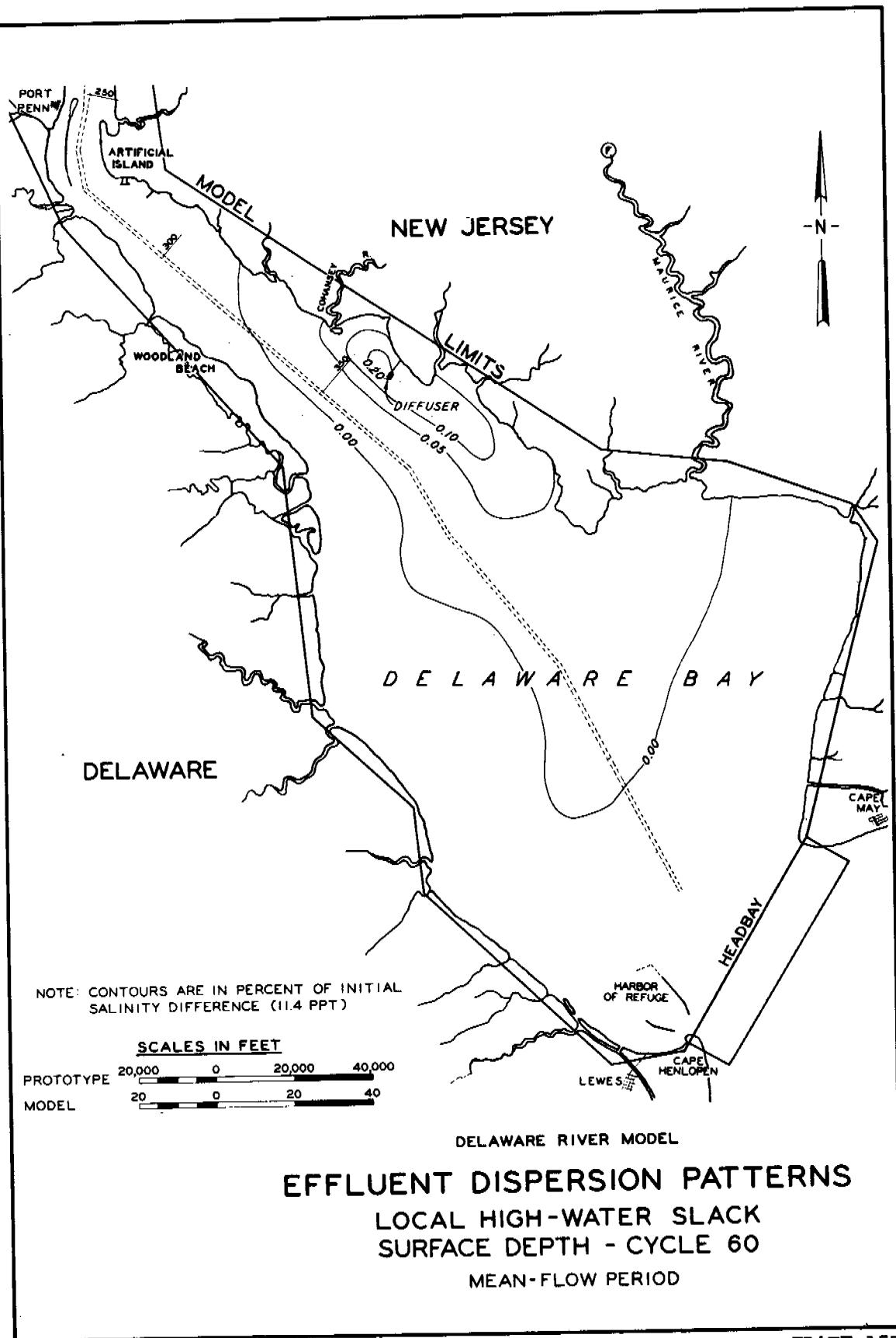
20200 CFS
 17.6 PPT
 29.0 PPT
 11.4 PPT
 21.2 MGD

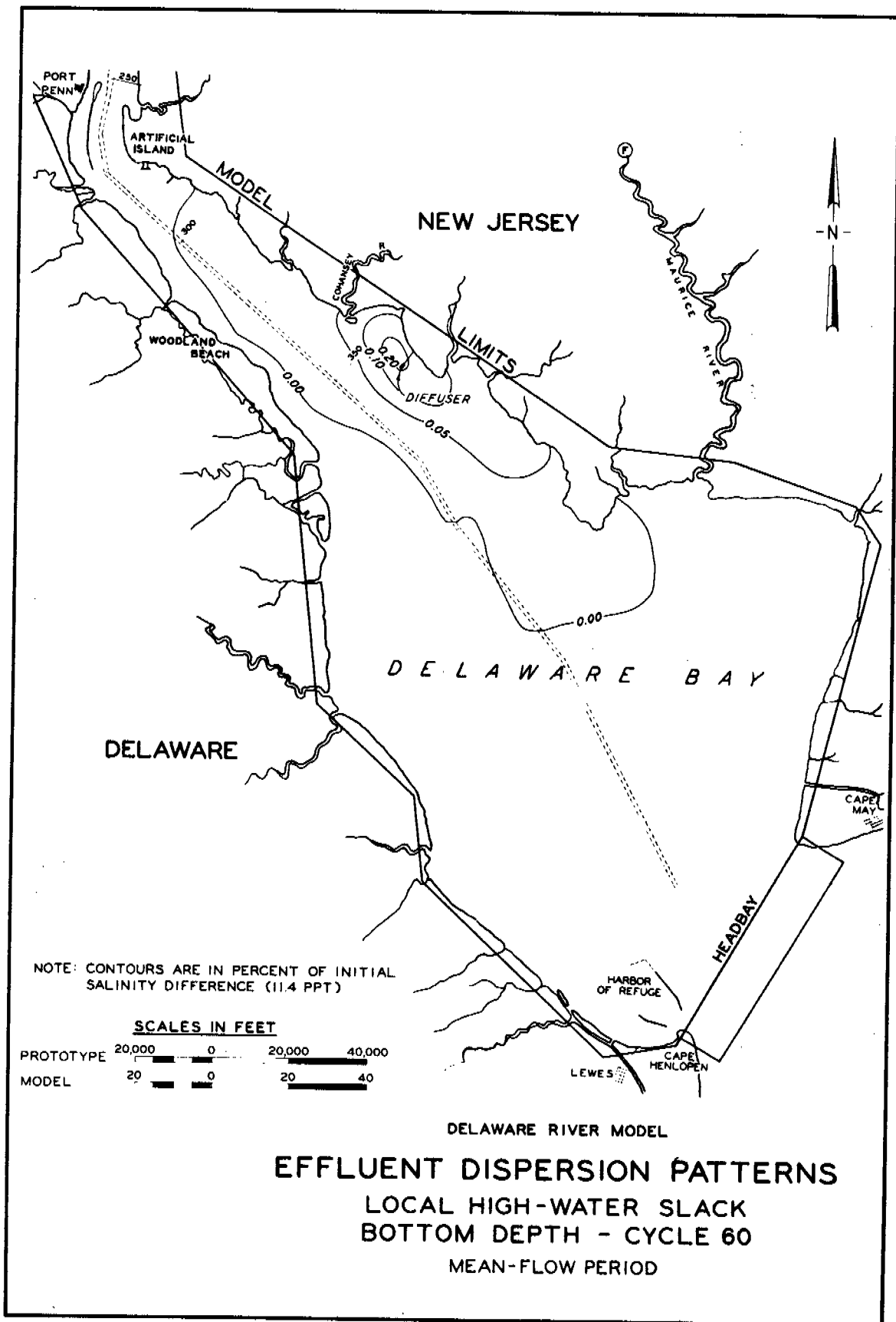
LEGEND

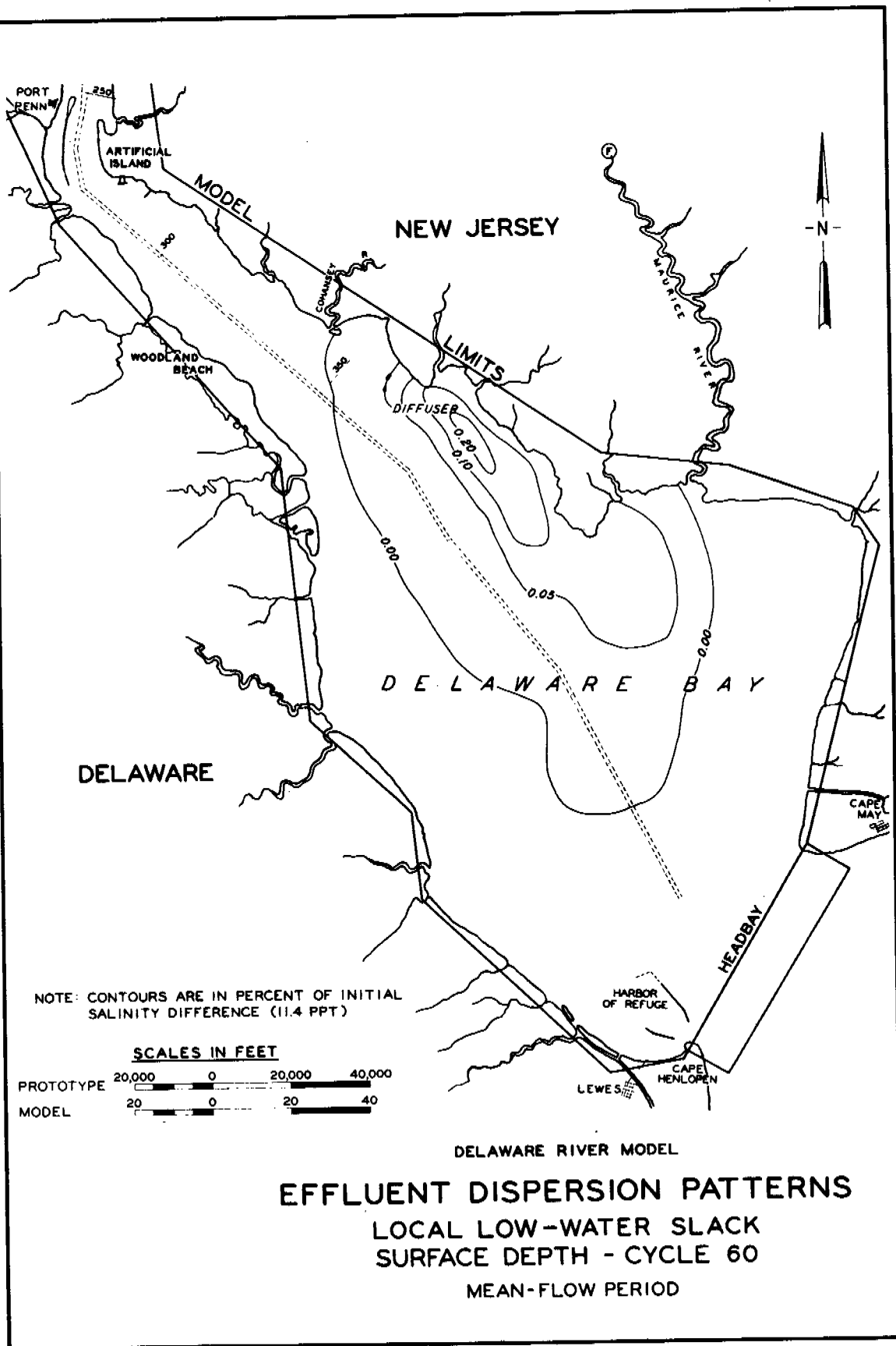
□ — SURFACE
 ▲ - - - BOTTOM

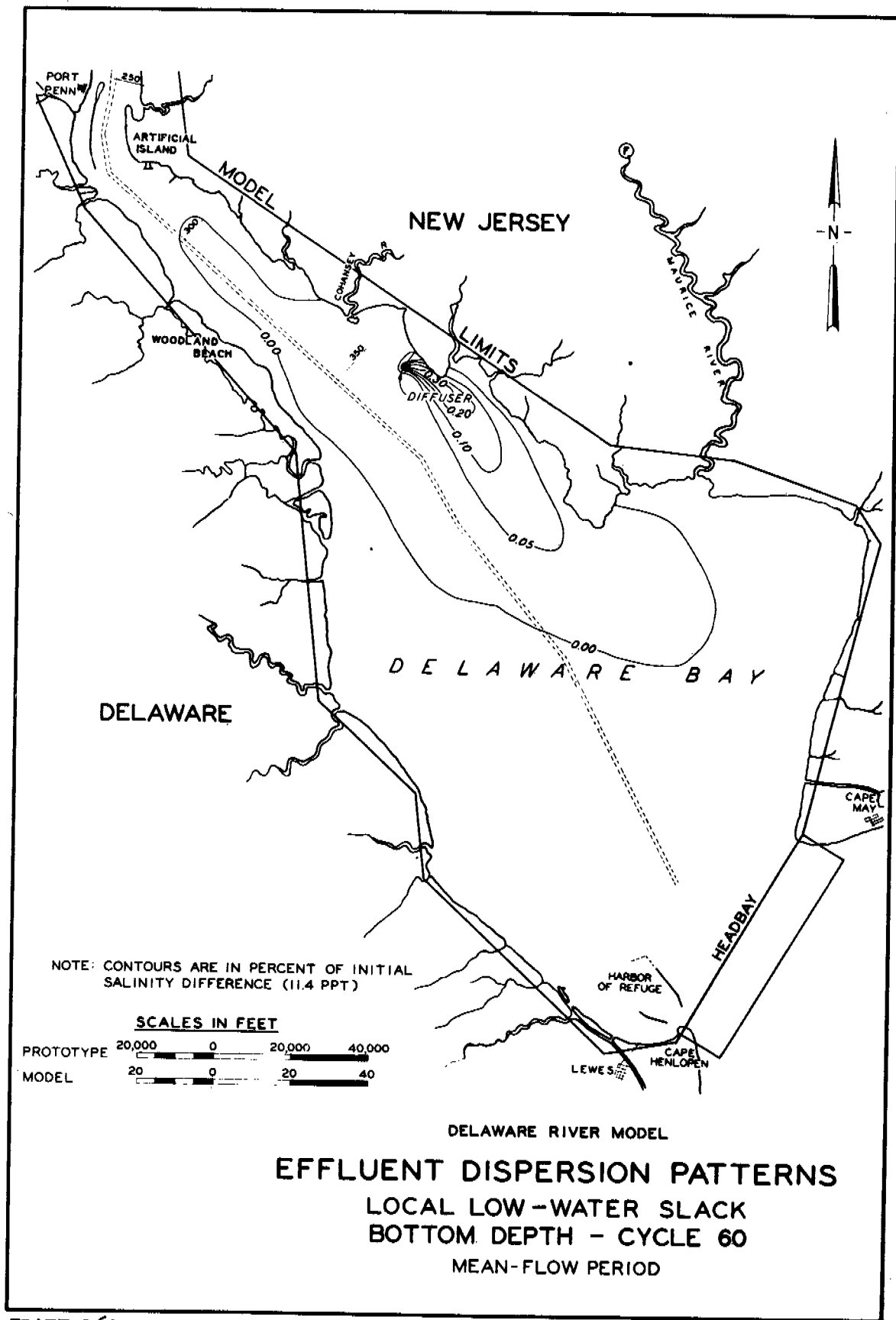
DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-MEAN FLOW PERIOD

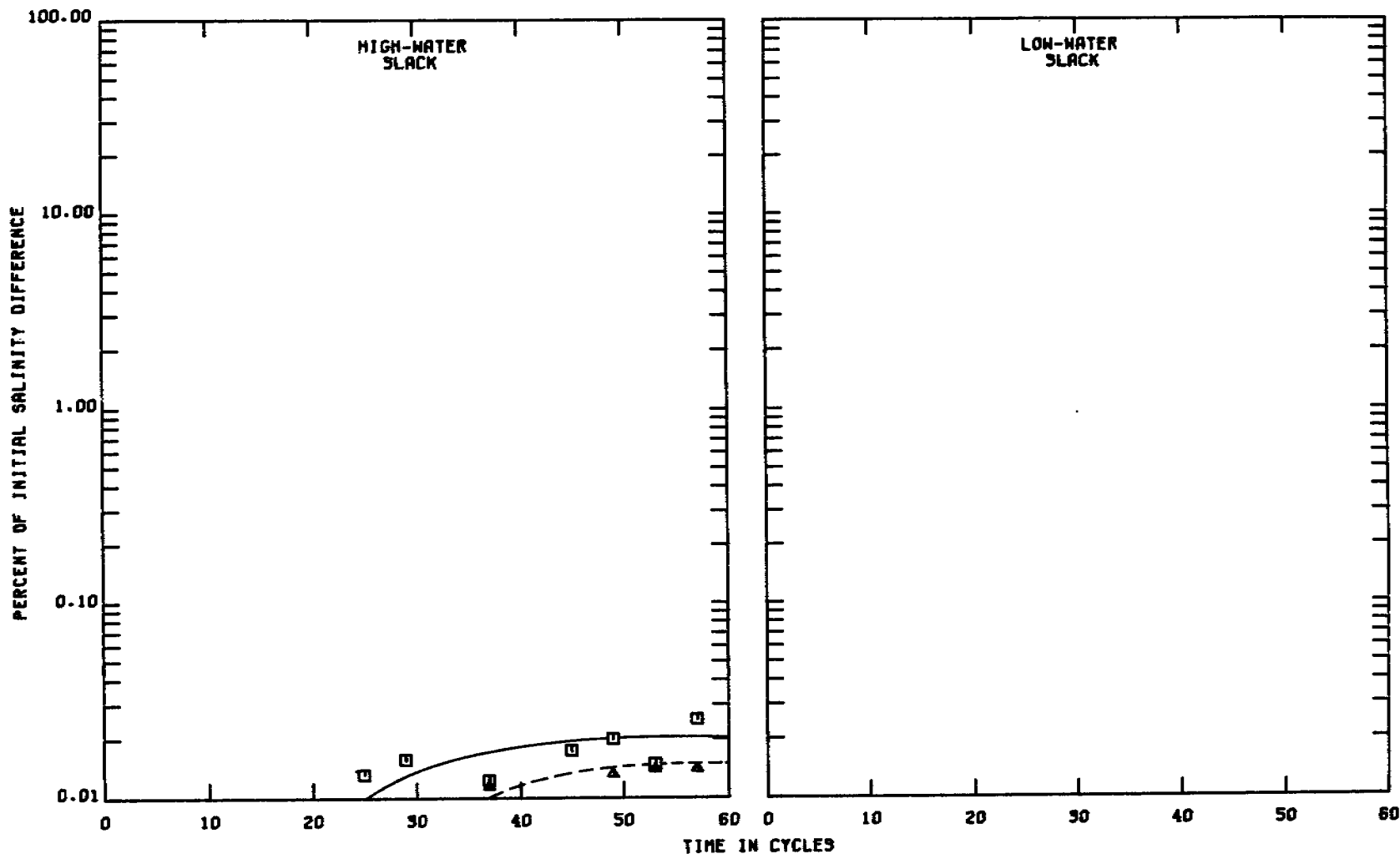
STATION CR2









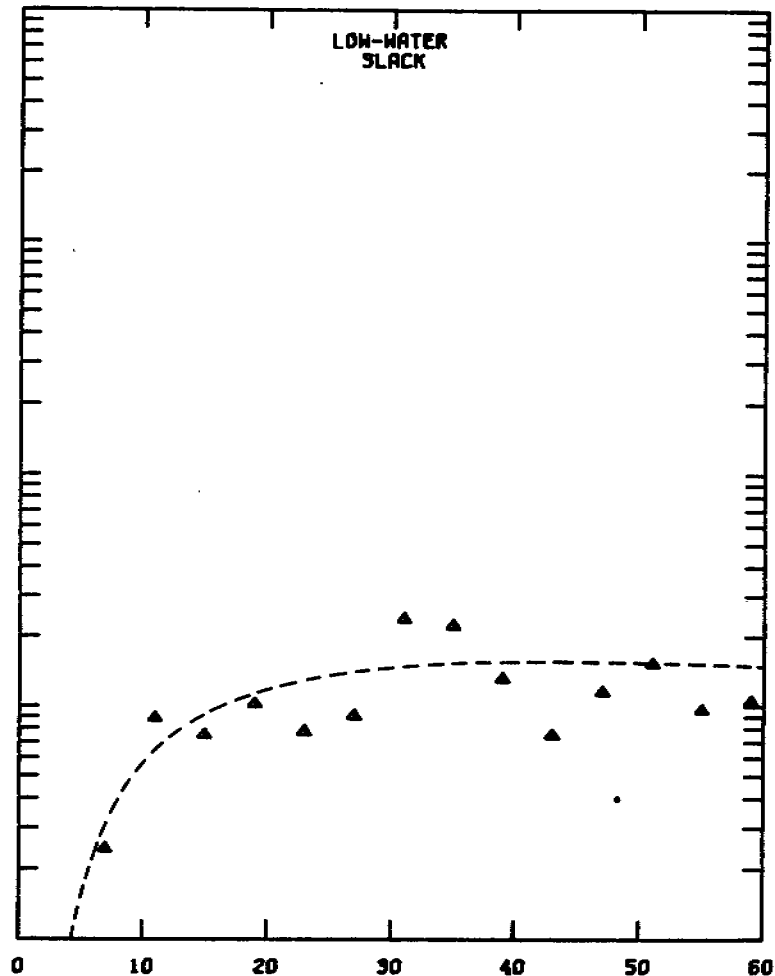
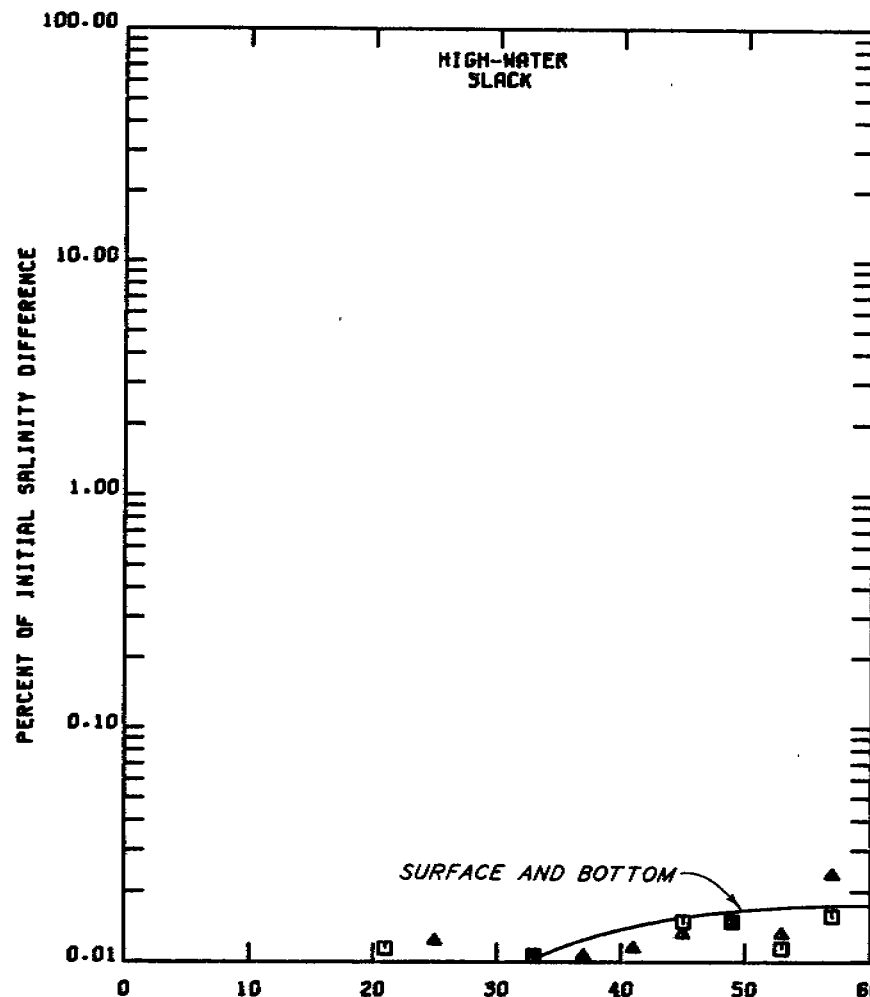


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60800 CF3
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ — SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD
 STATION D1



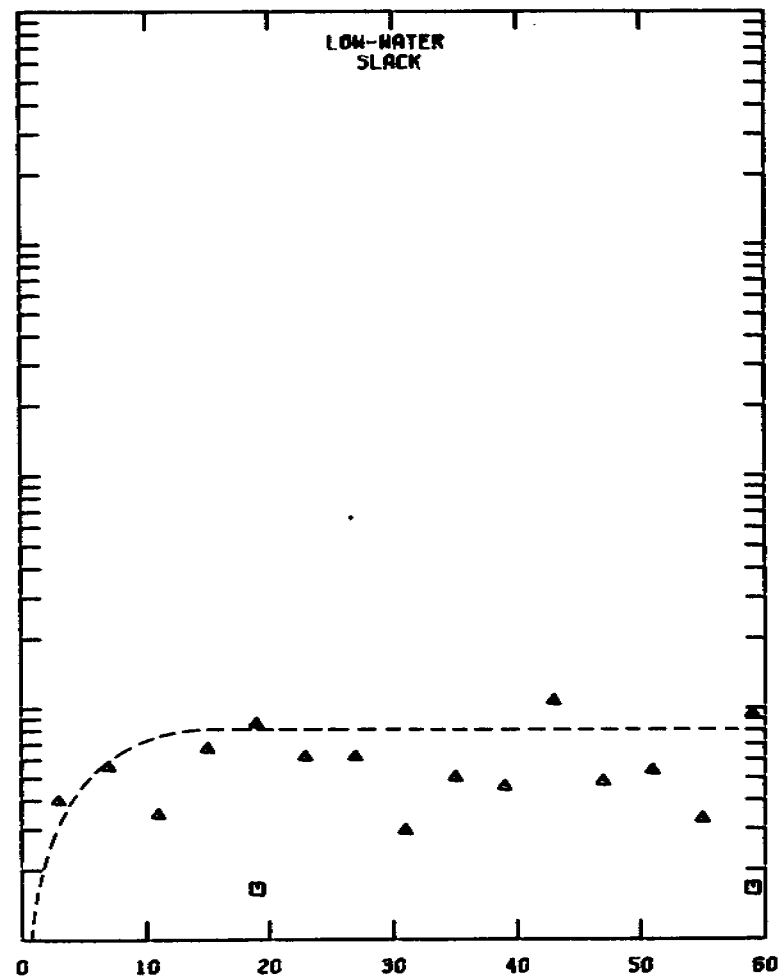
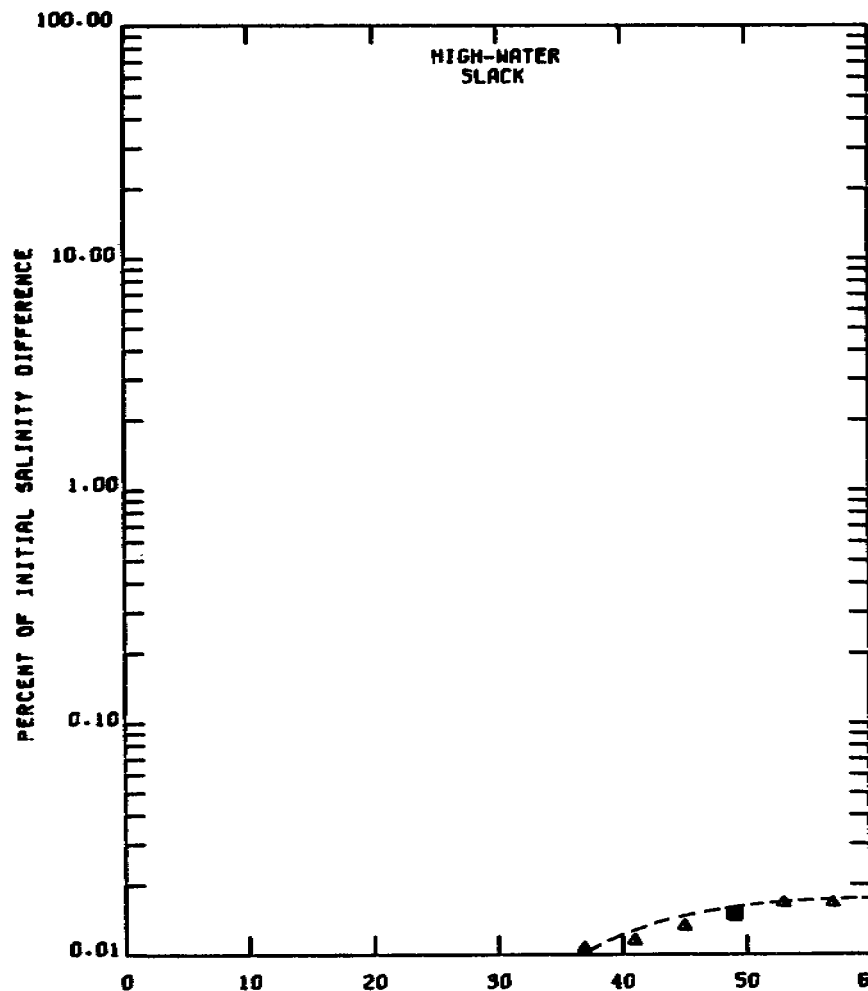
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60600 CFS
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD**

STATION D2



TIME IN CYCLES

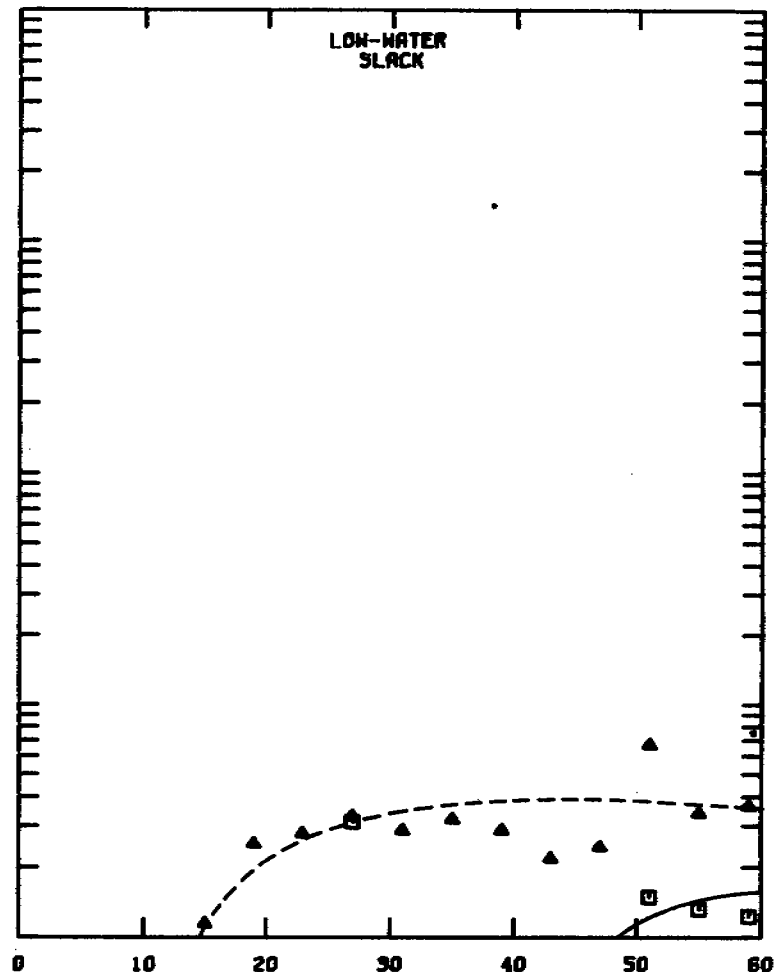
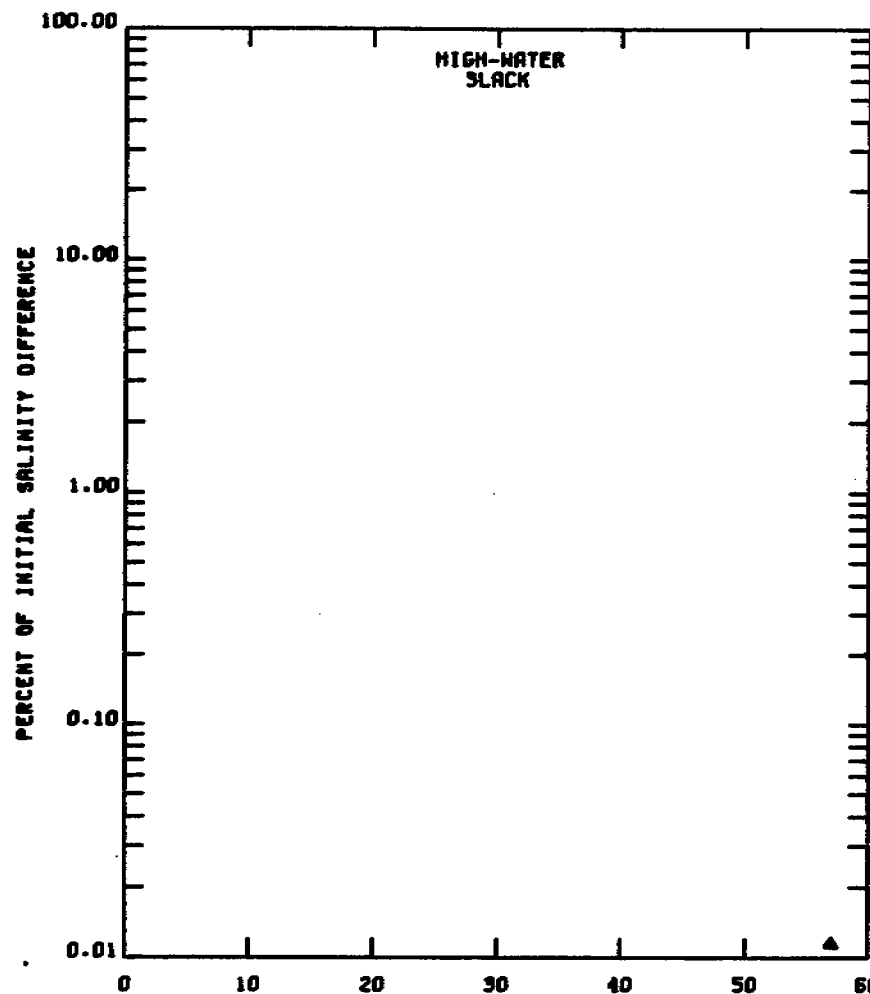
TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60600 CFS
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ ——— BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD**

STATION D3



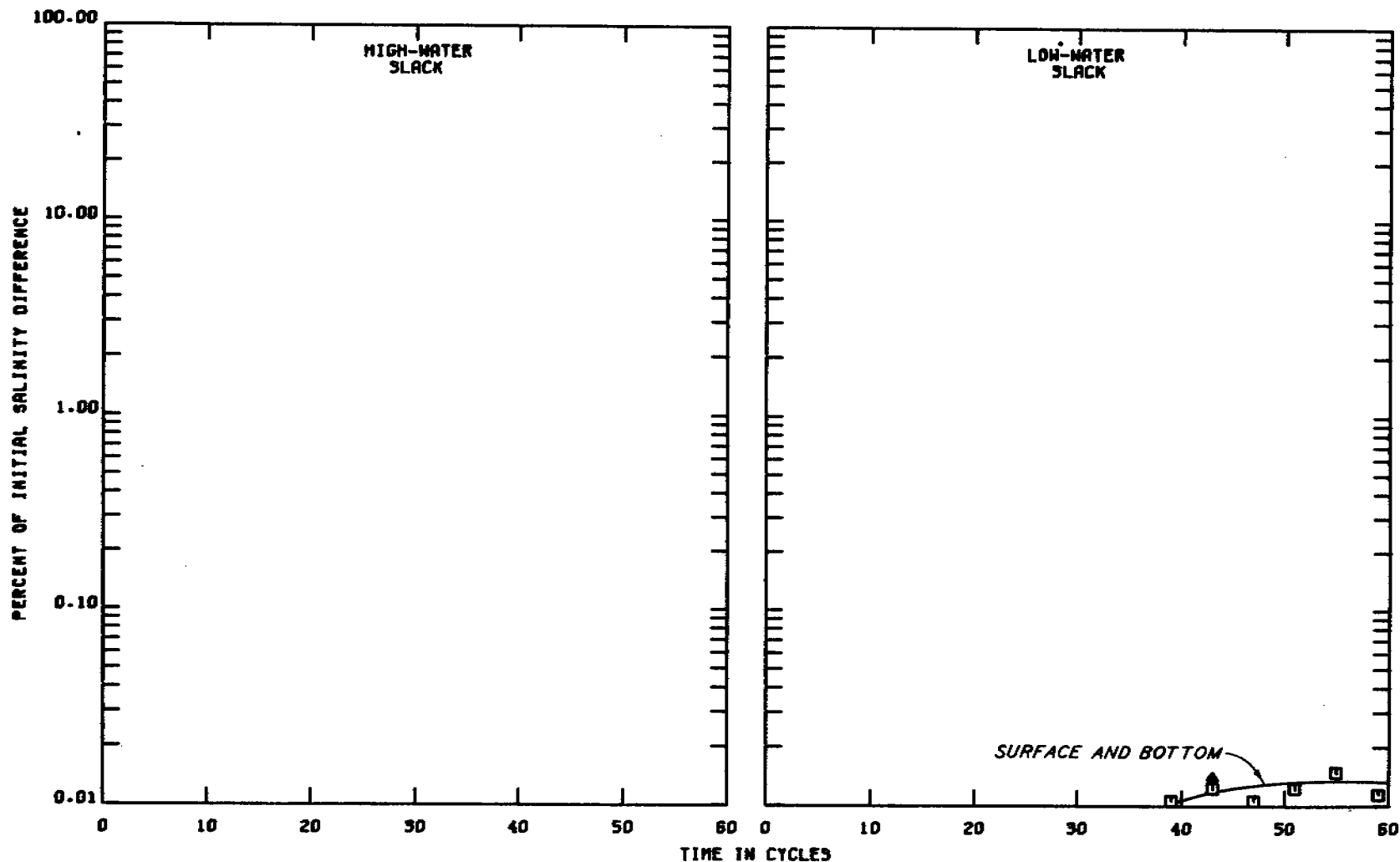
TIME IN CYCLES

TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60800 CFS
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

**DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD
 STATION D7**

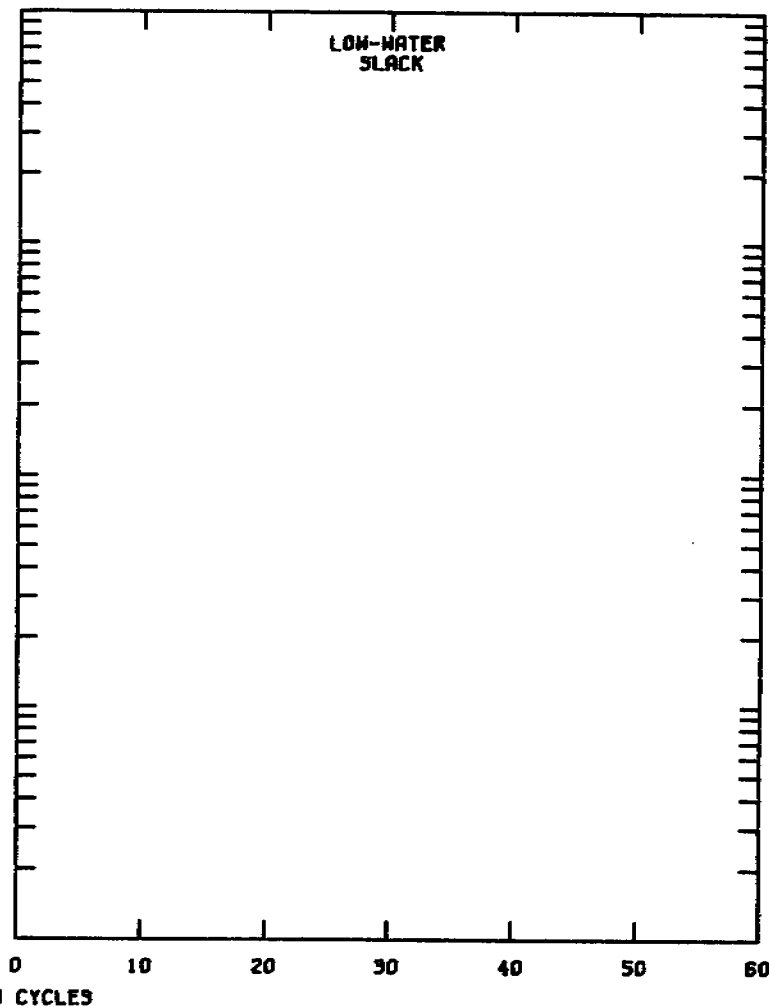
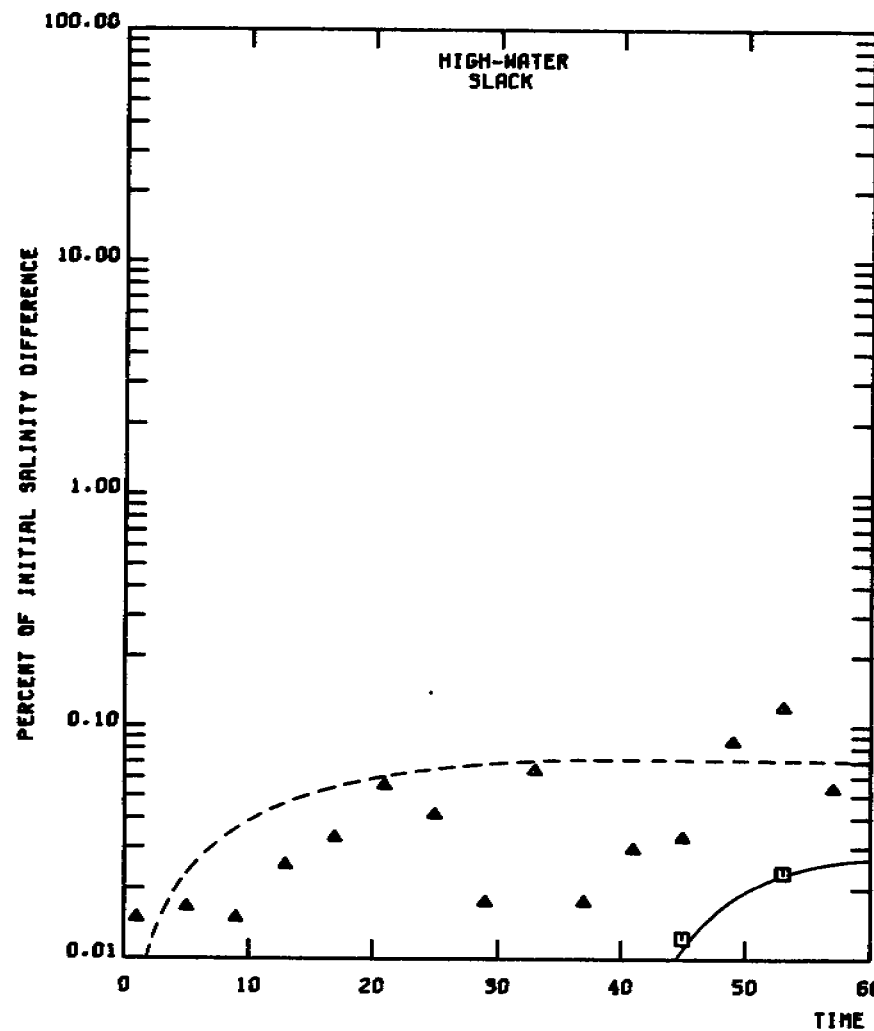


TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60600 CFS
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
 SALINE WATER
 DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD
 STATION D11



TEST CONDITIONS
 FRESH-WATER DISCHARGE
 BASE SALINITY AT DIFFUSER
 EFFLUENT SALINITY
 INITIAL SALINITY DIFFERENCE
 EFFLUENT INJECTION RATE

60600 CF3
 11.0 PPT
 22.4 PPT
 11.4 PPT
 21.2 MGD

LEGEND
 □ ——— SURFACE
 ▲ - - - BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
 10MGD PLANT-HIGH FLOW PERIOD
 STATION UI

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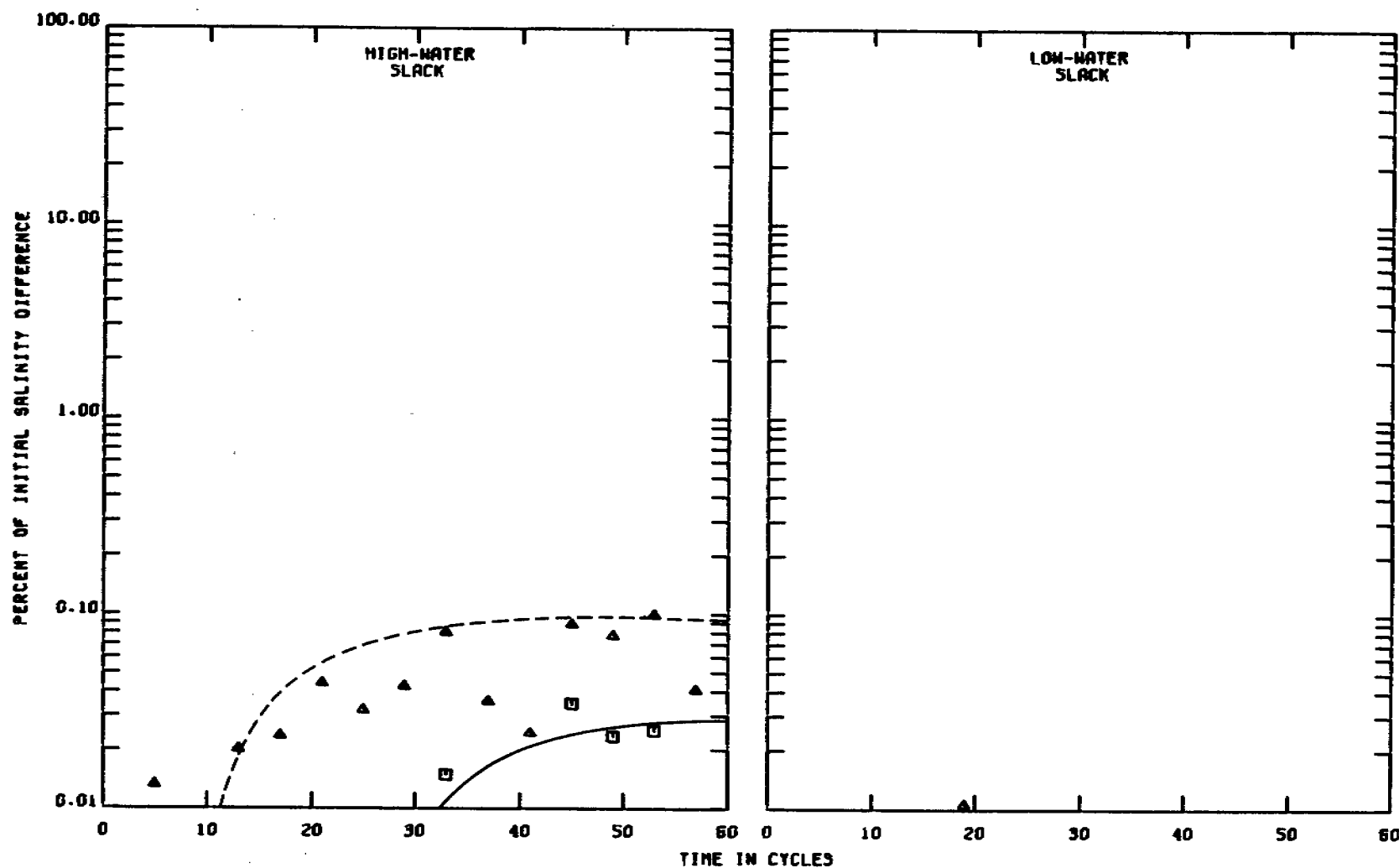


PLATE 167

TEST CONDITIONS

FRESH-WATER DISCHARGE	60600 CFS
BASE SALINITY AT DIFFUSER	11.0 PPT
EFFLUENT SALINITY	22.4 PPT
INITIAL SALINITY DIFFERENCE	11.4 PPT
EFFLUENT INJECTION RATE	21.2 MGD

LEGEND

□ ———	SURFACE
△ - - -	BOTTOM

DELAWARE RIVER MODEL
SALINE WATER
DISPERSION TEST
10MGD PLANT-HIGH FLOW PERIOD
STATION U2

